

EXPERIMENTAL AND NUMERICAL STUDY OF PREMIXED FLAME PROPAGATION
IN A CONSTANT VOLUME COMBUSTION CHAMBER

By

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ABSTRACT

EXPERIMENTAL AND NUMERICAL STUDY OF PREMIXED FLAME PROPAGATION IN A CONSTANT VOLUME COMBUSTION CHAMBER

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This work presents the experimental and numerical investigation of premixed flame propagation in a constant volume rectangular channel that serves as a combustion chamber. Flames inside closed vessels undergo distinct transformations in their physical structure; ignition event is followed by an accelerating convex shaped flame-front, then a deceleration of the flame is followed by the formation of a concave “tulip” shaped flame-front. Eventually, the flame is dissipated either because of quenching by the cold wall or by collision with a flame that has been ignited on the opposite end of the confined channel. Phenomena observed include both the formation of concave flame-fronts and oscillating convex-concave flame-fronts. The flame structure and speed of flame propagation is characterized for changes in the equivalence ratio, initial pressure, timing and placement of the ignition sources. Numerical and analytical calculations of the combustion phenomena are performed to understand the effect of the pressure waves and various instabilities causing the changes to the flame structure. The transient numerical results are validated using the experimental results.

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KEY TO SYMBOLS

m - Mass flow rate

C_p - Specific heat, at constant pressure

λ - Thermal conductivity

δ - Flame thickness

A - Area of cross-section

ρ - Density

U - Velocity

S_L - Laminar flame speed

k - Rate of reaction

T_i - Ignition temperature

T_u - Unburnt temperature

T_f - Flame temperature

w - Reaction rate

α - Thermal diffusivity

δ_L - Laminar flame thickness

E_a - Activation energy

INTRODUCTION

This thesis is devoted to the investigation of the structure and propagation of premixed flames in constant volume combustion chambers and their application to wave rotor devices. The structure and speed of flame propagation in a constant pressure combustor is nearly constant as the combusted gases are allowed to expand under isobaric conditions. In a constant volume combustor, the temperature and pressure of the unburnt premixed mixture continuously changes throughout the combustion process, which leads to a varying flame speed. Experimental investigation performed by Ellis [1] showed that flames in closed tubes undergo distinct changes in their structure and speed when ignited at one end of the tube. The flame propagation was split into 3 stages: (1) ignition by spark followed by the growth of a spherical flame front; (2) quenching of the flame-skirt by the cold wall and flame shape inversion; and finally, (3) collision with the cold wall on the opposite end of the tube. The inward pointing cusp formed at stage two was referred to as the “tulip flame” by Salamandra [2].

The primary motivation for this research is the study of the influence of combustion chamber shape and initial conditions on the propagation of premixed flames in a wave disk engine. The wave disk engine research, funded by the US Department of Energy [DoE] and the Advanced Research Projects Agency-Energy [ARPA-E] involves the design of a rotary engine prototype which potentially utilizes shock-wave compression and constant volume combustion to generate power at a high thermal efficiency. The design of the engine prototype involved detailed analysis of the flame propagation and combustion time for the determination of the intake and exhaust port timing as well as the rotational speed of the engine (RPM).

CHAPTER 1

WAVE DISK ENGINE

A wave rotor is an unsteady flow device which uses shock waves to transfer energy between fluids at different pressure levels. The wave engine uses either an external turbine or curved channels to extract shaft work and uses the unsteady shock wave compression as a part of the compression stage. The initial prototype of an axial wave disk engine was constructed by the Ruston-Hornsby turbine company in the mid-1950s, which produced a maximum power of 26 kW at its design point. Further development of the axial wave engine took place at ABB and ETH-Zurich which designed an engine to generate up to 100 kW. The wave disk engine concept as proposed by M. Vagani et. al. [3] at Michigan State University consists of a radial disk with curved channels which compress premixed fuel-air mixture and expand combusted gases, producing shaft work. The radial design enables a compact layout of the engine which reduces cost and results in a high power density. The compression and expansion of the premixed mixture and burnt gases are achieved through shockwaves and expansion waves. The momentum of the flow is used to extract shaft work. The wave disk engine developed at MSU is discussed in greater detail in the following subsection.

1.1 WAVE DISK ENGINE INTRODUCTION

The simplified representation of the wave disk engine is shown in Fig. 1.1. The primary design emphasis at Michigan State University has been on the radial wave engines where power is generated by the radial turbine action of the channel geometry.

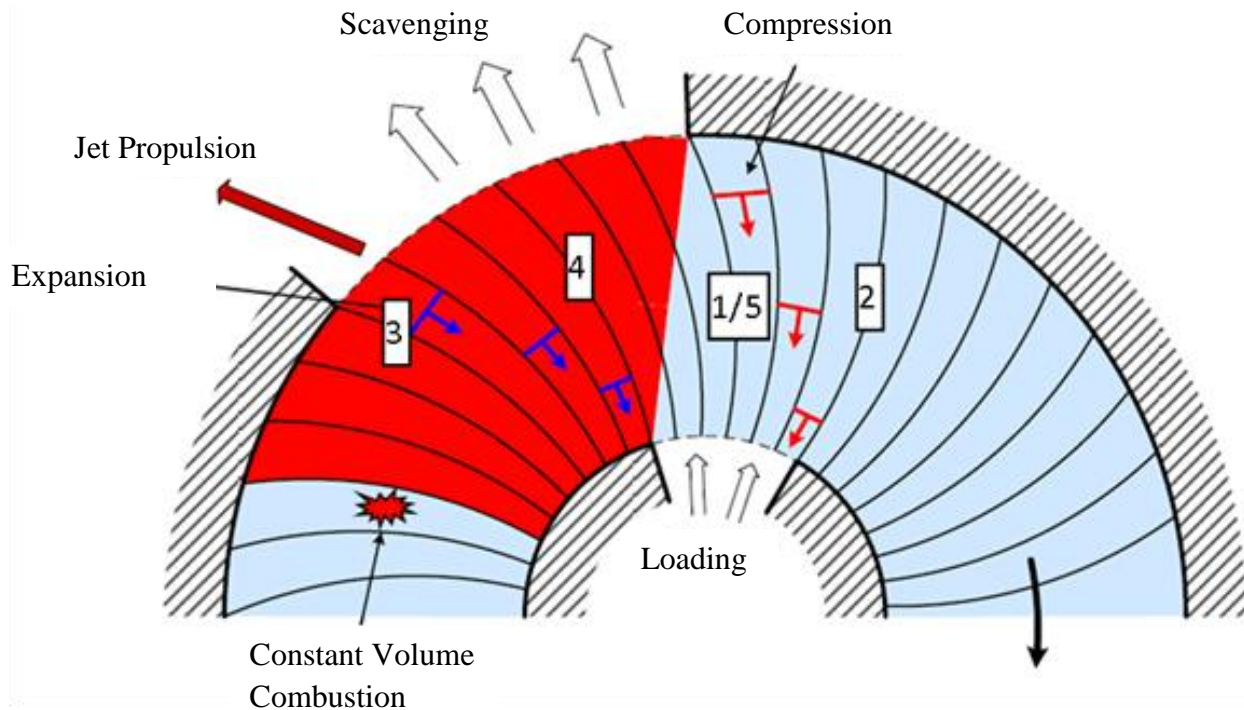


Figure 1.1 - Wave disk engine schematic representation [3]. “For interpretation of the references to color in this and all other figures, the reader is referred to the electronic version of this thesis”

The wave disk engine uses the Humphrey cycle, which involves isentropic compression followed by constant volume combustion and isentropic expansion of the combusted gases. The basic design element of the radial wave engine consists of a circular rotor which has curved channels machined inside, which act as combustion chambers. The rotor is surrounded on the outside by the exhaust assembly, on the inside by the intake port assembly. The intake and exhaust timing is controlled by the relative angle of opening of the intake and exhaust ports.

The initial calculation, based on 1-dimensional straight channel geometry and laminar combustion speed enabled the design and manufacture of the first generation wave engine at MSU [3].

The four distinct stages involved in the wave disk engine operation are as follows:

Stage I – Injection of fuel-air mixture

Once the hot exhaust gases at high pressure have been expelled from the previous cycle, the intake port is opened in conjunction with the exhaust port. This allows the premixed fuel-air mixture to flow into the combustion chamber of the wave rotor. The exhaust gas expulsion creates a temporary low pressure regime throughout the combustion chamber due to the action of expansion fans. This permits the injection of the fuel-air mixture through the mechanism of self-aspiration.

Stage II – Hammer shock compression

While the intake port is open, the exhaust port is abruptly closed. This creates a hammer shock which travels upstream of the flow of the fuel-air mixture. The hammer shock phenomenon occurs due to the sudden change in the velocity brought about by the closing of the exhaust port by the rotation of the channel. The hammer shock also increases the pressure and temperature of the air-fuel mixture and increases the effective mass inside the combustion chamber. The intake port is closed once the hammer shock reaches it. The compressed fuel-air mixture is essentially at zero velocity with respect to a rotating frame of reference attached to the combustion chamber.

Stage III – Constant volume combustion

The combustion chamber is maintained at a constant volume by the closure of the intake and exhaust ports. The fuel-air mixture is ignited by a spark plug placed either on the outer radius of the combustion chamber or axially above the channel. This enables the fuel-air mixture to undergo combustion. Once the combustion process is complete, the combustion chamber will contain gases at high pressure and temperature.

Stage IV – Isentropic expansion

The exhaust port of the channel is suddenly opened once combustion is complete. This enables the expulsion of the combusted gases through the formation of expansion waves. The pressure and temperature of the channel gradually decreases. After a certain time, the pressure inside the channel decreases below the ambient pressure. At this stage, the intake port is opened and fresh fuel-air mixture is let in as described in stage I.

The four stages described above repeat continuously as the rotor spins to generate power. The curved shape of the channel enables the extraction of work through jet propulsion principles. The amount of work extraction can be further increased by the addition of multiple turbine stages.

The emphasis of this thesis was to optimize both the extraction of power from the wave engine through a single stage turbine expansion process and to develop an accurate numerical model to estimate the time required for combustion. Extensive numerical analyses were carried out to optimize the structure of the channels and to study the structure and speed of flame propagation

inside the wave rotor. The simplified numerical calculation for the various stages for a straight channel is described below.

The numerical calculation for the wave disk engine is performed using commercially available computation fluid dynamics solvers to obtain the combustion and port timings and the theoretical power production. The explicit Navier-Stokes solver module in Ansys Fluent was used to obtain the initial results for the simplified straight channel geometry. The numerical scheme used in the following simulation results is discussed in greater detail in Appendix C.

The computational domain consists of a scaled straight channel which measures 50 mm in length and 10 mm wide. The two dimensional channel is meshed with a structured grid which consists of square cells measuring 0.1 mm. The schematic representation of the computational domain is shown in Fig 1.2.

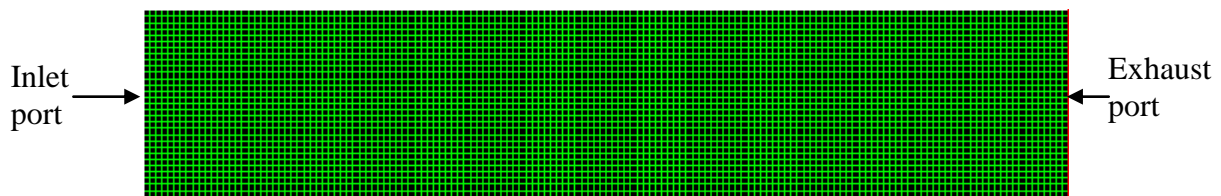


Figure 1.2 - Computational domain of straight channel.

The inlet and outlet ports of the straight channel are located at the left and right ends of the computational domain respectively. The domain is initialized with a pressure of 7 bar and a temperature of 2100 K to obtain the conditions after complete combustion. The exhaust port is opened and the combusted gases are allowed to escape. This creates expansion waves which reduce the pressure and temperature of the channel representing stage IV of the wave engine operation.

The inlet port is opened by setting it as a pressure inlet boundary when the average total pressure inside the channel achieves its minimum value. The inlet boundary injects stoichiometric methane-air mixture at ambient temperature and 10 kPa overpressure. This represents stage I of the wave engine operation.

Once the channel is completely filled with methane, the exhaust port is closed. This generates a hammer shock, which propagates towards the inlet. The hammer shock increases the pressure of the premixed gas by a factor of 1.75 representing stage II of the wave engine operation. The inlet port is closed once the hammer shock reaches the opposite end of the chamber. The premixed mixture is then ignited with a spark plug to produce constant volume combustion process, representing stage III of the wave engine cycle. Once the combustion is complete, the burnt gases are exhausted in stage IV described earlier.

The average static pressure inside the channel is shown in Fig. 1.3.

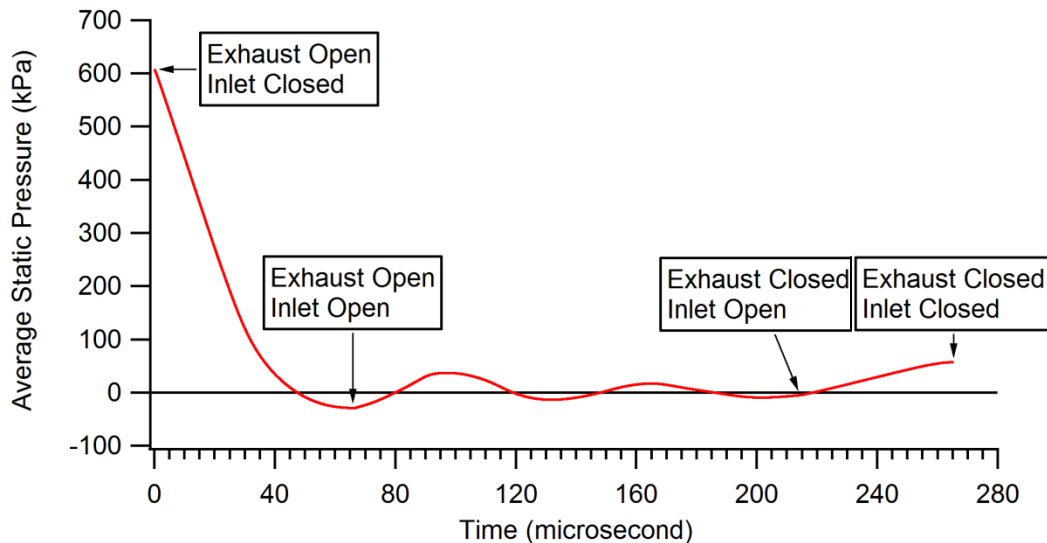


Figure 1.3 - Pressure inside the wave engine channel.

The time taken for the different stages depends on the length of the channel and its aspect ratio. For the present study, the time taken for combustion is calculated by utilizing both the theoretical laminar flame speed of premixed methane-air stoichiometric mixture at 1.75 bar and the experimentally observed combustion time. The time required for the different stages for the present channel design using the theoretical laminar flame speed is shown in table 1.

Wave Engine Cycle	Required Time (μs)
Stage I	148.3
Stage II	51.1
Stage III	30,000.0
Stage IV	66.0

Table 1.1 – Wave engine cycle timing, theoretical flame speed

An experimental analysis was performed using a channel of the same geometric dimensions to obtain an estimate of the total time needed for combustion. The combustion chamber was initially filled with premixed methane-air mixture at 75 kPa of overpressure to obtain the condition similar to the end of stage II. The total combustion time was observed to be 6,300 microseconds. The shorter time required was due to changing flow-field and temperature of the unburnt mixture during the combustion process. The data for the experimental time for combustion are shown in table 1.2.

Wave Engine Cycle	Required Time (μ s)
Stage I	148.3
Stage II	51.1
Stage III	6,300.0
Stage IV	66.0

Table 1.2 – Wave engine cycle timing, experimental flame speed

The comparative time taken for the four stages is shown graphically in Fig. 1.4.

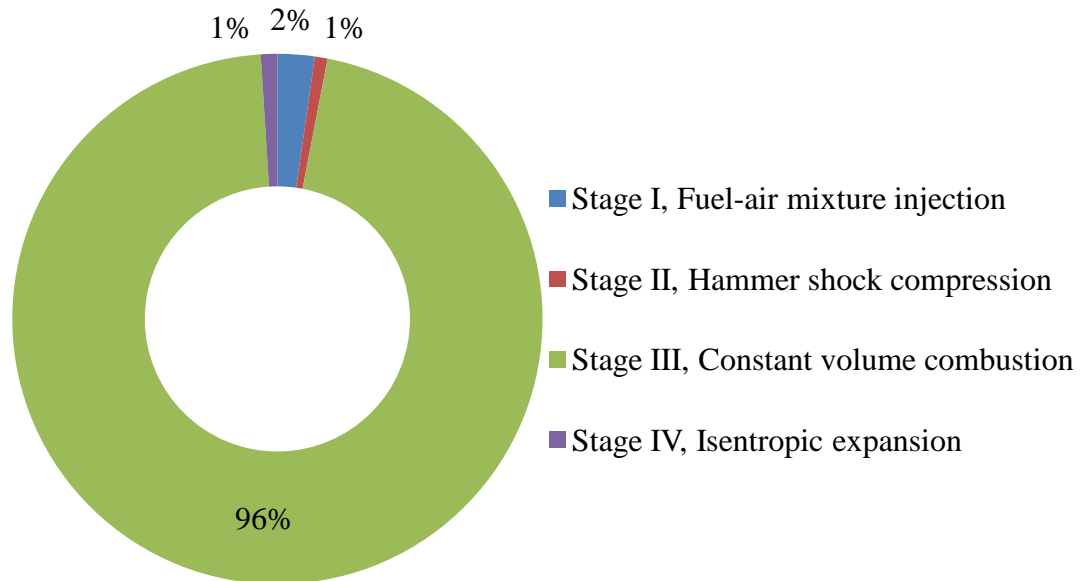


Figure 1.4 - Wave engine cycle time, in percentage.

The time required for combustion introduces restrictions in the speed of rotation of the wave rotor as well as inlet and exhaust port timings and opening angles.

1.2 COMBUSTION CHAMBER DESIGN

The first generation wave rotor was constructed using the research data obtained by a computational analysis of the one dimensional channel geometry [3]. This enabled the construction of a wave engine with “C” shaped channels with inlet and exhaust ports optimized for 20,000 RPM. The schematic representation of the first generation wave rotor is shown in Fig. 1.5. The wave rotor design was tested extensively for various operating conditions and port timings. The corresponding power production and pressure results were used in the setup and calibration of the numerical model.

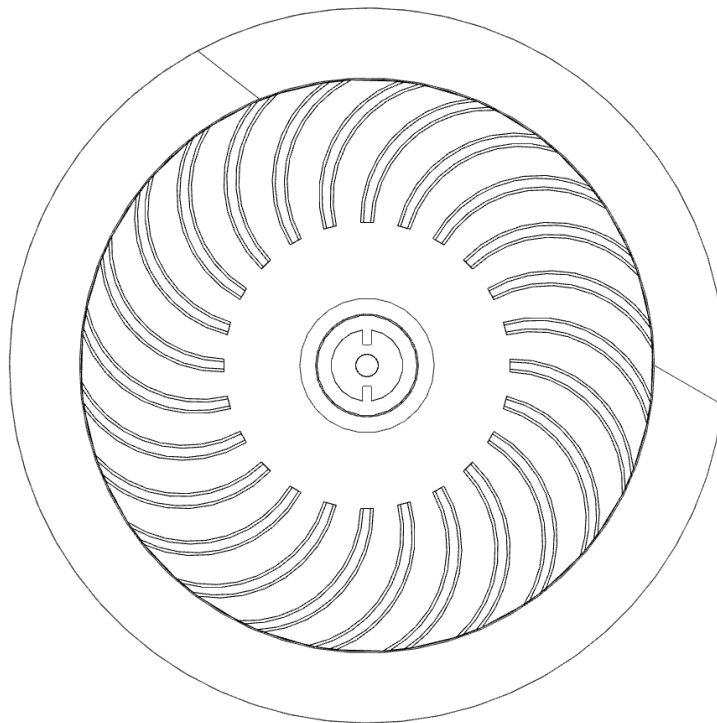


Figure 1.5 - First generation wave disk engine design.

The results from the numerical simulation enabled the design of the second generation of the channel geometry. The turbine efficiency of the wave rotor was numerically computed to be 16% which prompted modification to the channel geometry. The second generation rotor was designed to increase the turbine power extraction by the use of a converging channel section near the exhaust port. This allowed the high pressure combusted gases to increase the speed at exhaust allowing a greater torque. The second generation rotor design also featured a two cycle operation which enabled a slower rotational speed by decreasing the time allowed for the various stages. The design of the channel geometry, intake and exhaust port openings was optimized for a design rotational speed of 10,000 RPM. The engine assembly was modified to accommodate direct injection of fuel into the combustion chamber prior to spark ignition in order to enable stratified mixture combustion. The lean combustion process was used to reduce NO_x and SO_x emission while increasing the thermal efficiency of the engine. A schematic representation of the second generation wave disk engine is shown in Fig. 1.6.

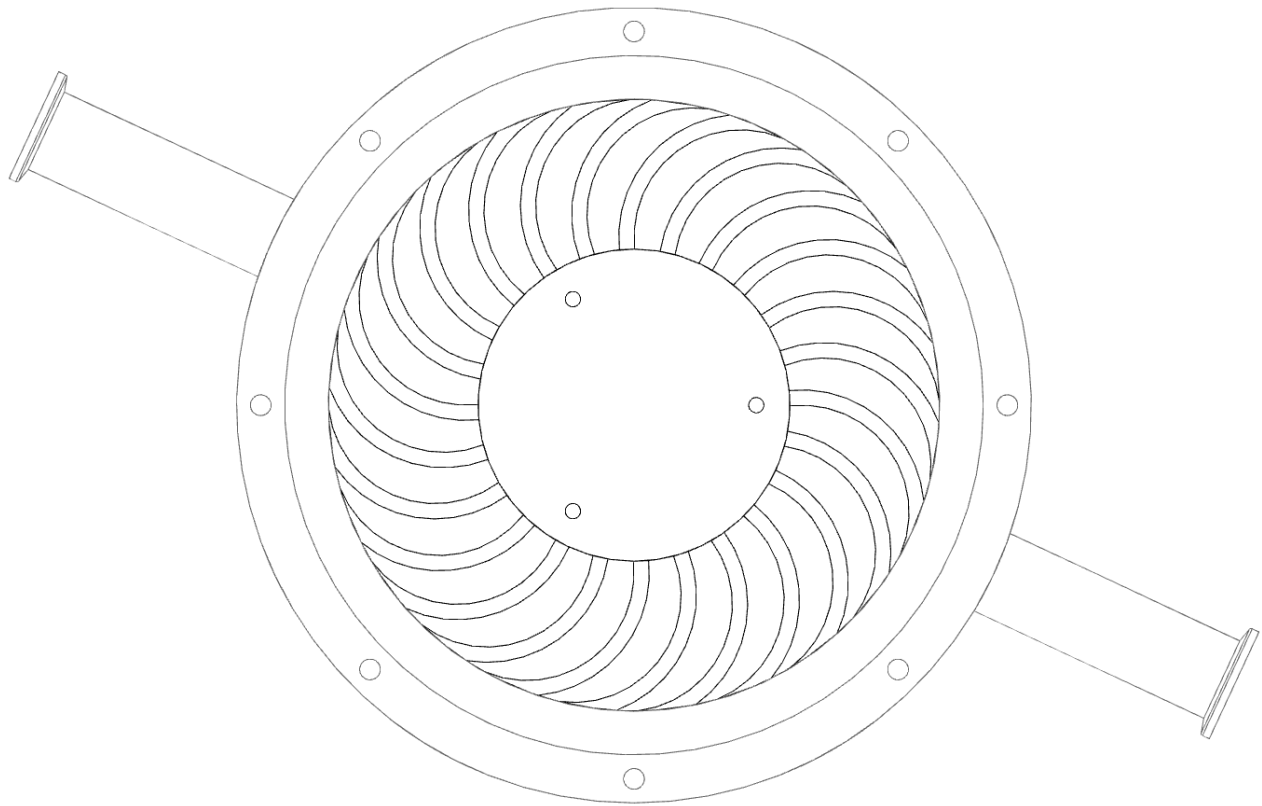


Figure 1.6 - Second generation wave disk engine design.

The second generation design incorporated additional features such as a secondary inlet, return channels for multistage turbine extraction and replaceable exhaust port geometries. The inlet geometry was modified to enable either the separate injection of air and fuel or the injection of scavenging air to create a buffer zone between hot exhaust gases and cold fuel-air mixture.

The third generation wave engine design featured a modification of the channel geometry to increase the turbine work extraction of the wave engine. The channel design was modified to accommodate a converging-diverging geometry to act as a nozzle to accelerate the speed of ejection of hot gases. The schematic representation of the wave engine is shown in Fig. 1.7.

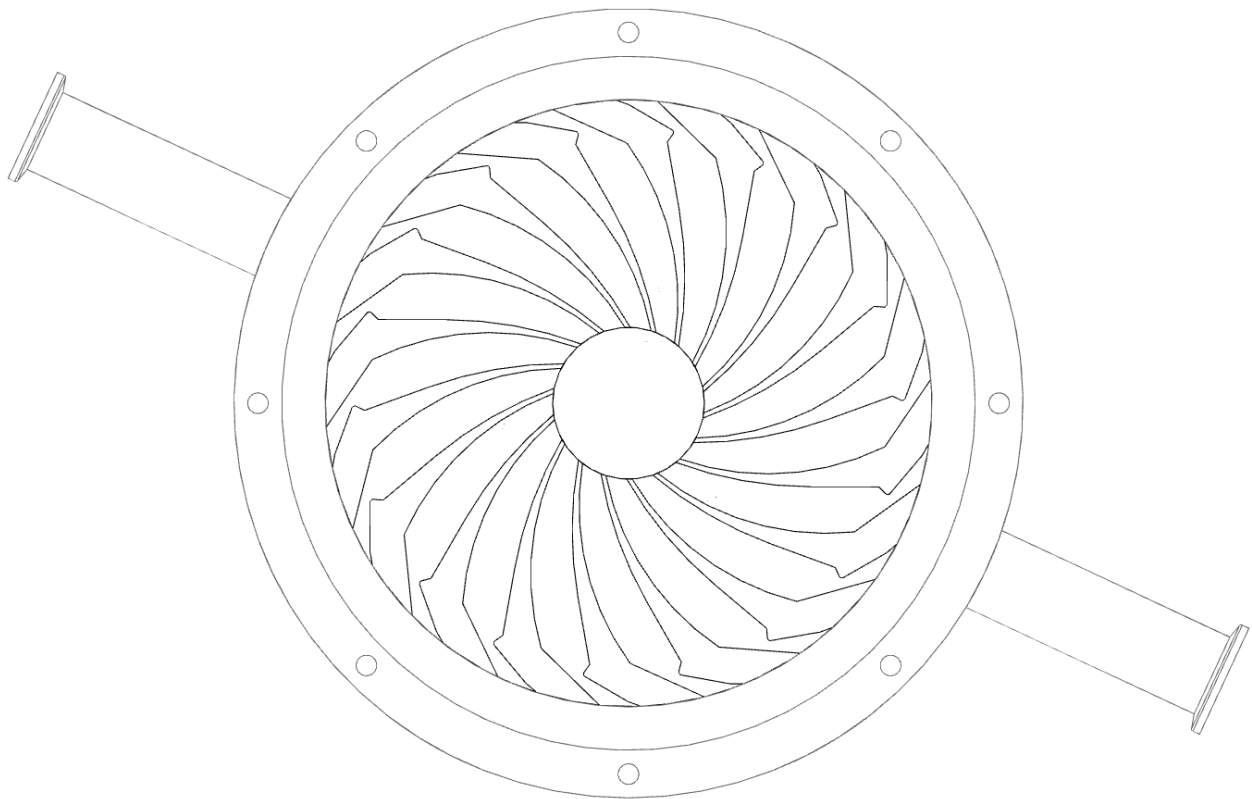


Figure 1.7 – Third generation wave disk engine design.

The nozzle geometry was optimized to enable the maximum torque generation for an initial pressure of 3 bar. The size of the inlet chamber was reduced to enable the design of a longer channel and increase the volume of the combustion chamber. The intake and exhaust port timings were optimized for a rotation speed of 5000 RPM and a two cycle design feature was utilized. The construction of the nozzle geometry allowed the exhaust gas to be expelled at supersonic velocities, further increasing the turbine power generated by the nozzle.

The use of the nozzle also allowed an increase in the time taken for the exhaust gases to be expelled. The contour plot of the Mach number during the exhaust stage of the channel is shown in Fig. 1.8. The channel is initially filled with burnt gases at high pressure and temperature of 7 bar and 2100K and the exhaust port is opened. This creates a choked flow at the nozzle and generates power due to the channel curvature.

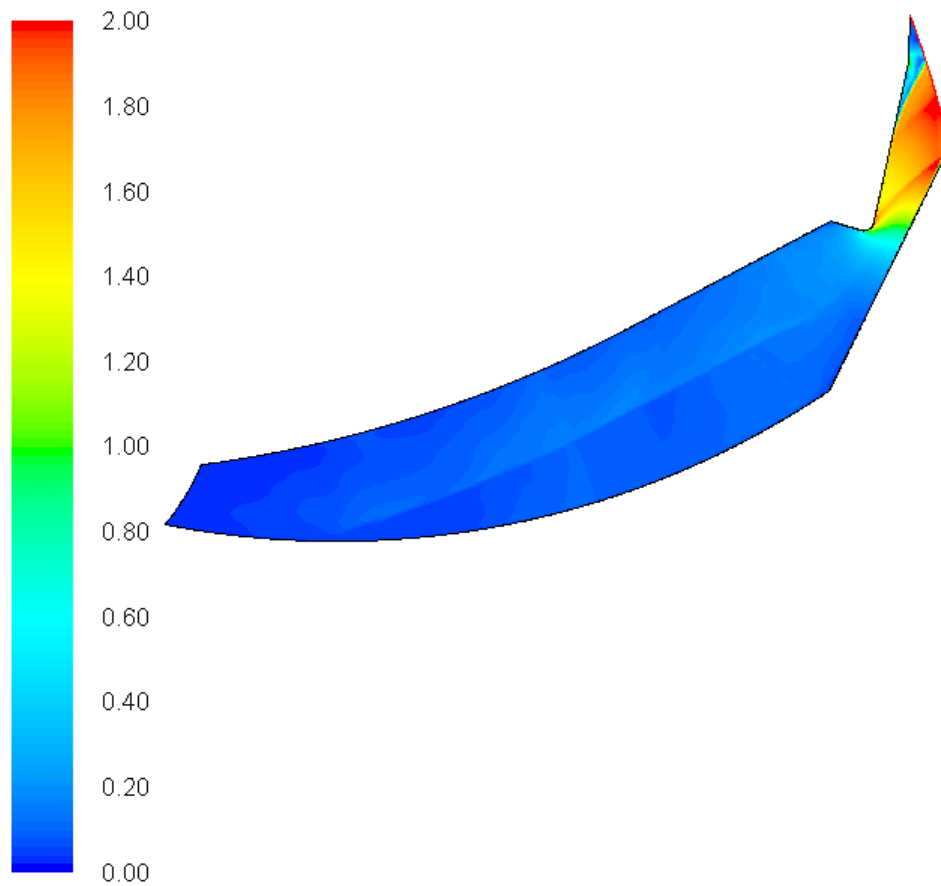


Figure 1.8 - Contour of Mach number during exhaust stage.

The nozzle reduces the static pressure of the exhaust gases, which increases the efficiency of the turbine. The contour plot of the static pressure is shown in Fig 1.9. The efficiency of the turbine is 86%.

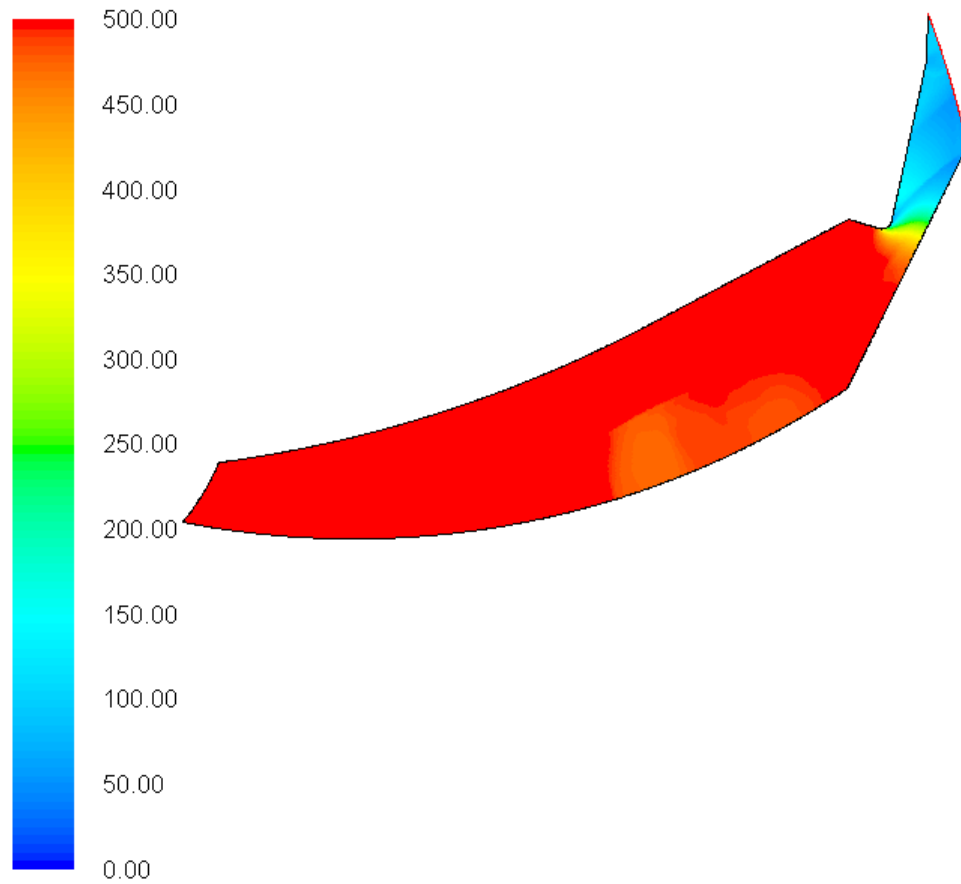


Figure 1.9 - Contour of static pressure during exhaust stage, units in kPa-g.

The time required for the four stages is shown in Table 1.3 and Fig 1.10.

Wave Engine Cycle	Required Time (μ s)
Stage I	341.1
Stage II	117.5
Stage III	3,638.5
Stage IV	1580.6

Table 1.3 – Wave engine cycle timing, third generation rotor

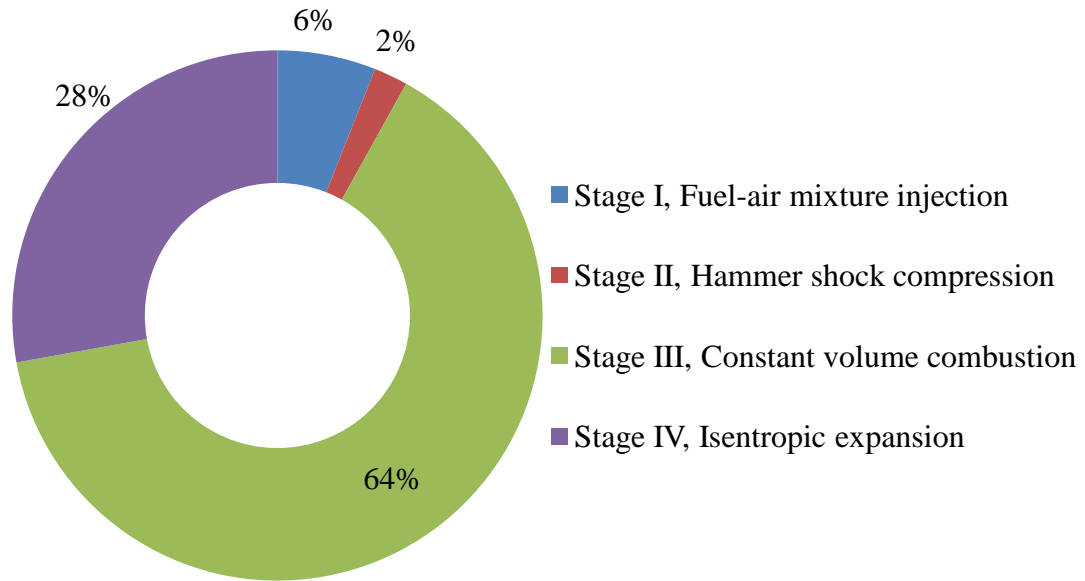


Figure 1.10 – Third generation wave engine cycle time, in percentage.

The total time taken for the four stages is equal to 5.7 milliseconds. For a two cycle wave disk engine, the maximum rotational speed for peak efficiency is computed to be 5300 RPM.

The two biggest challenges encountered in the operation of the wave disk engine were the efficiency of the turbine work extraction and the time required for constant volume combustion. The efficiency and work output of the radial turbine is directly proportional to the rotational speed of the turbine. The combustion process acts as a rate-limiting step which decreases the work and thermal efficiency of the engine. This prompted the need for a detailed study of combustion in a constant volume combustion chamber. Improvement in the flame speed would lead to faster rotational speed of the wave engine, potentially leading to an increase in the efficiency and power.

CHAPTER 2

LAMINAR FLAMES

Combustion in premixed fuel-air mixtures usually consists of a rapidly moving flame-front which travels into the unburnt mixture with a finite reaction rate. This type of reaction is typically called deflagration. The flame front propagates towards the unburnt mixture through the action of species and heat diffusion into the unburnt mixture.

The two main classifications of combustion depending on their speed of propagation are deflagration and detonation. When the speed of flame propagation is slower than the speed of sound, it is called deflagration. When the speed of flame propagation is faster than the speed of sound, it is known as detonation. The propagation of deflagration usually occurs due to the diffusion of species and thermal energy into the unburnt mixture. Detonation is sustained by the action of a shock wave travelling just ahead of the flame-front, which causes the reactants to dissociate and recombine into products, with the heat release of the chemical reaction further reinforcing the shock.

The part of the reaction zone which releases heat and light is typically called the flame. The location of the flame-front is dependent on the stoichiometric conditions of the reactants. In diffusion flames, the flame-front is sustainable only in those places where the fuel-air ratio is suitable for combustion. However, in premixed flames, the fuel and air are intimately mixed and the flame-front tends to propagate into the unburnt mixture at a speed proportional to the reaction rate.

Premixed flames undergo numerous instabilities caused by to the shape of the combustion structure, the Lewis number of the fuel-air mixture and intrinsic effects like the Darrius-Landau instability mechanism.

The premixed flame propagation process can be achieved in open or closed channels and burners. The flame structure can be described by establishing a reference frame and defining a profile for the variables under consideration (temperature, species mass fraction). The coordinate system is fixed to the moving flame front. In this coordinate system, the unburnt premixed mixture will be seen as approaching the flame front with a speed equal to the flame speed S_L . The spatial variation of the reactant concentration, temperature and reaction rate in a premixed, laminar flame front is shown in Fig. 2.1. The expansion ratio of the burnt gas is usually defined by σ , which is given here by ρ_u/ρ_b .

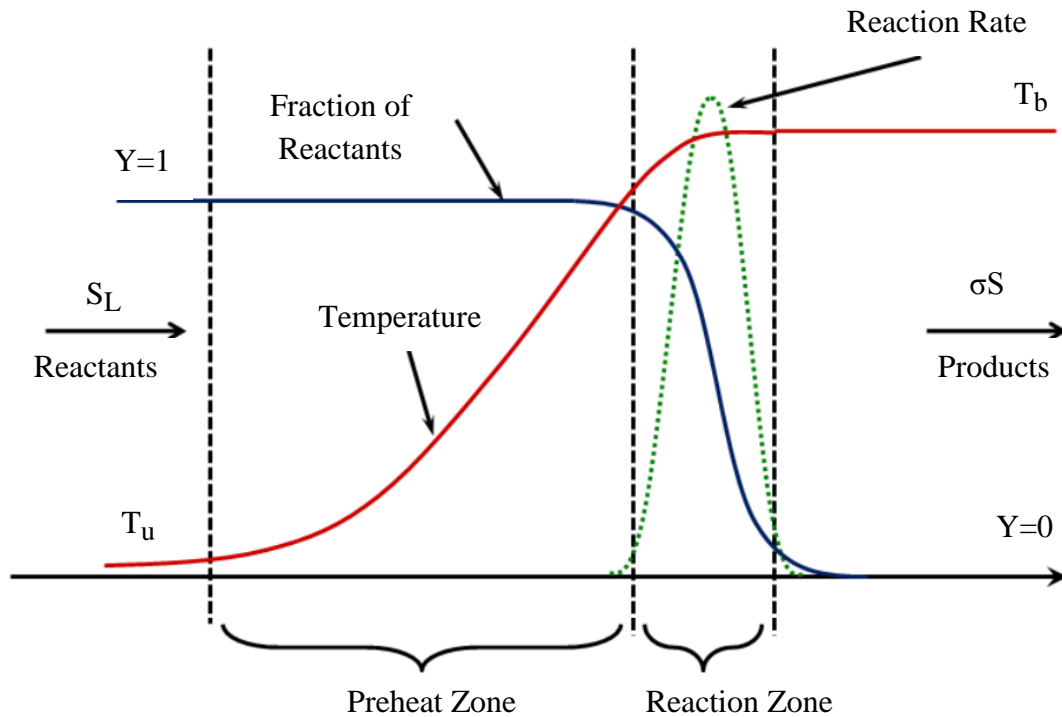


Figure 2.1 – Structure of a premixed flame in one dimension [4].

The two main zones are defined as preheat and reaction zones, dividing the flame front into two regions in which diffusion of radicals and heat occurs at different intensity. In the preheat zone, the amount of heat released is very small and the reaction rate is practically negligible. As the observer moves closer to the reaction zone, the heat transported from the flame front increases leading to higher temperature and faster reaction rates. The reaction occurs in a very thin zone typically about 1mm thick at atmospheric pressure. This region undergoes fast chemical reaction, and due to high reaction rate and heat release, the concentration gradients are very. The large thermal and concentration gradients drive the transport of energy and species into the upstream region know as the preheat zone, shown in Fig. 2.1 and render the flame propagation process self-sustaining.

2.1 LAMINAR AND TURBULENT PREMIXED FLAMES

There are two types of premixed flame depending on the nature of flow of the fluid: laminar and turbulent flames. The flow regime can be determined by the dimensionless number which is a function of flow velocity, kinematic viscosity, density and characteristic geometric dimension of the channel called the Reynolds number. In laminar flames, the combustion process is dominated by the chemical kinetics of the mixture and flame propagation occurs through diffusion of heat and species. In turbulent flames, the velocity and scalar properties are subjected to rapid, random changes at a given point in space; therefore the combustion process is strongly affected by it. The fluctuating temperature and species concentration due to turbulence is the dominant force for flame propagation in turbulent flames.

Combustion processes are usually characterized by highly exothermic chemical reactions, in which the reaction rate is a strong function of temperature. As mentioned previously, the combustion of a premixed mixture is strongly dependent on the chemical-kinetics of the mixture, thus the modeling of a detailed and accurate multi-step and multi-species reaction system represents a major challenge in the analysis of laminar flames.

2.2 LAMINAR FLAME SPEED

A detailed study of the propagation of a flame through an unburnt mixture is made in this section. First, a definition of laminar flame speed and laminar burning velocity is established. It is common to find ambiguities in literature in which laminar flame speed and laminar burning velocities have the same meaning, which is the velocity at which unburnt gas moves through the combustion wave in the direction normal to the wave surface.

The two flame speeds are defined below:

- (i) The laminar burning velocity is defined as the velocity at which unburnt gases move through the combustion wave in the direction normal to the wave surface.
- (ii) The laminar flame velocity is the velocity of the flame with respect to a fixed outside observer.

In the case of a standing or stationary flame, like the flame in a Bunsen burner, the laminar flame velocity is equal to the laminar burning velocity. For freely propagating flames, the laminar burning velocity is equal to the sum of the laminar flame speed and the flow velocity of the unburnt mixture. For example, the laminar flame velocity of methane-air and stoichiometric mixture at STP is 36.2 cm/s.

The three main flame propagation theories are broadly classified as thermal, diffusion and comprehensive theories.

The first theory describing flame propagation was the thermal theory of Mallard and LeChatelier [5], who stated that the controlling mechanism of flame propagation is heat diffusion from the burnt region to the unburnt region. This formulation defined the flame as a composite region

comprising two zones, separated by a layer where ignition occurs. Ignition was postulated to occur when the local temperature reached the ignition temperature and δ was described as the reaction zone thickness. This model is shown in Fig. 2.2.

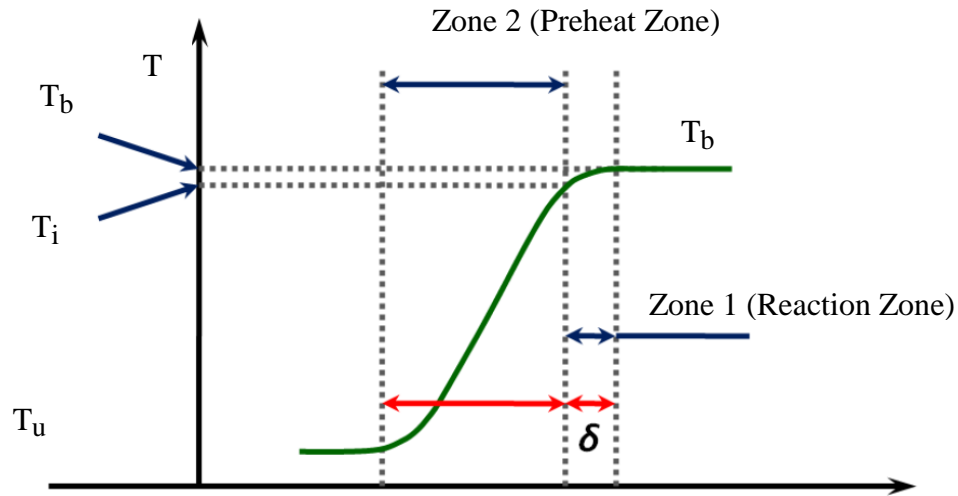


Figure 2.2 - Mallard and LeChatelier model [4].

Improvements were made to the thermal energy model by Zeldovich and Frank-Kamenetskii [6]. Their formulation included the diffusion of molecules and heat, but did not involve dissociation and the diffusion of free radicals. Tanford and Pease [7] developed this theory further, stating that the mechanism for flame propagation depends only on the diffusion of radicals and not on heat propagation as proposed by earlier theories.

These two theories of heat and radical diffusion drove the experimental research on the determination of flame velocity on initial parameters, pressure and temperature in order to examine the validity of the theoretical models of flame propagation. As is often the case, neither model was entirely correct.

The following observations follow from the two models of flame propagation –

- According to the thermal theory, increasing the initial pressure leads to a higher temperature. This leads to a faster rate of reaction and a higher flame speed is achieved.
- According to the diffusion theory, increasing the initial temperature leads to higher dissociation. The higher concentration of radicals causes greater species diffusion leading to a higher flame speed.

A comprehensive theory combining the species and thermal diffusion theories was developed by Hirshfelder et al. [8]. A complex set of non-linear equations describing the diffusion and energy balance were developed that could be solved by numerical methods. The Arrhenius equation for the reaction rate, by definition, has a very small non-zero value at regions far upstream of the flame, where the local temperature is equal to the ambient temperature. This was modified to enable a zero reaction rate model at ambient temperature and equating the wall surface to act as a heat sink. The exact solution of laminar flame propagation requires the use of fluid dynamics equations with modifications done to accommodate heat release and species/thermal diffusion. The two theories are comprehensively discussed by Irvin Glassman and Richard A. Yetter in their book “Combustion” [4]. A short description of the two theories is provided in the following section.

2.2.1 Mallard and Le Chatelier Theory

The theory developed by Mallard and Le Chatelier states that the heat conducted from zone 1 in Fig. 2.2 is equal to that required to raise the temperature of the unburnt mixture to the ignition temperature. The rate of temperature increase is assumed to be linear and is approximated to equal $[(T_f - T_i)/\delta]$. Here, T_f is the flame temperature, T_i is the ignition temperature and δ is the thickness of the reaction zone.

The energy balance between the downstream inwardly convecting flow and the upstream outwardly conducting thermal energy is given by the simple relation -

$$\dot{m}C_p(T_i - T_u) = \lambda(T_f - T_i)/\delta A \quad (1)$$

where λ is the thermal conductivity of the mixture, m is the mass flow rate of the unburned gases into the combustion wave, T_u is the temperature of the unburnt gases and A is the area of cross section. The combustion wave is considered to be one dimensional.

From the continuity equation, we have, for the steady mass flow rate, the expression -

$$\dot{m} = \rho UA = \rho S_L A \quad (2)$$

where ρ is the density and U is the velocity of the unburnt gas, which is equal to the laminar flame speed, S_L .

Upon using the mass balance equation with the energy balance, we obtain -

$$\rho S_L C_p(T_i - T_u) = \lambda(T_f - T_i)/\delta \quad (3)$$

Solving for the flame speed, we obtain:

$$S_L = \frac{\lambda(T_f - T_i)}{\rho C_p(T_i - T_u)} \frac{1}{\delta} \quad (4)$$

For a steady flow condition, the total mass rate entering the reaction zone must be equal to the rate of consumption of the reactants, thus:

$$\frac{\dot{m}}{A} = \rho U \rightarrow \rho S_L = \dot{w} \delta \quad (5)$$

where, w represents the reaction rate in terms of concentration. Using this expression in the flame speed equation yields:

$$S_L = \left[\frac{\lambda(T_f - T_i)}{\rho C_p(T_i - T_u)} \frac{\dot{w}}{\delta} \right]^{\frac{1}{2}} \Rightarrow \left[\alpha \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} \quad (6)$$

where α is the thermal diffusivity. From the expression above, we obtain an expression for the mass consumed by the unburnt gas is equal to -

$$\rho S_L \approx \left[\frac{\lambda}{C_p} \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} \quad (7)$$

Thus, the Mallard-Le Chatelier approach yields the following result for the laminar flame speed -

$$S_L = \left[\alpha \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} \quad (8)$$

Equation (8) enables the estimation of laminar flame propagation speed for changes in the physical and chemical parameters. We note that in this analysis, the chemical variables appear implicitly in w .

A similar approach was used by Linan and Williams [9] based on Mikhelson's studies [10] where the heat release in the reaction zone is equated to the energy conduction from the hot products to the cool unburnt gases.

The total energy per unit mass that is conducted to the unburned mixture is:

$$h = C_p(T_f - T_u) \quad (9)$$

And the energy balance is calculated as:

$$h\dot{w}\delta_L = \lambda(T_f - T_u)/\delta_L \quad (10)$$

where, δ_L is the thickness of the reaction zone, which includes both region 1 and region 2 from the Mallard-Le Chatelier approach.

Combining the energy balance equations gives -

$$C_p(T_f - T_u)\dot{w}\delta_L = \lambda(T_f - T_u)/\delta_L \quad (11)$$

Solving the above equation for the reaction zone thickness leads to

$$\delta_L = \left[\frac{\lambda}{C_p} \frac{1}{\dot{w}} \right]^{\frac{1}{2}} \quad (12)$$

Using Equation (5) derived earlier, we obtain:

$$S_L = \left[\frac{\lambda}{\rho C_p} \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} = \left[\alpha \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} \quad (13)$$

The expression derived above is the same as that derived by Mallard-Le Chatelier, but the derivation here does not employ the temperature ratio between the ignition temperature and initial/final temperature.

Additionally, following the Zeldovich, Frank-Kamenetskii and Semenov theory, in which the temperature term is evaluated by assuming asymptotically narrow reaction rate region, we obtain the following expression for the temperature term:

$$\frac{RT_f^2}{E(T_u - T_f)} \quad (14)$$

This term was identified as the Zeldovich number -

$$Ze = \frac{RT_f^2}{E(T_u - T_f)} = \frac{\delta_L}{\delta} \quad (15)$$

The expression for the laminar flame speed can now be derived as:

$$S_L = \left[\frac{\alpha}{Ze} \frac{\dot{w}}{\rho} \right]^{\frac{1}{2}} \quad (16)$$

This expression allows a reasonably accurate global analysis of the flame speed with respect to changes in the physical and chemical parameters of the problem. We obtain that the reaction term is proportional to the pressure of the reactants as follows:

$$S_L \approx (P^{n-2})^{\frac{1}{2}} \quad (17)$$

Here, n is the overall order of the reaction.

The laminar flame speed's dependence on the temperature is mainly dictated by the exponential in the rate expression w. This gives the expression:

$$S_L \sim \left[\exp(-E/RT_f) \right]^{\frac{1}{2}} \quad (18)$$

We note that the maximum reaction rate and heat release takes place close to the highest temperature if Arrhenius kinetics as the controlling factor for the flame chemistry.

2.2.2 Zeldovich, Frank-Kamenetskii and Semenov Theory

The analytical model of flame propagation suggested by Zeldovich, Frank-Kamenetskii and Semenov, serves as a more detailed method to determine the flame propagation speed. This model combines both the effect of thermal diffusion and the diffusion of species into the unburnt mixture on the flame speed. This model ignores the effect of diffusion of radicals and their effect on reaction rate.

The main underlying assumption in this model is that the ignition temperature is very close to the flame temperature. The ignition temperature is defined as the threshold temperature above which most of the reaction occurs. In addition, the specific heat and thermal diffusivity are both assumed to be constant over the entire flame region. This enables the use of the non-dimensional Lewis number, which is the ratio between the thermal and mass diffusion. When the rate of thermal and mass diffusion is identical, the Lewis number is unity.

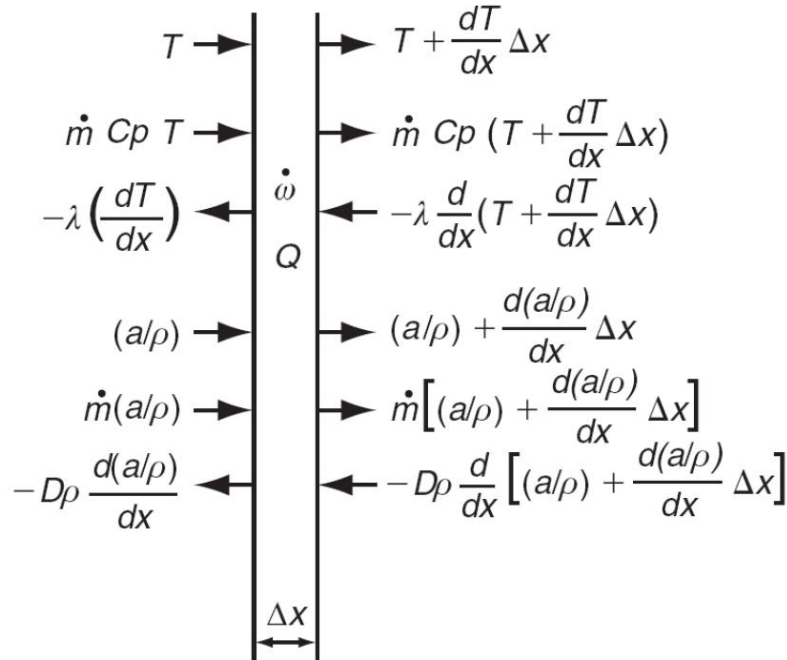


Figure 2.3 – Balances across a differential element of laminar flame [4].

The flame is assumed to be a one-dimensional wave of thickness Δx as shown in Fig. 2.3. Here, 'a' is the mass of reactant per cubic meter, w is the rate of reaction and Q is the heat of reaction per unit volume. Since this is a steady propagation process, there is no accumulation of species or heat within the control volume.

The equations of mass balance, mass diffusion and energy balance equation are formulated within the limits of the unburnt and burned gases from $X=-\infty$ to $X=+\infty$. The combustion wave is considered to consist of two parts. The unburnt part in which there is no reaction and the reaction part in which the reaction and diffusion processes dominate and the convective term is neglected. The energy equation is centered at $x=0$, which allows the local temperature at the origin to be specified as the ignition temperature.

Upon integration of the system of equation, the solution for the flame speed is obtained as follows:

$$S_L = \left[\frac{2}{a_0} \left(\frac{\lambda}{\rho_0 C_p} \right) \left(A e^{-E/RT} \right) \left(\frac{RT_f^2}{E(T_f - T_0)} \right) \right]^{\frac{1}{2}} \quad (19)$$

Here, A is the pre-exponential factor in the Arrhenius equation and the subscript 0 refers to the initial conditions.

2.3 Flame Speed Measurements

Depending on the method of measurement and the accuracy requirement, the measurement of flame speed can either be simple or complicated. Flat, adiabatic flames are difficult to obtain in laboratories due to heat losses and gravity, hence the most common flame shapes are either conical or spherical. The most common methods used in the calculation of flame speeds are by Bunsen burner, cylindrical tube, spherical flame and the flat flame burner methods. These are discussed in detail below.

Bunsen burner method –

In a Bunsen burner with long tubes, the velocity profile at exit is parabolic, leading to variable burning velocity over the flame surface. For this case, an average method is used to determine the normal velocity component, U_n over the “flame cone” that the Bunsen burner flame produces. The normal velocity U_n is equal to the flame speed S_L . It is assumed that U_n is constant over the flame area A_f . If m is the mass flow rate of the gas, and ρ is the unburnt gas density, from mass continuity, we obtain:

$$U_n = \frac{\dot{m}}{\rho_u A_f} \quad (20)$$

When suitably shaped nozzles are used, the flow is uniform and the flame has straight edges. The flame speed can then be computed as -

$$U_n = U_u \sin \alpha_u \quad (21)$$

The structure of the flame in a Bunsen burner is shown in Fig. 2.4.

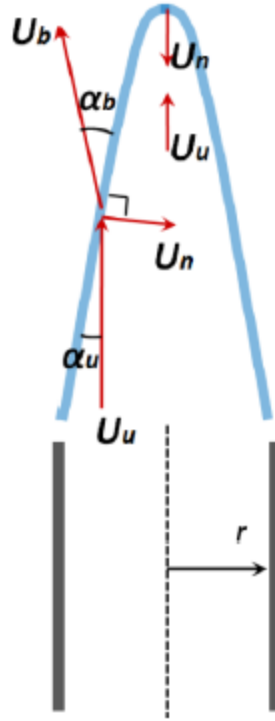


Figure 2.4 - Bunsen burner flame [4].

Cylindrical tube method –

This method utilizes a cylindrical open tube, typically made of glass, where the premixed fuel-air mixture is ignited at the open end. The speed of flame propagation is measured optically. Due to buoyancy effects, the flame shape is not planar and the area of the flame is larger than the cross-sectional area of the tube. The combustion induces pressure waves which travel faster than the flame and induce localized velocity in the unburnt mixture which can affect the speed of propagation of the flame with respect to the laboratory coordinates. Additionally, heat losses to the wall can influence the flame speed as the non-quenched region mixes with the quenched region of the flame.

Spherical flame method –

In this method, the premixed mixture is contained in a soap bubble and is ignited at the center, so that the flame will propagate radially through the unburnt mixture. Since the gas is enclosed by the soap film, the pressure remains constant. There is no heat loss to the outside as the soap bubble contains no heat sinks. The bubble grows as the premixed mixture burns and this growth is measured optically. The flame speed can be measured as follows:

$$S_L = U_n \left(\frac{\rho_b}{\rho_u} \right) \quad (22)$$

Flat flame burner method –

This method of flame speed measurement is performed by supplying combustible gas mixture to a series of thin, parallel tubes of diameter not larger than 1 mm. The mixture flow rate is adjusted to obtain a thin flat flame resting on top of the burner surface. The flame speed is obtained by dividing the volumetric flow rate with the flame area. Since the flame is perfectly flat, it is the most accurate method of measuring the flame speed of a fuel-air mixture.

2.4 Instabilities in Flame Propagation

Combustion in both open and closed channels is subjected to a number of instabilities which have been studied theoretically, computationally and experimentally. The three main types of instabilities which have the greatest impact on flame structure and propagation are listed below:

- i. The Landau-Darrieus instability, an intrinsic instability which occurs due to hydrodynamic effects.
- ii. Instability caused by the coupling of combustion and acoustics of the system. These instabilities are characterized by low-frequency oscillations in the longitudinal dimension of the channel.
- iii. Instability caused due to the coupling between combustion and acoustic modes. These instabilities are characterized by high frequency oscillations in the transverse dimension of the channel.

The last two types of instabilities are commonly classified as thermo-acoustic instabilities and the first one is referred to as a hydrodynamic instability. The three instabilities are discussed in great detail by G. Searby in the paper “Instability Phenomena during Flame Propagation” [11] and in Combustion Physics by C. K. Law [13]. A short description is provided in the following section.

2.4.1 Landau-Darrieus Hydrodynamic Instability

All premixed flames are intrinsically unstable due to the hydrodynamic effects, which is caused due to the expansion of hot, combusted gas into the denser, unburnt mixture. A one-dimensional representation of an infinitesimally thin laminar flame is shown in Fig. 2.5. The planar flame front is essentially a thin interface (a sheet) which separates the unburnt and burnt gases. The cold reactant gases at temperature and density, T_0 and ρ_0 , are separated from the hot combusted gases of temperature and density, T_b and ρ_b . The flame front propagates at velocity S_L into the unburnt gas mixture. Upon combustion, the gases undergo thermal expansion and they exit the flame front at $U_b = S_L \cdot (\sigma)$. The density ratio here is almost equal to the temperature ratio for standard hydrocarbon fuels, since the pressure is nearly constant.

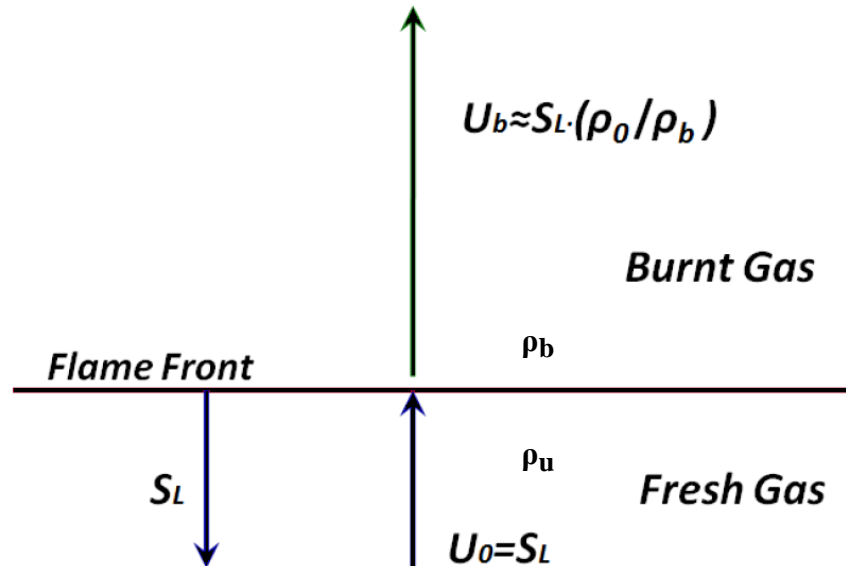


Figure 2.5 – Propagating flame front [11].

To conserve the momentum, the velocity jump must be accompanied by a small increase in pressure which is typically around 1 Pascal, given by:

$$\delta P = \frac{1}{2} \cdot (\rho_b U_b^2 - \rho_o U_o^2) \equiv \frac{1}{2} \cdot (\rho_o S_L^2) \left(\frac{\rho_o}{\rho_b} - 1 \right) \quad (23)$$

When the flame front is inclined with respect to the axis of propagation, as shown in Fig. 2.6, the propagation of the exhaust gases changes to conserve momentum.

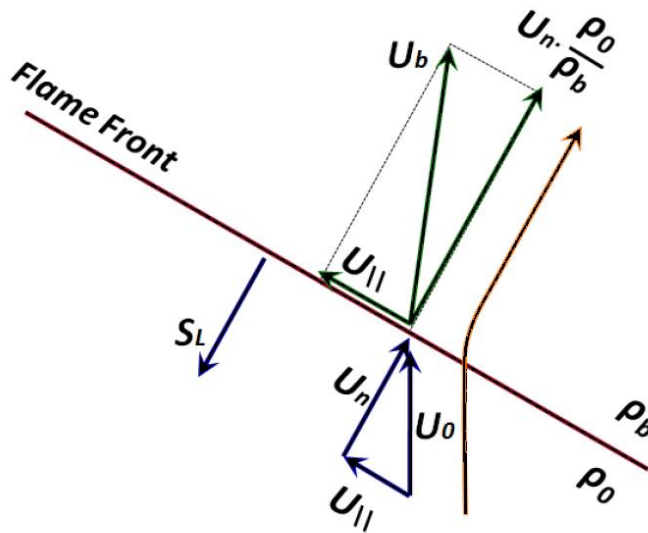


Figure 2.6 – Inclined flame front [11].

The incoming flow of the premixed fuel-air mixture can be decomposed into vector components which are parallel and normal to the flame front as $U_{||}$ and U_n respectively. If the flame front is the reference frame, then normal component of the incoming premixed mixture must be equal to

the flame velocity, $U_n = S_L$. The burnt gas leaving the flame front will have a normal component equal to $U_n(\rho_o/\rho_b)$ (thermal expansion). The parallel component of the flow remains unchanged as there is no physical mechanism to sustain the parallel pressure jump that would be necessary to accelerate the parallel component of the flow. Upon vector addition of the parallel and normal components, the resultant vector direction is now deviated to the outgoing normal. This causes the flow to change its direction after passing through the combustion wave if it is not perfectly normal to the flame-front sheet.

Consider a flame which is not planar, but is wrinkled at a wavelength λ as shown in Fig. 2.7. At the localized places where the streamlines are exactly normal to the flame-front, they are accelerated, but do not deviate, when they cross the flame. At places where the flame-front is inclined to the incoming mixture, the streamlines are deviated to the rear normal of the flame front. Although the streamlines in Fig 2.7 are locally correct, streamlines in a flow cannot cross each other and they must curve to become parallel in the far downstream as shown in Fig. 2.8.

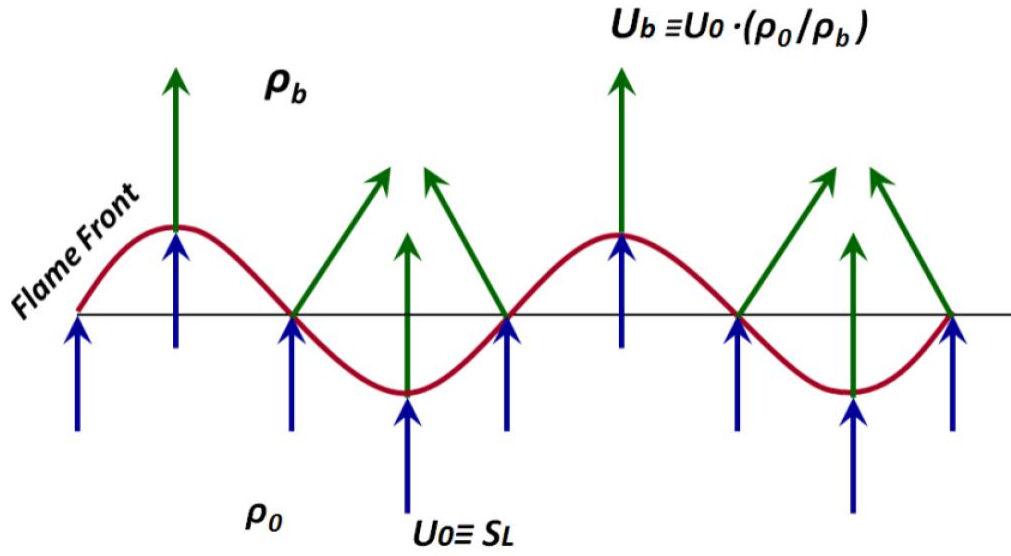


Figure 2.7 - Local streamline deviation in a wrinkled flame [11].

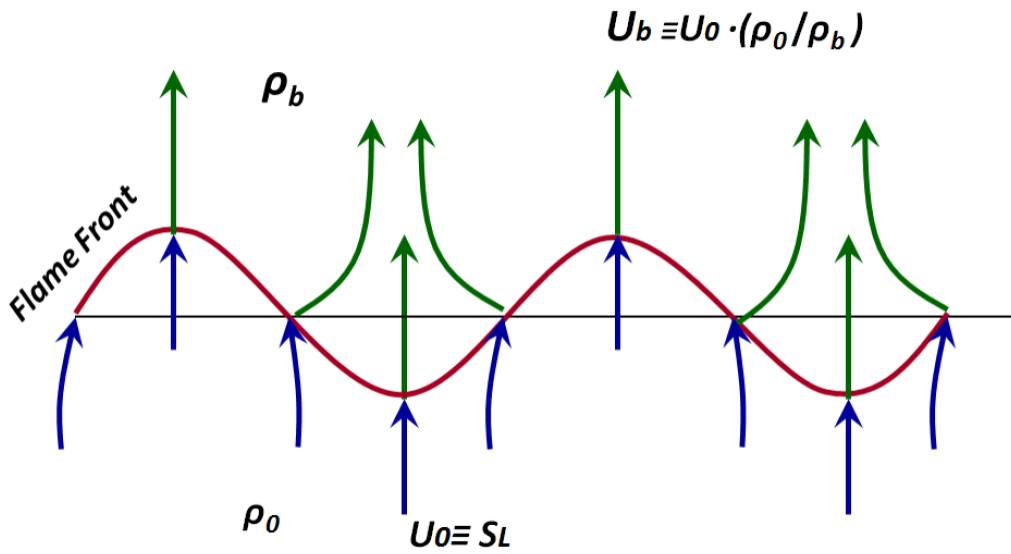


Figure 2.8 - Global streamline deviation in a wrinkled flame [11].

When the streamlines are curved, there are pressure gradients along the flow. This introduces perturbations which are not local. This non-locality of the presence of flame-induced pressure gradients will not only affect the downstream flow, but also the upstream flow. This effect causes the gas expansion through a curved flame to converge at places where the flame-front is concave and diverge where the flame-front is convex as shown in Fig. 2.8. Due to mass conservation, the upstream flow is either accelerated or decelerated where the flame front lags behind or is ahead of the mean position. Since we have assumed that the propagation velocity is constant, the flame front becomes unconditionally unstable and the wrinkling will grow with time.

2.4.2 Thermo-Diffusive Effects

The Zeldovich-Frank-Kamenetskii model of premixed flame propagation has high activation energy and the chemical reactions are confined to a thin layer on the high-temperature side of the flame front. The mechanism of flame propagation is primarily affected by the diffusion of the heat and species within the flame thickness, δ . In the case of a curved or wrinkled flame-front, the gradients of temperature and species concentration are not parallel to the average direction of flame propagation and therefore the local flame velocity can change.

At a place where the flame-front is concave towards the unburnt mixture, the heat flux is locally convergent. The local flame temperature and the local propagation velocity increase as a result. At a place where the flame-front is convex towards the unburnt gas, the heat flux is locally divergent. The local flame temperature and the local propagation velocity decrease as a result. The effect of thermal diffusion is to stabilize the wrinkled flame.

The gradient of the thermal diffusion is shown in blue arrows and that of species concentration is shown in green arrows in Fig. 2.8. The species gradient and the thermal gradient are in the opposite directions. At a place where the flame-front is concave towards the unburnt mixture, the species flux is locally divergent. The flux of reactive species into the reactive zone decreases as a result, leading to a decrease in the local propagation velocity. The effect of species diffusion is to destabilize a wrinkled flame. The net result of these two diffusive fluxes will depend on the ratio of the thermal and species diffusion coefficients. This ratio is called the Lewis number,

$$Le = D_{th}/D_{mol} \quad (24)$$

If the Lewis number is greater than unity, the effect of heat diffusion is prominent and the flame is thermo-diffusively stable. There is however an additional stabilizing contribution that arises from the inclination of the streamlines within the preheat zone. This internal inclination of the streamlines creates an additional transport of heat and species that is convergent or divergent with respect to the average direction of propagation. It has the effect of contributing an additional term in the expression for the flame velocity. This term is always stabilizing, independent of the Lewis number, and it increases with the gas expansion ratio.

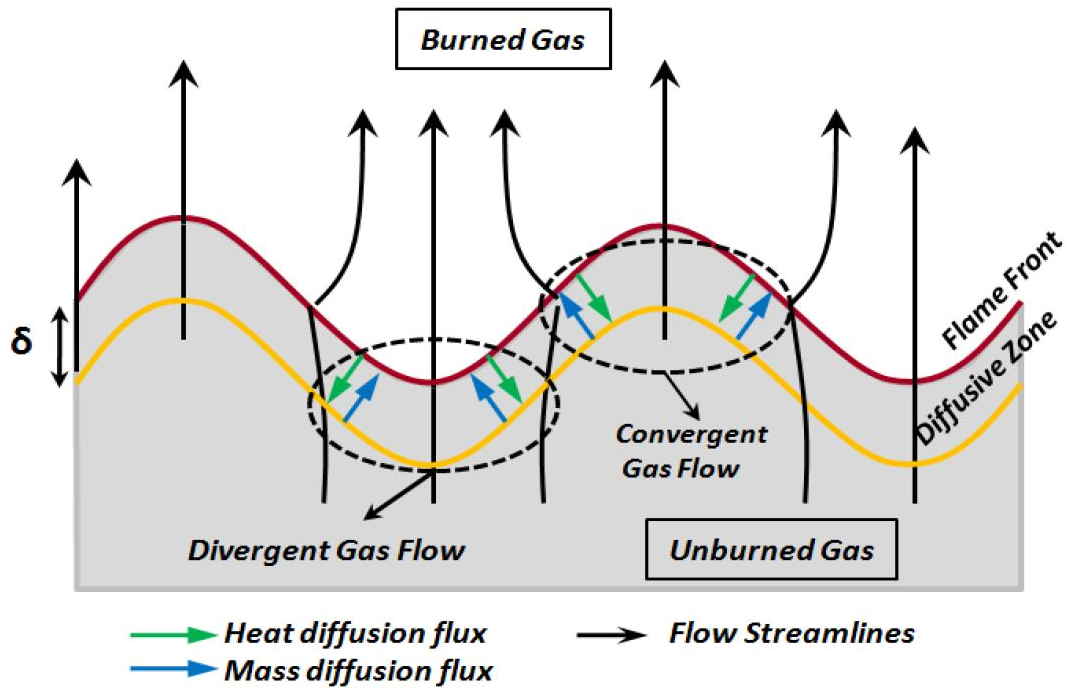


Figure 2.9 - Wrinkled premixed flame structure [11]. In the concave region of convergent gas flow, the streamlines move closer together, where the diffusion and mass flux is divergent (and the upstream heat flow is convergent).

2.4.3 Thermo-Acoustic Instabilities

Combustion in constant volume generates acoustic waves that can interact with the flame front and cause perturbations in the flames. These acoustic waves are usually reflected off of enclosing walls and internal obstacles. Instability mechanisms that produce such perturbations have been studied under different experimental conditions. Thermo-acoustic instabilities usually manifest itself as flame distortion leading to increased flame surface area, increased flame propagation speed and peak pressure enhancement. Lining of the combustion chamber walls with materials that can absorb acoustic waves, or using obstacles to deflect the acoustic waves can help to reduce the intensity of these acoustic instabilities.

Unsteady combustion is a strong source of acoustic noise, whose emission is governed by the conservation equations given by:

Mass conservation

$$\frac{D\rho}{Dt} + \nabla \cdot \rho \mathbf{V} = 0 \quad (25)$$

Momentum conservation

$$\rho \frac{D\mathbf{V}}{Dt} = -\nabla p \quad (26)$$

Energy Conservation

$$\rho C_p \frac{DT}{Dt} = \dot{q} + \frac{Dp}{Dt} + \nabla \cdot (\lambda \nabla T) \quad (27)$$

Equation of state

$$\frac{P}{\rho} = (C_p - C_v)T = \frac{C_v}{C_p} a^2 \quad (28)$$

where $D()/Dt$ is the material derivative, V is the gas velocity vector and a is the local speed of sound.

Combining the energy conservation and the equation of state, we obtain:

$$\frac{Dp}{Dt} = a^2 \frac{Dp}{Dt} + \left(\frac{C_p - C_v}{C_v} \right) \dot{q} \quad (29)$$

When an acoustic wave interacts with a flame-front, the heat released due to reaction will be a function of the acoustic pressure magnitude. This phenomenon was described by Rayleigh [12] as follows – “If heat is periodically supplied and removed from a mass of vibrating air, the effect produced will depend on the phase of vibration. If the heat is supplied at the moment of highest condensation and removed at the moment of highest rarefaction, the application of heat would lead to a support of the vibration.”

The Rayleigh criterion states that positive energy is transferred to the acoustic wave if pressure and heat release fluctuations are in phase and negative energy is transferred to the acoustic wave if pressure and heat release functions are out of phase.

The two major types of coupling between acoustic wave and the combustion process are pressure coupling and acceleration coupling, which are discussed in greater detail below.

Pressure Coupling

The standard form of the chemical reaction rate in the Zeldovich-Frank-Kamenetskii model [6] using Arrhenius law is described below:

$$\Omega = A\rho Y^{\frac{-E_a}{RT}} \quad (30)$$

Where A is the pre-exponential factor, Y is the mass fraction of the limiting reactant, E_a is the activation energy and ρ is the reactant density.

According to the above expression, the reaction rate is directly proportional to the density of the reactants. The density of the reactant is proportional to its pressure if the reactants obey ideal gas law, this leads to variation in the reaction rate with changes in density caused due to pressure waves. The propagation of acoustic waves also causes an increase in the local temperature due to its adiabatic nature. For reactions with high activation energies, the heat release is primarily sensitive to the temperature oscillation produced by the acoustic waves.

The coupling of acoustic pressure waves and the reaction depends on the acoustic frequency, angular velocity and the Lewis number of the reactant. The use of one-step Arrhenius equation to model the reaction leads to a mismatch between the theoretical result and experimental investigations performed on planar methane-air flame subjected to acoustic oscillation.

Acceleration Coupling

The local velocity field in an acoustic wave imparts a localized acceleration on the flame front, which leads to changes in the reaction rate. The flame-front is also influenced by other acceleration fields such as gravity due to the differences in the densities of the fluids separated by a flame-front.

When the localized velocity of the pressure wave is oriented towards the unburnt mixture, the size of the reaction cell increases and when the localized velocity of the pressure wave is oriented towards the burnt mixture, the size of the reaction cell decreases. The total reaction rate of the combustion process is directly proportional to the size of the reaction cell, hence the acceleration coupling between the flame-front and pressure wave has a major effect of the reaction rate of the flame.

CHAPTER 3

EXPERIMENTAL SETUP, TEST METHODOLOGY AND DATA ACQUISITION

The experimental setup consists of a constant volume combustion chamber with a square cross section, high speed camera to capture the ignition and propagation of the flame, pressure transducer and ignition control circuit to record the pressure and electronically control the ignition time and a Schlieren diagnostic setup to visualize the density change during combustion.

The pressure transducer and the ignition circuit are connected to a computer through data acquisition and control hardware. LabView program interface is used to initiate the spark and record the pressure inside the combustion chamber.

3.1 COMBUSTION CHAMBER SETUP

The combustion chamber apparatus consists of three metal parts, the center plate and two side plates which are bolted together to form a constant volume combustion chamber. The enclosed combustion chamber is 12 inches long and has a square cross section with each side measuring 2 inches. The total volume of the combustion chamber is 48 cubic inches. An exploded view of the apparatus is shown in Fig. 3.1. Its dimensions are specified in Fig. 3.5.

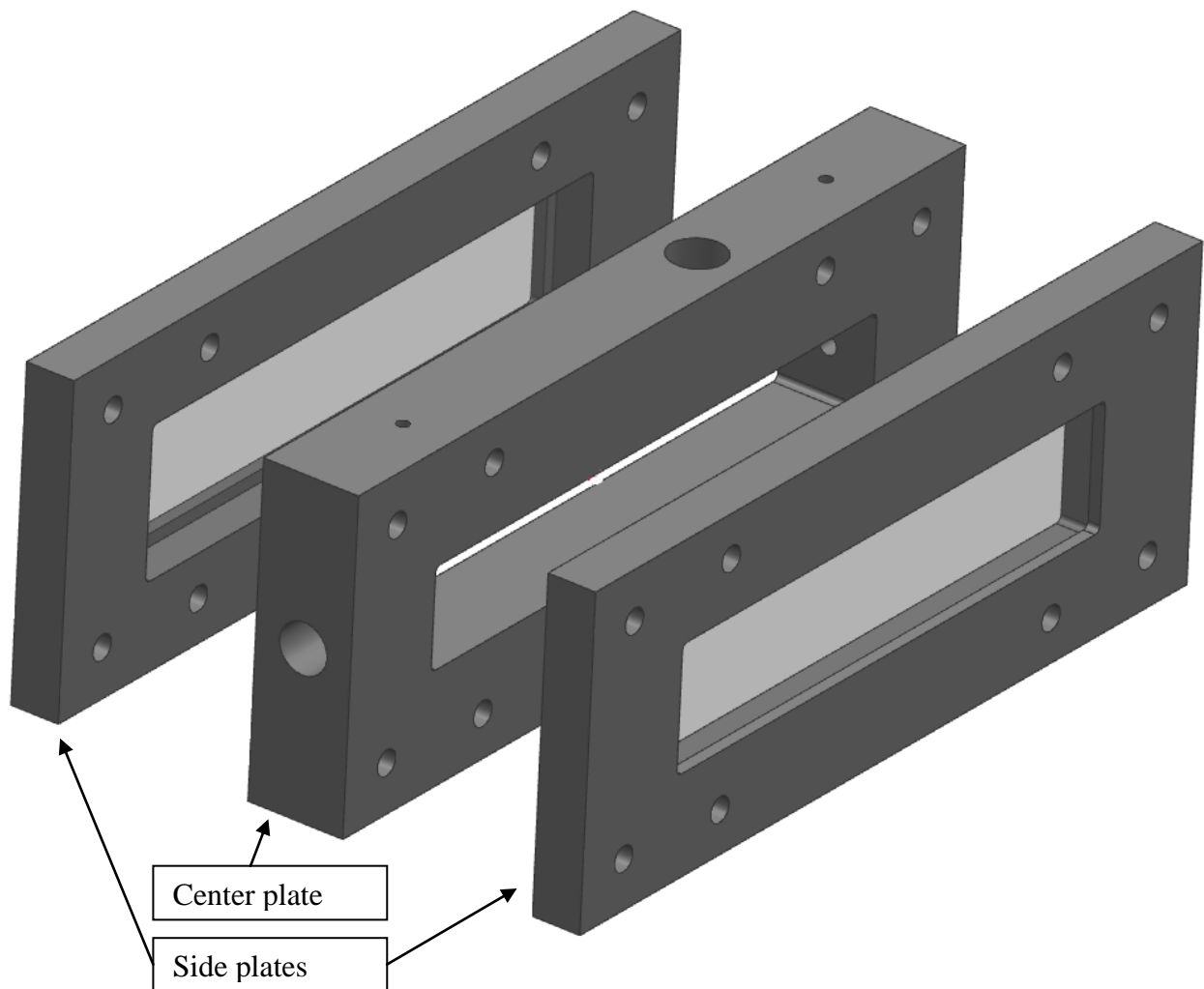


Fig 3.1 – Exploded view of combustion chamber apparatus.

The combustion chamber apparatus is designed to withstand a maximum pressure of 35 bar and a pressure relief valve rated at 20 bar is mounted to ensure pressure remains within the safe limits. The isometric view of the combustion chamber model is shown in Fig. 3.2. The manufactured apparatus is shown in Fig. 3.3. Teflon tape is used to form an air-tight seal between the pressure transducer, spark plugs, quick-disconnect valves and the combustion chamber apparatus. High-temperature transparent silicone sealant is used to attach the glass window to the side plate of the apparatus.

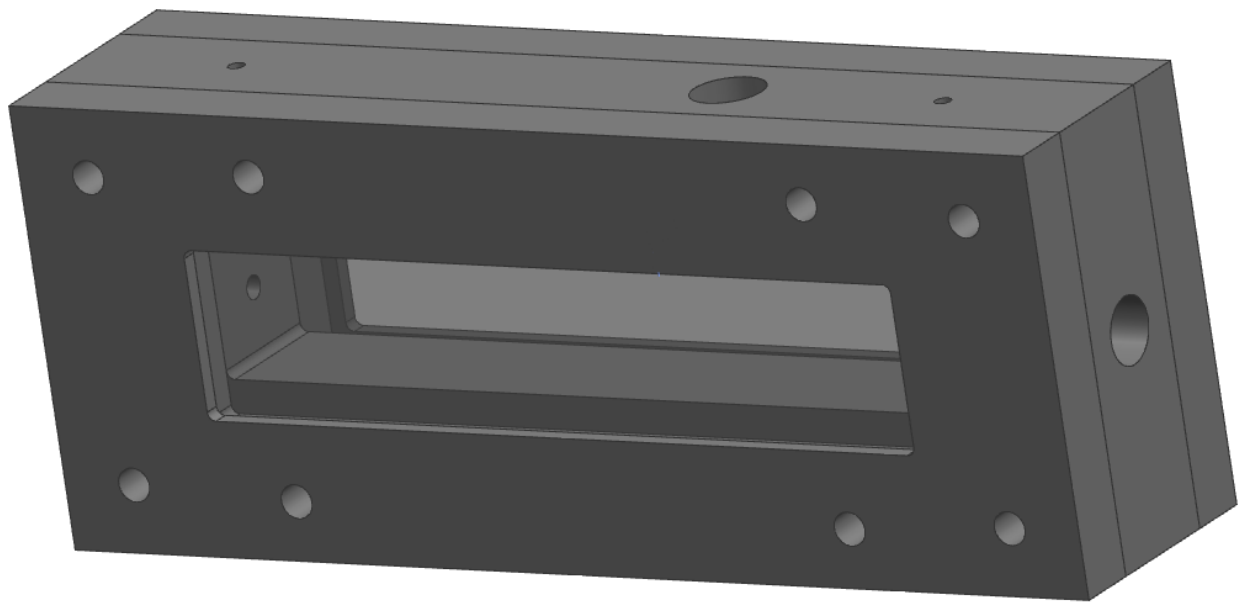


Fig 3.2 – Isometric view of combustion chamber apparatus.

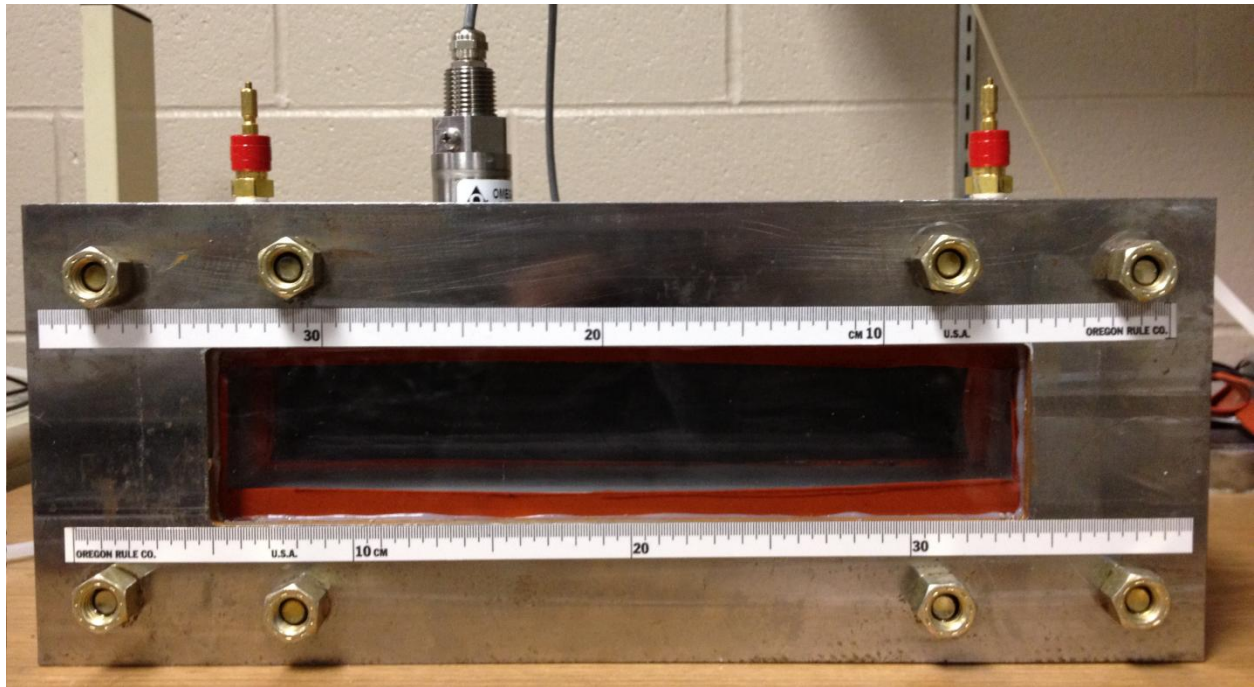


Fig 3.3 – Manufactured combustion chamber apparatus.

The center plate made of aluminum measures 16.5x6.5x2 inches. A hollow channel measuring 12x2x2 inches is machined into the plate which forms the combustion channel. The center plate is machined further to mount the flush-diaphragm pressure transducer, spark plugs, and inlet and exhaust ports. The inlet and exhaust ports are used to remove the combusted gases and fill the combustion chamber with fresh fuel-air mixture. The ports have a diameter of 0.125 inches, located near both ends of the combustion chamber to avoid disrupting the flame structure. The isometric and orthographic projection of the center plate is shown in Fig. 3.4 and Fig. 3.5.

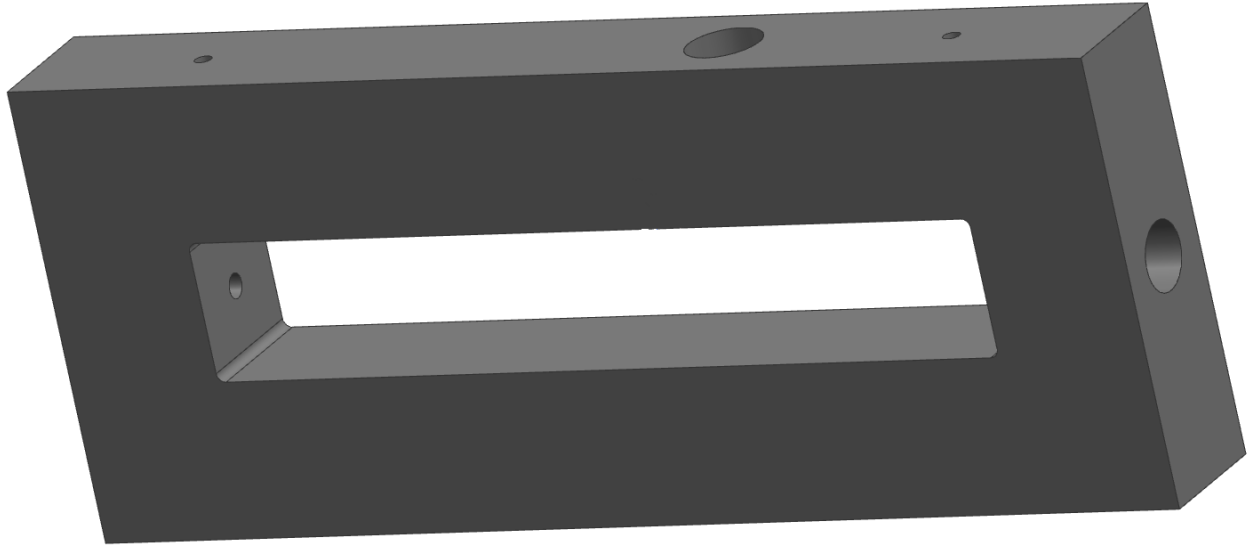


Fig 3.4 – Isometric view of center plate.

Fig 3.5 – Orthographic view of center plate. Dimensions are in inches.

The center plate is sandwiched between two side-plates. The side plate holds a glass window that forms the side wall of the combustion chamber. The side plate is made of steel and measures 16.5x6.5x1 inches. It has a recessed opening measuring 12x3x0.75 inches with a 0.25 inch lip along the sides to hold the glass window as shown in Fig. 3.6 and Fig. 3.7. A borosilicate glass plate measuring 12x3x0.75 inches is mounted on the recessed opening and forms the side-wall of the combustion chamber. The glass plate is attached to the side plate using Loctite high-temperature silicone sealant which forms an airtight seal. The side plate and center plate are bolted together with brass bolts of 0.5 inch diameter. An airtight seal is formed between the side plate and center plate by lining the contact surface with Loctite silicone gasket. The isometric and orthographic view of the side plate is shown in Fig. 3.6 and Fig. 3.7.

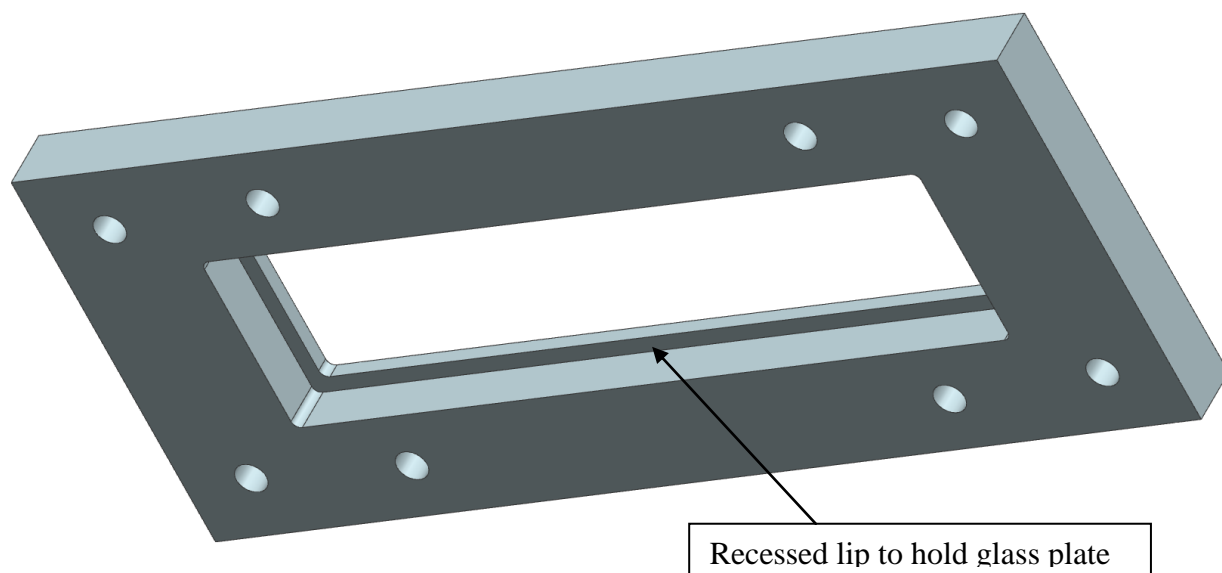


Fig 3.6 – Isometric view of the side plate.

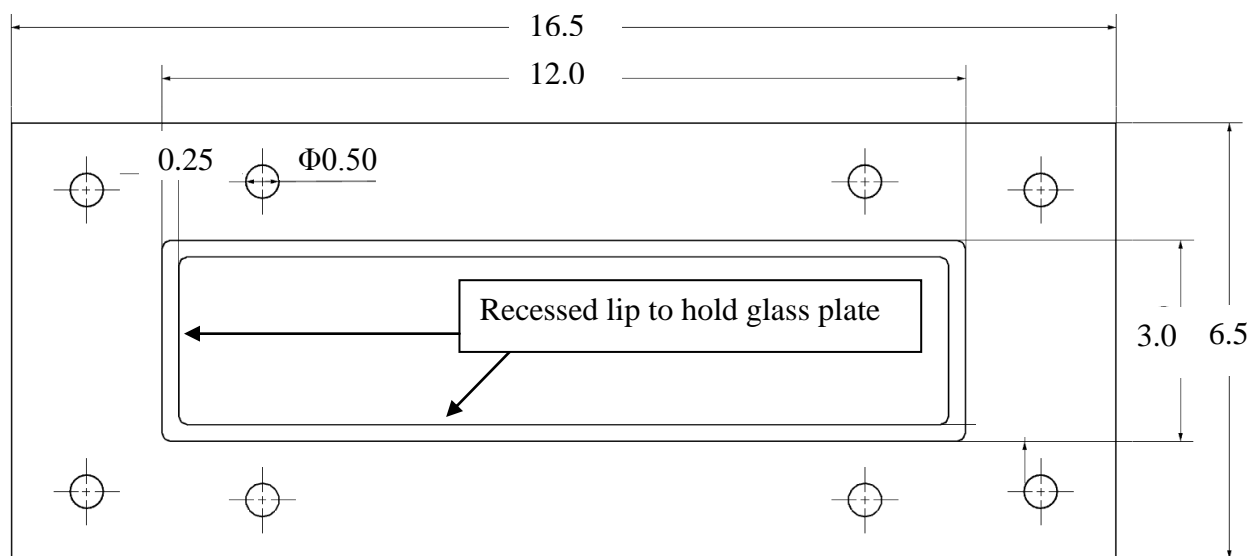


Fig 3.7 – Orthographic view of the side plate. Dimensions are in inches.

To maintain a constant volume during combustion and avoid leakage from the inlet and exhaust ports during rapid pressure changes, SwagelokTM quick-connect couplings (BQC4D2PM) are mounted on the inlet and exhaust ports. The quick-connect coupling has a shut-off valve with a pressure rating of 25 bar. An Omegadyne PX43EO-100GI flush-diaphragm pressure transducer

is mounted on the center plate for pressure measurement. The transducer is positioned to ensure the diaphragm is flush with the upper wall of the combustion chamber and Teflon tape is used to seal the screw interface. Two MSD 10mm spark-plugs are flush-mounted on both ends of the combustion chamber along its length. The spark plugs are powered by MSD Blaster 2 ignition coils which supply 10mJ of energy for every spark discharge. An optional high-energy discharge module can be plugged in to increase the energy deposited to 50mJ. The pressure transducer is connected to a National Instruments NI9203 data acquisition module. The ignition coils are attached to a National Instruments NI9841 digital relay module. The acquisition and relay modules are mounted on a National Instruments NI cDAQ-9172 data controller module which is connected to the computer. LabView is used to control the firing of the spark plugs and to record the pressure inside the combustion chamber. The pressure reading from the transducer is sampled at 10 kHz. A screenshot of the LabView interface is shown in Fig. 3.8. The flame propagation is optically recorded using a Photron SA5 high speed camera which is focused onto the glass window of the apparatus. The camera is configured to capture the combustion event at 20,000 FPS frame rate.

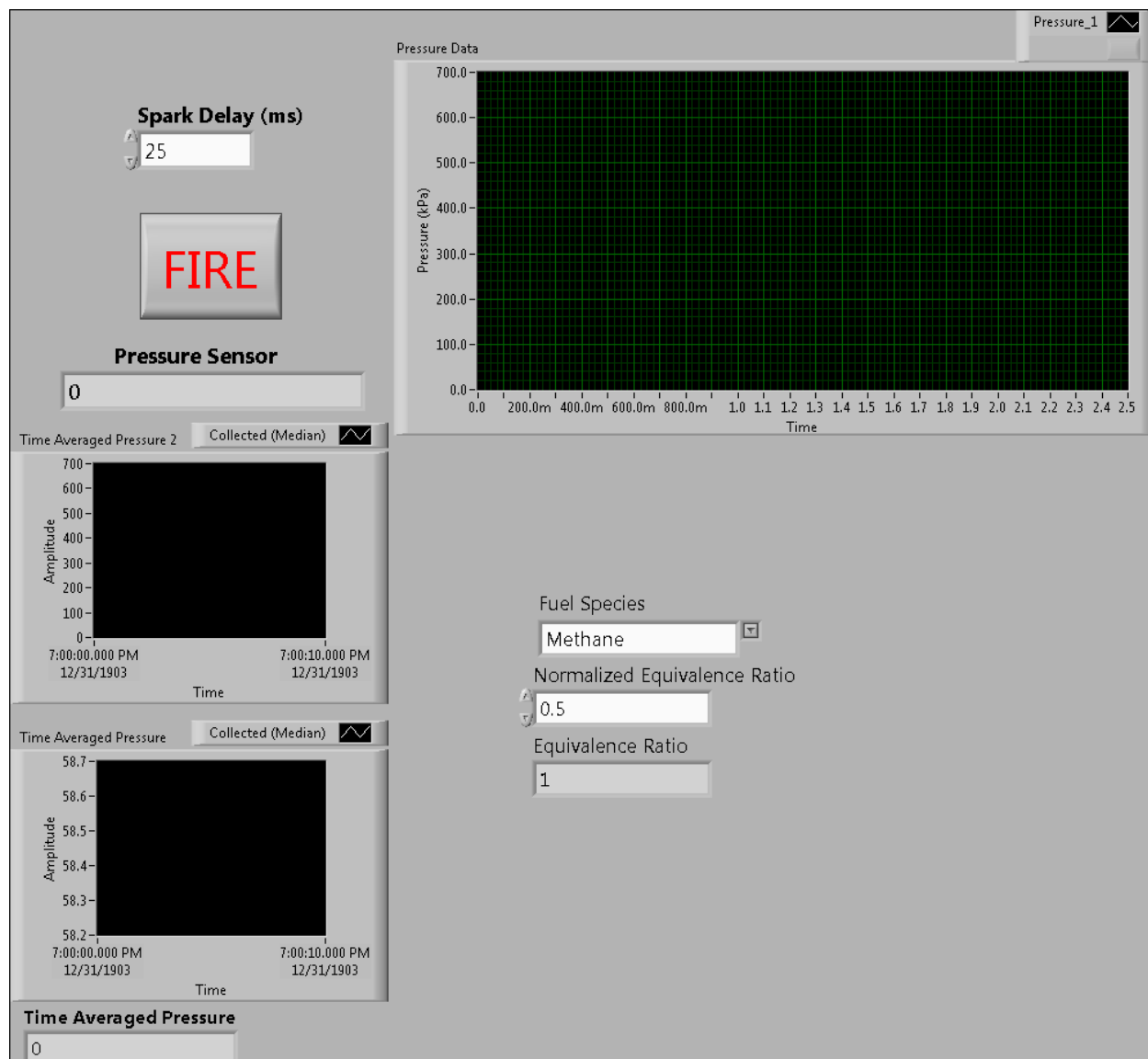


Fig 3.8 – LabView interface.

3.2 SCHLIEREN SETUP

To visualize the change in the density across the flame front and also study the structure of the flamefront, a Schlieren imaging system was constructed. The system consists of two spherical concave mirrors 6 inches in diameter with focal length 60 inches. A pin-hole light source forms a collimated beam of light along the test area. The light beam is focused onto the lens of the high speed camera after passing through a knife edge. A schematic arrangement of the Z-type schlieren imaging setup is shown in Fig. 3.9. The theory of schlieren imaging is discussed in Appendix B.

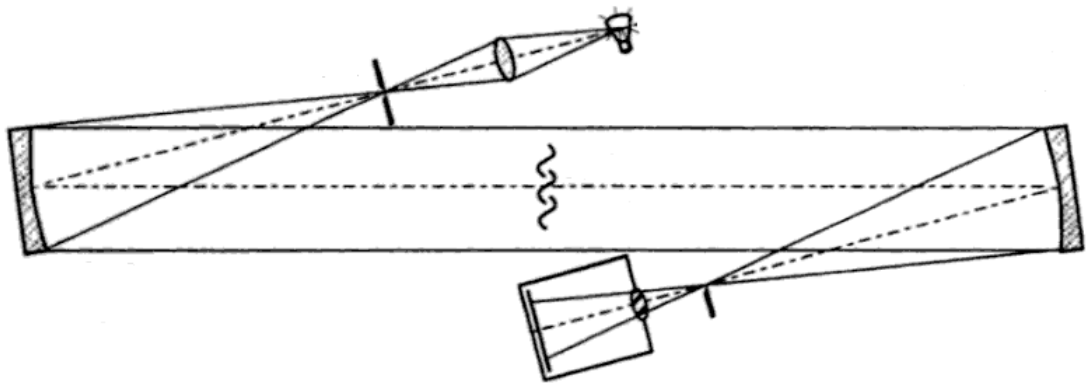


Fig 3.9 – Schlieren imaging setup.

3.3 TEST PROCEDURE

The test procedure involves filling the combustion chamber with a fuel-air mixture. Upon equilibration, the mixture is ignited with a spark plug. The pressure data along with optical imaging of the flame propagation is recorded electronically. The combustion chamber is initially filled with compressed air and tested for leakages every time it is disassembled and reassembled.

The procedure used in performing a test is as follows –

1. The combustion chamber is assembled to the required configuration and tested for leaks using compressed air.
2. The exhaust valve is closed and fuel is injected into the combustion chamber to the required equivalence ratio.
3. The fuel-air mixture is allowed to settle inside the combustion chamber for a period of 30 minutes to obtain a fully premixed mixture.
4. The mixture is ignited using at least one spark plug. The pressure and a video of the flame propagation is recorded and stored electronically.
5. The combusted gases are removed by flushing the system with compressed air for a period of 10 minutes and the cycle is repeated for a new set of experimental conditions.

The waiting time for the diffusion of fuel in air to obtain a fully premixed mixture and the time required to remove combusted gases from the combustion chamber by flushing compressed air through the system was determined after performing tests for varying mixing and flushing times and empirically ascertaining the minimum time required for repeatable test results.

The amount of fuel that needs to be injected to obtain the required equivalence ratio is obtained using Dalton's law of partial pressure, which states that the total pressure exerted by the mixture of non-reactive gases is equal to the sum of the partial pressures of individual gases.

$$\frac{P_i}{P_{\text{total}}} = x_i \quad (31)$$

Using this equation, we obtain the final pressure of the combustion chamber after filling it with fuel. Depending on the fuel used, the initial air pressure is either maintained at ambient pressure or a partial vacuum is created in the combustion chamber to maintain a final total pressure that is close to atmospheric pressure.

The optical measurements were conducted by focusing the camera on the side of the combustion chamber. For optical measurement of flame propagation, one of the glass plates of the combustion chamber is closed to produce a dark background for the flame. When using the Schlieren technique, collimated light is allowed to pass through either side of the glass plates to form an image of the flame structure. The camera records the experiments at either 5000 or 20,000 frames per second (FPS) depending on the flame speeds and test conditions. In order to reduce noise and capture an accurate structure of the flame, background light is eliminated by running the tests in a dark room. The pressure data are recorded at 10 kHz and stored along with the ignition data. Once the experiment is completed, the recorded images are post processed in MATLAB to obtain the instantaneous position of the flame along with the flame speed. The MATLAB program used to post-process the recorded images is described in appendix A.

CHAPTER 4

EXPERIMENTAL RESULTS

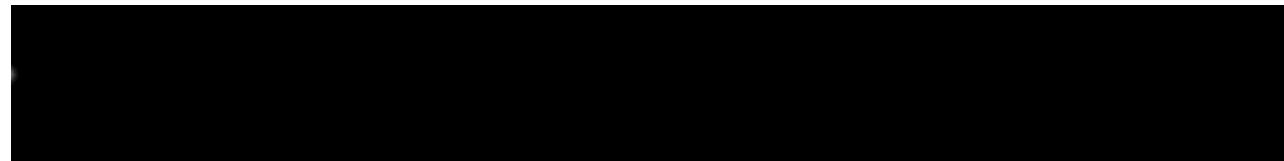
A stoichiometric mixture of methane and air is used as the combustible mixture in all the experimental tests performed. This is done to ensure that the results of different combustion chamber configuration and ignition conditions can be compared with each other. Based on Dalton's law of partial pressure, for stoichiometric methane-air mixtures, the final pressure of the combustion chamber is calculated to be 111.96 kPa. The initial condition is obtained by flushing the system with compressed air. Methane is pumped into the combustion chamber at ambient pressure until the final pressure is 111.96 kPa. The inlet and exhaust valves are closed. The mixture is allowed to settle for 30 minutes to allow complete mixing to form a fully premixed fuel-air mixture.

The structure and propagation of flames in a variety of test conditions was studied. A detailed analysis for the structure of a flame in a long, straight channel is discussed in Chapter 6. In order to maintain consistency between different test results, the pressure transducers are recalibrated every 10 cycles of usage. To ensure an accurate mixture ratio inside the combustion chamber, an Omega PX43EO-25GI pressure transducer, with an accuracy of 0.1% over the range of 25 psi, is used to measure the amount of methane injected into the combustion chamber.

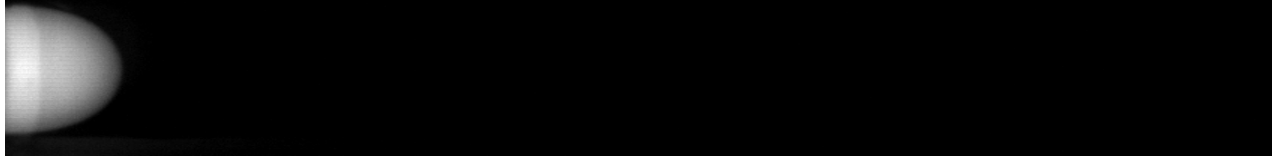
4.1 SINGLE SPARK IGNITION

In the single spark ignition setup, the combustion chamber is filled with stoichiometric methane air mixture at an initial pressure of 1 bar. The premixed fuel air mixture is ignited by a single spark source. A record of the pressure and flame propagation is made. The video is post-processed in MATLAB to obtain the position of the flame front for every frame.

Upon ignition by a spark plug, a growing spherical flame kernel is initially formed. The flame-front grows faster along the length of the tube when compared to the width, which leads to the elongation of the flame. The flame area grows rapidly to form a “finger” shaped flame front. When the sides of the finger flame touch the cold walls, the side skirt is extinguished, the surface area of the flame rapidly decreases and it progressively flattens and takes the shape of a planar flat flame. The planar flame subsequently changes its shape to eventually form an inward pointing cusp near its center; this shape is has been called the “tulip-flame”. The flame front maintains its tulip shape as it propagates along the length of the tube until it is extinguished by the cold wall on the opposite end of the tube. Small distortions to the tulip flame are caused by the influence of pressure waves and gravity. The optical record of the flame propagation is shown in Fig. 4.1 for every 10 milliseconds time intervals from ignition until extinction.



t=0 ms, Ignition.



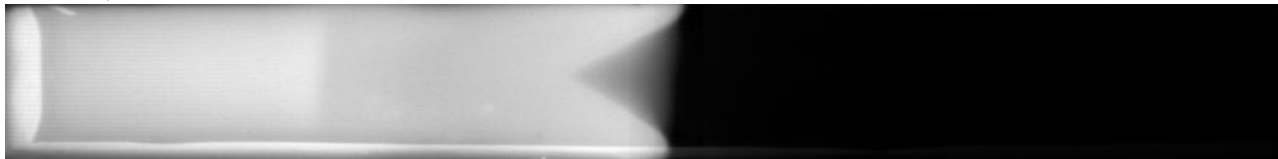
t=10 ms, Spherical flame.



t=20ms, Finger-flame formation.



t=30 ms, Planar flame.



t=40 ms, Formation of tulip flame.



t=50 ms, Propagation of tulip flame.



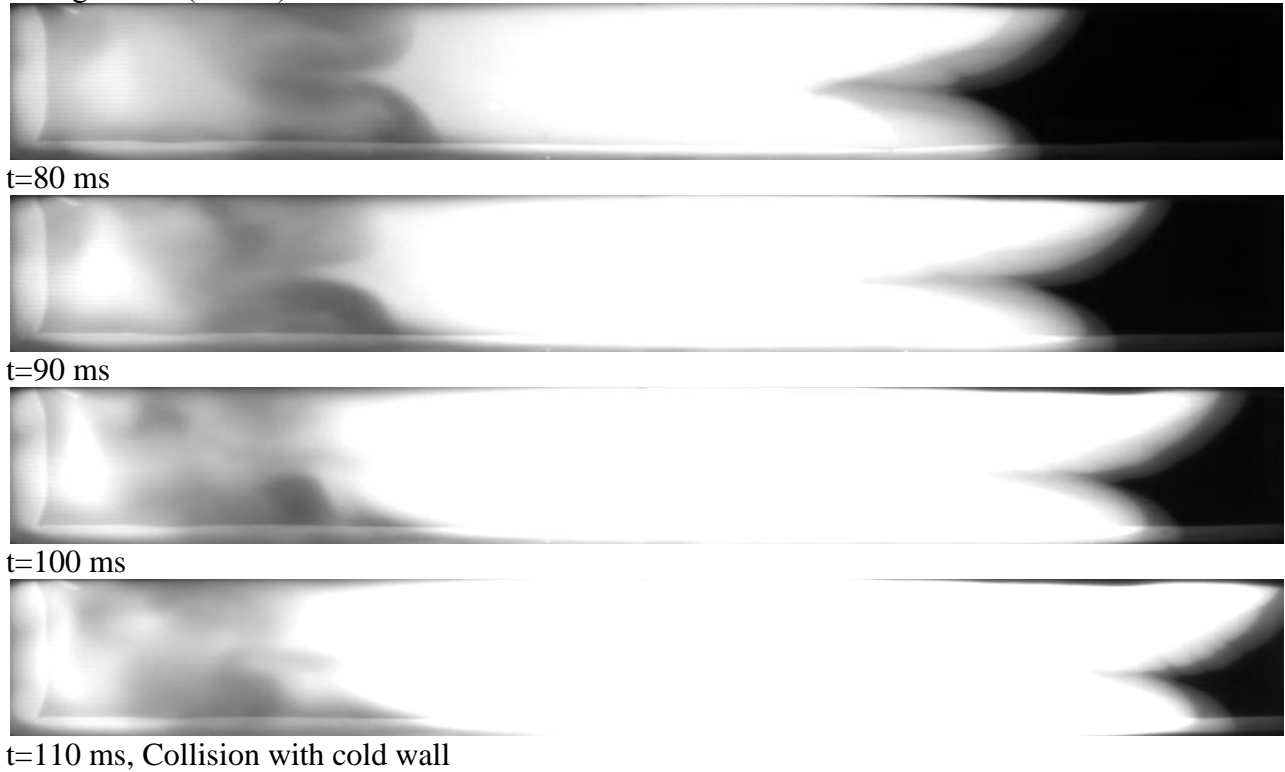
t=60 ms



t=70 ms

Figure 4.1 – Flame propagation along the tube, showing the evolution of the flame structure

Figure 4.1 (cont'd)



Upon ignition, the spherical flame-front grows rapidly and 10 milliseconds after ignition, a finger flame develops. At $t=30$ milliseconds, the finger flame skirt is quenched by the cold wall and the flame surface area rapidly decreases. This causes the flame to slow down and the flame front collapses to form an inward pointing cusp called the “tulip flame” at $t=40$ milliseconds. The flame front eventually collides with the cold wall at the opposite end of the tube at $t=120$ milliseconds while preserving its tulip shape. The schlieren imaging of the ignition event is shown in Fig. 4.2.

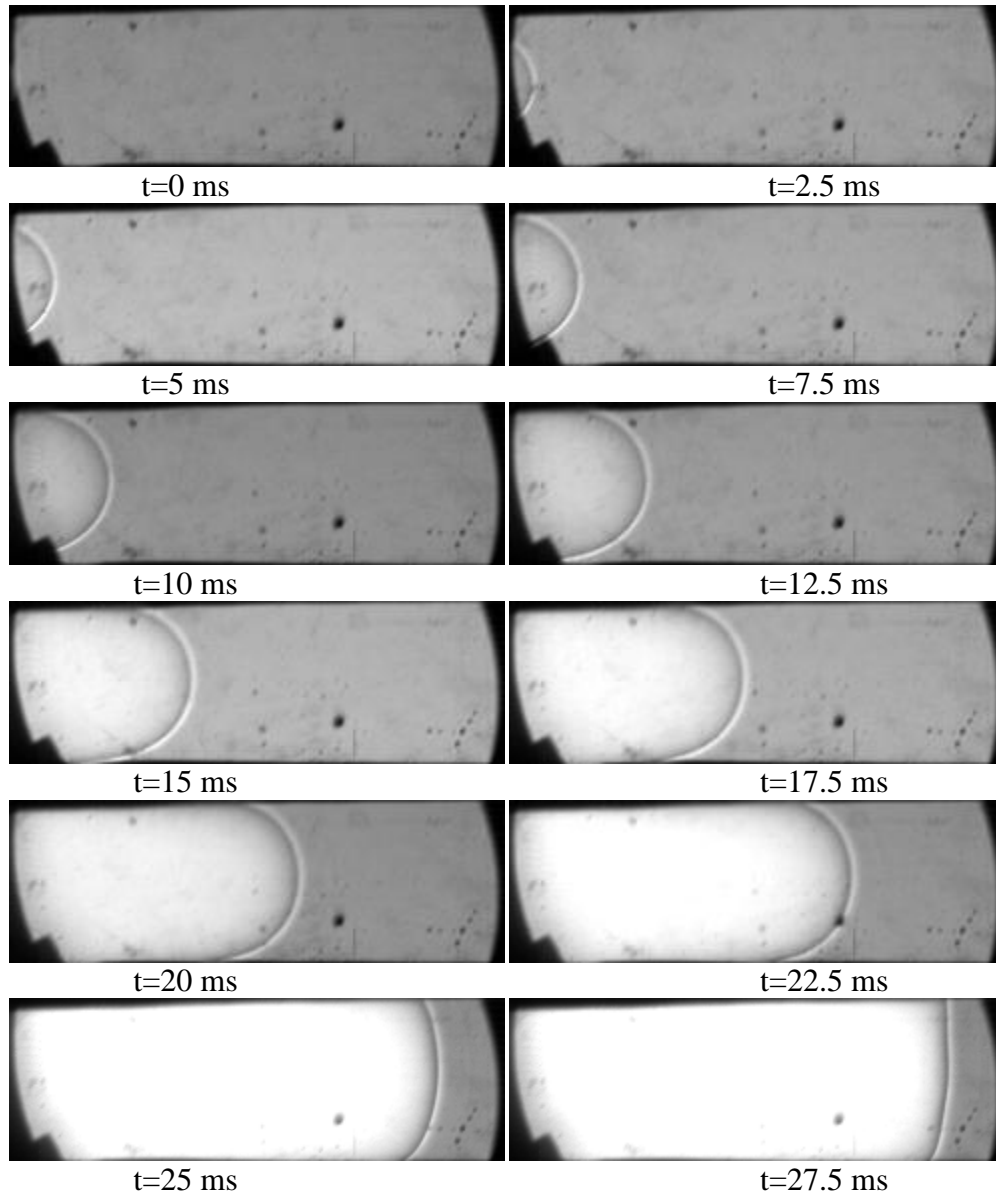


Figure 4.2 – Schlieren image of ignition.

We observe that ignition by the spark plug is followed by a rapidly expanding spherical flame front, which can be observed from 2-10 milliseconds. The tip of the flame travels faster than the sides of the flame. This leads to the formation of an elongated “finger flame”, which can be seen at 15 milliseconds in Fig. 4.2. The sides of the finger flame are quenched by the cold wall and cause the flame surface area to decrease rapidly. A planar flame shape occurs at 27.5 milliseconds.

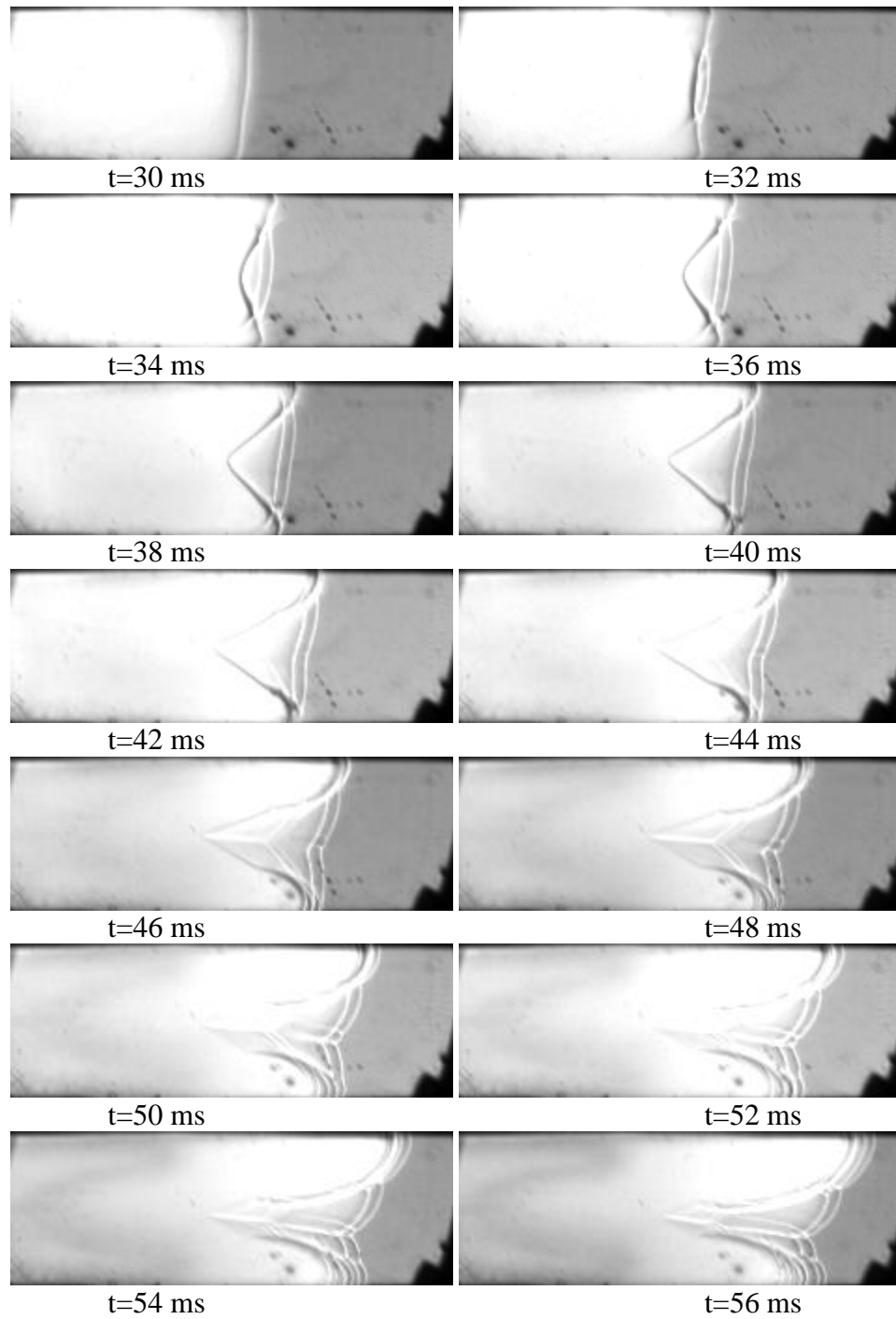


Figure 4.3 – Schlieren image of tulip formation.

The transition from a planar flame front to a tulip flame takes place in 10 milliseconds. At $t=38$ milliseconds, we observe the 3-D structure of the tulip, which is an inward pointing cusp at the center from which four “petals” emerge. The two vertical lines near the outer edge of the lobe are

the flame close to the glass walls. At $t=50$ milliseconds, the tulip shape undergoes distortion to its structure from thermo-acoustic instabilities and the influence of gravity. This causes the formation of smaller cells to grow along the lobes of the tulip flame. The effect of gravity driven buoyancy causes the upper lobe of the tulip flame to travel a little faster than the lower lobe.

The normalized position of the flame front is shown in Fig. 4.4. The various stages of flame front structure are marked. Stage I indicates the ignition event followed by the growth of the spherical flame. Stage II begins with the formation of the finger flame. Stage III indicates the transition from a finger flame to a planar flame. The planar flame which subsequently changes to a tulip flame is shown in stage IV.

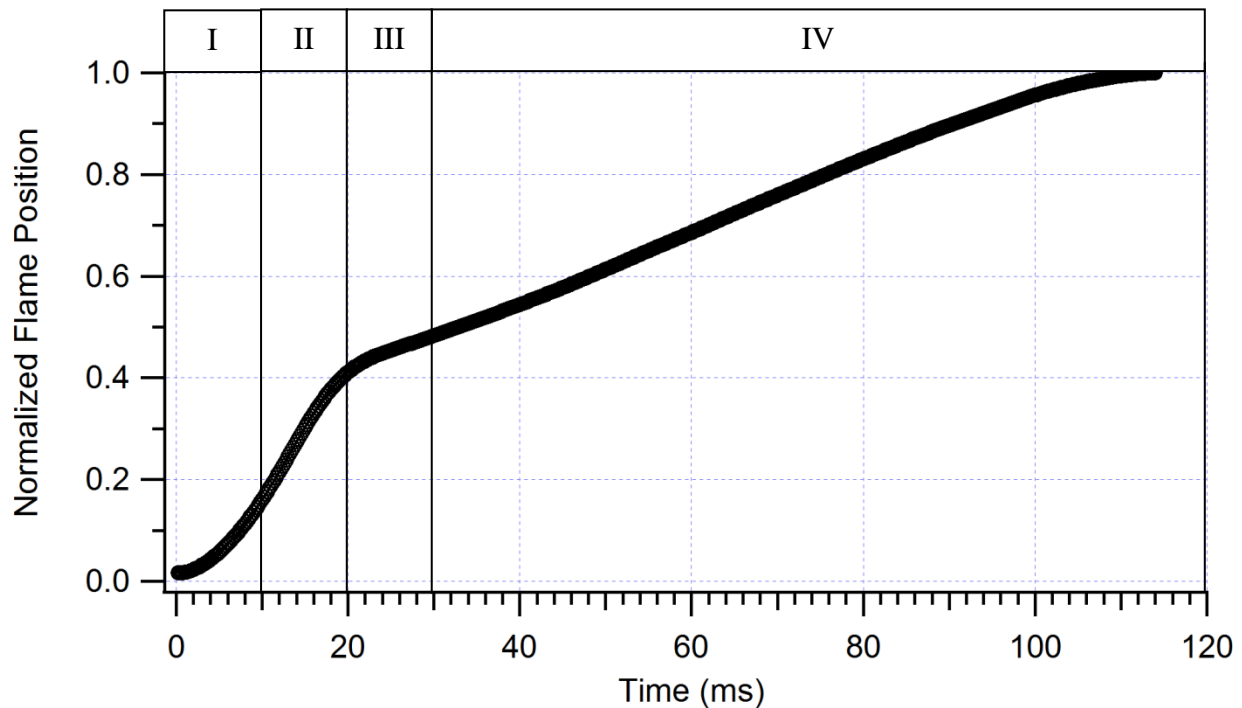


Figure 4.4 - Flame position vs time, showing the four stages of flame propagation (I=ignition; II=finger flame; III=transition to planar flame; IV=propagating tulip flame).

The normalized flame position data shows the mean position of the flame front for each instant of time. The flame position changes rapidly from 0 to 20 milliseconds, after which the rate of change in the mean flame position is slower. The flame speed data are obtained by calculating the time-derivative of the flame position as shown in Fig. 4.5.

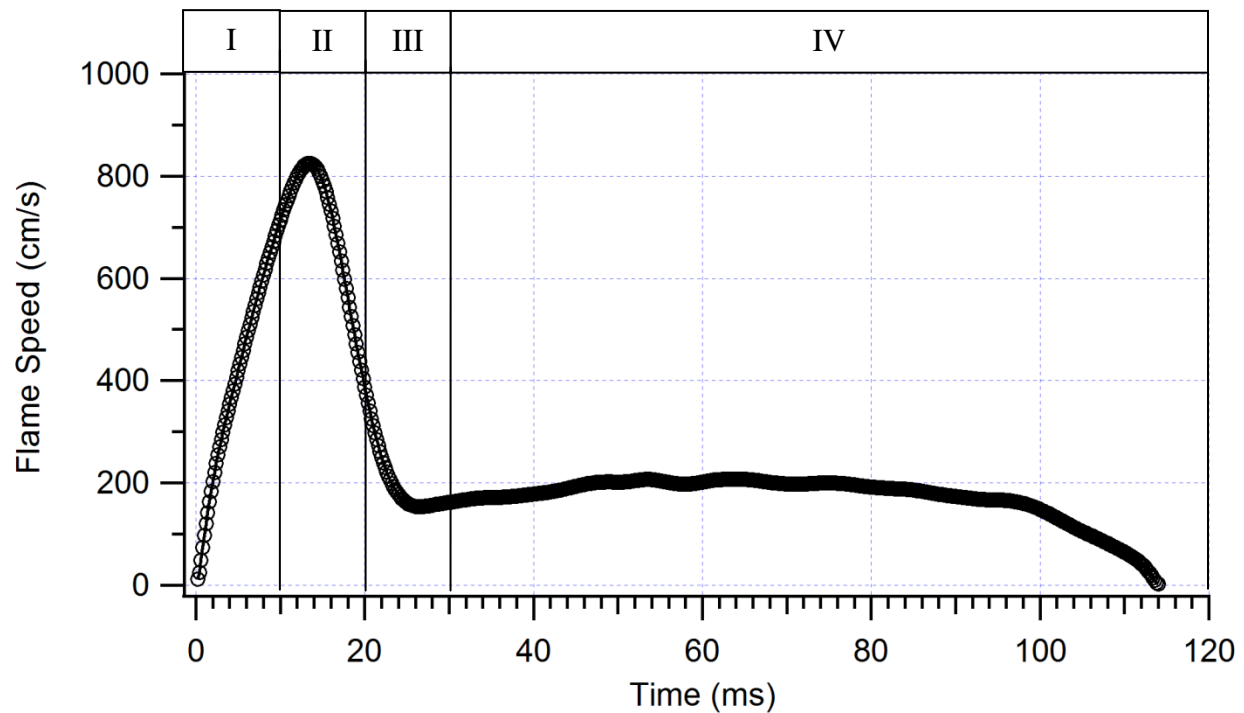


Figure 4.5 - Flame speed vs time.

The flame speed plot in Fig. 4.5 indicates that the fastest physical flame speed occurs shortly after ignition. The spherical flame kernel accelerates towards the unburnt mixture. Its surface area increases correspondingly. At $t=15$ ms, the surface area of the flame-front reaches its maximum. The speed of the flamefront starts to decrease as the flame shape becomes planar. At $t=25$ ms, the flame transforms to a tulip shape. The speed of propagation remains approximately constant until it is quenched by the cold wall on the opposite end of the tube at $t=118$ ms.

The instantaneous flame speed for the normalized position on the tube is shown in Fig. 4.6. It is observed that the transformation of the flame front from planar to tulip shape takes place at roughly half the length of the tube. The speed of propagation of the flame front is approximately constant after the tulip shaped flame front has formed.

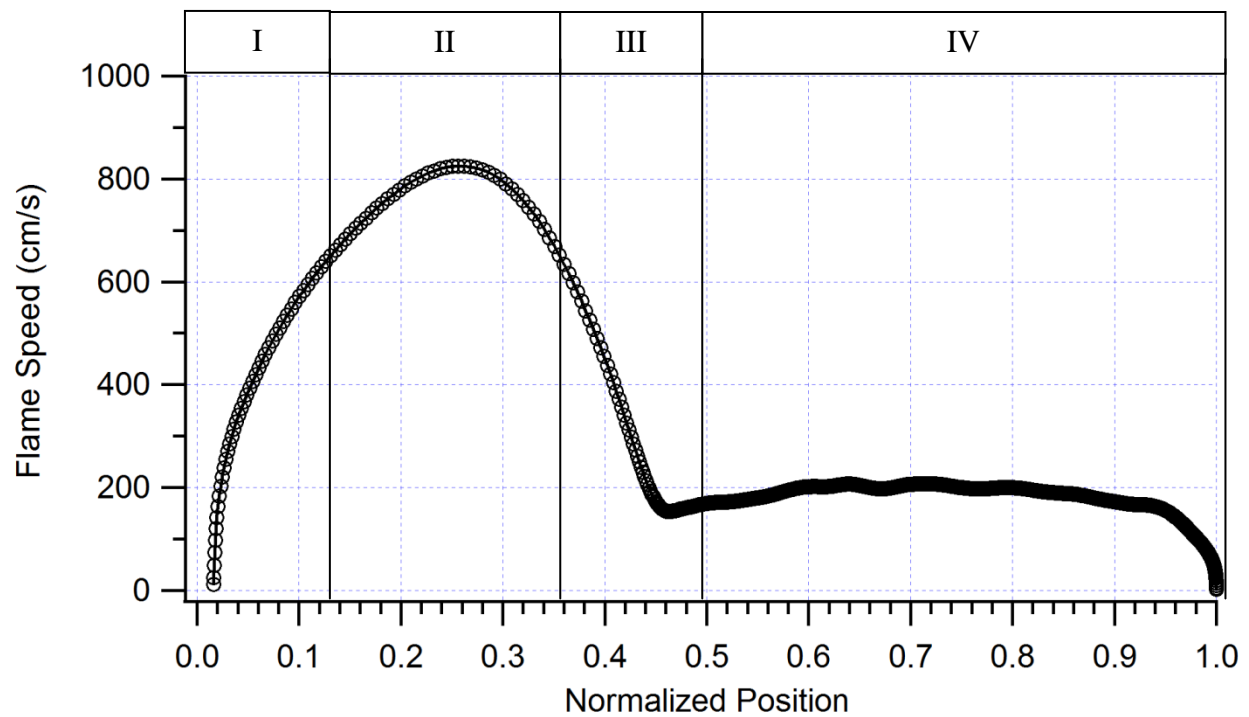


Figure 4.6 - Flame speed vs normalized position.

The corresponding pressure plot for the single spark combustion is shown in Fig. 4.7. The pressure inside the combustion chamber reaches its maximum value about 15 ms before flame extinction. This occurs due to the loss of heat from the burnt mixture to the cold aluminum wall which causes a decrease in temperature in the burnt mixture with increase in time.

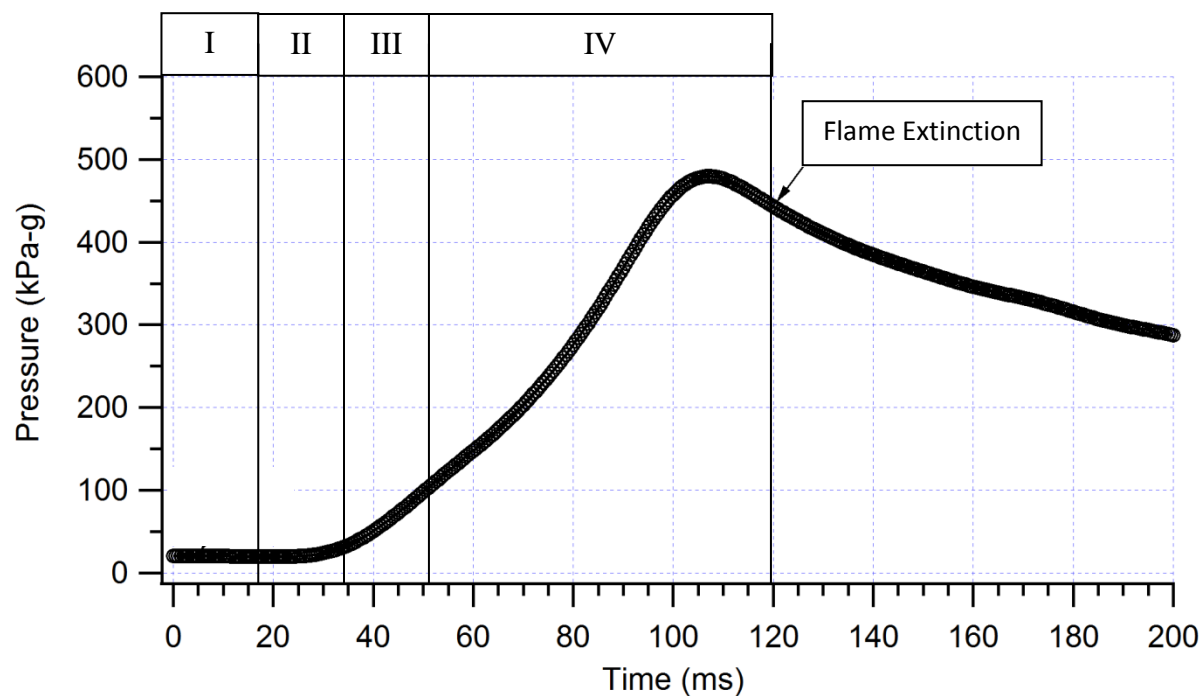


Figure 4.7 - Pressures vs time plot.

4.2 Dual Spark Ignition

The dual spark ignition setup consists of two spark plugs on the opposite ends of the tube along its length. This allows the effect of ignition from multiple sources to be studied in more detail. Both spark plugs are flush mounted on the combustion chamber. The exact time of the spark discharge can be electronically controlled through a delay circuit. Experiments are conducted for spark delay timings of 0, 25 and 50 milliseconds. The flame front from the initial spark is affected differently based on the stage of propagation. The ignition from the opposite end has a bigger influence when the tulip shape is fully developed than when the initial flame is still a spherical or planar flame. The experiments are discussed in greater detail in the following subsections.

4.2.1 Dual Spark, 0 millisecond delay

In this experiment, the two spark plugs are fired at the same time, and two separate flame fronts are formed which travel towards each other. The amount of energy deposited by each spark is the same as that released by a single spark. The optical record of the flame propagation is shown in Fig. 4.8. We observe that the different stages of flame propagation are preserved when compared to a single spark ignition. Shortly after ignition, a spherical flame front is formed at each end of the combustion chamber near the spark plug. The accelerating spherical flame fronts change to planar flame fronts after which the tulip shape is formed. The time taken for complete combustion is approximately equal to half the time taken by a single spark.

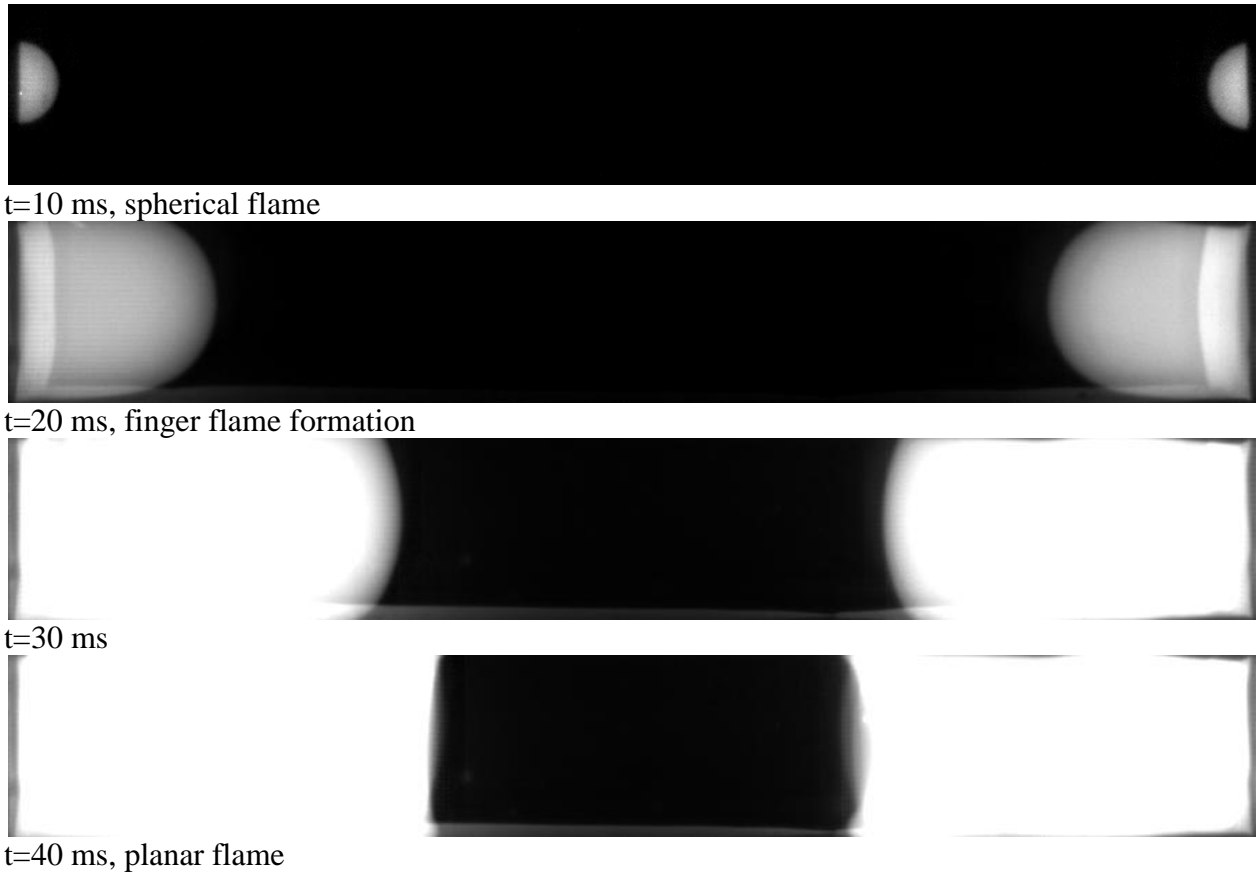
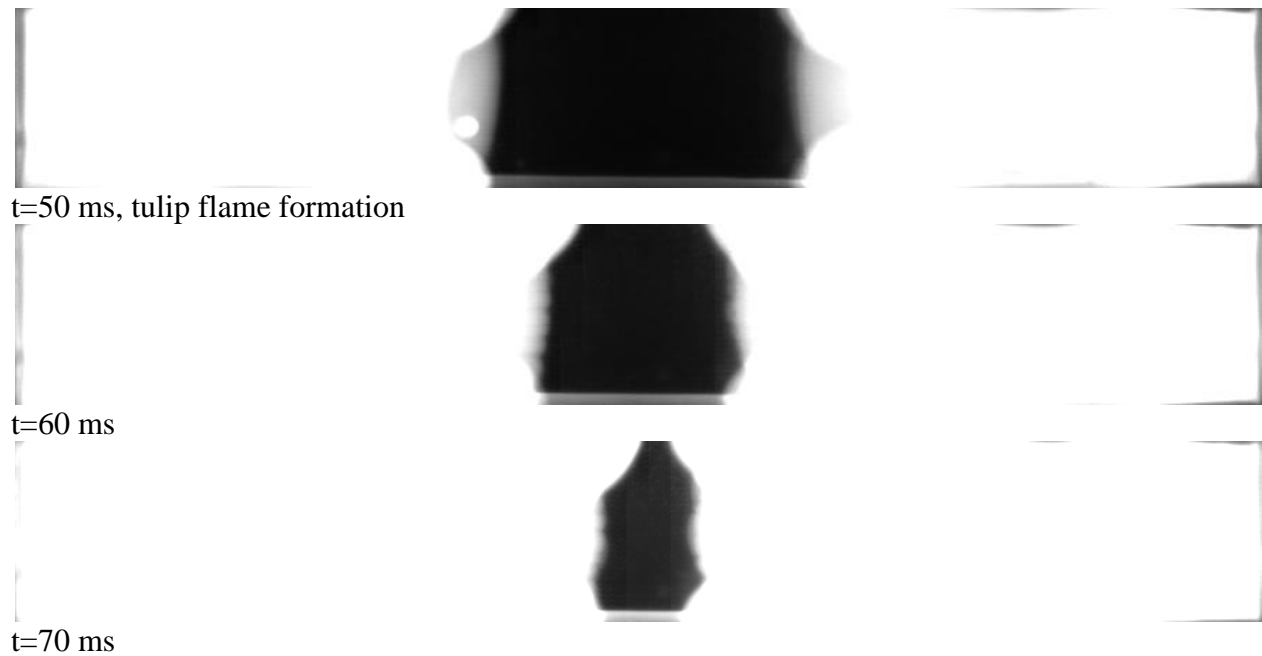


Figure 4.8 – Flame propagation along tube, dual spark with 0 ms delay.

Figure 4.8 (cont'd)



The normalized position of the flame fronts is shown in Fig. 4.9. The flame travelling from the left end of the tube to the right end is called flame L-R and the flame travelling in the opposite direction is called flame R-L. We observe from Fig. 4.9 that the traces for both the flame fronts follow a similar profile as they propagate from each end of the tube to the middle. The flame fronts collide with each other at half the length of the tube at the normalized position of 0.5.

Flame R-L ignition takes place at $X=1$ in the normalized scale and flame L-R ignition takes place at $X=0$ in the normalized scale.

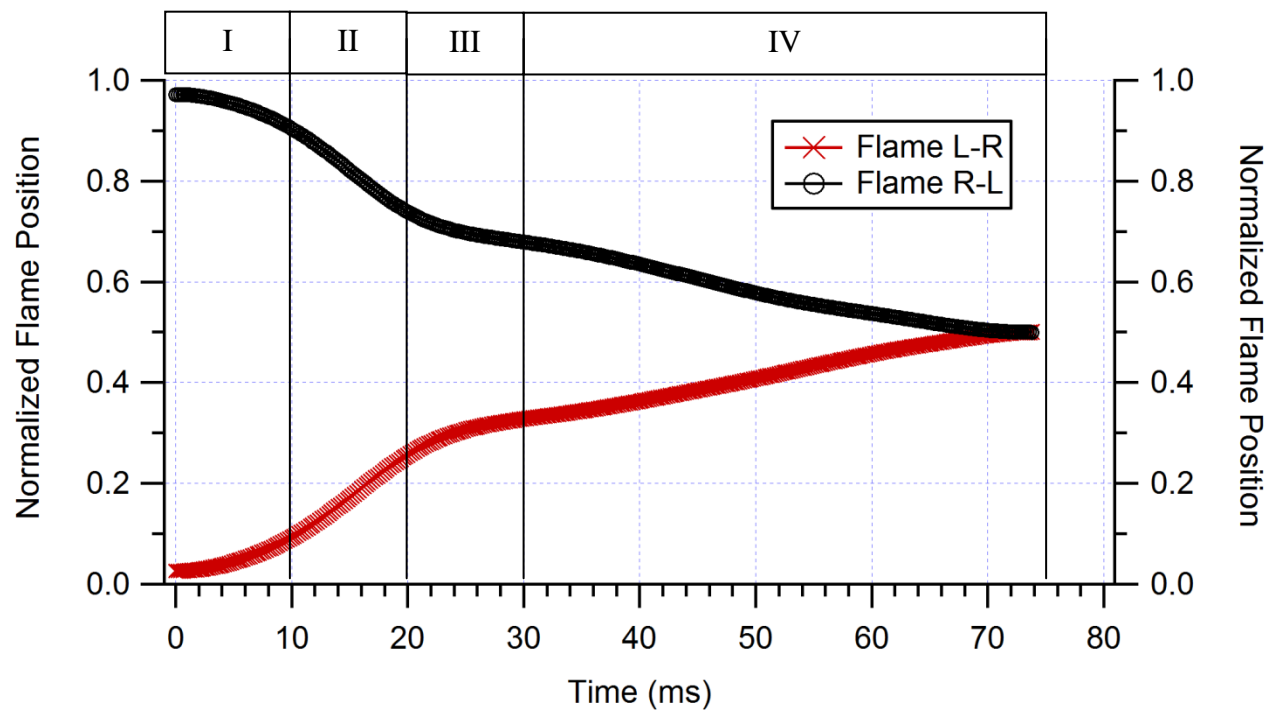


Figure 4.9 – Flame position vs. time.

The instantaneous speed of flame propagation can be calculated by calculating the time derivative of the flame position and is shown in Fig 4.9.

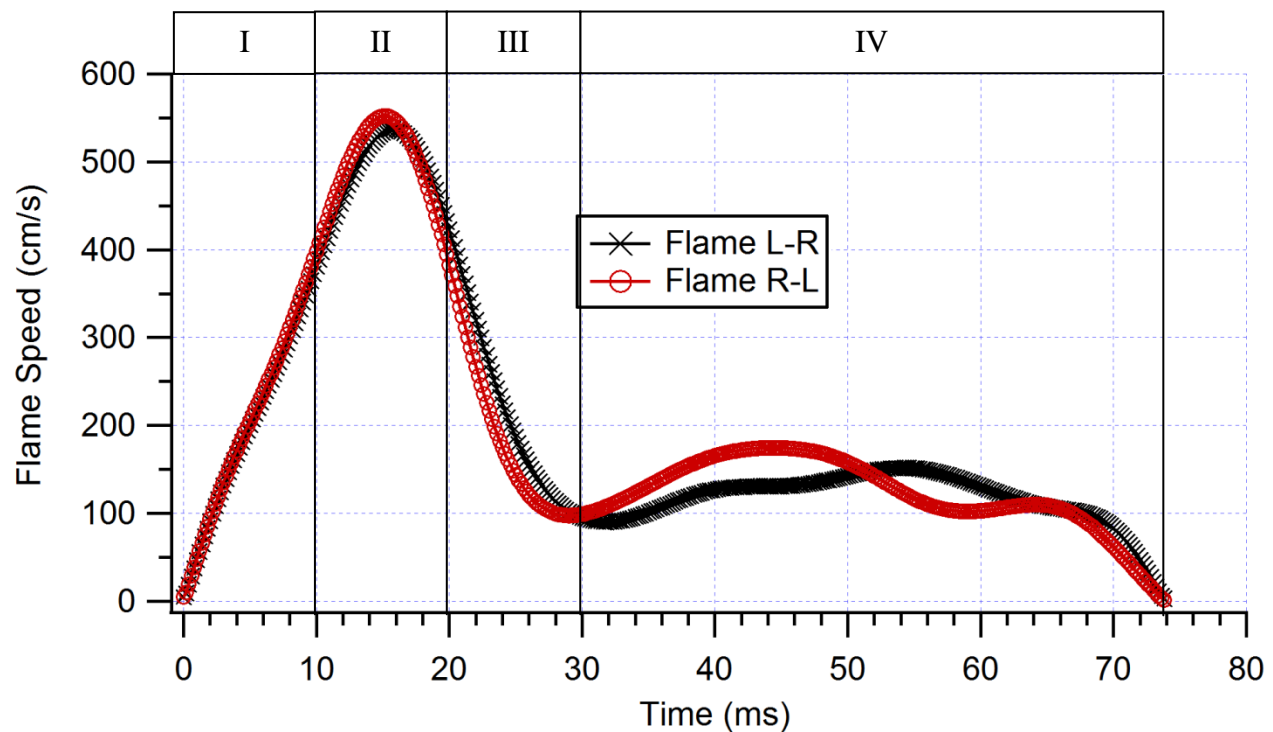


Figure 4.10 – Flame speed vs time.

It is observed that the flame speed profile is similar to the single spark combustion process. The ignition event is followed by an accelerating spherical flame on both ends of the combustion chamber. The spherical flame undergoes elongation along its length to form a finger shaped flame front. The side skirts of the finger flame are then quenched by the cold walls to create a planar flame front. This causes a decrease in the flame surface area and also reduces the speed of propagation. The planar flame then transforms to a tulip structure, which preserves its shape and speed until the two flames collide with each other. An oscillating behavior is observed in the speed of propagation of the tulip flame caused by small changes in the shape of the tulip as it propagates along the combustion chamber. The speed of flame propagation with the normalized tube length is shown in Fig 4.11.

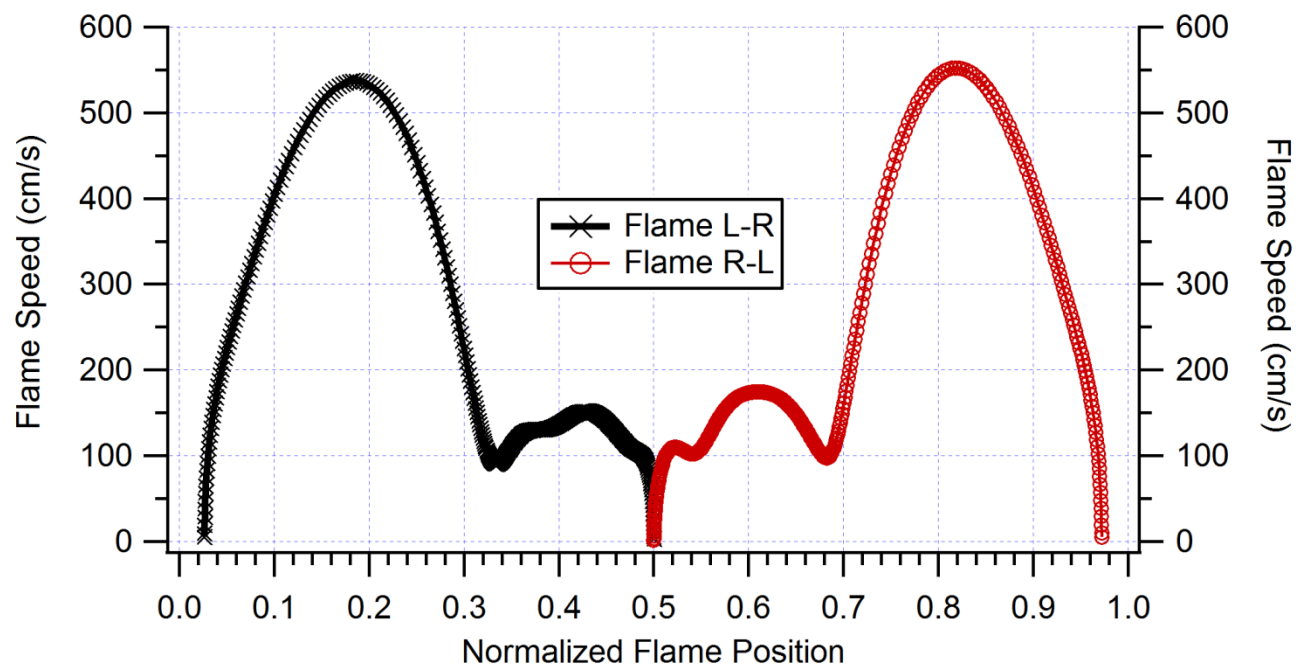


Figure 4.11 – Flame speed vs normalized flame position.

Fig. 4.8 shows that the planar flame changes its shape to the tulip flame at approximately one-third of the distance from either ends of the tube. The tulip flames then travel at a constant velocity until they collide with each other at the geometric center of the tube.

The pressure trace of the combustion process is shown in Fig. 4.12.

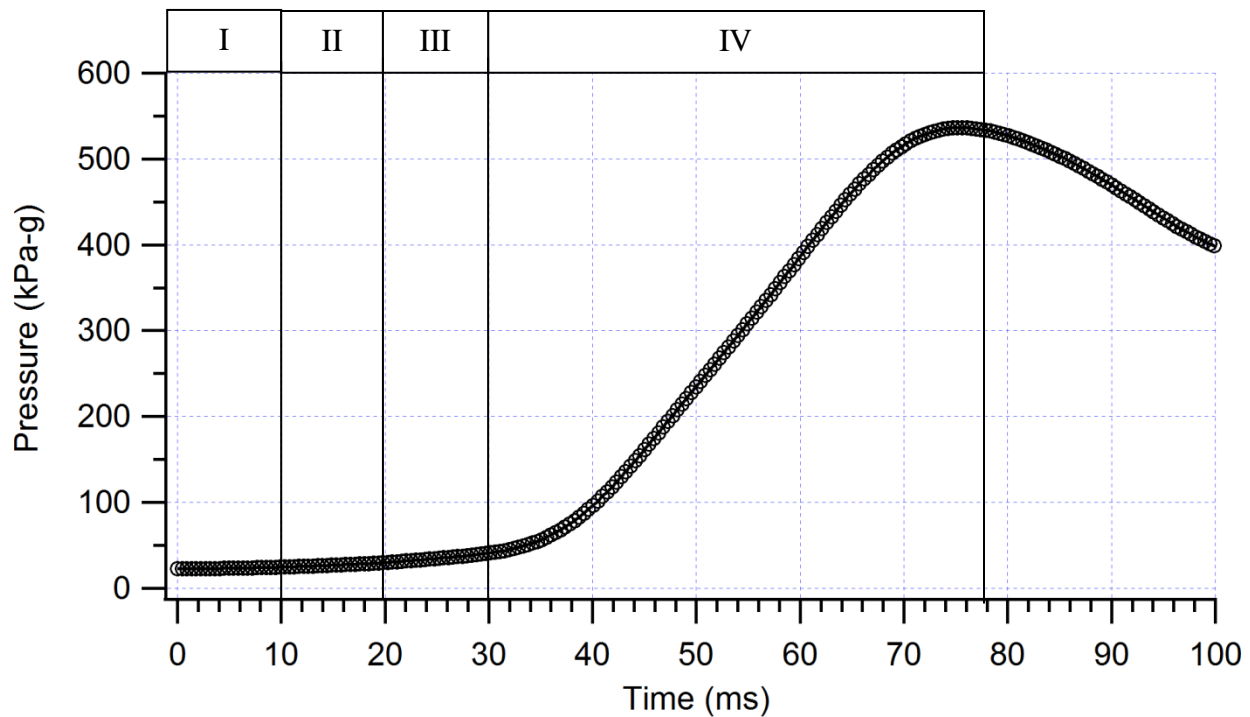


Figure 4.12 – Pressure vs time.

We observe that the peak pressure precedes flame collision. The rate of heat losses to the cold walls is maximum before flame collision which reduces the peak pressure. The pressure increase becomes dominant after the formation of the tulip flame indicating an increase in the burn rate of the premixed mixture once the tulip flame is formed.

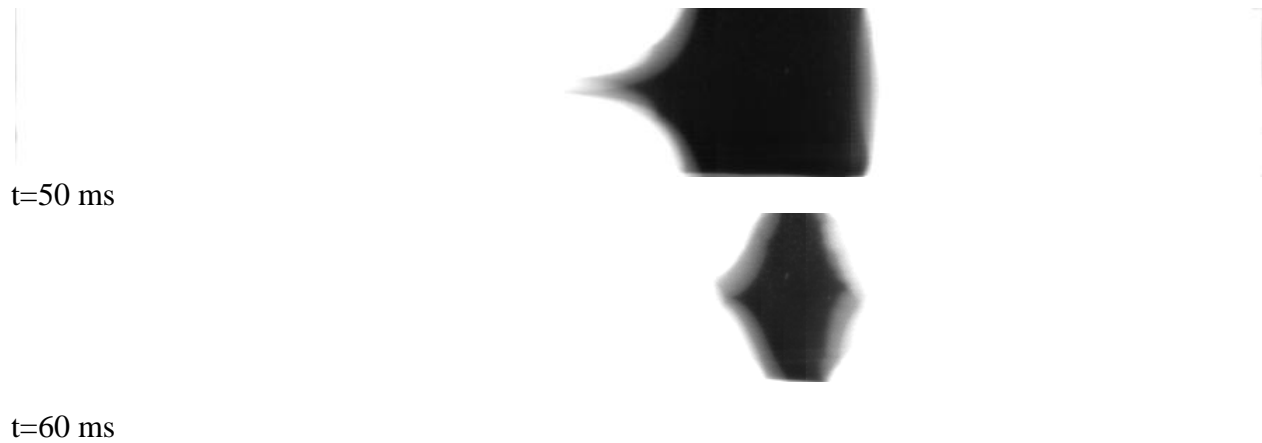
4.2.2 Dual Spark, 25 milliseconds delay

In this experiment, the two spark plugs are fired with a delay of 25 milliseconds. The spark plug on the left side of the combustion chamber is fired first followed by the one on the right side. The optical record of the flame propagation is shown in Fig. 4.13.



Figure 4.13 – Flame propagation along tube, dual spark with 25 ms delay.

Figure 4.13 (cont'd)



From the above figure, we observe that the ignition even at the left side of the combustion chamber is followed by a growing spherical flame front. While the flame front is in the process of transforming from planar to tulip shape, at 25 milliseconds, the second spark plug is ignited. The flame ignited by the second spark follows the structural changes undergone by the first flame front.

Ignition I occurs at the normalized position $X=0$ and ignition II occurs at the normalized position $X=1$, 25 milliseconds after the initial ignition. The delay in the firing of the spark plug is set and controlled through a digital delay circuit.

The instantaneous position of the flame front is shown in Fig. 4.14. The total time required for complete combustion is observed to be 70 milliseconds.

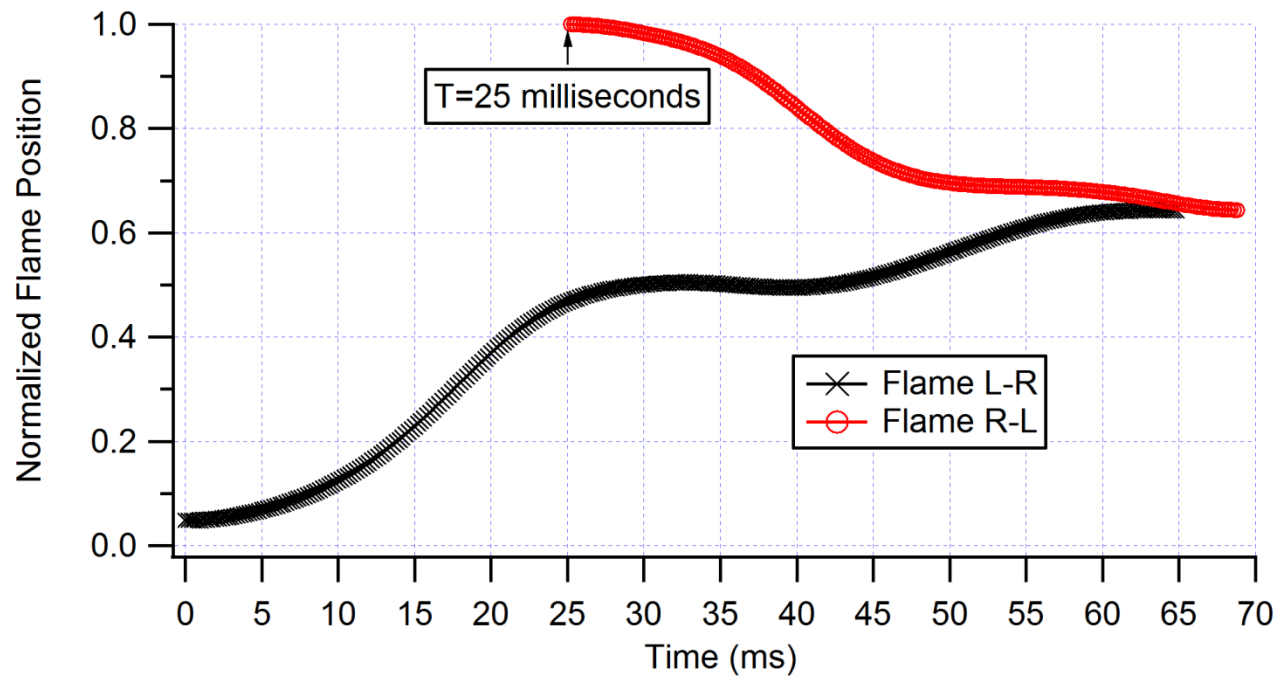


Figure 4.14 – Normalized flame position vs time.

The speed of propagation of the flame front can be determined by calculating the time derivative of the flame position data. The flame speed is shown in Fig. 4.15. Upon ignition of the first spark, the flame front follows the structure and speed profile of a single spark combustion flame. When the flame front is in the process of changing from planar to tulip shape, the second spark plug is ignited. This causes the initial flame front to attain a negative flame speed in the laboratory coordinate. A sinusoidal profile of the flame speed curves is obtained with a phase difference as the flames undergo transformation in their shape and their physical flame speed changes.

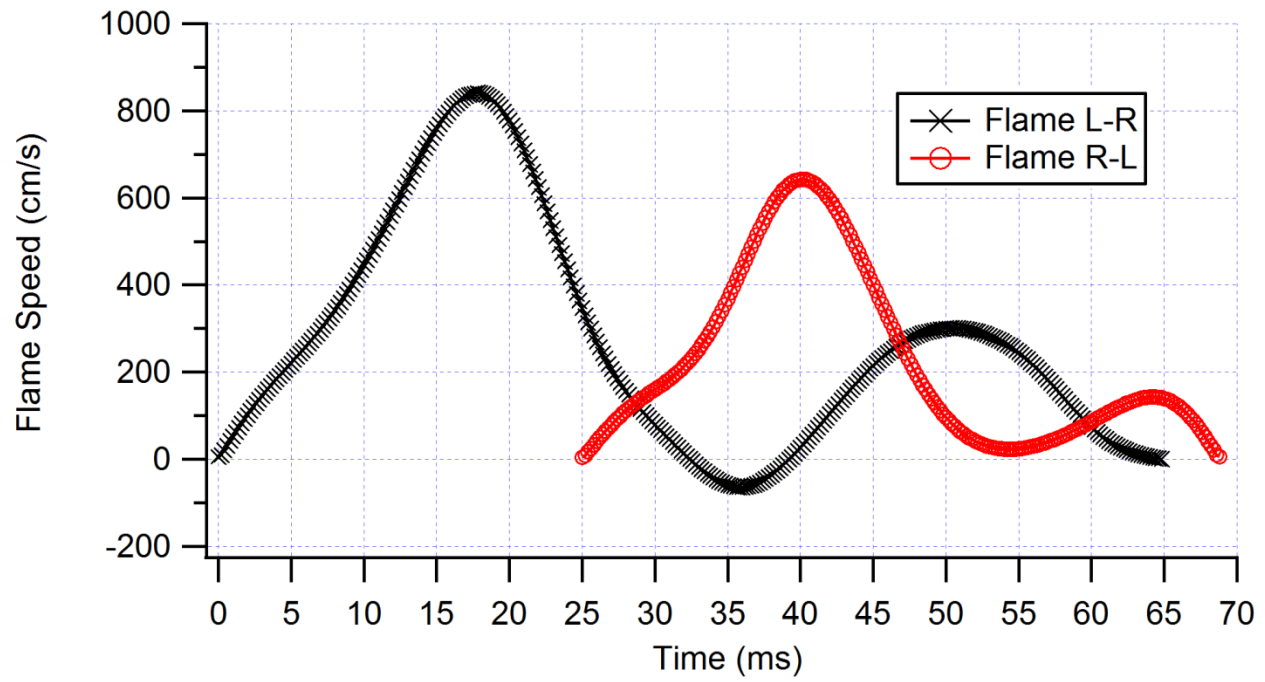


Figure 4.15 – Flame speed vs time.

The flame speed profile for the normalized position along the tube length is shown in Fig. 4.16.

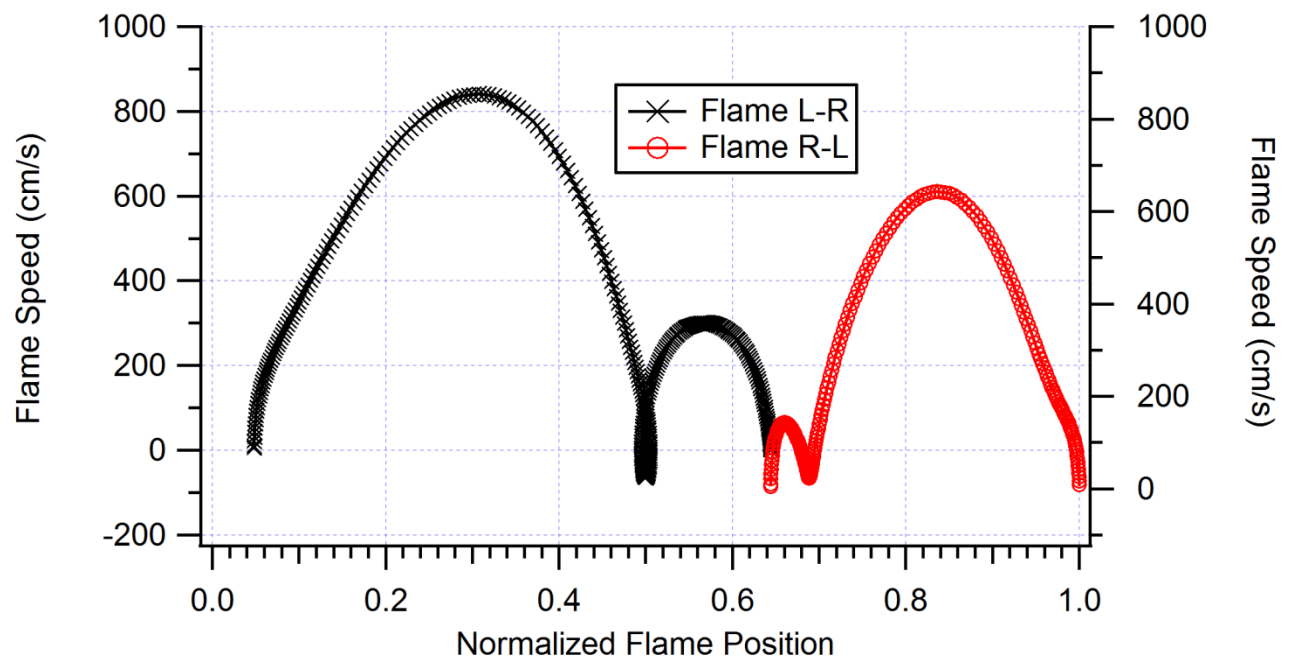


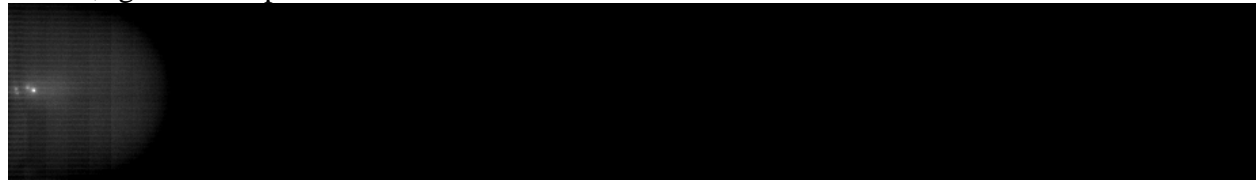
Figure 4.16 – Flame speed vs normalized flame position.

4.2.3 Dual Spark, 50 milliseconds delay

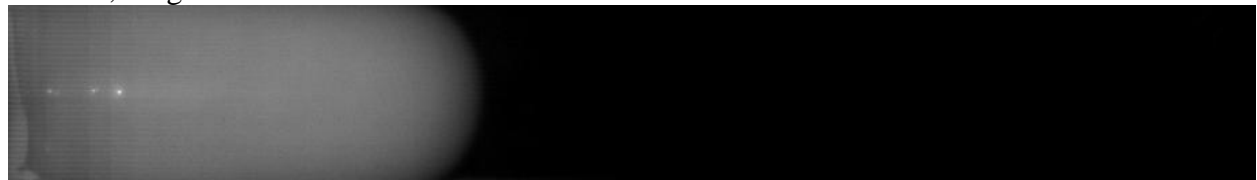
In this experimental test, the delay between the firing of the two sparks is set at 50 milliseconds. The spark on the left side of the tube is ignited first followed by the spark on the right side. The firing of the two spark plugs is controlled by a digital delay circuit. The optical record of the flame propagation is shown in Fig. 4.17.



t=0 ms, Ignition of spark I



t=10 ms, Finger flame formation



t=20 ms



t=30 ms, Planar flame



t=40 ms, Tulip flame formation

Figure 4.17 – Flame propagation along tube, dual spark with 25 ms delay.

Figure 4.17 (cont'd)



t=50 ms, Ignition of spark II



t=60 ms, Finger flame formation



t=70 ms, Planar flame



t=80 ms, Tulip flame formation



t=90 ms, Flame collision

From Fig. 4.17, we observe that the flame formed due to the initial spark ignition follows the profile of the single spark ignition test condition. At $t=50$ milliseconds, the second spark plug is ignited. This causes distortion in the structure of the tulip shape in the initial flame front travelling from left to right. The R-L flame front undergoes the 4 stages of flame structure and the two flame fronts collide with each other at 90 milliseconds from ignition.

The normalized position of the flame front is determined by post-processing the optical record of the flame propagation and is shown in Fig. 4.18.

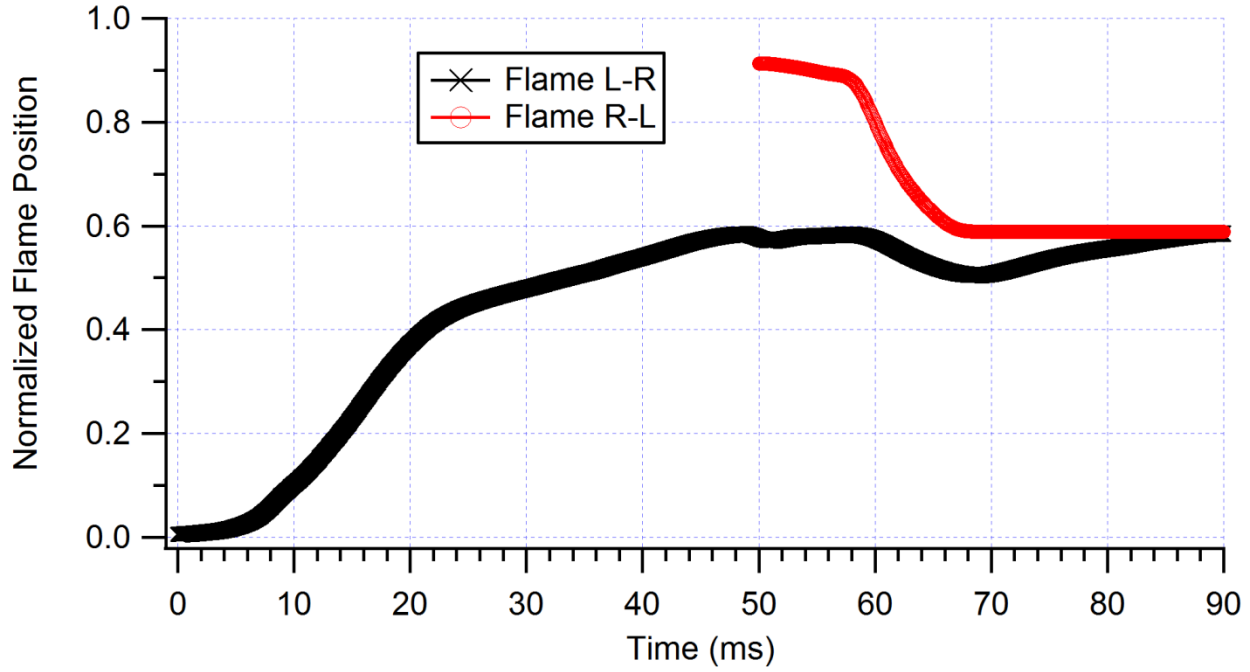


Figure 4.18 – Normalized flame position vs time.

The speed of propagation of the flame front can be obtained by calculating the time derivative of the flame position. The instantaneous speed of flame propagation is shown in Fig 4.19.

We observe that the second ignition event at 50 ms causes the flame L-R to momentarily move in reverse and causes a negative flame speed to occur in the laboratory coordinate. The speed of flame L-R becomes negative again when the flame R-L transforms from a spherical to a finger flame. A reversal in the speed of propagation of flame R-L occurs when it transforms from a planar flame to a tulip flame. The R-L flame becomes stationary and L-R flame speed increases once again until the two flame fronts collide. This alternating flame speed profile is similar to that observed in ignition delay of 25 ms.

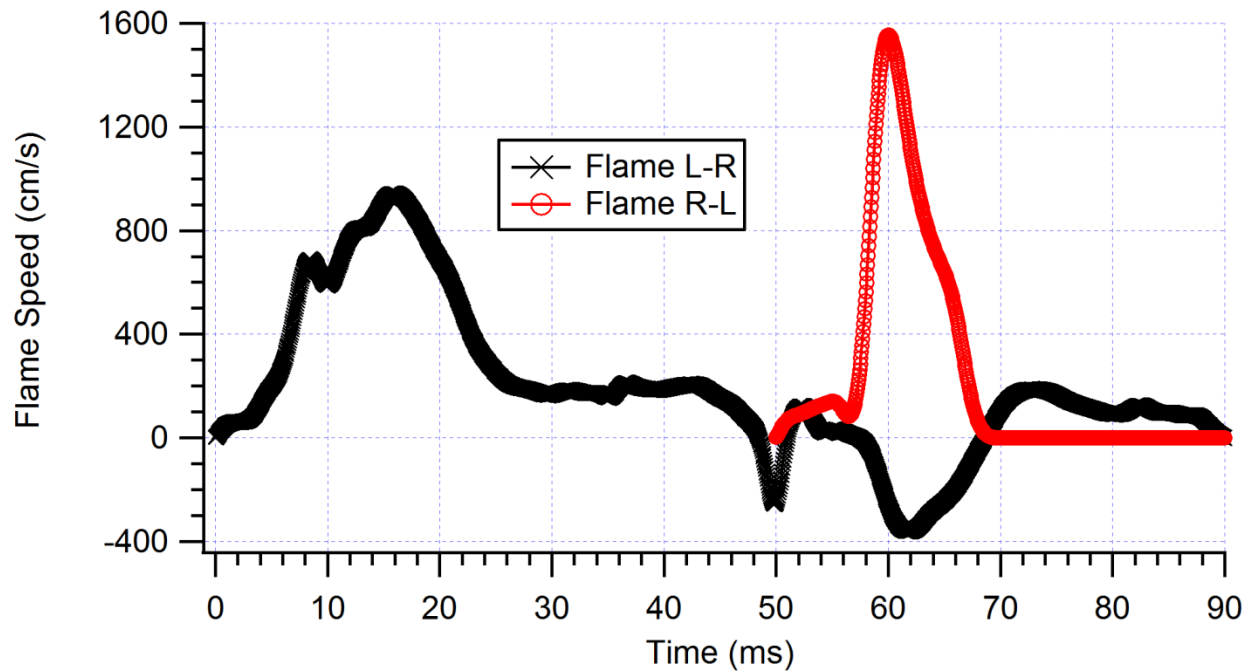


Figure 4.19 – Flame speed vs time.

The speed of flame propagation with the normalized flame position is shown in Fig. 4.20. It is observed from the figure that the L-R flame undergoes reversal in its propagation direction which is seen as a cyclic flame speed curve near the middle of the combustion tube.

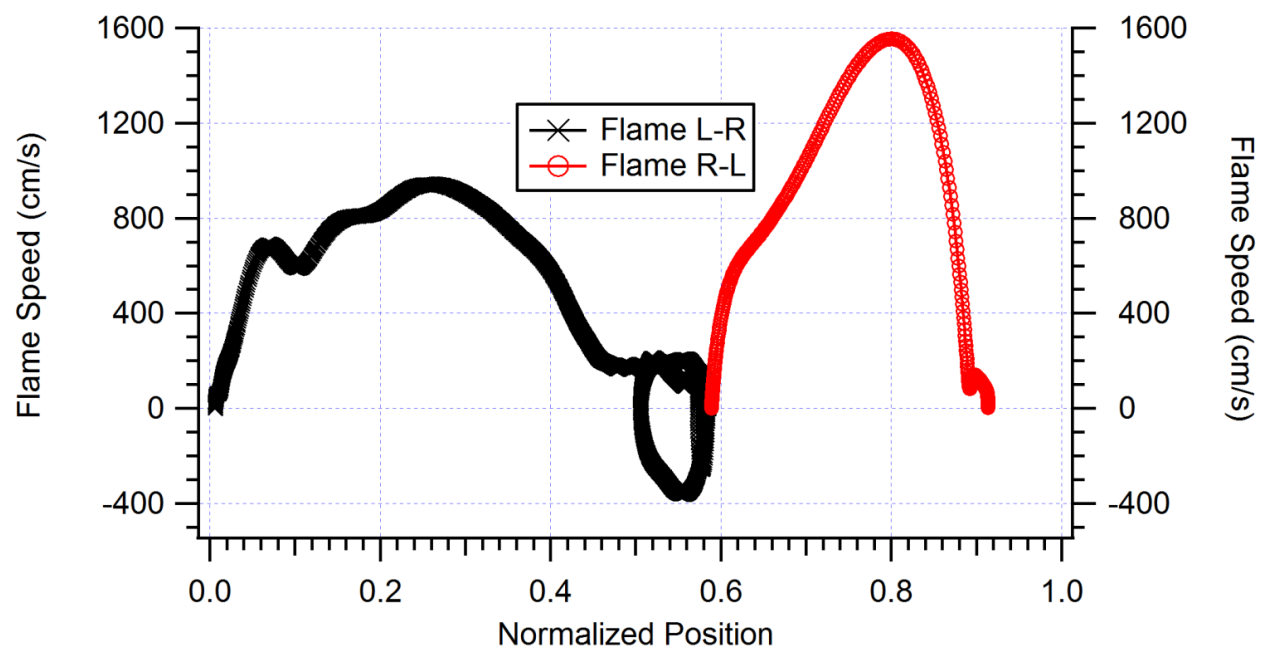


Figure 4.20 – Flame speed vs normalized flame position.

CHAPTER 5

NUMERICAL RESULTS

A numerical simulation of the constant volume combustion process was performed to obtain the flow field inside the combustion chamber for different stages in the combustion process and the influence of pressure waves on the flame front. A detailed study of the formation of the tulip flame will be performed.

A simplified 2 dimensional representation of the combustion chamber is constructed measuring 12 inches long and 2 inches wide. The computational domain consists of structured quadrilateral cells, each with an edge of 0.1 millimeters as shown in Fig. 5.1 and Fig. 5.2. The domain contains a total of 1.54 million elements.

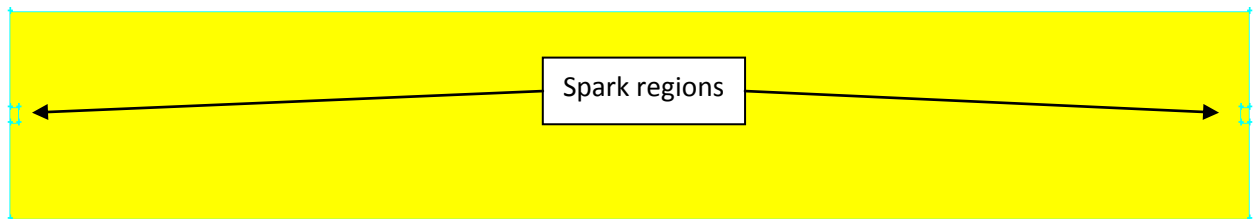


Figure 5.1 - Combustion chamber computational domain.

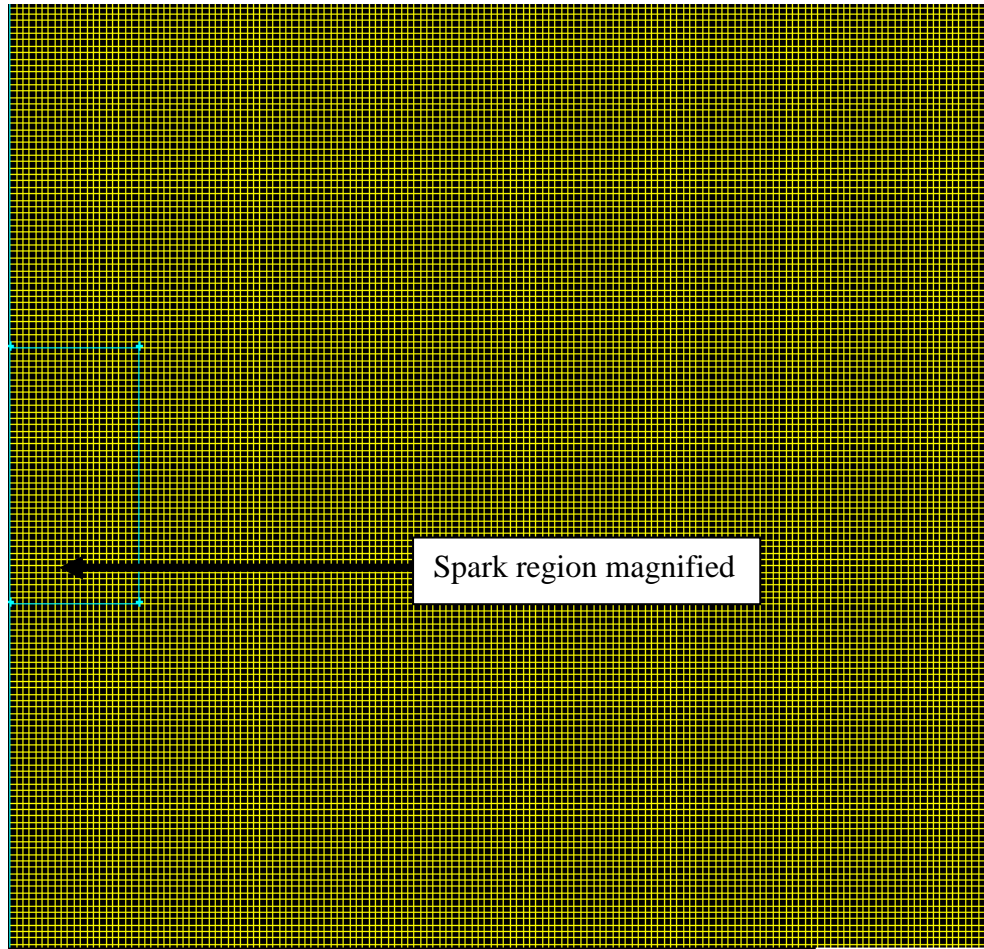


Figure 5.2 - Combustion chamber mesh, spark region; square cell measuring 0.1 mm.

The commercial computational fluid dynamics software “Ansys Fluent” is used to perform the numerical calculation. A Navier-Stokes solver is used to calculate the transient results using an explicit scheme with a fourth-order Runge-Kutta solver. The Courant-Friedrich-Levy number is set at 0.9 for the entire simulation domain. The solver methodology, boundary and operating conditions are discussed in appendix C.

The control volume is initialized with a stoichiometric mixture of methane and air. A single-step Arrhenius reaction rate mechanism is used. The walls surrounding the control volume are

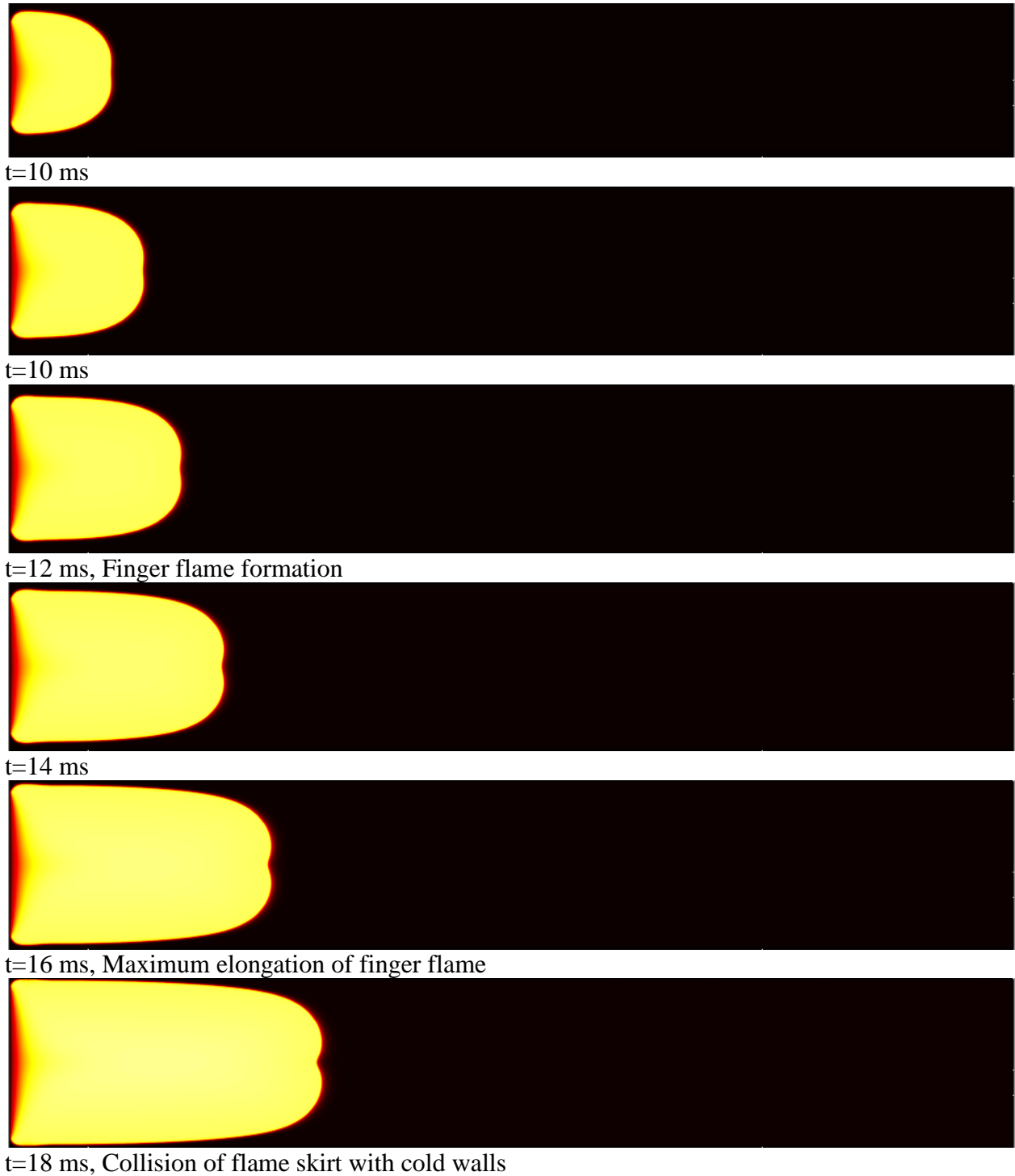
initialized to be a no-slip boundary with constant temperature of 293 K. The combustion process is initialized by patching a localized spot near the physical spark location to 2100 K.

The propagation of the flame from ignition until the formation of the finger flame is shown in Fig. 5.3 as a contour plot of the temperature.



Figure 5.3 – Flame propagation along the combustion tube, showing the evolution of the flame structure from ignition to finger flame formation.

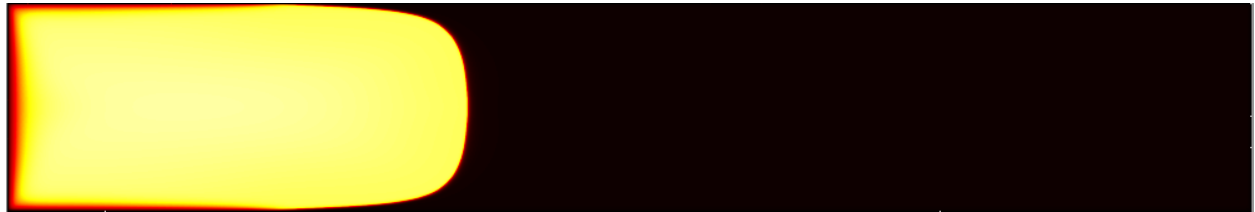
Figure 5.3 (cont'd)



The contour plot of the temperature representing the propagation of flame from the elongated finger flame structure to the tulip shape is shown in Fig. 5.4.



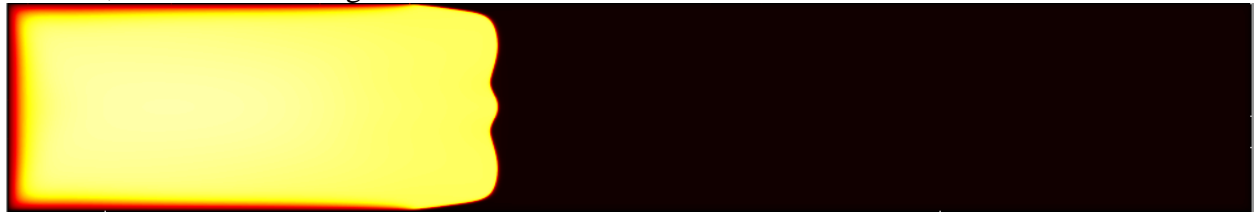
t=20 ms



t=22 ms



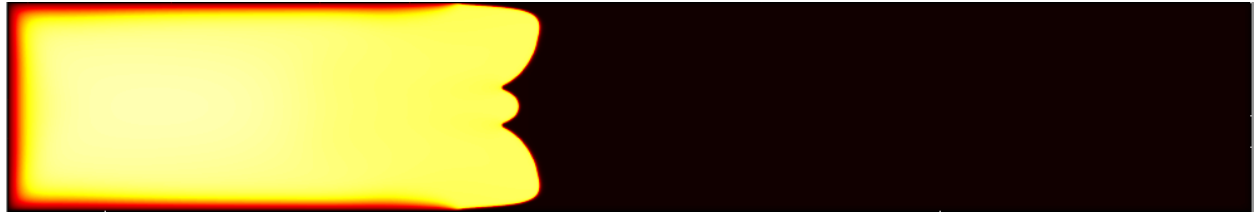
t=24 ms, Note the flattening of the flame.



t=26 ms, Planar flamefront.



t=28 ms



t=30 ms, Tulip flame formation.

Figure 5.4 – Flame propagation along the combustion tube, showing the evolution of the flame structure from planar flame to tulip flame propagation.

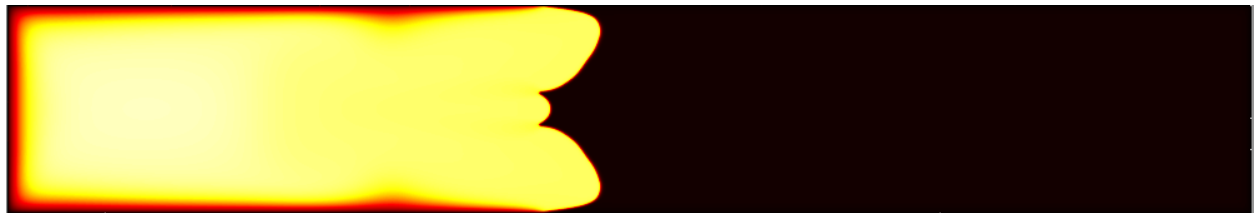
Figure 5.4 (cont'd)



t=32 ms



t=34 ms



t=36 ms



t=40 ms



t=45 ms



t=50 ms, Final tulip shape.

The formation and propagation of the tulip flame in both the spatial and temporal dimensions has been captured with a numerical scheme using a single-step Arrhenius chemical reaction process and laminar fluid flow model. The result obtained by uncoupling the pressure waves from the Navier-Stokes (N-S) equations is comparable to that obtained by solving the coupled N-S equations. We infer that the trigger for the formation of tulip flame is not dependent on the influence of pressure waves. A detailed analysis of the flow field of the burnt gas during the expansion and subsequent quenching of the finger flame skirts by the cold wall shows a reversal in the direction of the local velocity field of the burnt gases as the flamefront nears the cold wall. This induces a recirculation to be produced near the finger flame skirts. A moving stagnation point along the centerline is observed, travelling through the burnt mixture towards the flamefront as marked in Fig. 5.5. The velocity components are shown in the laboratory reference frame. The local stagnation points are indicated by a yellow circle.

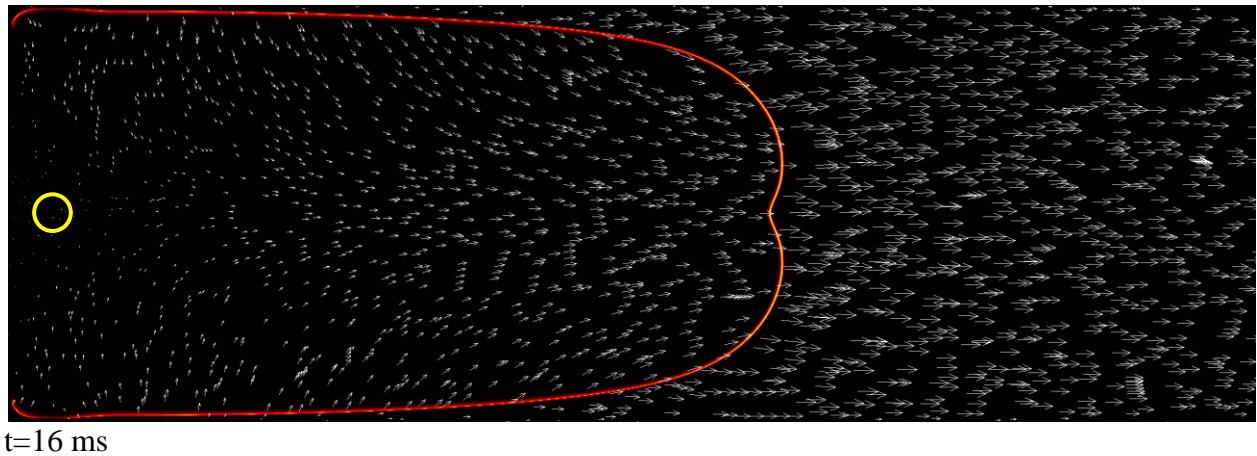
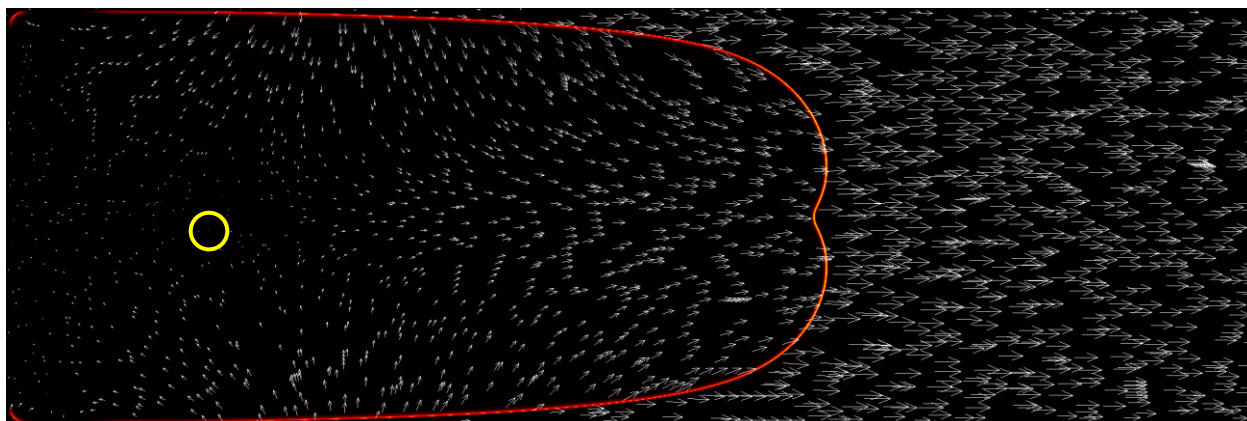
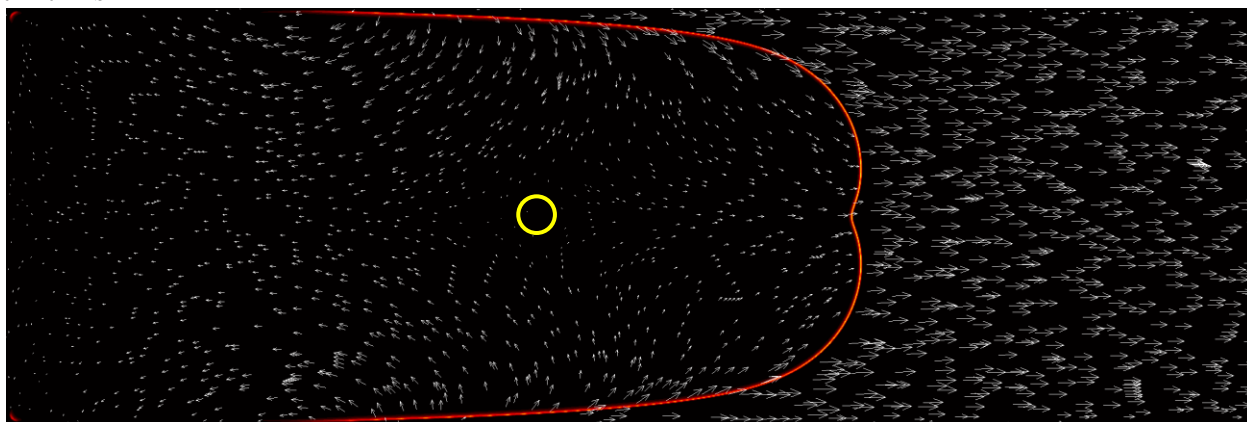


Figure 5.5 – Velocity vector of flow inside combustion tube, finger flame extinction.

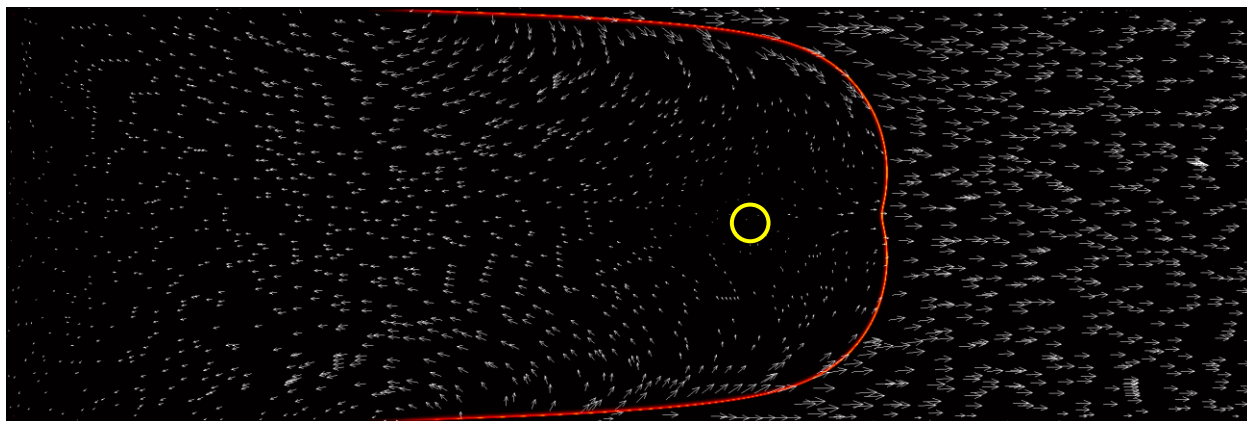
Figure 5.5 (cont'd)



t=17 ms

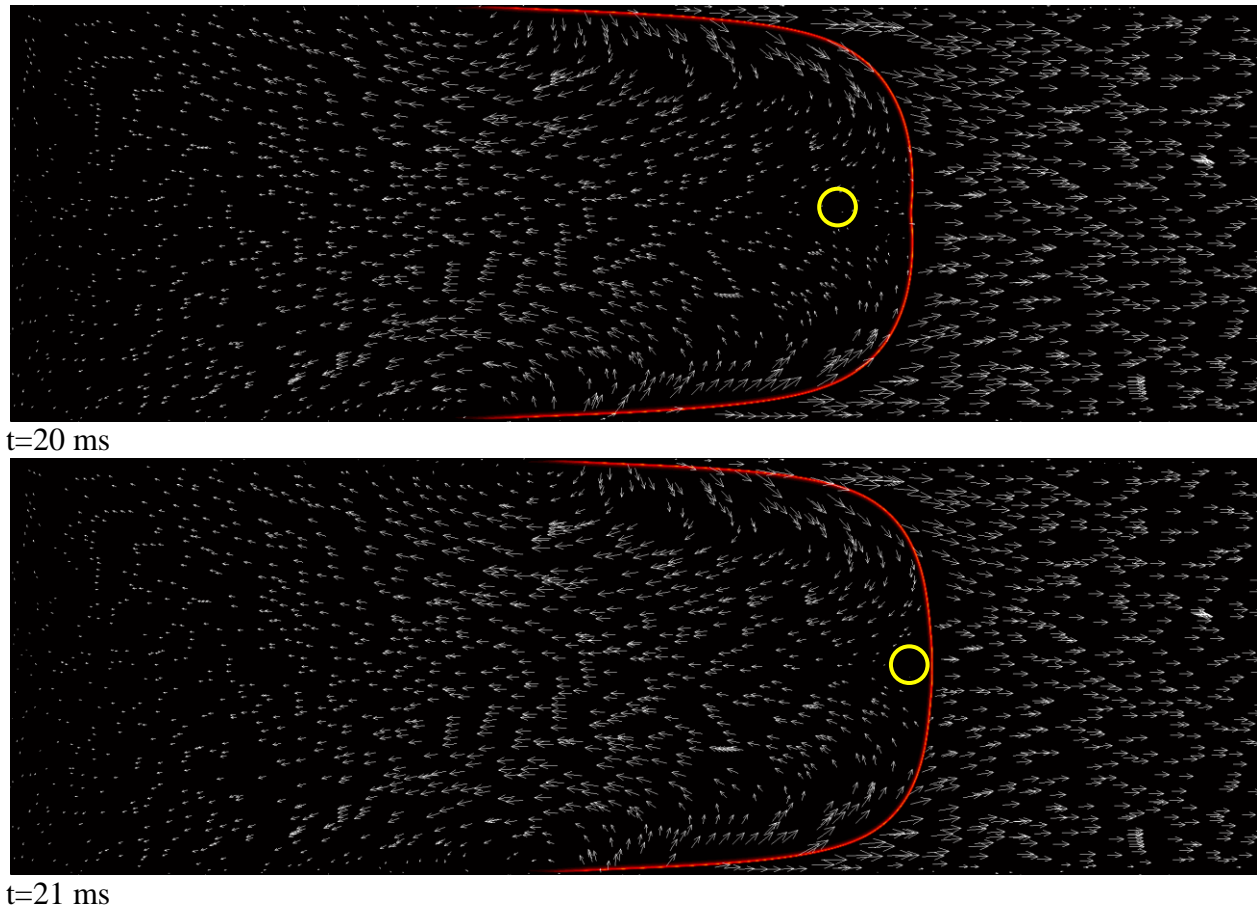


t=18 ms



t=19 ms

Figure 5.5 (cont'd)



As the stagnation point moves closer to the flamefront, a “stagnation line” develops which eventually merges with the reaction front. As observed in laboratory coordinates, the burnt gases move towards and the unburnt mixture moves away from the flamefront during the initial stages of flame propagation (spherical and finger flame). The speed of the flamefront during the first two stages is higher than the local velocity field, when observed from the flamefront coordinates, the unburnt gas moves towards the flamefront and the burnt gas moves away from the flamefront. As the speed of the flame decreases, there is a reversal in the direction of the burnt gas and a subsequent reduction in the magnitude of velocity in the unburnt mixture as shown in Fig. 5.6.

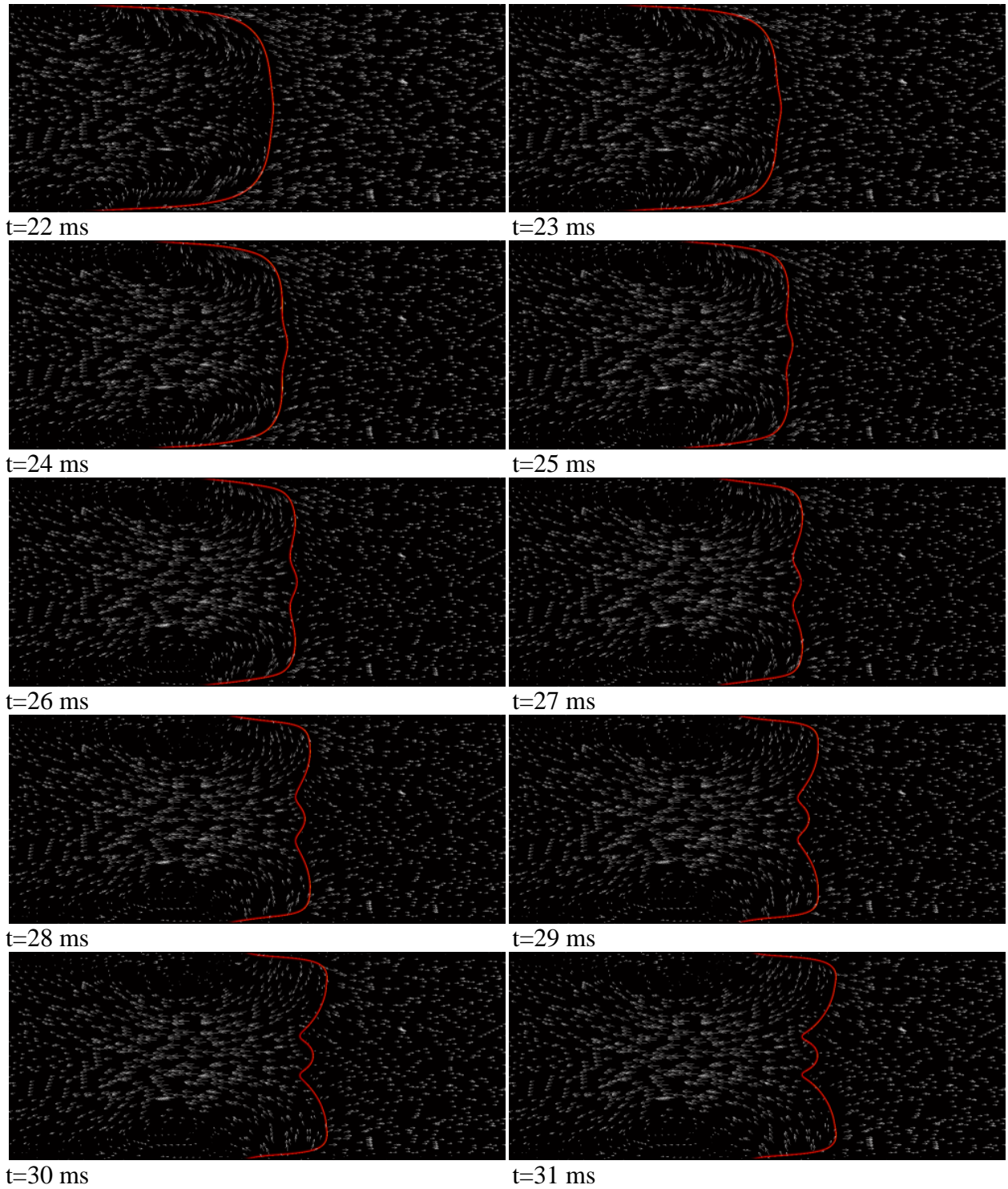


Figure 5.6 – Velocity vector of flow inside combustion tube, tulip formation.

It is observed that a recirculation of the burnt gas is produced when the flame skirt of the finger flame collides with the cold wall. This recirculation moves towards the leading flamefront as its speed decreases. For tulip flames in short tubes, it has been theorized by Dunn-Rankin that “the recirculation produces the initial trigger for a Darrieus-Landau instability which subsequently grows to the entire tulip flame” [5].

The properties of the unburnt mixture vary continuously during the combustion process. The flamefront typically acts as a “piston” by compressing the unburnt mixture as the flame front travels towards the other end of the tube. The data for the unburnt mixture properties is collected at a point on the combustion chamber which is located 1 inch away from the cold wall of the opposite end of the ignition point, along the centerline. There is a separation of an inch between the data point and the cold wall to eliminate the effect of conductive heat loss. The data point on the computational domain is marked with a yellow circle as shown in Fig. 5.7.



Figure 5.7 - Unburnt mixture data point.

The change in the pressure of the unburnt mixture during the combustion process is shown in Fig. 5.8. It is observed that the effect of pressure waves produced by combustion is negligible and pressure changes can be assumed to be uniform throughout the control volume.

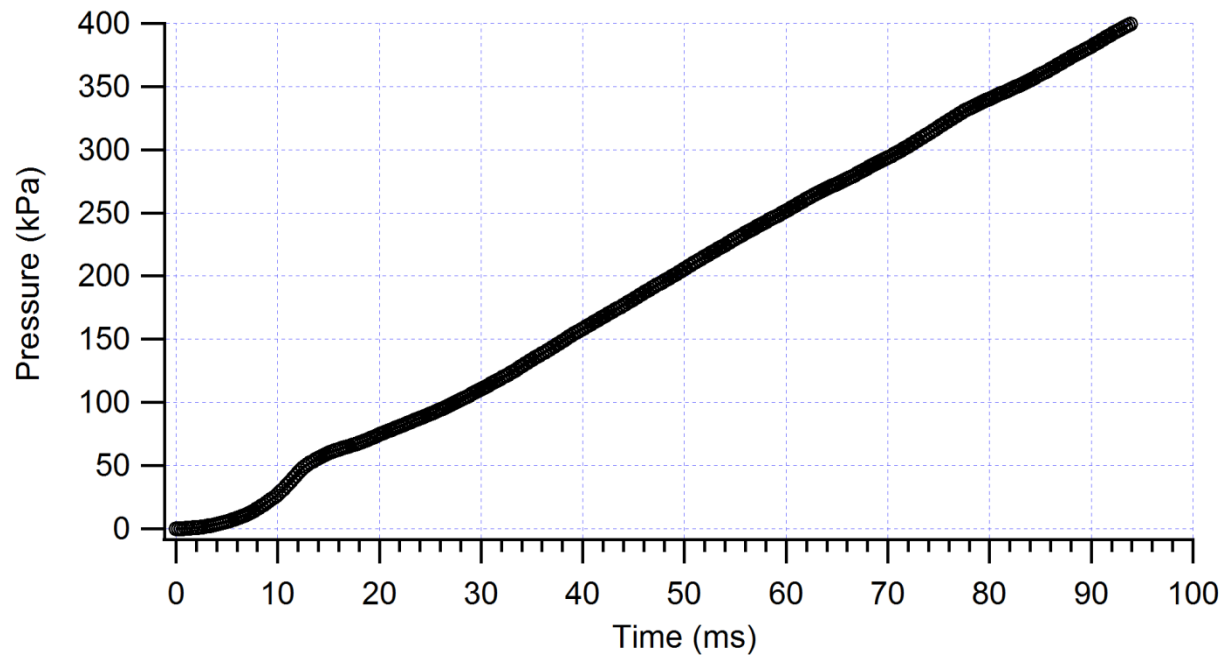


Figure 5.8 - Pressure vs. time in the unburnt mixture.

The increase in pressure is accompanied with an increase in the temperature of the unburnt mixture which increases by 180 K from ignition start to the point where the flame surface reaches the data point. The change in temperature of the unburnt mixture is shown in Fig. 5.9 and the comparison of the change in pressure for a constant specific heat ratio and variable heat ratio is shown in Fig. 5.10.

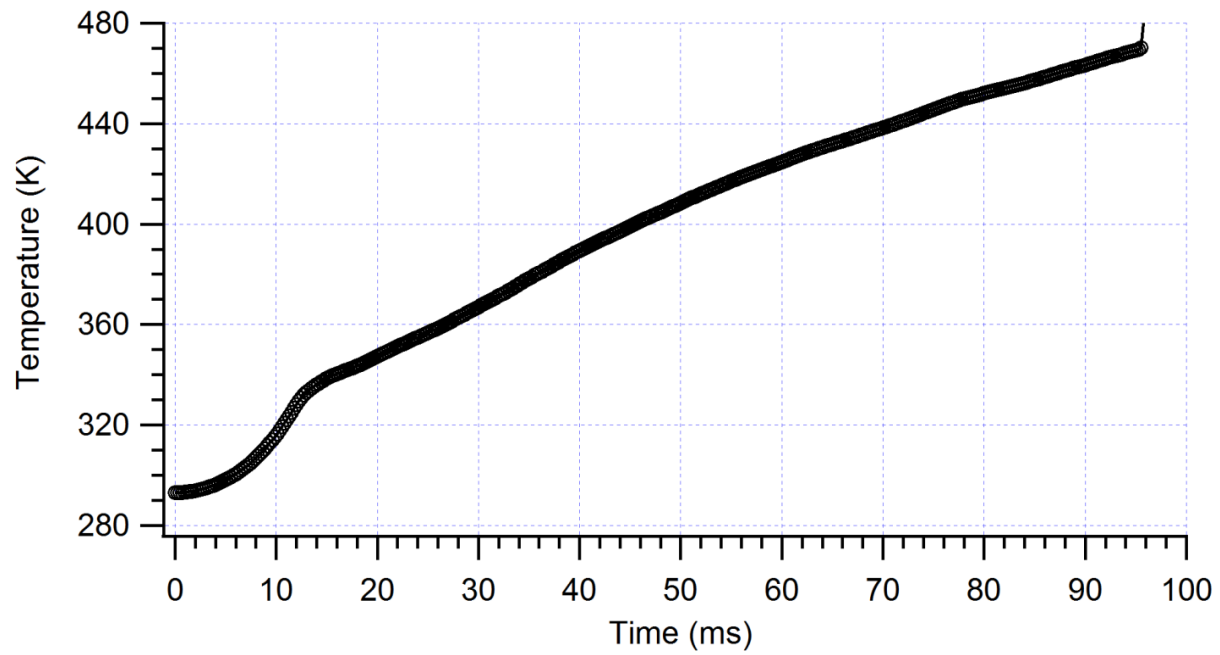


Figure 5.9 - Temperature vs. time in the unburnt mixture.

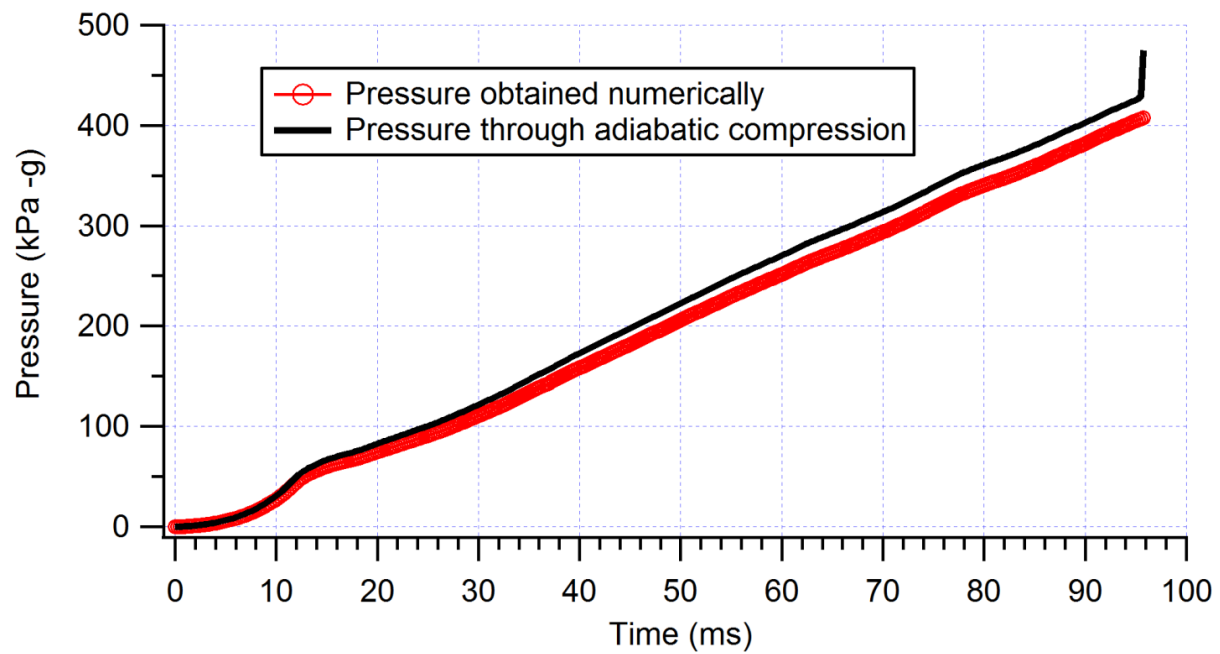


Figure 5.10 - Pressure comparison in unburnt mixture.

It is observed that the adiabatic pressure and numerical pressure are similar for temperatures close to ambient conditions and the two pressures diverge at higher temperatures due to the change in the value of the specific heat ratio. The Lewis number remains unchanged when the flamefront is far from the unburnt mixture. The change in temperature and pressure has little effect on the Lewis number and the reaction proceeds with a small dominance of species diffusivity as shown in Fig. 5.11. This leads to the formation and propagation of thermo-diffusive instabilities in the flame front, which is observed both numerically and experimentally.

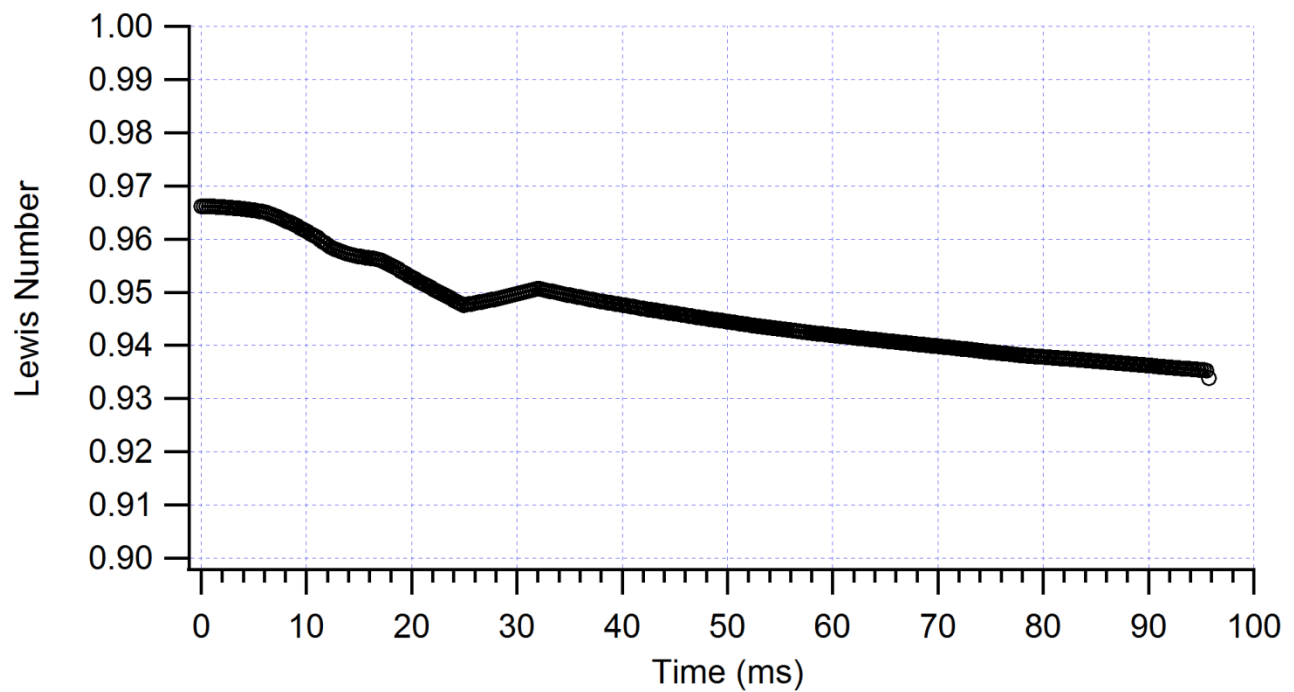


Figure 5.11 - Lewis number of unburnt mixture.

CHAPTER 6

RESULTS AND DISCUSSION

The results from the numerical and experimental and schlieren tests are used to develop a better understanding behind each stage of flame propagation in a constant volume combustion chamber.

An analytical model of the flame propagation is constructed where the flame front is approximated to basic geometric shapes with which approximate value of flame surface area and volume of burnt and unburnt regions can be calculated.

For a flame ignited by a single spark, the flame propagation process is divided into 4 stages. In the first stage, spark ignition is followed by a growing hemispherical flame front. The maximum radius attained by the flame front is visually identified to be three-fourths of the side of combustion chamber. In the second stage, the hemispherical flame front undergoes an elongation process along the length of the combustion chamber, which resembles a finger flame. The finger flame is approximated to be a combination of a cylinder which expands along its radius and length with a hemispherical cap. Upon reaching the normalized length $L=0.45$, the finger flame's side skirts are extinguished by the cold wall and a planar flame front is formed, which forms the third stage. In the final stage of flame propagation, the planar flame begins to develop an inward pointing cusp, which is approximated to be a pyramid with base equal to the area of cross section and height visually determined to be half the length of its side. This shape is maintained until the flame front collides with the opposite wall.

For the first 10 milliseconds after spark plug ignition, the flame front assumes the shape of a uniformly growing hemisphere. The surface area of the flame front grows at a square rate of its radius growth. In this stage, the effect of lateral walls and recirculation of unburnt gas is negligible and the flame front expansion takes the shape of a physically unconfined premixed flame. The analytical representation is shown in Fig. 6.1 which consists of a hemisphere of radius ' r ' which grows from 0-0.75 R , where R is the hydraulic radius of cross section of the tube.

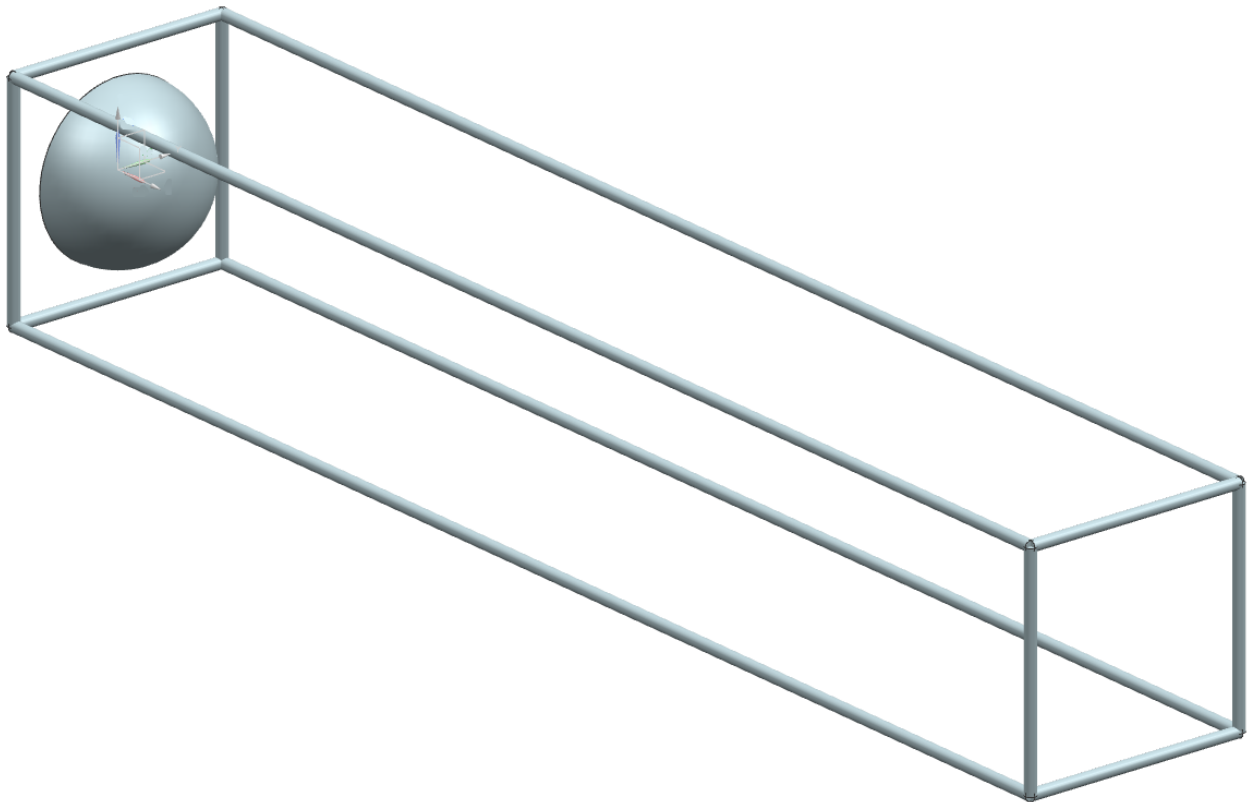


Figure 6.1 – Analytical representation of spherical flame front.

When the skirt of the flame is close to the tube wall, the axial velocity of the flame becomes higher than the radial velocity, which leads to the formation of an elongated flame front called the finger flame shown in Fig.6.2. The proximity of the wall prevents the flame front from pushing the unburnt gas radially outward, which reduces the radial expansion of the flame front. To develop the analytical representation, the flame front is modeled as a cylindrical surface of radius ' r ' which ranges from $0.75-1 R$, and the length range from $0.75-5.5 R$, with a hemispherical cap. The radius and length of the cylinder increase over a period of 10 milliseconds.

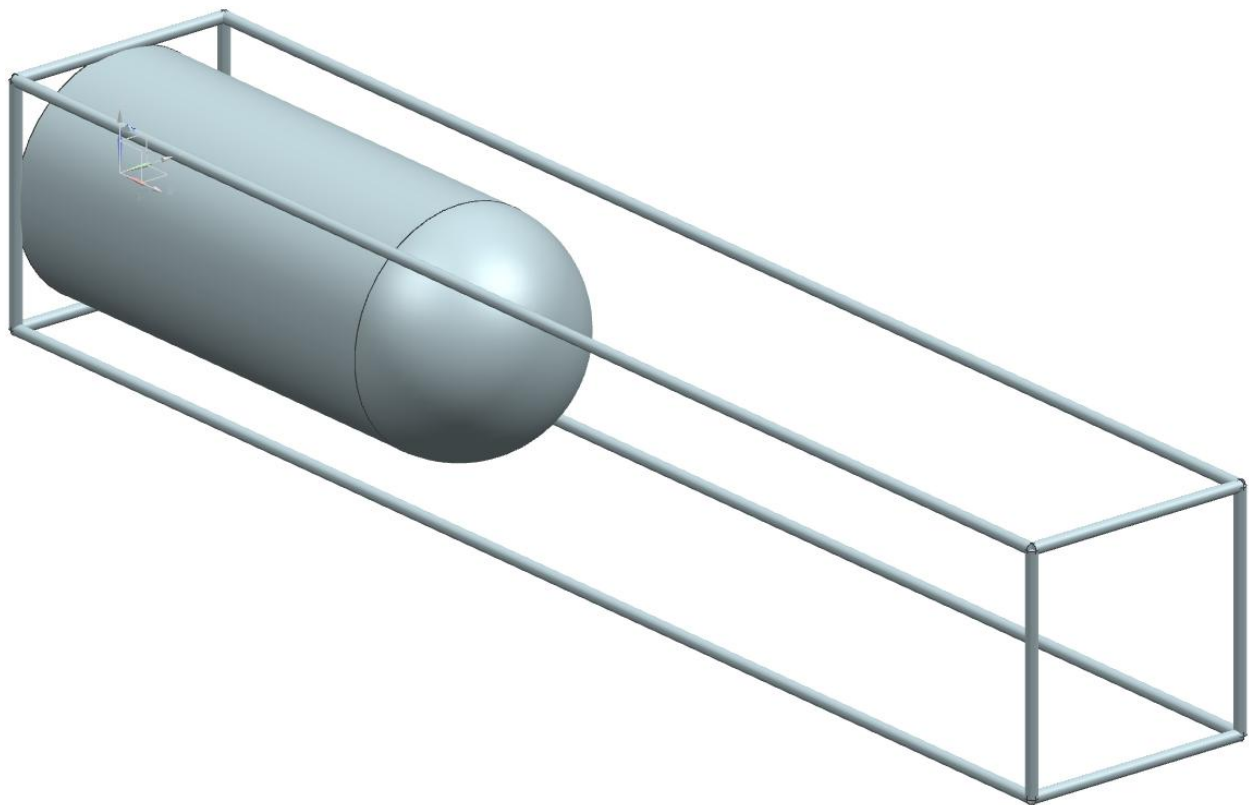


Figure 6.2 - Analytical representation of finger flame front.

The side skirt of the finger flame is eventually quenched by the cold wall, which leads to the formation of a planar flame front as shown in Fig. 6.3. The surface area of the flame front decreases drastically, and this leads to the decrease in the rate of pressure increase in the combustion chamber as shown in Fig. 4.7. The planar flame area is analytically modeled as a cuboid with a square cross section measuring $0.5 L$ in length, where L is the total length of the combustion chamber.

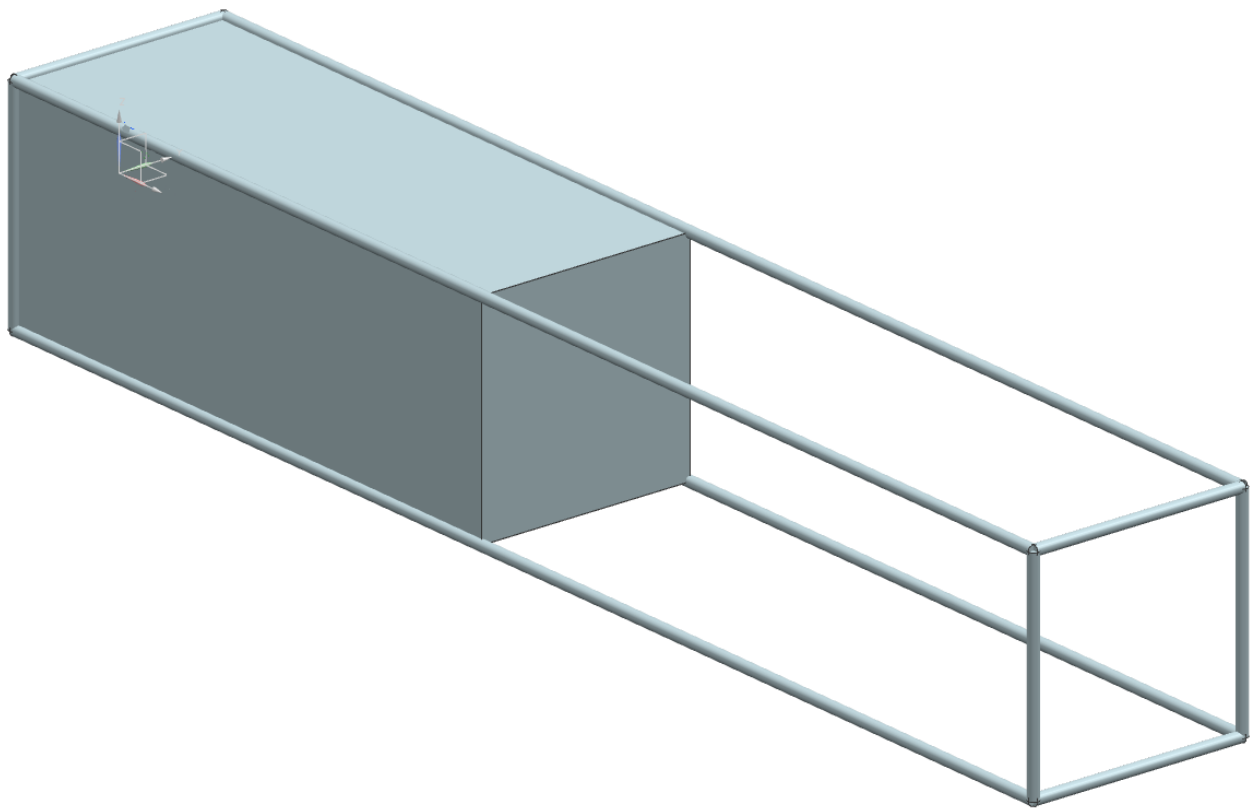


Figure 6.3 - Analytical representation of planar frame.

The planar flame rapidly undergoes a change in its structure to form an inward pointing cusp called a tulip flame. The total time taken by the flame to change its shape from an outward pointing finger flame to an inward pointing tulip flame takes 15 milliseconds. The dominant factor influencing the transition appears to be the hydrodynamical effects. The recirculation of the unburnt gas causes the mass burning rate to be the highest close to the center of the cross section when compared to the periphery. The analytical model of the tulip flame is represented as a pyramid with a four sided base whose height is R . The height of the pyramid remains constant throughout its propagation from $L=0.5$ to $L=1$. The analytical shape of the tulip flame is shown in Fig. 6.4 and Fig. 6.5.

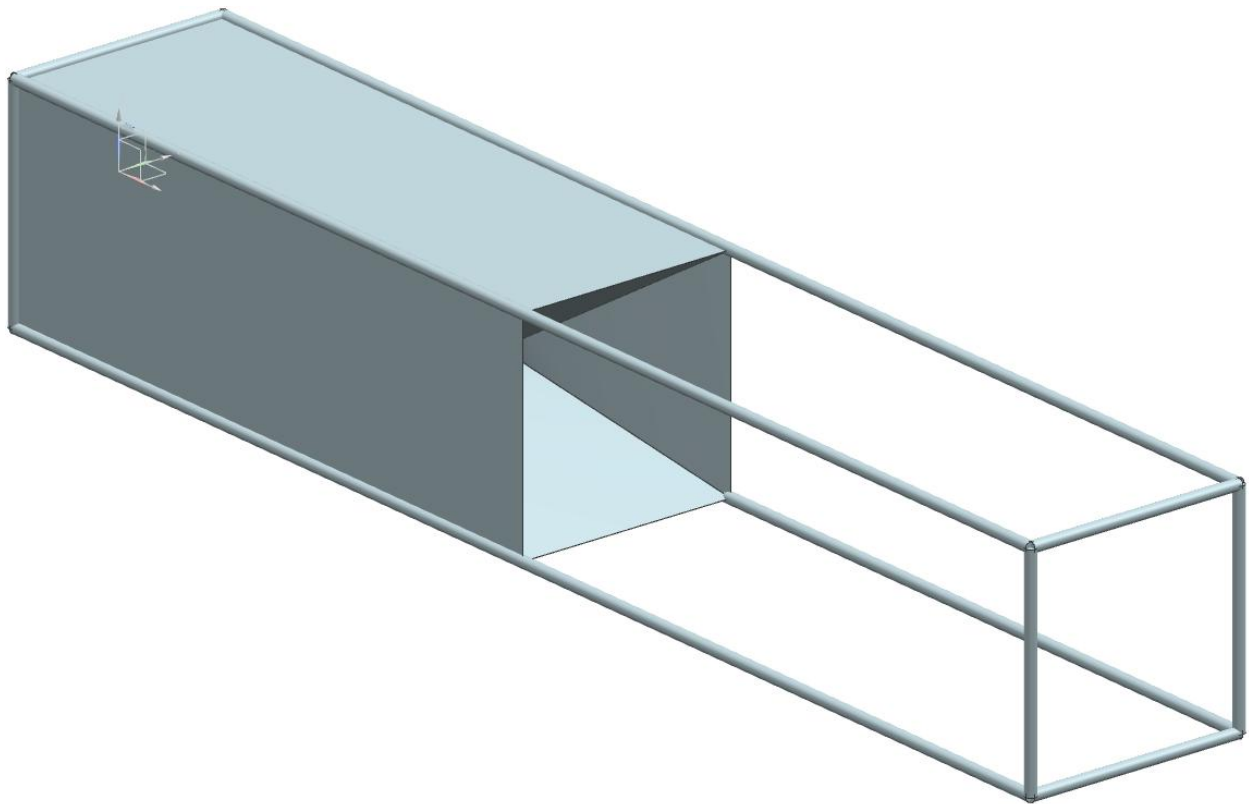


Figure 6.4 - Analytical representation of tulip flame.

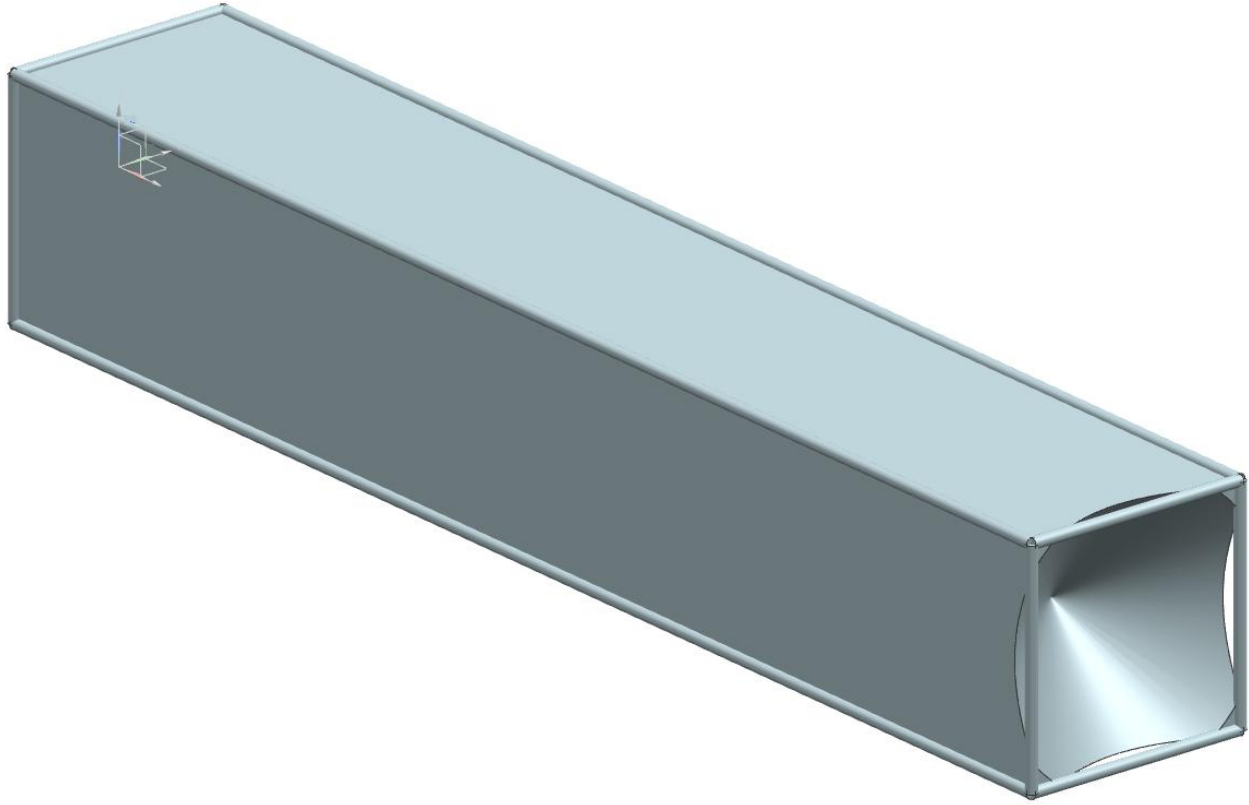


Figure 6.5 - Analytical representation of tulip flame collision with cold wall.

The approximations used in the calculation of the flame area and volume of burnt gases are shown below:

Stage I – Spherical Flame Front

Volume of burnt gas: $V_1 = \frac{2}{3} \cdot \pi \cdot r^3$

Flame surface area: $S_1 = 2 \cdot \pi \cdot r^2$

Where $0 < r < 0.75R$.

Stage II – Finger Flame Front

Volume of burnt gas: $V_2 = V_1 + 2.\pi.r.h + \frac{2}{3}.\pi.r^3$

Flame surface area: $S_2 = 2.\pi.r.h + 2.\pi.r^2$

where $0.75R < r < 1R$ and $0 < h < 5.4R$

Stage III – Planar Flame Front

Volume of burnt gas: $V_3 = R^2.h$

Flame surface area: $S_3 = R^2$

where $5.4R < h < 6R$

Stage IV – Tulip Flame Front

Volume of burnt gas: $V_4 = R^2.h - \frac{1}{3}.R^3$

Flame surface area: $S_4 = \frac{1}{\sqrt{2}}.R^3$

where $6R < h < 12R$

The flame surface area and burnt gas volume is computed using a MATLAB program. The corresponding plots are shown in Fig. 6.6 and Fig. 6.7.

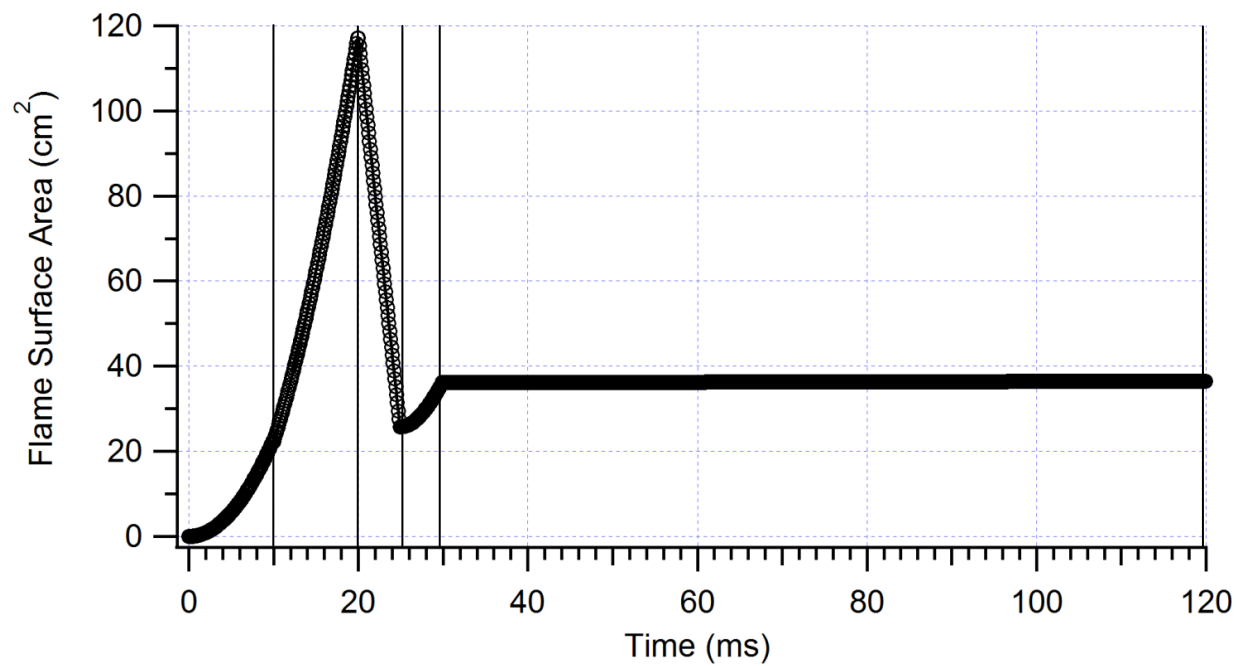


Figure 6.6 - Flame surface area vs. time.

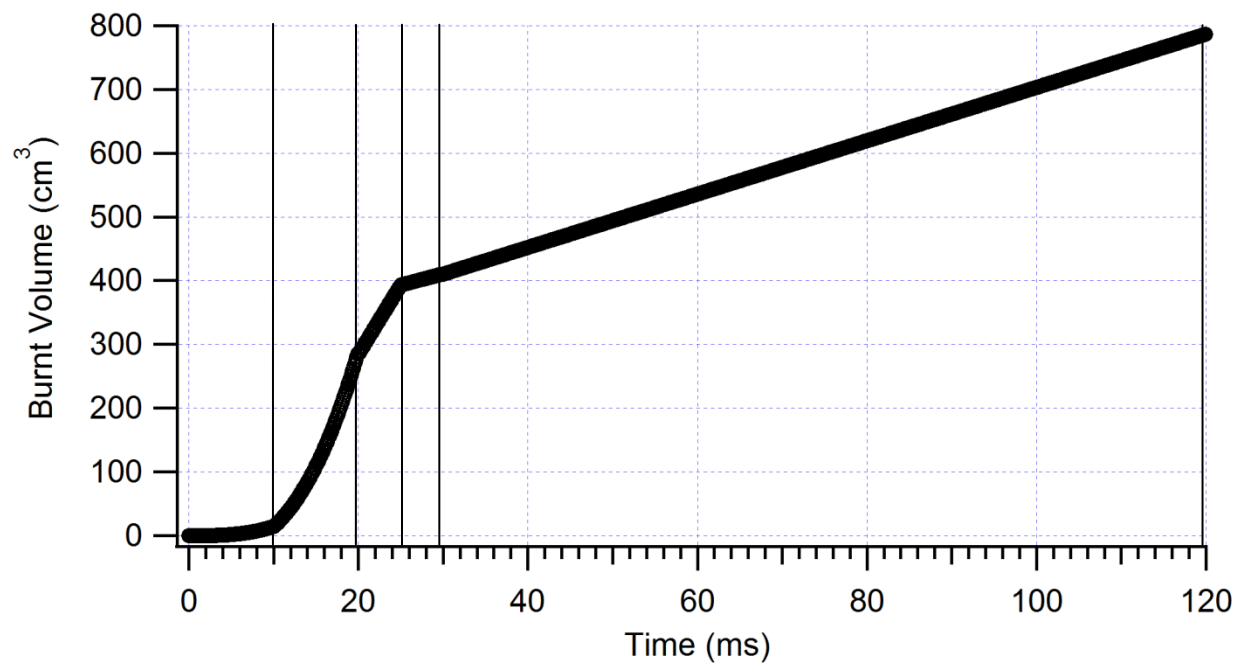


Figure 6.7 - Burnt volume vs. time.

CHAPTER 7

CONCLUSIONS AND FUTURE WORK

The results obtained through experimentation and numerical analysis correspond to those obtained by C. Clanet [14], S. T. Lee [15] and R. Starke [16]. Additional experimental results of the velocity field, using laser doppler anemometry, shown by D. Dunn-Rankin [20] enable the comparison to the velocity field obtained numerically. Analytical calculation performed on the formation of the tulip flame is shown by M. Matalon [17], M. Gonzales [18] and J. W. Dold [19]. The progression of the various structures formed during the propagation of a premixed flame front in a closed tube is verified with previous research work. Previous experimental research work involved the propagation of a premixed flame either in semi-open or closed tubes with circular cross-section. It is observed that an inward pointing cusp occurs in tubes with both rectangular and square cross-section, indicating that the aspect ratio is the primary factor in the formation of a tulip flame and not the shape of cross-section.

The flame speed profile obtained from the straight channel combustor can be utilized to obtain port timing and rotational speed of the wave disk engine. The use of obstacles along the length of the channel and the use of other turbulence generation mechanisms to increase the flame speed further can be investigated in the future. The use of obstacles in long channels has been investigated by A. R. Marsi [21], G. Cicarelli [22] and V. N. Gamezo [23].

APPENDICES

APPENDIX A

FLAME ANALYSIS MATLAB PROGRAM

The flame analysis program is written using the MATLAB programming language. The high speed camera generates a series of images recorded at the desired frame rate. The image is recorded in the TIFF format. The focus area of the image is equal to the camera focus area.

Step 1 –

The first step involves cropping the image from the camera output to the required combustion chamber window. This step involves batch processing the images using IrfanView image processing toolkit.

Step 2 –

Once the image has been cropped, the MATLAB program is used to convert the grayscale image to a binary image based on a threshold light intensity. The value of intensity in each pixel ranges from 0 to 255 in the grayscale image. This value is converted to either a 0 or 1 based on the user input threshold parameter. This step is performed to eliminate noise in the image from external sources or reflection from the glass plate.

Step 3 –

The program then uses progressive scans to capture the exact position of the flame front for each position along the height of the combustion chamber. This is done by capturing the position of the image where the value of intensity changes from 0 to 1. This ensures that the only the position of tip of the flame front is recorded by the program. The position of the flame front along the entire height of the channel is captured. If the program is unable to find a flame for a specific height, the position is reset to 0.

Step 4 –

The average position of the flame front is calculated by taking the mean position of the non-zero flame position for each image. The average position is converted from pixel units to physical distance in centimeters using a scaling ratio. The average position of the flame front for a sequence of images is now used to find the flame speed and flame acceleration. Additional data calculated by the program includes calculating the position of the lobes of the tulip flame, centerline flame speed, flame front area and difference between centerline and average flame front position.

The MATLAB program source code used to post-process the cropped images is given below –

```
clc
clear all
filedir=uigetdir('','Select image folder');
oldfolder=cd(filedir);
imagelist=[ls('*.*tif') ls('*.*bmp') ls('*.*jpg')];
numimages=length(imagelist);

%% Initial Parameters define the focus area, tube length, frame rate and variables to compute

left2right=0;
right2left=1;
tubefocuswidth=4;
tubefocuslength=28;
framerate=20000;
rawimage=imread(imagelist(1,:));
[d1,d2]=size(rawimage);
time=zeros(numimages,1);
binconvert=zeros(d1,d2);
flamepos=zeros(d1,numimages);
avflamepos=zeros(1,numimages);
centerflamepos=zeros(1,numimages);
flamediv=round(d1/3);
upperlobeflame=zeros(1,numimages);
lowerlobeflame=zeros(1,numimages);
userinput=75;
userflame=zeros(1,numimages);

%% Image Conversion from grayscale to binary based on threshold intensity value

for imagenumber=1:numimages
    rawimage=imread(imagelist(imagenumber,:));
    [d1,d2]=size(rawimage);
    maxint=max(max(rawimage));
    minint=min(min(rawimage));
    thresh=(maxint-minint)/24;
    for i=1:d1
        for j=1:d2
            if rawimage(i,j)>thresh
                binconvert(i,j)=1;
            else
                binconvert(i,j)=0;
            end
        end
    end
end
```



```

dispimage=255*binconvert;
image(dispimage)
colormap gray
axis image
M(imagenumbers)=getframe;
if right2left == 1
    binconvert=flipdim(binconvert,2);
end
for i=1:d1
    for j=d2:-1:1
        if binconvert(i,j)==1
            flamepos(i,imagenumbers)=(j);
            break
        end
    end
end
end
end

```

%% Flame Position Calculation based on intensity along the height
 %% Average Flame Position

```

for i=1:numimages
    avflamepos(1,i)=(sum(flamepos(:,i))/nnz(flamepos(:,i)));
end

```

%% Centerline Flame Position

```

for i=1:numimages
    centerflamepos(1,i)=flamepos((d1/2),i);
end

```

%% Lower and Upper Lobe Flame Position

```

for i=1:numimages
    lowerlobeflame(1,i)=flamepos((flamediv),i);
    upperlobeflame(1,i)=flamepos((2*flamediv),i);
end

```

%% User Input Flame Position

```

for i=1:numimages
    userflame(1,i)=flamepos(userinput,i);
end

```

```
%% Flipping position matrix
```

```
avflamepos=avflamepos';  
centerflamepos=centerflamepos';  
lowerlobeflame=lowerlobeflame';  
upperlobeflame=upperlobeflame';  
userflame=userflame';
```

```
%% Computing deviation from center flame
```

```
deviation1=avflamepos-centerflamepos;  
deviation2=lowerlobeflame-centerflamepos;  
deviation3=upperlobeflame-centerflamepos;  
deviation4=userflame-centerflamepos;
```

```
%% Converting from pixel to cm
```

```
mulfac=tubefocuslength/d2;  
avflamepos=avflamepos*mulfac;  
centerflamepos=centerflamepos*mulfac;  
lowerlobeflame=lowerlobeflame*mulfac;  
upperlobeflame=upperlobeflame*mulfac;  
userflame=userflame*mulfac;  
deviation1=deviation1*mulfac;  
deviation2=deviation2*mulfac;  
deviation3=deviation3*mulfac;  
deviation4=deviation4*mulfac;
```

```
%% Flame Speed Calculations
```

```
avflamespeed = diff(avflamepos)*framerate;  
centerflamespeed = diff(centerflamepos)*framerate;  
lowerlobeflamespeed = diff(lowerlobeflame)*framerate;  
upperlobeflamespeed = diff(upperlobeflame)*framerate;  
userflamespeed = diff(userflame)*framerate;
```

```
%% Flame Surface Area Calculation
```

```
flamearea=diff(flamepos);  
flamearea=flamearea*mulfac;  
flamearea=flamearea.*flamearea;  
flamearea=flamearea+(1/tubefocuswidth);  
flamearea=sqrt(flamearea);  
for i=1:(d1-1)  
    for j=1:numimages  
        if flamearea(i,j)==(2/tubefocuswidth)
```

```

        flamearea(i,j)=0;
    end
end
end
totalflamearea=sum(flamearea);
totalflamearea=totalflamearea';
clear d1 d2 binconvert dispimage filedir flamearea flamedir flamepos framerate i imagenumber j
clear left2right right2left maxint minint numimages oldfolder rawimage thresh time
tubefocuslength tubefocuswidth flamediv mulfac

%% Writing Output to MS Excel files

heading1 = {'Average Flame Speed','Center Flame Speed','Lower Lobe Flame Speed', 'Upper
Lobe Flame Speed','User Flame Speed'};
datawrite=[avflamespeed,centerflamespeed,lowerlobeflamespeed,upperlobeflamespeed,userflam
espeed];
xlswrite('flamespeed.xls',datawrite);
heading2 = {'Average Flame Position', 'Center Flame Position', 'Lower Lobe Flame Position',
'Upper Lobe Flame Position', 'User Flame Position', 'Average Deviation', 'Lower Lobe
Deviation', 'Upper Lobe Deviation', 'User Flame Deviation', 'Flame Area'};
datawrite=[avflamepos,centerflamepos,lowerlobeflame,upperlobeflame,userflame,deviation1,dev
iation2,deviation3,deviation4,totalflamearea];
xlswrite('flamepos.xls',datawrite);
xlswrite('flamespeedheading.xls', heading1);
xlswrite('flameposheading.xls',heading2);

```

APPENDIX B

SCHLIEREN DIAGNOSTIC SETUP

The Schlieren imaging technique is the method of visualization of density changes in a transparent media. The refractivity of a gas depends on gas composition, temperature and density. Compressible flows and combustion lead to sharp changes in the refractive index of the media due to the change in density. Optical inhomogeneities refract light rays in proportion to their gradients of refractive index. The resulting ray curvature is given by

$$\frac{\partial^2 x}{\partial z^2} = \frac{1}{n} \frac{\partial n}{\partial x}$$

$$\frac{\partial^2 y}{\partial z^2} = \frac{1}{n} \frac{\partial n}{\partial y}$$

The angular ray deflection is obtained by integrating the ray curvature equation described above.

$$\varepsilon_x = \frac{L}{n_0} \frac{\partial n}{\partial x}$$

$$\varepsilon_y = \frac{L}{n_0} \frac{\partial n}{\partial y}$$

These expressions provide the mathematical basis for the schlieren and shadowgraph techniques.

Z-Type 2-Mirror Schlieren System

The z-type Herschellian system using two oppositely tilted, on-axis spherical mirrors is the most popular schlieren setup. The combination of a diverging illuminator beam, an opposite converging analyzer beam and a parallel beam between the two mirrors suggest the letter “Z”, hence the name. The mirrors used in this arrangement are usually symmetrical, on-axis paraboloid or spherical mirrors. The advantage of using mirrors over lenses is primarily found in a larger aperture for a given cost.

A minimum distance of $2f$ is required between the two field mirrors, where f is the focus length of each mirror. While longer distance between the mirrors does not lead to any errors, shorter distances lead to a reduced sensitivity in the schlieren image. The schematic representation of the z-type schlieren setup is shown in Fig. 6.8.

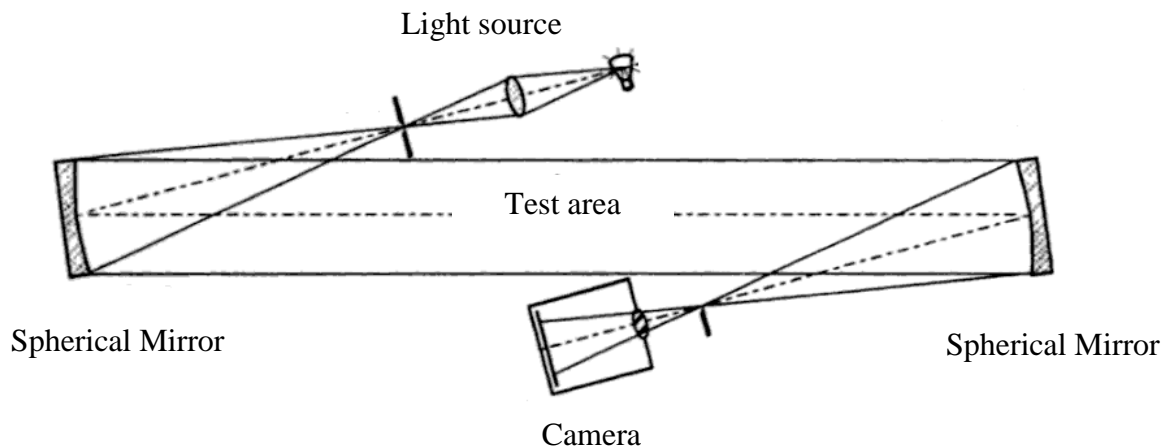


Figure A.1 - Z-type schlieren schematic

The apparatus requires the mirrors, light source and camera to be on the same plane, which is achieved by either mounting all the components on a breadboard or on a flat surface. First the light source is setup and focused to the required angle with respect to the mirror. The collimating spherical mirror is then set on the flat surface at a predetermined angle so as to form a collimated

beam of light. A white sheet of paper can be used to adjust the relative position of the light source and collimating mirror in order to obtain a perfectly parallel beam of light. A circle is drawn on the paper with diameter equal to the diameter of the mirror. The paper is then moved downstream of the mirror to verify that the light beam remains within the bounds of the circle and its size does not change. Once a parallel beam of light is obtained, the focusing mirror is set up at a distance twice the focal length of the mirror on axis downstream of the collimating mirror. The focusing mirror is set at an angle equal to that of the collimating mirror. The focusing mirror collects the parallel beam of light and focuses it onto the lens of the camera after it passes through a knife edge. The mirror used in the apparatus is a spherical mirror, 6 inches in diameter and a focal length of 60 inches. The mirror used is shown in Fig. 34.



Figure A.2 - Spherical mirror

The two mirrors were placed 120 inches apart and a razor blade is used as a knife edge. The combustion chamber is placed in the marked test area, 60 inches from either mirror. The focused light is pointed to the high speed camera after it passes through the knife edge. As the diameter of the mirror is 6 inches and the combustion chamber is 12 inches long, only half of the combustion chamber setup can be viewed by the schlieren set for a single experiment. To view the density change along the entire length of the combustion chamber, multiple experiments are conducted focusing on various parts of the tube and a composite video is constructed after verification is made on the consistency of the experiments. The video is compiled using commercially available VideoMach software, which stitches the boundaries of the images to form a continuous image.

APPENDIX C

NUMERICAL SCHEME

The numerical simulations are performed using the commercially available computational fluid dynamics software, Ansys Fluent. The numerical code uses the density based explicit scheme to discretize and solve the Navier-Stokes equation for a given control volume. The density-based scheme solves the fully-coupled Navier-Stokes equation at every time step based on the Courant-Friedrich-Levy conditions for stability.

This scheme solves the governing equations of continuity, momentum, energy and species transport simultaneously as a set, or vector, of equations. Governing equations for additional scalars are solved sequentially.

Governing Equations

The system of governing equations for a single component fluid, written to describe the mean flow properties, is cast in the integral Cartesian form for an arbitrary control volume V with differential surface area dA as follows:

$$\frac{\partial}{\partial t} \int_V W dV + \oint [F - G] \cdot dA = \int_V H dV$$

Here, the vectors W , F and G are defined below,

$$W = \begin{pmatrix} \rho \\ \rho u \\ \rho v \\ \rho E \end{pmatrix}$$

$$F = \begin{pmatrix} \rho v \\ \rho v u + p \hat{i} \\ \rho v v + p \hat{j} \\ \rho v E + p v \end{pmatrix}$$

$$G = \begin{pmatrix} 0 \\ \tau_{xi} \\ \tau_{yi} \\ \tau_{ij} v_j + q \end{pmatrix}$$

The vector H contains source terms such as body forces and energy sources. Here, ρ , v , E and p are the density, velocity, total energy per unit mass and pressure of the fluid respectively. τ is the viscous stress tensor and q is the heat flux.

The total energy E is related to the total enthalpy H by

$$E = H - p/\rho$$

Where

$$H = h + V^2/2$$

The Navier-Stokes equations represented above can be solved to capture the pressure waves produced due to combustion and the effect of pressure waves on the flame geometry when solved by satisfying the CFL conditions.

A fourth order Runge-Kutta scheme is used for the calculation of unsteady flows in the explicit solver. The solution is advanced from iteration n to iteration n+1 by the following steps –

$$Q^0 = Q^n$$

$$\Delta Q^i = -\alpha_i \Delta t \Gamma^{-1} R^{i-1}$$

$$Q^{n+1} = Q^m$$

Where $\Delta Q^i = Q^i - Q^n$ and i is the stage counter for the four stage scheme. α_i is the multistage coefficient for the i stage. The residual R^i is computed from the intermediate solution Q^i and is given by –

$$R^i = \sum^N_{faces} (F(Q^i) - G(Q^i)).A - VH$$

The time step is computed from the CFL (Courant-Friedrichs-Lewy) condition –

$$\Delta t = \frac{2CFL.V}{\sum_f \lambda_f A_f}$$

Where V is the cell volume, A is the face area and λ is the maximum of the local eigen values defined by the governing equations.

To enable successful capture of the pressure waves travelling through the control volume, the CFL number should always be set to a value below or equal to 1. This enables the numerical scheme to capture both the travel of pressure waves and calculate the thermal and species diffusion between the flame front interfaces.

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REFERENCES

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