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MEASURING THE SORPTION AND DIFFUSION OF WATER IN A MOISTURE SENSITIVE PRODUCT FOR USE IN SHELF LIFE SIMULATION
presented by

Patricia J. Allen
has been accepted towards fulfillment of the requirements for
Master degree in Packaging


Major professor
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# MEASURING THE SORPTION AND DIFFUSION OF WATER IN A MOISTURE SENSITIVE PRODUCT FOR USE IN BHELF LIFE SIMULATION 

BY<br>Patricia J. Allen

A THESIS
submitted to
Michigan state Oniversity
in partial fulfillment of the requirements for the degree of

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1994

# MEABURING TEE EORPTION AND DIFFUSION OF WATER IN A MOIETURE 8ENSITIVE PRODOCT FOR USE IN BHELF LIFE BIMULATION 

BY

Patricia J. Allen

A validation of a finite difference method computer program for estimating the shelf life of a packaged moisture sensitive pharmaceutical tablet is described. The parameters required to execute this computer model include the diffusion coefficient of the pharmaceutical product and the diffusion coefficient of the blister packaging material with respect to water vapor, as well as the solubility of water vapor in the packaging material. All of these parameters were determined experimentally using a Cahn electrobalance at various relative humidity values at 25.0 degrees Celsius.

In addition, the entire blister package / tablet system was monitored at two upper humidity levels for moisture gain as a function of time.

The GAB (Guggenheim-Anderson-de Boer) equation was used to fit the experimental moisture sorption isotherm data generated for the tablet.

A finite difference method computer program was found to be very helpful for predicting the shelf life of a moisture sensitive product, if all of the key physical characteristics of the product and packaging material are known.

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## PATRICIA JEAN ALLEN

1994

Dedicated to my grandmother, Marguerite Allen, who gave me the inspiration to achieve my goals.

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## LIST OF 8YMBOL8

| A | Surface area |
| :---: | :---: |
| A | Water activity |
| A.H. | Absolute humidity |
| a | Weight of filled blister package at time (t) |
| $\mathrm{b}_{1}$ | Statistical parameter for isotherm description |
| $\mathrm{b}_{2}$ | Statistical parameter for isotherm description |
| $\mathrm{b}^{2}$ | Weight of empty blister package at time (t) |
| C | Guggenheim constant |
| CMC | Critical Moisture Content |
| $\mathrm{C}_{\text {sat }}$ | Water concentration in air at saturation |
| $\mathrm{D}^{\text {bat }}$ | Diffusion coefficient |
| $\mathrm{D}_{\mathrm{L}}$ | Package diffusion coefficient |
| $\mathrm{D}_{\mathrm{R}}$ | Tablet diffusion coefficient |
| ${ }_{\text {d }}{ }^{\mathbf{R}}$ | Weight of water transferred across film |
| d8 | Change in time |
| EMC | Equilibrium Moisture Content |
| Exp. | Experimental |
| GAB | Guggenheim-Anderson-de Boer |
| $\mathrm{H}_{\mathrm{L}}$ | Henry's Law Constant |
| $\mathrm{H}_{\mathrm{m}}$ | Total heat of sorption of first layer on primary sites |
| $\mathrm{H}_{\mathrm{a}}$ | Total heat of sorption of multilayers |
| $\mathrm{H}_{1}$ | Heat of condensation of pure water vapor |
| IMC | Initial Moisture Content |
| k | Factor or slope |
| L, 1 | Average plastic film or product thickness |
| $\mathrm{M}_{\mathbf{t}}$ | Tablet weight gain at time (t) |
| $\mathrm{M}^{\mathbf{L}}$ | Final tablet weight gain |
| M.C. | Moisture content |
| N | Number of experimental data points in isotherm |
| P | Permeability |
| $\mathrm{p}_{\mathrm{i}}$ | Water vapor pressure outside film |
| $\mathrm{p}^{1}$ | Water vapor pressure inside film |
| PVC | Polyvinyl chloride |
| p | Water vapor pressure of product |
| $\mathrm{P}_{\boldsymbol{T}}$ | Laminate permeability |
| $\mathrm{R}_{\mathrm{p}}$ | Blister radius |
| $\mathrm{R}_{\mathrm{T}}$ | Tablet radius |
| R.H. | Relative humidity |
| r | radius |
| RMS | Root mean square |
| S | Solubility coefficient |
| T | Temperature |


| $t$ | Time |
| :---: | :---: |
| $t_{1 / 2}$ | Half time to reach steady state |
| $\mathrm{U}^{1 / 2}$ | Number of shells for tablet |
| $V_{p}$ | Blister volume |
| $\mathrm{V}_{\mathrm{T}}$ | Tablet volume |
| W | Water content on dry basis |
| $\mathrm{W}_{\mathrm{f}}$ | Final equilibrium tablet weight |
| $\mathrm{W}_{\mathbf{i}}{ }_{\text {* }}$ | Initial tablet weight |
| $\mathrm{W}_{\mathbf{i}}$ | Calculated water content |
| $\mathrm{W}_{\mathrm{m}}$ | Water content corresponding to saturation of adsorption sites |
| $\mathrm{W}_{\mathbf{t}}$ | Tablet weight at time (t) |
| WVTR | Water Vapor Transmission Rate |
| $\Delta \mathrm{W}$ | Weight change |
| X | Summation of experimental $A_{W}$ |
| $\mathrm{X}_{1}$ | Monolayer moisture content |
| Y | Summation of experimental A/EMC |
| $\boldsymbol{\theta}$ | Time lag |
| $\alpha$ | GAB constant |
| $\beta$ | GAB constant |
| $\boldsymbol{\gamma}$ | GAB constant |

## INTRODUCTION

In the pharmaceutical industry, a major concern lies in the determination of the necessary packaging materials to prevent moisture and other environmental factors from adversely affecting a product throughout its shelf life. The Food and Drug Administration requires extensive data supporting the choice of packaging a pharmaceutical product in a given packaging component. It would be very beneficial to have this information as early as possible, so that package design could be implemented based on actual realistic data as opposed to assumptions. In response to this need, several types of computer programs have been written to act as a simulation of the shelf life under certain conditions.

Many of these shelf life models consider different aspects of the product and package. One program in particular uses a finite difference method to compute the shelf life of a moisture sensitive product. This mathematical model requires knowledge of the diffusion properties of both the product and the packaging film. In addition, it takes into account the solubility of water vapor in the package system. This project involves experimental validation of a finite difference method. The objectives of this study are identified below:
A. To observe the sorption characteristics of a moisture sensitive pharmaceutical tablet and blister packaging material experimentally.
B. To calculate the diffusion coefficient of water vapor for both the product and package material.
C. To determine the moisture gain of the complete package/ product system at specific relative humidity levels and validate the calculated shelf life of the package.
D. To apply all of the acquired data to a finite difference computer model in order to generate the shelf life of the tablet.
E. To compare the experimental and simulated moisture gain profile to validate the simulation model based on a finite difference method.

## IITERATURE REVIEW

## Shelf Life of Moisture Sensitive Products

A very critical parameter in the selection of packaging for the food and pharmaceutical industries is the ability to obtain the proper shelf life needed for a product. Shelf life may be defined as the amount of time that a package or the product in the container will remain in a saleable or acceptable condition under specific storage conditions (Harte and Gray, 1987). Product shelf life can be altered by modifying its composition and form, the environment to which it is exposed, or the packaging system. The shelf life can be affected by environmental conditions, such as temperature and relative humidity. Therefore, it becomes necessary to have methods for predicting the shelf life based on product characteristics, external environment, and type of barrier packaging material utilized. In the case of moisture sensitive products, predictions for the end of shelf life, due to a gain of a critical amount of moisture, can be made if the temperature and relative humidity conditions are known as a function of time, and the package permeability to moisture is also known (Labuza, 1982).

It can be concluded that one of the primary environmental
factors that result in increased loss of quality and nutrition for most products is exposure to increased temperature (Labuza, 1982). In addition, gain of moisture by dry or semidry substances can lead to several modes of deterioration, such as microbial growth, softness, hardening, and caking.

The current FDA guidelines for documentation of acceptable packaging for human drugs and biologics require 3 years of shelf life data based on 2 kinetic concepts, one of which is reaction and the other is migration (Kim and Gilbert, 1989) .

Where solid dosage forms are concerned, moisture plays a very significant role in preformulation testing. Preformulation testing can be defined as an investigation of the physical and chemical properties of a drug substance alone and in combination with excipients. The ultimate objective of preformulation testing is to gather information useful to the formulator in the development of stable and bioavailable dosage forms which can be mass-produced (Schepky and Thomae, 1989). These sorption studies are designed to show quantitative relationships between the product samples and moisture. It is often possible to ensure that a final formulation exhibits the desired sorption properties by careful selection of the excipients.

If a container is empty, water vapor will pass through the container wall until the relative humidity inside the container is equal to the ambient atmosphere. In a drug-filled container, the difference in internal and external
relative humidity impels moisture to become introduced to the inside of the package and some amount of it will be absorbed by the product. The drug absorbs water in a predictable fashion, following its water absorption properties (Bonis, 1989). The package contents act as a moisture sink and retards equilibrium. When the product moisture content has reached an equilibrium with the ambient relative humidity, the humidities inside and outside the container are equal, therefore reducing the driving force to zero.

## Moisture sorption Isotherm

In order to analyze a moisture sensitive pharmaceutical product, it is necessary to produce a moisture sorption isotherm. The water sorption isotherms of foods and pharmaceuticals show the equilibrium relationship between the moisture content and the water activity ( $A_{w}$ ) at constant temperatures and pressures. These isotherms are generally described as a plot of the amount of water sorbed as a function of $A_{W}$ (Iglesias and Chirife, 1982). Packaging dehydrated foods is one of the most important applications of moisture sorption isotherms, since the prediction of storage life of these items packaged in flexible film materials is of considerable value in the food preservation area (Iglesias and Chirife, 1982). The rate of transport of water vapor through a film sample is shown by Eq. (1)

$$
\begin{equation*}
d w / d \theta=P A / l \quad\left(p_{i}-p_{0}\right) \tag{1}
\end{equation*}
$$

where $w$ is the weight of water transferred across the film, $\theta$ indicates the time, $P$ is the film's permeability, $l$ is the thickness of the film, $A$ is film area, $p_{i}$ is the vapor pressure of water outside the film, and $p_{0}$ is the vapor pressure of water on the other side of the film. This assumes that moisture entering the package equilibrates with the product almost immediately.

An interesting finding showed that the particle size distribution of a product often does not influence the sorption isotherm (Iglesias and Chirife, 1982). Isotherm equations are needed for evaluating the thermodynamic functions of the water sorbed. The need for mathematical models in order to use the isotherm with computer techniques was discovered.

The moisture isotherm serves as the translation between moisture influx into a hermetically sealed package and the effects of this water vapor on the product (Marsh, Ambrosio, and Guazzo, 1991). Computer modeling can be used to predict the time necessary for the moisture level inside the package to rise from a production moisture level to a critical level under specific environmental conditions. Marsh et al. developed a model for use in shelf life determination. The product examined was a Fibre Trim effervescent tablet, which became the first effervescent tablet to be introduced in a nonfoil package worldwide. This shelf life model calculates
the time for the moisture content within the product to rise from the initial moisture content to the critical content as influenced by the packaging system and environment. Packaging system refers to the package area, package volume, blister permeability and product net weight. Marsh's program considers the change in the driving force of moisture across the package as moisture traverses the film. Shelf life differences reflect the varying environmental conditions of 3 climactic regions at differing times in the product life cycle.

## Onit Dose Blister Packaging

Barrier plastics, which may be used for blister packaging, fill the gap between the infinite barriers to moisture mass transfer of metals and glass, and the finite barriers of coated cellulosic products and high permeability plastics. Often times, combinations of materials - laminates, coextrusions, or coated substrates - are necessary to provide for the unique requirements of foods and pharmaceuticals while supplying needed mechanical, thermal, optical and aesthetic properties (Brown, 1987).

Blister packages for pharmaceutical products have several advantages over bottles. Blisters allow for preparation of unit doses without having to physically handle the drug, leading to increased hygiene and better conservation of the drug (Dubouchet and Paisley, 1984). A blister provides good
mechanical protection of each individual tablet or capsule, has tamper evident features, and, being transparent, gives easy content identification. Also, blister packages aid in greater flexibility with regard to adapting the package size to the prescription size, reducing inventory requirements.

Over the last several years, there has been an entirely new use for coextruded film and sheet in packaging pharmaceuticals and medical devices in the U.S. (Bonis, 1989). The greatest threats to the physical condition, stability, and potency of drug products are heat, moisture, light and oxygen. Many drug products are completely inactivated by moisture exposure. Penicillin, for example, becomes totally inert unless packaged in containers with low water vapor transmission rates. Moreover, biological products such as vitamins, hormones, vaccines, antitoxins and certain antibiotics can degrade and be inactivated by excessive heat. Light and oxygen together may reduce or nullify the effectiveness of other substances, such as antibiotics, hormones, alkaloids, glucosides, vitamins, steroids (cortisone, prednisone) and vaccines.

Polymonochlorotrifluoroethylene (Aclar) is nearly impermeable to moisture, but it is an expensive material (Bonis, 1989). Aclar is suitable for packaging of pharmaceuticals because of its very low WVTR, fairly low gas transmission rate, inertness to most chemicals, resistance to ozone, clarity, good tear strength and excellent dimensional stability (Brennan, 1992). Due to its dramatically different
softening point from other thermoforming materials, Aclar laminates can complicate the thermoforming process. PVC (unplasticized) is one of the most commonly used materials because of low cost and ease of thermoforming. Unfortunately, it generally does not provide decent barrier protection to moisture. However, its barrier characteristics can be improved by lamination with different resins, especially Aclar.

Guise (1984) discussed some of the advantages of blister packaging. Blister packages offer protection against cross contamination, elimination of tablet abrasion caused by vibrations during distribution, decreased chance of overdose by over-the-counter (OTC) users, and storage space savings for reels of base and lidding materials over empty bottles.

Pires et al. (1988) conducted a study which evaluated Ibuprofen product stability in two multiple unit containers (30 and 50 count) and three blister package types. This project ultimately compared the effects of opening and closing the multiple unit containers with the different blister packs (PVC, Aclar/PVC and Saran coated PVC). Moisture sorption isotherms and WVTR data were generated. At the abusive storage conditions ( $78{ }^{\circ} \mathrm{F}$ and $85 \%$ R.H.), the moisture content of the tablets increased over time, with the greatest increase being in the PVC blister package and followed by the multiple unit 30 and 50 count containers subjected to repeated opening and closing. The Aclar blisters showed the best performance against moisture. Ambient conditions resulted in no
significant differences for the five package types. There are advantages to blister packaging in terms of barrier options and the one-time use feature.

## Diffusion and Permeability

Hernandez et al. (1986) applied the equilibrium vapor pressure and microbalance gravimetric method (i.e., sorption technique) to study the sorption and diffusion of toluene vapor in OPP and Saran film samples as a function of penetrant concentration. As part of this approach, the polymer sample was hung directly from one of the arms of the electrobalance while a constant concentration of penetrant vapor was flowed continually through the sample hang-down tube, such that the sample was completely surrounded by vapor (Hernandez et al., 1986) .

Understanding the diffusion, solubility and permeability of penetrants through plastic film structures is of both theoretical and practical importance. Theoretically, this knowledge can increase the understanding of diffusion mechanisms of penetrants through polymer membranes. Solubility and diffusion of organic penetrants will be critical for instances when product quality is related to the transfer of organic vapors from one element of the package to another element. Diffusion and solubility coefficients are usually determined by weight change observations of a polymer sample during a sorption process (Hernandez et al., 1986).

Diffusion and permeability values can be found from permeability studies where permeant transport through a film sample is monitored (isostatic procedure) or by quantifying the amount of permeant which has passed through the polymer and accumulated over time (quasi-isostatic procedure). The Cahn electrobalance is a very efficient tool for generating data of a vapor being sorbed by a film sample or any other product over a given time period.

At low concentrations, where plasticization is negligible and sorption kinetics are Fickian, the diffusivities of gases and vapors in glassy polymers are extremely strong functions of the size and shape of the penetrant molecules (Berens, 1989) .

The rate of permeability is affected by the temperature, humidity, and package surface area; polymer properties such as density, molecular orientation, plasticizer content and chain stiffness. In addition, the hydrophobic or hydrophilic character of the film will affect permeability (Brennan, 1992). Permeation through a plastic film occurs in three stages:

1. Absorption and solution of the penetrant on one polymer surface
2. Diffusion of the penetrant through the polymer
3. Desorption and evaporation of the penetrant from the other polymer surface.

There are several ways in which a gas can permeate a membrane. This will depend on the membrane structure. A
material with a capillary porous structure will produce gas transport by the phenomena which takes place in the pores, while a non-porous material will give rise to migration by molecular diffusion (Rudobashta et al., 1978).

Steffe and Singh (1980) conducted a study to determine the liquid diffusivity of the starchy endosperm, bran and hull of rough rice. Mathematical equations based on Fick's Law of Diffusion were used to model the thin-layer drying of brown, white and rough rice. Diffusion coefficients were found by minimizing the sum of squared deviations between the theoretically predicted and observed drying curves. The distinct feature of this research is that this rough rice product is viewed as a composite body with different diffusion properties for each component.

Several assumptions were made in order to develop the drying models used. Specifically:

1. Liquid diffusion is the mechanism of moisture movement.
2. Diffusion coefficients are not a function of moisture concentration.
3. Rice was considered to be isothermal during the drying process.
4. The rough rice kernel was considered as a sphere (starchy endosperm) surrounded by two concentric shells (bran and hull) for geometric purposes.
5. Rough rice components are homogeneous, isotropic materials.
6. Rice kernel shrinkage is negligible during drying.

## Fitting Models for Sorption Isotherms

Several mathematical models exist to fit the experimental sorption isotherm data for a given pharmaceutical tablet or food substance. One example is the BET (Brunauer-EmmettTeller) equation (Iglesias and Chirife, 1982) found below

$$
\begin{equation*}
a_{w} /\left(1-a_{W}\right) x=1 / x_{M} c+a_{w}(c-1) / x_{M} c \tag{2}
\end{equation*}
$$

which calculates $X_{n}$ (the monolayer moisture content). This parameter $\left(X_{N}\right)$ has significance in the physicochemical stability of foods.

Another such example is the Henderson equation (Iglesias and Chirife, 1982)

$$
\begin{equation*}
1-a_{w}=\exp \left\{-\left[b_{2}(x)_{1}\right]\right\} \tag{3}
\end{equation*}
$$

where $X$ is the moisture content expressed on a percent dry basis, and $b_{1}$ and $b_{2}$ are statistical parameters to be used for the isotherm description. To represent sorption data for interpolations or inclusion into computer models of drying processes, closed functions are used; the Guggenheim-AndersonDe Boer (GAB) equation is one of the relations most often applied (Spiess and Wolf, 1986).

Until recently, most of the mathematical models for prediction of the shelf life were simple in nature. Some of these models were developed by Labuza, Karel and coworkers and
focused on water vapor and oxygen deterioration. Peppas and Khanna have analyzed a mathematical theory of gaseous transport through polymer films, which in connection with a variety of food sorption models, can lead to concise prediction of shelf life of foods in storage environments (Peppas and Sekhon, 1980). With this approach, it is possible to predict shelf life of food products for moisture transport through plastic films, with minimal or no swelling due to sorption, and for sorption on food described by linear, Langmuir, BET, Halsey, Oswin, Freundlich and other isotherms. Generalized graphs were produced which exhibit the dependence of internal water activity on storage time for packaging systems characterized by a permeability-sorption constant. This constant is a packaging system quality and can be found from food sorption and polymer diffusion characteristics, as well as from specific geometric properties of the food package. Additionally, this theory was extended to include such parameters as oxygen diffusion, sorption and reaction on the food product.

The previous mathematical analysis combined diffusive and sorptive concepts in a simple, but accurate fashion. Assumptions inherent in this development include thermodynamically ideal systems, no swelling of the polymer film due to water vapor diffusion (i.e., thermodynamic incompatibility between moisture and polymer), isothermal conditions, single polymer packaging, no pressure difference during packaging, and constant temperature and relative
humidity (R.H.) storage conditions (Peppas and Sekhon, 1980). The model also assumes that there is no degradation or physical change of the polymer from time-temperature history, that sorption on the food is the rate limiting step once the vapors have diffused through the film, and that water diffusion through the food is not significant.

The specific amount of water associated with a solid at a particular relative humidity and temperature depends on its chemical affinity for the solid and the number of available sites of interaction. Zografi et al. (1988) studied the situation where various solids of differing moisture contents are mixed together into a solid dosage form and stored in a sealed container at a known temperature and headspace volume. Assumptions include a completely closed system and transfer of moisture occurs via the vapor phase.

A mathematical method to predict the amount of moisture associated with each ingredient in a mixture was presented. This model requires the initial moisture contents of the individual components, their dry weights, headspace volumes, temperature and an equation which can describe the sorption or desorption isotherms for the solid. This approach is significant for desiccant prediction and quantity necessary to maintain a relative humidity in a package. In addition, the headspace volume to be used to reduce moisture sorbed to an active ingredient may be estimated.

Computer simulation Programs

Various computer simulation programs have been developed at the School of Packaging (Michigan State University, East Lansing, MI) to predict shelf life of moisture sensitive products for a range of temperature and relative humidity values. Kirloskar (1991) interpolated data of the isotherm from data at three temperatures. Two different pharmaceutical products generated the experimental results which were being sought for this program. An orange flavored multivitamin tablet and an Ibuprofen tablet were evaluated. This development provides the effect of temperature on the coefficients of the equation selected to describe the equilibrium sorption isotherm of the tablet. The program combines the expression for the isotherm as a function of temperature and the expression for the water vapor permeability of the package with the equation for predicting the moisture gain of the tablet as a function of storage condition and time, within the three sorption isotherm temperatures.

Kirloskar evaluated three moisture sorption fitting equations as part of the shelf life program. The equations used were the Chen equation, the Henderson equation and the BET equation. The BET and Henderson equations were presented in Eq. (2) and Eq. (3), respectively. Chen's equation is shown in Eq. (4).

$$
\begin{equation*}
M=\left(k-\ln \left(-\ln A_{w}\right)\right) / a \tag{4}
\end{equation*}
$$

These equations were used to fit the experimental sorption isotherm data. The following criteria were used to select the best fitting equation out of the three possible: 1.) the best linear regression coefficient and, 2.) the minimum sum of the squared difference between the equation and experimental values. Kirloskar's shelf life predictive modeling assumed a steady state mass transfer of moisture through a package expressed as a permeability.

A different approach of a shelf life computer program was presented by Kim (1992). This program estimates the shelf life of a packaged moisture sensitive pharmaceutical product based on the solutions of a set of partial differential equations that correlate the amount of sorbed water by the product and the diffusion coefficient of water of the packaging material and the tablet. The set of differential equations is solved using the finite difference method. Some of the key parameters which are taken into consideration include the diffusion coefficient of water in the pharmaceutical product and the packaging material, as well as the solubility of the material to water.

One conclusion found as part of Kim's work was that the shelf life tends to decrease and reach an equilibrium state as the diffusion coefficient of the tablet and material increases. In addition, Kim observed that when the diffusion coefficient of water in the product is significantly higher
than the diffusion coefficient of the packaging material, the shelf life value for a circular plate shaped product was in agreement with an analytical solution. This model should prove to be extremely useful and accurate for package and material selection for a moisture sensitive product.

The shelf life of the pharmaceutical product is associated with the total moisture content in the tablet. Product performance depends on other characteristics besides moisture. The shelf life modeling does not provide information about these issues, such as any degradation from oxygen, light sensitivity, dissolution rate or change in potency of active ingredients. Perhaps at the present time, there is no predictive mathematical model which addresses all product areas. Moisture is the key parameter considered as part of this finite difference model to predict the shelf life by calculating moisture content at different levels (shells) of the tablet and determining the amount of water in the package headspace. All other changes in the quality of the product that affect the product's shelf life has to be correlated with the moisture content.

Contrary to the model that uses permeability, this program, based on a finite difference method, considers the unsteady steady state transfer of moisture through a packaging material, into the headspace of the package and into the food or pharmaceutical product. Due to the development of many polymers with strong resistance to water vapor, this study of mass transfer is useful. Several assumptions are made as part
of this simulation program and are found in the following list.

1. Water is transferred through the packaging film and pharmaceutical product by molecular diffusion.
2. Moisture sorption isotherms of packaging material and product are known.
3. The shelf life of the product depends on physical and/or chemical qualities which are only related to the moisture content of the product.
4. The temperature and relative humidity outside the package are constant.
5. Sorption/desorption hysterysis in the product is negligible.
6. The water vapor concentration in the headspace surrounding the product is homogeneous.
7. Initial concentrations of moisture in the product, headspace, and packaging material are all in thermodynamic equilibrium.
8. The diffusion coefficient of the polymer and product depend solely on temperature.
9. Product has simple geometry, such as a sphere or circular plate.
10. If the shape is that of a circular plate, moisture transfer occurs through the circular faces only and not through the edge of the tablet.
11. Diffusion of water vapor into the product is one
dimensional.
12. Product responds to changes in relative humidity instantly by absorbing moisture immediately.
13. Computer model considers only single layer packaging film materials.

The necessary parameters needed to execute this shelf life simulation model include all external conditions and specific characteristics of the packaging material and pharmaceutical product. External conditions were those such as relative humidity, absolute humidity and temperature. Package properties required were blister volume, blister surface area, package thickness, package diffusion coefficient, number of package layers and Henry's Law constant found from the solubility data. For the pharmaceutical tablet, characteristics investigated for this program included the tablet diffusion coefficient, both the initial and critical moisture contents, the dry tablet weight, the tablet radius and thickness, the number of shells used and the three GAB (Guggenheim-Anderson-de Boer) constants. All of these parameters comprised the input data for the mathematical model using the finite difference technique for unsteady state moisture uptake of a packaged product.

The diffusion coefficient of the tablet and the polymer film to water, as well as the solubility of the film to water, are the most critical parameters of this program. These characteristics have the greatest impact on the outcome of the
shelf life and exhibit adsorption and diffusion behavior of the water molecules. Polymer structure and percent crystallinity, along with product composition, affect the diffusion. It is important to know the constant temperature and relative humidity conditions outside of the package for the model. Diffusion coefficients of the tablet and material are dependent on the temperature.

Moisture content is the only indicator of moisture the product held before exposure to the external conditions. When the critical moisture content is reached, the shelf life is determined based on the period of time needed to obtain this value. Therefore, the CMC is a required variable of the program.

The GAB equation describes the moisture sorption isotherm of the product. From this equation of sorption character, the GAB coefficients are derived and are needed for the model to function. The GAB equation is ideal for analysis of food and pharmaceutical isotherms.

Blister volume determines package headspace available for the product with specific dimensions.

## MATERIALS AND METHODS

## Materials

As part of this experimental project, UpJohn Company (Kalamazoo, MI) supplied pharmaceutical tablets and blister packaging materials. The pharmaceutical product was a 20 mg Deltasone tablet (Lot No. 286 HW ), which is a brand of Prednisone. This drug is often used as an anti-inflammatory agent for the treatment of arthritis. Deltasone ( 20 mg ) is the active ingredient in these tablets. Calcium stearate, corn starch, FD \& C Yellow No. 6, lactose, sorbic acid and sucrose are listed as the inactive ingredients. The following dimensions and characteristics were determined and are listed in Table 1.

Table 1. Tablet dimensions

| Tablet Thickness | $0.392 \mathrm{~cm} \pm 0.001 \mathrm{~cm}$ |
| :--- | :--- |
| Tablet Radius | $0.50 \mathrm{~cm} \pm 0.005 \mathrm{~cm}$ |
| Tablet Mass | $0.4077 \mathrm{~g} \pm 0.0016 \mathrm{~g}$ |
| Surface Area of Tablet | $1.57 \mathrm{~cm}^{2} \pm 0.005 \mathrm{~cm}^{2}$ |
| Volume of Tablet | $0.308 \mathrm{~cm}^{3} \pm 0.005 \mathrm{~cm}^{3}$ |
| Shape of Tablet | Flat cylinder plate |

The blister packaging film sheet construction consisted
of 7.5 mil Polyvinyl Chloride / Adhesive layer / 1.6 mil Aclar from inside to outside. The following dimensions and characteristics were determined in Table 2. Figure 1 shows a schematic of a single blister cavity with thickness variations of the formed blister.

Table 2. Dimensions of blister package

| Height of Blister | $0.65 \mathrm{~cm} \pm 0.005 \mathrm{~cm}$ |
| :--- | :--- |
| Radius of Blister | $0.625 \mathrm{~cm} \pm 0.005 \mathrm{~cm}$ |
| Surface Area of Blister <br> Package | $3.78 \mathrm{~cm}^{2} \pm 0.005 \mathrm{~cm}^{2}$ |
| Inner Volume of Blister | $0.80 \mathrm{~cm}^{3} \pm 0.005 \mathrm{~cm}^{3}$ |



Figure 1. Schematic of a blister cavity with thickness measurements

MOIETURS BORPYION IEOTEERM OF TABLET

## Sample Preparation

For the determination of moisture gain over a specific period of time, the Cahn D-200 Model Electrobalance was used. This is a very sensitive mass measurement instrument. The electrobalance is able to detect mass changes as small as 0.1 microgram and is computer operated. The data which was generated by the electrobalance was stored in and retrieved from the hard disk in the computer, and plotted on a plotter using the Cahn software package. A detailed drawing of the electrobalance and the hangdown tube where the sample was held is shown in Figure 2.

The sample tablet used to generate data for the moisture sorption isotherm was prepared in the following manner. A thin strip of aluminum foil was cut to the same dimension as the tablet thickness and attached with adhesive around the entire edge of the tablet. Epoxy resin/hardener (Elmers) was used as the adhesive. The two end tabs of the foil were adhered to one another to form a "tab" and the tablet/foil arrangement was allowed to set for at least two hours. This aluminum strip surrounding the tablet was done in order to fully seal off the edge of the product so that moisture exposure could occur only at the two tablet faces. It was desirable to have water vapor enter only the tablet faces and not the edge, due to the single dimension diffusion character


Figure 2. Cahn Electrobalance and hangdown tube for sample
of the shelf life predictive model. A sketch of the tablet/foil sample is in Figure 3. A tiny pinhole was formed in the foil "tab" producing an area for a hanger-shaped wire to be placed.


Figure 3. Deltasone tablet sample with foil on edge

Drying the Tablet

The tablet was dried to nearly $0 \%$ moisture content in a vacuum oven for 4 - 6 hours at room temperature. A metal stand was put into a large glass beaker in order to support the tablet and wire while drying. During this time, the electrobalance went through a calibration process. After
drying the sample, it was quickly moved to the electrobalance tube inside of the environmental chamber and hung from the electrobalance hangdown wire. Additional drying took place through nitrogen flushing until the sample displayed a steady state condition. The sample tablet was contacted with several relative humidity values ranging from 11.50 to $91.70 \%$ R.H. at $25.0^{\circ}$ Celsius. It was possible to measure the relative humidity condition with the use of hygrosensors attached to a hygrometer (Newport Scientific HYGRODYNAMICS, Newport Scientific, Inc., 8246 E. Sandy Court, Jessup, MD 20794-0189). The relative humidities considered were 11.50\%, 15.25\%, 23.20\%, 27\%, $34.50 \%$, 40\%, 48.80\%, 60.35\%, 66\%, 73.40\%, 77.75\%, 82.45\%, 87.30\% and 91.70\%. These values were used to construct the moisture sorption isotherm for the product. A schematic of the electrobalance and system can be found in Figure 4.

## sorption Isotherm of Blister

The blister film material, a laminate of PVC film and Aclar, was delaminated in order to analyze the components of the structure on an individual basis for moisture sorption character. This was necessary to determine the diffusion coefficient of water through both polymers. Also, this delamination can ultimately show that separation of these materials doesn't affect their overall properties, such as water vapor transmission and permeability. Each material


T - Nitrogen tank
Te - Tee connection
EC - Environmental Chamber
EB - Can electrical balance
Vv - Venting valve

S - Humidity sensor
N - Needle valve
R - Rotameter
B - Gas washing bottle

sample was $6.45 \mathrm{~cm}^{2}$ and was cleaned with Hexane to remove any remaining adhesive. Each sample was given a pinhole in order to hang from a small wire. A similar procedure employed to dry the pharmaceutical tablet was utilized for drying these film samples. Relative humidities studied were approximately 26.90\%, 43.50\%, 58.20\%, and 77\%.

## I. R. Identification

The two blister packaging film samples, PVC and Aclar, were analyzed using a Perkin Elmer Infrared Spectrophotometer. The PVC sample required the Attenuated Total Reflectance unit (ATR) due to its thickness being in excess of a few mils. This unit, with the aid of specific angled mirrors and a crystal attachment, allows a clear scan to be obtained on thicker plastic films. Standard IR transmission techniques were used to generate a scan of the Aclar material. Before running the samples on the IR Spectrophotometer, they were cleaned with Hexane in order to remove any adhesive that could have been remaining after delamination of the material. IR scans provide the distinct identification that is characteristic of various materials. IR transmissions were conducted to verify that the PVC and the Aclar had no additional adhesive left after delamination and for individual film identification purposes.

## Water Vapor Transmission Rate of Packaging Material

Water Vapor Transmission Rates (WVTR) were determined for the blister materials using a dish method (ASTM E96). Three different samples were prepared in triplicate. There was a PVC sample, an Aclar sample, and a sample of the PVC/Aclar lamination which were tested. Each dish was cleaned thoroughly and enough fresh desiccant was added to cover the bottom of the dish. Circular samples of each material were cut out and sealed to a dish with a hot paraffin wax mixture. The dishes were weighed on a Mettler Analytical Balance and placed into an environmental chamber at $37.78^{\circ} \mathrm{C}$ and 85\% R.H. These dishes were weighed 4 separate times over a 1.25 month time period. The WVTR of these materials was calculated based on the weight gain of the dish samples.

## Moisture Gain of the Tablet and Blister Package

As an experimental way to validate the calculation of shelf life, Deltasone tablets packaged in blisters were also studied for moisture uptake over time. Two separate relative humidity environments with controlled conditions were created using salt solutions in tightly closed 5 gallon plastic (high density polyethylene) buckets. Salt solutions were prepared by adding the specific salt to a crystallization dish containing warm distilled water until saturation was clearly visible. One humidity condition was $78.5-80 \%$ R.H. and was
prepared with Ammonium Sulfate $\left(\mathrm{NH}_{4}\right)_{2} \mathrm{SO}_{4}$. The other environmental container used Potassium Nitrate ( $\mathrm{KNO}_{3}$ ) to provide a humidity condition of 88.5 - $90 \%$ R.H. The relative humidity levels were measured with a digital hygrometer periodically.

Five full blister cards were placed inside of each bucket, along with one empty blister card to be used as a control. Each blister card contained 10 blisters and held a total of 10 tablets. The packages were weighed over a several month period in order to monitor weight gain with a Mettler Analytical Balance. Forceps were used to handle the blisters at all times. Before placing in to the controlled humidity buckets, all of the blister packages were dried in a convection oven at $40.0^{\circ} \mathrm{C}$, until a steady state weight occurred.

## RESULTS AND DIECUS8ION

## Tablet 8orption

Sorption equilibrium experiments were conducted using the Cahn electrobalance at $25.0^{\circ} \mathrm{C}$. Equilibrium moisture values of the tablet were obtained at selected conditions of humidity, such as 0 , $11.50,15.25,23.20,27,34.50,40$, $48.80,60.35,66,73.40,77.75,82.45,87.30$ and $91.70 \%$ R.H.. Since the electrobalance operates by a stepwise change of the humidity value surrounding the tablet, several sorption experiments were necessary to carry out the whole isotherm. Besides obtaining the moisture equilibrium value, this mode of operation allowed the determination of the diffusion coefficient of water at various values of relative humidity.

The electrobalance, in combination with the computer and software, allowed for storage of the tablet weight at a specific time point. The amount of time between each tablet weighing was selected prior to the experimental test at a given relative humidity. For each humidity test, the time was expressed in hours, and the weight gain of the tablet $\left(M_{t}\right)$ was calculated. For each experiment, there was an initial weight, $W_{i}$, and an equilibrium weight. The equilibrium weight of one experiment became the initial weight for the next interval of
humidity. Moisture weight gain, $M_{t}$, of the tablet is calculated as

$$
\begin{equation*}
M_{t}=W_{t}-W_{i} \tag{5}
\end{equation*}
$$

where $W_{t}$ is the tablet weight at time $(t)$ and $W_{i}$ is the initial tablet weight. The final tablet weight gain ( $M_{\infty}$ ) is calculated as

$$
\begin{equation*}
M_{0}=W_{f}-W_{i} \tag{6}
\end{equation*}
$$

where $W_{f}$ indicates the equilibrium weight of the tablet at the end of an experimental humidity value. From these values, $M_{\tau} / M_{0}$ was determined by dividing each consecutive weight gain, $M_{t}$, by the final weight gain, $M_{\infty}$. Values of $M_{t} / M_{0}$ were plotted against time ( $t$ ), as well as $M_{t}$ vs. time ( $t$ ). An example of this is represented in Figure 5. Nearly all of the graphs for the tablet displayed a rapid weight gain of water vapor and then leveled off at steady state.

## Material sorption

The individual PVC and Aclar film samples were also used to calculate the moisture sorption for the packaging material. Similar graphs were produced to illustrate the moisture gain of PVC and Aclar at selected relative humidities. A typical graph of the moisture uptake by PVC film is presented in

Figure 6, and Aclar film shows a similar type plot which is presented in Figure 7. This allows a graphical analysis to be generated of the films' sorption character over a given humidity range. It was found that


Figure 5. Experimental sorption of tablet at 82.05-87.30\% R.H., $25.0^{\circ} \mathrm{C}$
both films absorbed moisture rapidly and attained steady state within 5.0 hours for relative humidity levels ranging from 0 to $26.90 \%$ R.H. for PVC film and within 2.0 hours for relative humidity levels ranging from 43.50 to $58 \%$ R.H. for Aclar film.


Figure 6. Experimental sorption of PVC film at 0-26.90\% R.H., $25.0^{\circ} \mathrm{C}$


Figure 7. Experimental sorption of Aclar film at 43.50-58\% R.H., $25.0^{\circ} \mathrm{C}$

## 8orption Isotherm

For each value of relative humidity, the equilibrium moisture content (EMC) of the product is defined as the gain of moisture per 100 grams dry weight of product or packaging material and is calculated in the following equation.

$$
\begin{equation*}
E M C=\left[\left(W_{f}-W_{i}\right) /\left(W_{i}\right)\right] \times 100 \tag{7}
\end{equation*}
$$

A moisture sorption isotherm can be generated by plotting EMC against relative humidity. The isotherm gives the amount of water per unit of dry weight of the substance at a particular humidity value at a given temperature. A sorption isotherm describes the manner in which the moisture content will change due to relative humidity fluctuations. Isotherms can also be plotted using EMC vs. $A_{W}$ (water activity) per Eq. (8). For the Deltasone tablet, the greatest increase in the moisture content occurred between 87.30 and $91.70 \%$ R.H. (last point on isotherm). The actual isotherm data is given in Table 3. This isotherm is presented in Figure 8. Equation 8 is described below.

$$
\begin{equation*}
A_{w}=p / p_{0}=\text { Relative Humidity } / 100 \tag{8}
\end{equation*}
$$

In this equation, $p$ is the water vapor pressure of the product and $p_{0}$ is the saturation vapor pressure of pure water at the temperature of test (Iglesias and Chirife, 1982). Isotherms are typically similar for most pharmaceutical products.

The sorption isotherms for the Aclar and PVC film samples were generated using the same techniques described for the Deltasone tablet above in Eq. (7). The moisture sorption isotherms for the packaging materials showed fairly linear curves. Increases in moisture content were quite consistent at the various levels of relative humidity. Tables 4 and 5

Table 3. Moisture sorption isotherm data for Deltasone tablet at $25.0^{\circ} \mathrm{C}$ (Experimental and Calculated)

| Relative Humidity <br> $(\%)$ | Exp. Equilibrium <br> Moisture Content <br> $(\mathrm{g} \mathrm{H} \mathrm{H} / 100 \mathrm{~g}$ dry) | Calc. Equilibrium <br> Moisture Content <br> $\left(\mathrm{g} \mathrm{H} \mathrm{H}_{2} / 100 \mathrm{~g}\right.$ dry) |
| :---: | :---: | :---: |
| 0 | 0 | 0 |
| 11.5 | 0.375 | 0.441 |
| 15.25 | 0.394 | 0.485 |
| 23.2 | 0.524 | 0.562 |
| 27.0 | 0.642 | 0.598 |
| 34.5 | 0.699 | 0.673 |
| 40.0 | 0.743 | 0.734 |
| 48.8 | 0.932 | 0.851 |
| 60.35 | 1.05 | 1.062 |
| 66.0 | 1.221 | 1.202 |
| 73.4 | 1.365 | 1.451 |
| 77.75 | 1.606 | 1.653 |
| 82.45 | 1.904 | 1.938 |
| 87.3 | 1.976 | 2.351 |
| 91.7 | 3.514 | 2.917 |



Figure 8. Moisture sorption isotherm of 20 mg Deltasone tablet at $25.0^{\circ} \mathrm{C}$ showing Equilibrium Moisture Content (EMC) vs. relative humidity
provide the sorption data for the PVC and Aclar film. Moisture sorption isotherms for the PVC and Aclar material samples are presented in Figures 9 and 10, respectively.

Table 4. Moisture sorption isotherm data for PVC film at $25.0^{\circ} \mathrm{C}$

| Relative Humidity (\%) | Equilibrium Moisture <br> Content (g $\mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry) |
| :---: | :---: |
| 0 | 0 |
| 26.9 | 0.036 |
| 43.5 | 0.076 |
| 58.2 | 0.10 |
| 77.0 | 0.133 |

Table 5. Moisture sorption isotherm data for Aclar film at $25.0^{\circ} \mathrm{C}$

| Relative Humidity (\%) | Equilibrium Moisture <br> Content (g H20/100 g dry) |
| :---: | :---: |
| 0 | 0 |
| 27.35 | 0.055 |
| 43.5 | 0.084 |
| 58.0 | 0.121 |
| 74.45 | 0.131 |



Figure 9. Moisture sorption isotherm of PVC film at $25.0^{\circ} \mathrm{C}$ showing Equilibrium Moisture Content (EMC) vs. relative humidity


Experimental _ Calculated

Figure 10. Moisture sorption isotherm of Aclar film at $25.0^{\circ} \mathrm{C}$ showing Equilibrium Moisture Content (EMC) vs. relative humidity

Solubility of Packaging Material

The linear change in moisture content by the PVC and Aclar materials can be described by Eq. (9). The slope of Eq. (9) gives the solubility coefficient of both the PVC and Aclar materials.

$$
\begin{equation*}
\text { EMC }=k \text { Relative Humidity } \tag{9}
\end{equation*}
$$

For this equation, $k$ is the slope of the sorption isotherm. For PVC, the solubility coefficient was found to be 0.001704 g $\mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ PVC \% R.H. (see Appendix C). A solubility coefficient of $0.001838 \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ Aclar of R.H. was calculated for Aclar film (see Appendix D).

## Water Vapor Transmission Rate of Materials

The ASTM dish method (ASTM E96) was applied to determine the Water vapor Transmission Rate (WVTR) of the various blister packaging materials. Continuous weight gain of the desiccant filled metal dishes was monitored over a specific period of time. This illustrated the passage of water through the material over time, which resulted in moisture gain of the desiccant.

$$
\begin{equation*}
\text { WVTR }=\Delta W / A * T \tag{10}
\end{equation*}
$$

$\Delta W$ is the weight change over time (g), A is the surface area of the exposed material $\left(\mathrm{m}^{2}\right)$, and T is the time period of the test (day). The WVTR test was conducted at $37.78{ }^{\circ} \mathrm{C}$ and 85\% R.H. over a 35 day interval. Surface area is calculated using

$$
\begin{equation*}
A=\pi r^{2} \tag{11}
\end{equation*}
$$

where $r$ is the radius of the circular film section within the dish. Graphs of dish weight gain over time for each material display water vapor transmission properties. Results are presented graphically in Figure 11 (PVC), Figure 12 (Aclar), and Figure 13 (PVC/Aclar). Film samples of PVC, Aclar, and PVC/Aclar were analyzed in triplicate for this experiment (see Appendix E).

In order to evaluate the packaging materials, it was necessary to determine the permeability and the diffusion coefficients for the PVC and the Aclar samples. The WVTR and $P$ were measured experimentally for each individual material and for the laminate structure in order to compare the results. With the following equation, the calculated composite $W$ VTR $\left(\right.$ WVTR $\left._{T}\right)$ may be analyzed against the actual data generated.

$$
\begin{equation*}
1 / \text { WVTR }_{T}=1 / \text { WVTR }_{\text {PVC }}+1 / \text { WVTR }_{\text {Aclar }} \tag{12}
\end{equation*}
$$

It was found that the calculated WVTR was very close to the WVIR obtained in the laboratory with $0.169 \mathrm{~g} / \mathrm{m}^{2}$ day


Figure 11. WVTR of PVC film at $37.78{ }^{\circ} \mathrm{C}$ and $85 \%$ R.H.


Figure 12. WVTR of Aclar film at $37.78{ }^{\circ} \mathrm{C}$ and $85 \%$ R.H.


Figure 13. WVTR of PVC/Aclar film at $37.78{ }^{\circ} \mathrm{C}$ and $85 \%$ R.H.
(calculated) and $0.1616 \mathrm{~g} / \mathrm{m}^{2}$ day (average experimental).
In addition, a comparison of the permeability (experimental) for the laminate blister material and the calculated permeability was determined. Eq. (13) provided the results of the permeability for the total laminate.

$$
\begin{equation*}
P_{T}=L_{T} /\left(\left(L_{P V C} / P_{P V C}\right)+\left(L_{A c l a r} / P_{A c l a r}\right)\right) \tag{13}
\end{equation*}
$$

$P_{T}$ is the permeability for the total film structure, $L_{T}$ is the total thickness of the laminate, $L_{\text {pvc }}$ is the thickness of the PVC sample, $L_{\text {Actor }}$ is the thickness of the Aclar, and $P_{\text {PVC }}$ and $P_{\text {Aclar }}$ are the permeability values for the PVC and the Aclar, respectively. Permeability is calculated from the following equation. Experimental permeability (average) was found to be $0.0348 \mathrm{~g} \mathrm{mil} / \mathrm{m}^{2}$ day mmHg and the comparative calculated permeability was $0.0364 \mathrm{~g} \mathrm{mil} / \mathrm{m}^{2}$ day mmHg showing outstanding agreement of the laminate structure.

$$
\begin{equation*}
P=W V T R * L / \Delta p \tag{14}
\end{equation*}
$$

$P$ is the permeability, $L$ is the thickness of the material sample and $\Delta p$ is the change in pressure of the internal and external environment of the film.

Permeability may also be expressed using other variables as noted below.

$$
\begin{equation*}
P=D * S \tag{15}
\end{equation*}
$$

$D$ is the diffusion coefficient and $S$ is the solubility coefficient.

It was critical to show the correlation between the calculated $W V T R$ and permeability of the laminate and the experimental $W V T R$ and permeability values for the laminate. This helped to verify that separation of the composite film into PVC and Aclar layers can yield expected and accurate results for most film characteristics.

## Diffusion Coefficient

The diffusion coefficients for water vapor through both the Deltasone pharmaceutical tablet and the packaging films need to be determined as a parameter in the finite difference method computer program (Kim, 1992). For the circular plate shaped pharmaceutical product, the diffusion coefficient is described by the following expression

$$
\begin{equation*}
D=0.049 L^{2} / t_{1 / 2} \tag{16}
\end{equation*}
$$

where $L$ is the average thickness of the tablet (cm) and $t_{1 / 2}$ (seconds) is half the time required for $M_{t} / M_{0}$ to reach the equilibrium steady state condition at any given relative humidity value.

It is important to discuss the procedure used to calculate the diffusion coefficient for the tablet, as well as the packaging materials. The diffusion coefficient takes into
account the $t_{1 / 2}$ value as seen from Eq. (16). $T_{1 / 2}$, the time required to reach one half of the steady state, was difficult to identify exactly. Therefore, several $t_{1 / 2}$ values were analyzed to produce several D values. Based on Eq. (17), various curves of $M_{t} / M_{\infty}$ were generated using the different tablet diffusion coefficients. At any given relative humidity range, the experimental $M_{t} / M_{\odot}$ vs. time was compared to the calculated $M_{t} / M_{0}$ vs. time using a least squares method. This method involved taking the sum of the differences squared for the $M_{t} / M_{0}$ values (calculated and experimental). The diffusion coefficient which provided for the least sum was used as the result for a particular humidity level (see Appendix B). Product diffusion is a required component of the shelf life model. This process should improve the accuracy for the determination of the diffusion coefficient.

The mass uptake of a flat specimen surrounded by a sorbate at constant concentration is given by the following equation (Crank, 1975).
$M_{t} / M_{\infty}=1-8 / \pi^{2}\left[\exp \left(-D \pi^{2} t / L^{2}\right)+1 / 9 \exp \left(-9 D \pi^{2} t / L^{2}\right)\right](17)$

This equation allows a comparison between the calculated $M_{t} / M_{0}$ values and the experimental $M_{t} / M_{0}$ values. Figure 14 presents a comparison of the calculated and experimental moisture uptake curves for the Deltasone tablet. It is evident from the two curves that the agreement is excellent for the experimental and calculated data.


Figure 14. Comparison of experimental and calculated $M_{t} / M_{\odot}$ for 20 mg Deltasone tablet at 72.25-77.75\% R.H. and $25.0^{\circ} \mathrm{C}$

The values for the diffusion coefficient which were calculated for the Deltasone tablet had some degree of variability across the different humidity levels. This variability may have been caused by the change in environmental conditions (relative humidity). Based on the
calculation for the diffusion coefficient, the $t_{1 / 2}$ value is the only variable which can fluctuate with the humidity as the average thickness of the tablet remains constant. Therefore, the time required to obtain half of the steady state condition varied with the R.H. in this instance. Diffusion coefficient results extended through the range of $0.603 \mathrm{E}-06 \mathrm{~cm}^{2} / \mathrm{sec}$. at 40.75-48.80\% R.H. to $1.62 \mathrm{E}-06 \mathrm{~cm}^{2} / \mathrm{sec}$. at $66-73.40 \%$ R.H. The standard deviation was found to be $3.30 \mathrm{E}-07 \mathrm{~cm}^{2} / \mathrm{sec}$. Table 6 summarizes the values for the diffusion coefficient of water at various relative humidity levels. Figure 15 shows the graphical presentation of the tablet diffusion coefficient and the relative humidity. It is evident that there is no trend in the data.

For the tablet, the average diffusion coefficient value was used in the shelf life computer program.

Equation (16) was used to compute $D$ for the film samples and the tablet. Figure 16 and Figure 17 demonstrate the same concept for the packaging materials as Figure 14 showed for the tablet comparison (see Appendices C and D). Again, the experimental and calculated moisture uptake profiles are very similar. Many of the points coincide graphically. These figures are shown below. Table 7 lists the diffusion coefficients of water for the PVC film sample and the Aclar film sample at two relative humidity ranges.

When a laminate is composed of two layers of thickness in series, $L_{1}$ and $L_{2}$, and two diffusion coefficients, $D_{1}$ and $D_{2}$, the effective diffusion coefficient, $D$, is given by the
following equation (Crank, 1975).

$$
\begin{equation*}
\left(L_{1} / D_{1}\right)+\left(L_{2} / D_{2}\right)=\left(L_{1}+L_{2}\right) / D \tag{18}
\end{equation*}
$$

This equation can also be written as shown in Eq. (19).

$$
\begin{equation*}
D=\left(L_{1}+L_{2}\right) /\left(\left(L_{1} / D_{1}\right)+\left(L_{2} / D_{2}\right)\right) \tag{19}
\end{equation*}
$$

The effective diffusion coefficient was used in the shelf life computer program and was calculated to be $2.0 \mathrm{E}-09 \mathrm{~cm}^{2} / \mathrm{sec}$.

Table 6. Diffusion coefficient of tablet at R.H. conditions.

| Relative Humidity (\%) | Diffusion Coefficient <br> $\left(\mathrm{cm}^{2} / \mathrm{sec}\right)$ |
| :---: | :---: |
| $0-11.50$ | $1.22 \mathrm{E} \mathrm{-06}$ |
| $36-40$ | $0.85 \mathrm{E}-06$ |
| $40.75-48.80$ | $0.603 \mathrm{E}-06$ |
| $60.70-66$ | $1.26 \mathrm{E}-06$ |
| $66-73.40$ | $1.62 \mathrm{E} \mathrm{-06}$ |
| $72.25-77.75$ | $1.27 \mathrm{E}-06$ |
| $77.90-82.45$ | $1.60 \mathrm{E}-06$ |
| $82.05-87.30$ | $0.996 \mathrm{E}-06$ |
| Average | $1.179 \mathrm{E}-06$ |
| Standard Deviation | $3.30 \mathrm{E} \mathrm{-07}$ |



Figure 15. Diffusion coefficient of Deltasone tablet over
R.H. ranges at $25.0^{\circ} \mathrm{C}$


Figure 16. Comparison of experimental and calculated $M_{t} / M_{0}$ for PVC film at 58.20-77\% R.H. and 25.0 ${ }^{\circ}$ C


Figure 17. Comparison of experimental and calculated $M_{c} / M_{0}$ for Aclar film at 43.50 - $58 \%$ R.H. and $25.0{ }^{\circ} \mathrm{C}$

Table 7. Diffusion coefficient of packaging materials at R.H. conditions

| PVC Film -7.5 mils |  |
| :---: | :---: |
| Relative Humidity (\%) | Diffusion Coefficient <br> $\left(\mathrm{Cm}^{2} / \mathrm{sec}\right)$ |
| $0-26.90$ | $5.58 \mathrm{E}-09$ |
| $58.20-77$ | $4.5 \mathrm{E} \mathrm{-09}$ |
| Average | $5.04 \mathrm{E}-09$ |
| Aclar Film -1.6 mils | $3.36 \mathrm{E}-10$ |
| $27.35-43.50$ | $7.03 \mathrm{E}-10$ |
| $43.50-58$ | $5.195 \mathrm{E}-10$ |
| Average |  |

## Sorption Isotherm Model for the Tablet

The GAB (Guggenheim-Anderson-de Boer) sorption isotherm model was used to fit the experimental isotherm data of the tablet obtained in the present study. The equation is given in Eq. (20) (Bizot, 1991).

$$
\begin{equation*}
W / W_{m}=C k A_{w} /\left(1-k A_{w}\right)\left(1-k A_{w}+C k A_{w}\right) \tag{20}
\end{equation*}
$$

$A_{w}$ is water activity, $W$ is water content on a dry basis, $W_{m}$ is water content corresponding to saturation of all primary adsorption sites by one water molecule (previously called the monolayer in BET theory), $C$ is the Guggenheim constant $=c$ 'exp
$\left(H_{1}-H_{m}\right) / R T, H_{q}$ is total heat of sorption of the multilayers (which is different from the heat of condensation of pure water), $H_{m}$ is total heat of sorption of the first layer on primary sites, $k$ is a factor correcting properties of the multilayer molecules with respect to the bulk liquid [k = $\left.k^{\prime} \exp \left(H_{1}-H_{q}\right) / R T\right]$, and $H_{1}$ is the heat of condensation of pure water vapor.

This GAB model has been reported as a very good model for fitting sorption isotherms over a range of water activities. It also provides a means to evaluate the amount of water tightly bound by the primary adsorption sites ( $W_{m}$ ).

Equation (20) can also be written in the following manner

$$
\begin{equation*}
A_{w} / W=\alpha A_{w}^{2}+\beta A_{w}+\gamma \tag{21}
\end{equation*}
$$

where

$$
\begin{align*}
\alpha & =k / W_{m}[1 / C-1]  \tag{22}\\
\beta & =1 / W_{m}[1-2 / C]  \tag{23}\\
\gamma & =1 / W_{m} C k \tag{24}
\end{align*}
$$

and a regression (quadratic) can be conducted on experimental numbers. From Eq. (23)

$$
\begin{equation*}
W_{m}=1 / \beta[1-2 / C] \tag{25}
\end{equation*}
$$

and combining Eq. (22) and Eq. (23) gives the following equation.

$$
\begin{equation*}
\alpha=k \beta /[1-2 / C] \quad[1 / C-1] \tag{26}
\end{equation*}
$$

Eq. (24) and Eq. (25) provided

$$
\begin{equation*}
\gamma=\beta /[1-2 / C] \quad C k \tag{27}
\end{equation*}
$$

which simplified to Eq. (28).

$$
\begin{equation*}
k=\beta / \gamma[C-2] \tag{28}
\end{equation*}
$$

From Eq. (26) and Eq. (28), Eq. (29) is defined.

$$
\begin{equation*}
\alpha=\beta^{2}(1-C) / \gamma(C-2)(C-2) \tag{29}
\end{equation*}
$$

The constants (GAB) were calculated to be

$$
\begin{aligned}
& \alpha=-1.79 \\
& \beta=1.922 \\
& \gamma=0.064
\end{aligned}
$$

and can be used in the above computations. The constants ( $\alpha$, $\beta$, and $\gamma$ ) were figured using matrices which consisted of combinations of $X, X^{2}, X^{3}, X^{4}, Y, X Y, X^{2} Y$, and $N$. $X$ was the summation of experimental $A_{w}, Y$ was the summation of experimental $A_{W} / E M C$, and $N$ was the number of experimental points. A plot of the experimental moisture sorption isotherm against the GAB model produced a very good fit of the two curves. This plot is found in Figure 18.

The quality of the fit can be analyzed from the result of


Figure 18. Plot of experimental moisture sorption isotherm and calculated GAB isotherm of 20 mg Deltasone tablet at $25.0^{\circ} \mathrm{C}$
the relative percent root mean square (\% RMS)

$$
\begin{equation*}
\text { of RMS }=\sqrt{ }\left[\Sigma\left(W_{i}-W_{i}^{*} / W_{i}\right)^{2} / N\right] \times 100 \tag{30}
\end{equation*}
$$

where $N$ is the number of experimental points, $W_{i}$ is the experimental water content, and $W_{i}$ is the calculated water
content (Bizot, 1991). The RMS was calculated to be 11.11\%, which verifies the strength of the fit for the experimental and calculated data.

## Calculations of Package / Product Dimensions

There are four additional parameters of the packaging material and the pharmaceutical product which must be determined. They include the surface area of the tablet, the volume of the tablet, the surface area of the blister package, and the inner volume of the blister package. The surface area of the Deltasone tablet ( $A_{T}$ ) is found by

$$
\begin{equation*}
A_{T}=2 \pi R_{T}^{2} \tag{31}
\end{equation*}
$$

where $R_{T}$ is the radius of the tablet. Likewise, the volume of the pharmaceutical tablet $\left(V_{T}\right)$ is deduced from the following equation.

$$
\begin{equation*}
V_{T}=\left(\pi R_{T}{ }^{2}\right) \quad\left(T_{T}\right) \tag{32}
\end{equation*}
$$

$T_{T}$ is the tablet thickness. The surface area of the blister package ( $A_{p}$ ) is as follows

$$
\begin{equation*}
A_{p}=\pi R_{p}^{2}+2 \pi R_{p} T_{p} \tag{33}
\end{equation*}
$$

where $R_{p}$ is the radius of the blister, and $T_{p}$ is the height of
the blister package. Lastly, the inner volume of the blister package ( $V_{p}$ ) has the following calculation.

$$
\begin{equation*}
V_{p}=\pi R_{p}^{2} T_{p} \tag{34}
\end{equation*}
$$

For this project, the permeable blister package area did not include the aluminum foil backing, as it would be impermeable to moisture.

## Other Parameters for Computer Program

The absolute humidity (A.H.) is a necessary component for the finite difference computer model since the driving of water is based on the absolute concentration of water through the system. The absolute humidity can be located from a psychrometric chart at saturation temperature.

$$
\begin{equation*}
C_{\text {sat }}=\text { A.H. } / 1.5829 \mathrm{~T} \tag{35}
\end{equation*}
$$

$C_{\text {sat }}$ is the concentration of water in the air at saturation (gram / ml) and $T$ is in ${ }^{\circ} R$.

Henry's Law Constant needed to be determined as well using different units as those described by Eq. (9) with the following equation.

$$
\begin{equation*}
C_{L E}=H_{L} C_{E} \tag{36}
\end{equation*}
$$

 and is dependent on packaging material and temperature. $C_{L E}$ is the concentration of absorbed water vapor on the outer surface of the package (constant). $C_{E}$ is the concentration of water vapor outside the package (constant).

Table 8 lists all of the experimental values which were used in this finite difference simulation computer model.

## Moisture Optake of Blister Package with Product

Over a several week period, the water uptake of the total 10 cavity blister package with tablets was monitored. Five samples were contained in an $80 \%$ R.H. condition, and five were also stored in a $90 \%$ R.H. condition at $22.2^{\circ} \mathrm{C}$. Each container also held one empty 10 cavity blister package in order to factor in the moisture sorption of the packaging material alone. The percent moisture content of an individual tablet was calculated with the following equation

$$
\begin{equation*}
\text { M.C. }=[((\mathrm{a}-\mathrm{b}) / 10) /(\mathrm{W})] * 100 \tag{37}
\end{equation*}
$$

where $W$ is the dry weight of the tablet, "a" is the weight of the filled blister package at any timepoint, and "b" is the weight of the empty blister package at the same timepoint. The results of this portion of the study are presented in Table 9 (80\% R.H. level) and Table 10 (90\% R.H. level), respectively. Graphical presentations are shown in Figures

Table 8. Values for use in simulation model

| Variable | Value | Reference |
| :---: | :---: | :---: |
| Temperature (T) | $25.0^{\circ}$ Celsius | Given |
| Storage Relative Humidity (R.H.) | 80\%, 90\% | Given |
| $\begin{gathered} \text { Absolute Humidity } \\ \text { (A.H.) } \\ \hline \end{gathered}$ | $\begin{gathered} 0.0163,0.0183 \\ \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / \mathrm{g} \text { Air } \end{gathered}$ | Equation (35) |
| Package Diffusion Coefficient ( $\mathrm{D}_{1}$ ) | $\begin{gathered} 0.02 \mathrm{E}-07 \\ \mathrm{~cm}^{2} / \mathrm{sec} . \\ \hline \end{gathered}$ | Equation (19) |
| Henry's Law Constant ( $H_{1}$ ) | 125.12 | Equation (36) |
| Package Thickness | 0.023, 0.0114 cm | Measured |
| $\begin{gathered} \text { Blister Surface } \\ \text { Area }\left(A_{\rho}\right) \\ \hline \end{gathered}$ | $3.78 \mathrm{~cm}^{2}$ | Equation (33) |
| $\begin{aligned} & \text { Blister volume } \\ & \left(V_{p}\right) \end{aligned}$ | $0.80 \mathrm{~cm}^{3}$ | Equation (34) |
| Number of Package Layers (L) | 5 | Selected |
| Tablet Diffusion Coefficient ( $\mathrm{D}_{\mathrm{p}}$ ) | $\begin{gathered} 0.1179 \mathrm{E} \mathrm{-05} \\ \mathrm{~cm}^{2} / \mathrm{sec} . \end{gathered}$ | Equation (16) |
| Initial Moisture Content (IMC) | $\frac{0.0001 \mathrm{a}_{2} \mathrm{H}_{2} \mathrm{O}}{100 \mathrm{~g} \mathrm{dry} \text { product }}$ | Estimated |
| Critical Moisture Content (CMC) | $\frac{2.0 \mathrm{~g} \mathrm{H}_{2} \mathrm{O}}{100 \mathrm{~g} \mathrm{dry} \mathrm{product}}$ | Selected |
| Dry Tablet Weight (W) | 0.4077 g | Measured |
| Tablet Radius ( $\mathrm{R}_{\mathrm{T}}$ ) | 0.50 cm | Measured |
| $\begin{gathered} \text { Tablet Thickness } \\ \left(\mathrm{T}_{\mathrm{J}}\right) \end{gathered}$ | 0.392 cm | Measured |
| G.A.B. Constant $\alpha$ | -1.79 | Equation (22) |
| G.A.B. Constant $\beta$ | 1.922 | Equation (23) |
| G.A.B. Constant $\gamma$ | 0.064 | Equation (24) |
| Number of Shells <br> (U) | 5 | Selected |



19 and 20.
Tables 9 and 10 give the moisture gain for each of the five sample blister packages and the empty control sample over time for each environmental condition. The average moisture gain and standard deviation of these packages are also provided. The average moisture content per tablet calculated using Eq. (37) is tabulated and plotted. It is apparent from the standard deviation that there is variability among the samples for moisture uptake. All blister packs did show a steady increase in mass over the duration.

Figure 21 and Figure 22 compare the experimental packaged tablet moisture content curves with the curves generated by the shelf life simulation model using a finite difference method at 80 and $90 \%$ R.H., respectively. For these figures, the blister laminate thickness used in the computer program was 9.1 mils, which was the thickness of the flat sheet material. In addition, the program was tested with a package thickness of 4.5 mils, which was the measured value for the formed blister. The comparative results are available in Figures 23 and 24. With the decrease in thickness, there were significant variations between the experimental and calculated data.
Table 9. Moisture gain of complete blister package with tablets at

$$
0
$$




AVERAGE
AVERAGE
$\underset{5}{\text { SAMPLE }}$
 $\circ 0_{0}^{\circ} 0^{\circ} 0000$




## 0

0.0062 $\circ 0^{\circ} 0^{\circ} 0^{\circ} 0^{\circ} 0^{\circ}$


| - ${ }^{\circ}$ |
| :---: |
|  |  |



Figure 19. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and 80\% R.H.
Table 10. Moisture gain of complete blister package with tablets at 90\% R.H. and 22.2 deg. C
Moisture Gain of 10 Cavity Blister Samples with 10 Tablets (grams)




|  | Moisture Gain of 10 Cavity Blister Samples with 10 Tablets (grams) |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & \text { TIME } \\ & \text { (weeks) } \end{aligned}$ | EMPTY <br> (Control) | $\underset{1}{\text { SAMPLE }}$ | $\begin{gathered} \text { SAMPLE } \\ 2 \end{gathered}$ | $\underset{3}{\text { SAMPLE }}$ | $\begin{gathered} \text { SAMPLE } \\ 4 \end{gathered}$ | $\begin{gathered} \text { SAMPLE } \\ 5 \end{gathered}$ | AVERAGE | STD. DEV. | AVERAGE MOISTURE CONTENT PER TABLET (\%) |
| 0 |  | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 |
| 1 |  | 0.0074 | 0.0124 | 0.0072 | 0.0094 | 0.0076 | 0.0088 | 0.001964 | 0.215845 |
| 2 |  | 0.0074 | 0.0163 | 0.0092 | 0.0204 | 0.0102 | 0.0127 | 0.004875 | 0.311504 |
| 3 | 0 | 0.0109 | 0.0202 | 0.0133 | 0.023 | 0.015 | 0.01648 | 0.004467 | 0.404219 |
| 4.29 | 0.001 | 0.0265 | 0.0188 | 0.0178 | 0.0177 | 0.0153 | 0.01922 | 0.003818 | 0.446897 |
| 6.57 | 0.0032 | 0.0244 | 0.0304 | 0.035 | 0.0462 | 0.0303 | 0.03326 | 0.007293 | 0.737307 |
| 7.57 | 0.006 | 0.0324 | 0.0365 | 0.0366 | 0.0385 | 0.0385 | 0.0365 | 0.002228 | 0.748099 |
| 9.57 | 0.0076 | 0.0356 | 0.0515 | 0.0364 | 0.0512 | 0.0404 | 0.04302 | 0.006994 | 0.868776 |
| 13.86 | 0.0044 | 0.0403 | 0.0407 | 0.0611 | 0.0488 | 0.0558 | 0.04934 | 0.008206 | 1.102281 |
| 43.57 | 0.0376 | 0.1136 | 0.098 | 0.0733 | 0.0827 | 0.0714 | 0.0878 | 0.015968 | 1.231298 |



Figure 20. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and 90\% R.H.


Figure 21. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and 80\% R.H. for experimental and computer program data


Figure 22. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and $90 \%$ R.H. for experimental and computer program data


Figure 23. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and $80 \%$ R.H. for experimental and computer program data ( 4.5 mils thickness)


Figure 24. Moisture content of tablets in blisters at $22.2^{\circ} \mathrm{C}$ and 90\% R.H. for experimental and computer program data ( 4.5 mils thickness)

## ERROR ANALY8I8

Throughout the process of performing this research-based project, there were many opportunities to introduce both operator and machine error. Errors are possible even in the most controlled situations. For example, the relative humidity produced within the hangdown tube of the electrobalance, where the sample was located, was dependent on both the humidity sensors (hygrosensors) and the hygrometer unit used. The hygrometer and hygrosensors had been calibrated, but there may have been some error of approximately +/- 1\%.

Secondly, there were a few instances when the light in the chamber where the hangdown tube was located was left on causing a potential temperature fluctuation of $+/-1-2{ }^{\circ} \mathrm{C}$. This increased heat in the chamber could have resulted in some changes in the tablet weight gain during the creation of the sorption isotherm. The extra heat in the chamber decreased the relative humidity for a short period of time.

Another error in relative humidity could have occurred inside of the five gallon buckets containing the salt solutions. Therefore, there could be a greater or lesser weight gain over time due to this inaccuracy of about 4-5\%. Also, temperature variations could have existed in the storage
location of $+/-2-3^{\circ} \mathrm{C}$.
It is uncertain whether or not the Deltasone pharmaceutical tablet was thoroughly dried to 0\% moisture content at the onset of this experiment. However, initial desorption studies showed that the product had reached equilibrium during the nitrogen flush.

Lastly, calibration of the electrobalance could have been inaccurately performed with the calibration weights. This calibration occurs before the sample product is put into the hangdown tube. Calibration weights are placed in the sample dish for a specified period of time for the process to take place.

## CONCLUEIONS

## Comparison Between Calculated Data and Validation Experiment


#### Abstract

A finite difference computer program for shelf life simulation calculated the shelf life of the 20 mg Deltasone tablet packaged in such a way as described in this research project, using the values in Table 8. This simulation program estimated the shelf life to be 10,010 hours (417 days) under the conditions of $25.0^{\circ} \mathrm{C}$ and $90 \%$ R.H. for a package thickness of 9.1 mils. This translates into a shelf life value of nearly 60 weeks. The finite difference program showed that at $25.0^{\circ} \mathrm{C}$ and $80 \%$ R.H., the product would not reach the critical moisture content of $2.0 \mathrm{~g} \mathrm{H} \mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry product from an initial moisture content of $0.0001 \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / 100$ $g$ dry product. This occurs since the equilibrium moisture content at $80 \%$ R.H. is less than $2.0 \mathrm{~g} \mathrm{H} \mathrm{H} / 100 \mathrm{~g}$ dry product from the sorption isotherm in Figure 18. For this case, the maximum value for the moisture content came out to be 1.5477 g $\mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry product at 9,200 hours (383 days). Through several trials using the model, it was evident that the value of the dimensionless constants, $Q$ and $G$, played a key role in the stability of the computational process (see Appendix A). When compared to the experimental blister packages which


were stored at $80 \%$ R.H., the program agreed quite well with the data, when the packaging film thickness used was 9.1 mils. For example, when the EMC reached $0.6412 \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry product, the shelf life was calculated to be 6.6 weeks from the finite difference program. The experimental data of the packaged product found the shelf life to be 6.6 weeks at a moisture content of $0.64 \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry product. This can be seen in Figure 21. In addition, the $90 \%$ R.H. condition had satisfactory agreement with the shelf life simulation model, when using a value for the package thickness of 9.1 mils. This program computed a shelf life of 13.9 weeks at an EMC of $1.1321 \mathrm{~g} \mathrm{H}_{2} \mathrm{O} / 100 \mathrm{~g}$ dry product. Experimental data at 90\% R.H. revealed a shelf life of 13.9 weeks at $1.1023 \mathrm{~g} \mathrm{H} \mathrm{H} / 100 \mathrm{~g}$ dry product. Also, this is expressed in Figure 22. The input/output results of the computer program with all of the data can be found in Appendix A.

It was found that the formed blister structure of PVC and Aclar had a package thickness close to 4.5 mils, as seen in Figure 1. An assumption was made that the two laminated materials are proportionally formed during the blister manufacturing process in relation to the original unformed film sheet ( 9.1 mils ). At this value of 4.5 mils , the finite difference program computed changes in moisture content over time which far exceeded the experimental data. This deviation became more pronounced with an increase in time. There could be several reasons for these results. The relative humidity in the buckets could have been decreasing over time causing
less moisture to be gained in later weeks. On the other hand, this computer program for the prediction of shelf life may be overestimating the moisture content of this product. In addition, this program was designed for single layer packaging materials.

## RECOMMENDATIONS FOR FUTURE WORK

A recommendation for future work in this area of mathematical modeling and shelf life prediction for packaged food and pharmaceutical products would include some research into a program which could evaluate multi-layer packaging films. In addition, another interesting project for further development would be an expansion of the shelf life program using the finite difference method to analyze other packaging containers. Currently, the focus of this model is blister packaging, but could possibly also involve bottles with closures and bulk materials, such as boxes or lined fiber drums. This type of predictive model could have value for the pharmaceutical industry as various package configurations need to be considered. Ideally, a program with the capabilities to advise on product quantity per container based on product size, available headspace and product characteristics would be a useful tool.

Another addition to a shelf life model might be the incorporation of oxygen transmission rates through a package component, which can also cause product degradation. A program which integrates all environmental conditions surrounding a product/package system would have great benefit.

APPENDICES

APPENDIX A

## APPENDIX A

## Program stability Given $Q$ Value, Input/Output Data sheets

This finite difference computer program uses a number of dimensionless constants as part of the computation of the shelf life. The dimensionless constant, $Q$, was of particular interest while running various trials with this model. According to Kim (1992), Q is used to solve the diffusion equation of the packaging material to moisture. In any application of this program, $Q$ must be less than 0.5 in order to avoid a negative concentration value using (1-2Q). $Q$ is also dependent on the geometry of the product under investigation.

With the data generated for this project, $Q$ needed to be determined by trial and error as to the optimum value for use. It was found that an appropriate $Q$ constant for the data was between 0.001 and 0.00142 . It was apparent that as the critical moisture content increased, $Q$ needed to decrease. In addition, $Q$ affects $G$, another dimensionless constant, which must be less than 0.3 for purposes of numerical stability (Kim, 1992).

All input and output data used from the computer program are found in the following section.

## Computer Program Input/Output Data

```
All data are checked successfully !!!
Re-check all data entered
Temperature of storage environment incelsius =25.00
Relative humidity of storage environment in : =80.00
Absolute humidity of storage environment ingH20/gAix =.0163
Diffusion coefficient of packaging materialin 10^-7 cm^2/sec =0.020
Henry constant of packaging material in(gH20/cm^3 PKG)/(gH20/cm^^ Air) - 125.12
    000
Thickness of packaging material in cm = 0.01140
Surface area of packaging material in cm^2 - 3.78000
Volume of packaging material in cm^3 = 0.80000
Diffusion coefficient of product in 10^-5cm^2/sec = 0.11790
Initial moisture content in gH2O/100g dryproduct =0.00
Critical moisture content in gH2O/100g dryproduct =2.00
Dry weight of product in g = 0.40770
Chemical reaction rate = 0.0
Chemical reaction order = 0.0
Aw/M=-.1790E+01 Aw^2 + 0.1922E+01 Aw+ 0.6400E-01
Radius of product in cm = 0.50000
Thickness of product (Only Plate shape) incm = 0.39200
    Hit any key to continue.....
INITIAL CONCENTRATION
Concentration of outside environment (CE) - 0.01534 g/L
Concentration of outside surface of PKG(CLE) = 1.91945 g/L
Concentration of inside surface of PKG(CLH) = 0.00002 g/L
Concentration of headspace (CH) = 0.00000 g/L
Concentration of outside surface of product (CRH) = 0.00132 g/L
    DIMENSSIONLESS CONSTANT
---------------------------------------------------------------------------------
Q=0.1420E-02
G-0.1520E-02
A1=0.1822E-04
B1=0.1902E-03
S-0.1981E+01
X=0.9000E+03
    = }
    ---------------------------------------------------------------------------------
                            Hit any key to continue
        Enter the number of time to calculateconcentrations at once.
            <NOTICE !!! It must be over 200 and be times of 200>
```

|  | (Plate Shape) <br> Each step is 152000 . steps ( 83.6379 hrs ) < of the divided shell of product is |  |  |  |  | 5 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| CLE | CL1 | CL2 | CL3 | CL4 |  | CH | Meq |
| CRH | CR1 | CR2 | CR3 | CR4 | CRC | GAIN | TIME (hrs) |
| 1.9194 | 1.6483 | 1.3771 | 1.1060 | 0.8349 | 0.5639 | 0.2930 | 0.0222 |
| 0.0002 | 0.1134 |  |  |  |  |  |  |
| 1.5014 | 1.4755 | 1.4560 | 1.4430 | 1.4366 | 1.4366 | 0.1100 | 83.6379 |
| 1.9194 | 1.6535 | 1.3877 | 1.1219 | 0.8562 | 0.5906 | 0.3252 | 0.0600 |
| 0.0005 | 0.2253 |  |  |  |  |  |  |
| 2.9841 | 2.9587 | 2.9397 | 2.9270 | 2.9206 | 2.9206 | 0.2220 | 167.2758 |
| 1.9194 | 1.6635 | 1.4076 | 1.1518 | 0.8962 | 0.6409 | 0.3858 | 0.1312 |
| 0.0010 | 0.3340 |  |  |  |  |  |  |
| 4.4225 | 4.3981 | 4.3799 | 4.3677 | 4.3616 | 4.3616 | 0.3307 | 250.9138 |
| 1.9194 | 1.6827 | 1.4460 | 1.2096 | 0.9736 | 0.7380 | 0.5030 | 0.2686 |
| 0.0021 | 0.4361 |  |  |  |  |  |  |
| 5.7747 | 5.7523 | 5.7355 | 5.7243 | 5.7186 | 5.7186 | 0.4331 | 334.5517 |
| 1.9194 | 1.7114 | 1.5036 | 1.2960 | 1.0888 | 0.8822 | 0.6763 | 0.4713 |
| 0.0038 | 0.5274 |  |  |  |  |  |  |
| 6.9836 | 6.9640 | 6.9493 | 6.9395 | 6.9346 | 6.9346 | 0.5248 | 418.1896 |
| 1.9194 | 1.7402 | 1.5612 | 1.3823 | 1.2039 | 1.0259 | 0.8485 | 0.6719 |
| 0.0054 | 0.6063 |  |  |  |  |  |  |
| 8.0291 | 8.0122 | 7.9996 | 7.9911 | 7.9869 | 7.9869 | 0.6041 | 501.8275 |
| 1.9194 | 1.7638 | 1.6083 | 1.4530 | 1.2980 | 1.1434 | 0.9892 | 0.8356 |
| 0.0067 | 0.6746 |  |  |  |  |  |  |
| 8.9334 | 8.9187 | 8.9077 | 8.9004 | 8.8967 | 8.8967 | 0.6727 | 585.4654 |
| 1.9194 | 1.7824 | 1.6455 | 1.5087 | 1.3721 | 1.2359 | 1.1000 | 0.9646 |
| 0.0077 | 0.7344 |  |  |  |  |  |  |
| 9.7256 | 9.7127 | 9.7030 | 9.6965 | 9.6933 | 9.6933 | 0.7327 | 669.1033 |
| 1.9194 | 1.7972 | 1.6750 | 1.5530 | 1.4311 | 1.3095 | 1.1881 | 1.0672 |
| 0.0085 | 0.7876 |  |  |  |  |  |  |
| 10.4292 | 10.4177 | 10.4090 | 10.4032 | 10.4003 | 10.4003 | 0.7860 | 752.7413 |
| 1.9194 | 1.8092 | 1.6990 | 1.5889 | 1.4789 | 1.3692 | 1.2597 | 1.1505 |
| 0.0092 | 0.8353 |  |  |  |  |  |  |
| 11.0615 | 11.0510 | 11.0432 | 11.0380 | 11.0354 | 11.0354 | 0.8339 | 836.3792 |
| 1.9194 | 1.8191 | 1.7188 | 1.6186 | 1.5185 | 1.4186 | 1.3189 | 1.2195 |
| 0.0097 | 0.8786 |  |  |  |  |  |  |
| 11.6351 | 11.6256 | 11.6184 | 11.6137 | 11.6113 | 11.6113 | 0.8774 | 920.0171 |
| 1.9194 | 1.8275 | 1.7355 | 1.6437 | 1.5519 | 1.4603 | 1.3688 | 1.2776 |
| 0.0102 | 0.9182 |  |  |  |  |  |  |
| 12.1596 | 12.1509 | 12.1443 | 12.1399 | 12.1378 | 12.1378 | 0.9171 | 1003.6550 |
| 1.9194 | 1.8346 | 1.7498 | 1.6651 | 1.5804 | 1.4959 | 1.4115 | 1.3273 |
| 0.0106 | 0.9547 |  |  |  |  |  |  |
| 12.6424 | 12.6343 | 12.6283 | 12.6242 | 12.6222 | 12.6222 | 0.9536 | 1087.2930 |
| 1.9194 | 1.8408 | 1.7622 | 1.6836 | 1.6051 | 1.5267 | 1.4485 | 1.3704 |
| 0.0110 | 0.9884 |  |  |  |  |  |  |
| 13.0892 | 13.0817 | 13.0761 | 13.0724 | 13.0705 | 13.0705 | 0.9874 | 1170.9308 |
| 1.9194 | 1.8462 | 1.7730 | 1.6998 | 1.6267 | 1.5537 | 1.4808 | 1.4081 |
| 0.0113 | 1.0198 |  |  |  |  |  |  |
| 13.5046 | 13.4976 | 13.4924 | 13.4889 | 13.4872 | 13.4872 | 1.0189 | 1254.5687 |
| 1.9194 | 1.8510 | 1.7825 | 1.7141 | 1.6458 | 1.5775 | 1.5094 | 1.4414 |
| 0.0115 | 1.0491 |  |  |  |  |  |  |
| 13.8924 | 13.8859 | 13.8810 | 13.8778 | 13.8762 | 13.8762 | 1.0482 | 1338.2067 |
| 1.9194 | 1.8552 | 1.7911 | 1.7269 | 1.6628 | 1.5988 | 1.5349 | 1.4710 |
| 0.0118 | 1.0765 |  |  |  |  |  |  |
| 14.2557 | 14.2496 | 14.2450 | 14.2420 | 14.2405 | 14.2405 | 1.0757 | 1421.8446 |
| 1.9194 | 1.8591 | 1.7987 | 1.7384 | 1.6781 | 1.6178 | 1.5577 | 1.4977 |
| 0.0120 | 1.1023 |  |  |  |  |  |  |


| 14.5971 | 14.5913 | 14.5870 | 14.5841 | 14.5827 | 14.5827 | 1.1015 | 1505.4825 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.9194 | 1.8625 | 1.8056 | 1.7487 | 1.6918 | 1.6351 | 1.5783 | 1.5217 |
| 0.0122 | 1.1266 |  |  |  |  |  |  |
| 14.9187 | 14.9132 | 14.9092 | 14.9065 | 14.9051 | 14.9051 | 1.1259 | 1589.1204 |
| 1.9194 | 1.8656 | 1.8118 | 1.7581 | 1.7043 | 1.6507 | 1.5971 | 1.5435 |
| 0.0123 | 1.1495 |  |  |  |  |  |  |
| 15.2223 | 15.2172 | 15.2134 | 15.2108 | 15.2095 | 15.2095 | 1.1488 | 1672.7583 |
| 1.9194 | 1.8685 | 1.8175 | 1.7666 | 1.7157 | 1.6649 | 1.6141 | 1.5634 |
| 0.0125 | 1.1712 |  |  |  |  |  |  |
| 15.5097 | 15.5048 | 15.5012 | 15.4988 | 15.4976 | 15.4976 | 1.1706 | 1756.3962 |
| 1.9194 | 1.8711 | 1.8228 | 1.7745 | 1.7262 | 1.6780 | 1.6298 | 1.5817 |
| 0.0126 | 1.1918 |  |  |  |  |  |  |
| 15.7822 | 15.7775 | 15.7741 | 15.7718 | 15.7706 | 15.7706 | 1.1912 | 1840.0342 |
| 1.9194 | 1.8735 | 1.8276 | 1.7817 | 1.7358 | 1.6900 | 1.6442 | 1.5985 |
| 0.0128 | 1.2113 |  |  |  |  |  |  |
| 16.0409 | 16.0365 | 16.0333 | 16.0311 | 16.0300 | 16.0300 | 1.2108 | 1923.6721 |
| 1.9194 | 1.8757 | 1.8320 | 1.7883 | 1.7447 | 1.7010 | 1.6575 | 1.6139 |
| 0.0129 | 1.2299 |  |  |  |  |  |  |
| 16.2870 | 16.2829 | 16.2798 | 16.2777 | 16.2766 | 16.2766 | 1.2294 | 2007.3101 |
| 1.9194 | 1.8778 | 1.8361 | 1.7945 | 1.7529 | 1.7113 | 1.6698 | 1.6283 |
| 0.0130 | 1.2476 |  |  |  |  |  |  |
| 16.5215 | 16.5175 | 16.5146 | 16.5126 | 16.5116 | 16.5116 | 1.2471 | 2090.9480 |
| 1.9194 | 1.8797 | 1.8399 | 1.8002 | 1.7605 | 1.7208 | 1.6812 | 1.6416 |
| 0.0131 | 1.2645 |  |  |  |  |  |  |
| 16.7451 | 16.7413 | 16.7385 | 16.7366 | 16.7357 | 16.7357 | 1.2640 | 2174.5859 |
| 1.9194 | 1.8815 | 1.8435 | 1.8055 | 1.7676 | 1.7297 | 1.6918 | 1.6540 |
| 0.0132 | 1.2806 |  |  |  |  |  |  |
| 16.9587 | 16.9550 | 16.9523 | 16.9505 | 16.9496 | 16.9496 | 1.2802 | 2258.2236 |
| 1.9194 | 1.8831 | 1.8468 | 1.8105 | 1.7742 | 1.7380 | 1.7018 | 1.6656 |
| 0.0133 | 1.2961 |  |  |  |  |  |  |
| 17.1628 | 17.1593 | 17.1567 | 17.1550 | 17.1542 | 17.1542 | 1.2956 | 2341.8616 |
| 1.9194 | 1.8847 | 1.8499 | 1.8152 | 1.7804 | 1.7457 | 1.7111 | 1.6764 |
| 0.0134 | 1.3108 |  |  |  |  |  |  |
| 17.3582 | 17.3548 | 17.3524 | 17.3507 | 17.3499 | 17.3499 | 1.3104 | 2425.4995 |
| 1.9194 | 1.8861 | 1.8528 | 1.8195 | 1.7863 | 1.7530 | 1.7198 | 1.6866 |
| 0.0135 | 1.3249 |  |  |  |  |  |  |
| 17.5453 | 17.5421 | 17.5397 | 17.5381 | 17.5373 | 17.5373 | 1.3245 | 2509.1375 |
| 1.9194 | 1.8875 | 1.8556 | 1.8236 | 1.7917 | 1.7598 | 1.7280 | 1.6962 |
| 0.0136 | 1.3385 |  |  |  |  |  |  |
| 17.7246 | 17.7216 | 17.7193 | 17.7178 | 17.7170 | 17.7170 | 1.3381 | 2592.7754 |
| 1.9194 | 1.8888 | 1.8581 | 1.8275 | 1.7969 | 1.7663 | 1.7357 | 1.7052 |
| 0.0136 | 1.3515 |  |  |  |  |  |  |
| 17.8967 | 17.8938 | 17.8916 | 17.8902 | 17.8894 | 17.8894 | 1.3511 | 2676.4133 |
| 1.9194 | 1.8900 | 1.8606 | 1.8311 | 1.8017 | 1.7723 | 1.7430 | 1.7136 |
| 0.0137 | 1.3640 |  |  |  |  |  |  |
| 18.0620 | 18.0592 | 18.0571 | 18.0557 | 18.0550 | 18.0550 | 1.3636 | 2760.0510 |
| 1.9194 | 1.8911 | 1.8629 | 1.8346 | 1.8063 | 1.7780 | 1.7498 | 1.7216 |
| 0.0138 | 1.3759 |  |  |  |  |  |  |
| 18.2208 | 18.2181 | 18.2161 | 18.2147 | 18.2140 | 18.2140 | 1.3756 | 2843.6892 |
| 1.9194 | 1.8922 | 1.8650 | 1.8378 | 1.8106 | 1.7835 | 1.7563 | 1.7292 |
| 0.0138 | 1.3875 |  |  |  |  |  |  |
| 18.3734 | 18.3708 | 18.3689 | 18.3676 | 18.3669 | 18.3669 | 1.3871 | 2927.3269 |
| 1.9194 | 1.8933 | 1.8671 | 1.8409 | 1.8147 | 1.7886 | 1.7625 | 1.7364 |
| 0.0139 | 1.3986 |  |  |  |  |  |  |
| 18.5203 | 18.5178 | 18.5159 | 18.5147 | 18.5141 | 18.5141 | 1.3982 | 3010.9651 |
| 1.9194 | 1.8942 | 1.8690 | 1.8438 | 1.8186 | 1.7934 | 1.7683 | 1.7432 |
| 0.0139 | 1.4092 |  |  |  |  |  |  |
| 18.6617 | 18.6593 | 18.6575 | 18.6563 | 18.6557 | 18.6557 | 1.4089 | 3094.6028 |
| 1.9194 | 1.8952 | 1.8709 | 1.8466 | 1.8223 | 1.7981 | 1.7738 | 1.7496 |
| 0.0140 | 1.4195 |  |  |  |  |  |  |


| 18.7979 | 18.7956 | 18.7938 | 18.7927 | 18.7921 | 18.7921 | 1.4192 | 3178.2407 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.9194 | 1.8960 | 1.8726 | 1.8492 | 1.8258 | 1.8025 | 1.7791 | 1.7558 |
| 0.0140 | 1.4294 |  |  |  |  |  |  |
| 18.9291 | 18.9269 | 18.9252 | 18.9241 | 18.9235 | 18.9235 | 1.4291 | 3261.8787 |
| 1.9194 | 1.8969 | 1.8743 | 1.8517 | 1.8292 | 1.8066 | 1.7841 | 1.7616 |
| 0.0141 | 1.4390 |  |  |  |  |  |  |
| 19.0557 | 19.0535 | 19.0519 | 19.0508 | 19.0503 | 19.0503 | 1.4387 | 3345.5166 |
| 1.9194 | 1.8977 | 1.8759 | 1.8541 | 1.8323 | 1.8106 | 1.7889 | 1.7672 |
| 0.0141 | 1.4482 |  |  |  |  |  |  |
| 19.1777 | 19.1756 | 19.1741 | 19.1730 | 19.1725 | 19.1725 | 1.4479 | 3429.1545 |
| 1.9194 | 1.8984 | 1.8774 | 1.8564 | 1.8354 | 1.8144 | 1.7934 | 1.7725 |
| 0.0142 | 1.4571 |  |  |  |  |  |  |
| 19.2955 | 19.2935 | 19.2920 | 19.2910 | 19.2905 | 19.2905 | 1.4568 | 3512.7925 |
| 1.9194 | 1.8991 | 1.8788 | 1.8586 | 1.8383 | 1.8180 | 1.7978 | 1.7775 |
| 0.0142 | 1.4657 |  |  |  |  |  |  |
| 19.4092 | 19.4073 | 19.4058 | 19.4049 | 19.4044 | 19.4044 | 1.4654 | 3596.4302 |
| 1.9194 | 1.8998 | 1.8802 | 1.8606 | 1.8410 | 1.8215 | 1.8019 | 1.7824 |
| 0.0142 | 1.4740 |  |  |  |  |  |  |
| 19.5190 | 19.5172 | 19.5158 | 19.5148 | 19.5144 | 19.5144 | 1.4737 | 3680.0684 |
| 1.9194 | 1.9005 | 1.8816 | 1.8626 | 1.8437 | 1.8248 | 1.8059 | 1.7870 |
| 0.0143 | 1.4820 |  |  |  |  |  |  |
| 19.6252 | 19.6233 | 19.6220 | 19.6211 | 19.6206 | 19.6206 | 1.4818 | 3763.7061 |
| 1.9194 | 1.9011 | 1.8828 | 1.8645 | 1.8462 | 1.8279 | 1.8096 | 1.7914 |
| 0.0143 | 1.4897 |  |  |  |  |  |  |
| 19.7277 | 19.7260 | 19.7247 | 19.7238 | 19.7233 | 19.7233 | 1.4895 | 3847.3442 |
| 1.9194 | 1.9017 | 1.8840 | 1.8663 | 1.8486 | 1.8309 | 1.8133 | 1.7956 |
| 0.0144 | 1.4972 |  |  |  |  |  |  |
| 19.8269 | 19.8252 | 19.8239 | 19.8231 | 19.8227 | 19.8227 | 1.4970 | 3930.9819 |
| 1.9194 | 1.9023 | 1.8852 | 1.8681 | 1.8509 | 1.8338 | 1.8167 | 1.7997 |
| 0.0144 | 1.5045 |  |  |  |  |  |  |
| 19.9228 | 19.9211 | 19.9199 | 19.9191 | 19.9187 | 19.9187 | 1.5043 | 4014.6201 |
| 1.9194 | 1.9029 | 1.8863 | 1.8697 | 1.8532 | 1.8366 | 1.8201 | 1.8036 |
| 0.0144 | 1.5115 |  |  |  |  |  |  |
| 20.0156 | 20.0140 | 20.0128 | 20.0120 | 20.0116 | 20.0116 | 1.5113 | 4098.2578 |
| 1.9194 | 1.9034 | 1.8874 | 1.8713 | 1.8553 | 1.8393 | 1.8233 | 1.8073 |
| 0.0144 | 1.5183 |  |  |  |  |  |  |
| 20.1054 | 20.1038 | 20.1027 | 20.1019 | 20.1015 | 20.1015 | 1.5181 | 4181.8960 |
| 1.9194 | 1.9039 | 1.8884 | 1.8729 | 1.8573 | 1.8418 | 1.8263 | 1.8109 |
| 0.0145 | 1.5248 |  |  |  |  |  |  |
| 20.1923 | 20.1908 | 20.1897 | 20.1889 | 20.1886 | 20.1886 | 1.5246 | 4265.5337 |
| 1.9194 | 1.9044 | 1.8894 | 1.8743 | 1.8593 | 1.8443 | 1.8293 | 1.8143 |
| 0.0145 | 1.5312 |  |  |  |  |  |  |
| 20.2764 | 20.2750 | 20.2739 | 20.2732 | 20.2728 | 20.2728 | 1.5310 | 4349.1719 |
| 1.9194 | 1.9049 | 1.8903 | 1.8758 | 1.8612 | 1.8466 | 1.8321 | 1.8176 |
| 0.0145 | 1.5373 |  |  |  |  |  |  |
| 20.3579 | 20.3566 | 20.3555 | 20.3548 | 20.3545 | 20.3545 | 1.5372 | 4432.8096 |
| 1.9194 | 1.9053 | 1.8912 | 1.8771 | 1.8630 | 1.8489 | 1.8348 | 1.8208 |
| 0.0146 | 1.5433 |  |  |  |  |  |  |
| 20.4369 | 20.4356 | 20.4346 | 20.4339 | 20.4335 | 20.4335 | 1.5431 | 4516.4473 |
| 1.9194 | 1.9058 | 1.8921 | 1.8784 | 1.8648 | 1.8511 | 1.8374 | 1.8238 |
| 0.0146 | 1.5491 |  |  |  |  |  |  |
| 20.5134 | 20.5121 | 20.5112 | 20.5105 | 20.5102 | 20.5102 | 1.5489 | 4600.0854 |
| 1.9194 | 1.9062 | 1.8929 | 1.8797 | 1.8664 | 1.8532 | 1.8400 | 1.8267 |
| 0.0146 | 1.5547 |  |  |  |  |  |  |
| 20.5876 | 20.5863 | 20.5854 | 20.5848 | 20.5844 | 20.5844 | 1.5545 | 4683.7231 |
| 1.9194 | 1.9066 | 1.8937 | 1.8809 | 1.8681 | 1.8552 | 1.8424 | 1.8296 |
| 0.0146 | 1.5601 |  |  |  |  |  |  |
| 20.6595 | 20.6583 | 20.6574 | 20.6567 | 20.6564 | 20.6564 | 1.5599 | 4767.3613 |
| 1.9194 | 1.9070 | 1.8945 | 1.8821 | 1.8696 | 1.8572 | 1.8447 | 1.8323 |
| 0.0146 | 1.5654 |  |  |  |  |  |  |


| 20.7292 | 20.7280 | 20.7271 | 20.7265 | 20.7262 | 20.7262 | 1.5652 | 4850.9990 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.9194 | 1.9074 | 1.8953 | 1.8832 | 1.8711 | 1.8590 | 1.8470 | 1.8349 |
| 0.0147 | 1.5705 |  |  |  |  |  |  |
| 20.7968 | 20.7957 | 20.7948 | 20.7942 | 20.7939 | 20.7939 | 1.5703 | 4934.6372 |
| 1.9194 | 1.9077 | 1.8960 | 1.8843 | 1.8726 | 1.8608 | 1.8491 | 1.8374 |
| 0.0147 | 1.5754 |  |  |  |  |  |  |
| 20.8624 | 20.8613 | 20.8604 | 20.8599 | 20.8596 | 20.8596 | 1.5753 | 5018.2749 |
| 1.9194 | 1.9081 | 1.8967 | 1.8853 | 1.8739 | 1.8626 | 1.8512 | 1.8399 |
| 0.0147 | 1.5802 |  |  |  |  |  |  |
| 20.9260 | 20.9249 | 20.9241 | 20.9236 | 20.9233 | 20.9233 | 1.5801 | 5101.9126 |
| 1.9194 | 1.9084 | 1.8974 | 1.8863 | 1.8753 | 1.8643 | 1.8532 | 1.8422 |
| 0.0147 | 1.5849 |  |  |  |  |  |  |
| 20.9878 | 20.9867 | 20.9859 | 20.9854 | 20.9851 | 20.9851 | 1.5848 | 5185.5508 |
| 1.9194 | 1.9087 | 1.8980 | 1.8873 | 1.8766 | 1.8659 | 1.8552 | 1.8445 |
| 0.0147 | 1.5894 |  |  |  |  |  |  |
| 21.0477 | 21.0467 | 21.0459 | 21.0454 | 21.0451 | 21.0451 | 1.5893 | 5269.1890 |
| 1.9194 | 1.9090 | 1.8986 | 1.8882 | 1.8778 | 1.8675 | 1.8571 | 1.8467 |
| 0.0148 | 1.5938 |  |  |  |  |  |  |
| 21.1059 | 21.1049 | 21.1041 | 21.1036 | 21.1034 | 21.1034 | 1.5937 | 5352.8267 |
| 1.9194 | 1.9093 | 1.8992 | 1.8892 | 1.8791 | 1.8690 | 1.8589 | 1.8488 |
| 0.0148 | 1.5981 |  |  |  |  |  |  |
| 21.1623 | 21.1614 | 21.1607 | 21.1602 | 21.1599 | 21.1599 | 1.5980 | 5436.4644 |
| 1.9194 | 1.9096 | 1.8998 | 1.8900 | 1.8802 | 1.8704 | 1.8606 | 1.8509 |
| 0.0148 | 1.6022 |  |  |  |  |  |  |
| 21.2172 | 21.2162 | 21.2155 | 21.2151 | 21.2148 | 21.2148 | 1.6021 | 5520.1021 |
| 1.9194 | 1.9099 | 1.9004 | 1.8909 | 1.8814 | 1.8718 | 1.8623 | 1.8528 |
| 0.0148 | 1.6062 |  |  |  |  |  |  |
| 21.2704 | 21.2695 | 21.2688 | 21.2684 | 21.2682 | 21.2682 | 1.6061 | 5603.7407 |
| 1.9194 | 1.9102 | 1.9009 | 1.8917 | 1.8824 | 1.8732 | 1.8640 | 1.8547 |
| 0.0148 | 1.6101 |  |  |  |  |  |  |
| 21.3221 | 21.3213 | 21.3206 | 21.3202 | 21.3199 | 21.3199 | 1.6100 | 5687.3784 |
| 1.9194 | 1.9105 | 1.9015 | 1.8925 | 1.8835 | 1.8745 | 1.8656 | 1.8566 |
| 0.0148 | 1.6139 |  |  |  |  |  |  |
| 21.3724 | 21.3715 | 21.3709 | 21.3705 | 21.3702 | 21.3702 | 1.6138 | 5771.0161 |
| 1.9194 | 1.9107 | 1.9020 | 1.8933 | 1.8845 | 1.8758 | 1.8671 | 1.8584 |
| 0.0149 | 1.6176 |  |  |  |  |  |  |
| 21.4212 | 21.4204 | 21.4197 | 21.4193 | 21.4191 | 21.4191 | 1.6175 | 5854.6538 |
| 1.9194 | 1.9110 | 1.9025 | 1.8940 | 1.8855 | 1.8770 | 1.8686 | 1.8601 |
| 0.0149 | 1.6212 |  |  |  |  |  |  |
| 21.4686 | 21.4678 | 21.4672 | 21.4668 | 21.4666 | 21.4666 | 1.6211 | 5938.2920 |
| 1.9194 | 1.9112 | 1.9030 | 1.8947 | 1.8865 | 1.8782 | 1.8700 | 1.8618 |
| 0.0149 | 1.6247 |  |  |  |  |  |  |
| 21.5147 | 21.5139 | 21.5133 | 21.5130 | 21.5128 | 21.5128 | 1.6246 | 6021.9302 |
| 1.9194 | 1.9114 | 1.9034 | 1.8954 | 1.8874 | 1.8794 | 1.8714 | 1.8634 |
| 0.0149 | 1.6281 |  |  |  |  |  |  |
| 21.5595 | 21.5588 | 21.5582 | 21.5578 | 21.5576 | 21.5576 | 1.6280 | 6105.5679 |
| 1.9194 | 1.9117 | 1.9039 | 1.8961 | 1.8883 | 1.8805 | 1.8727 | 1.8650 |
| 0.0149 | 1.6314 |  |  |  |  |  |  |
| 21.6031 | 21.6023 | 21.6018 | 21.6014 | 21.6012 | 21.6012 | 1.6313 | 6189.2056 |
| 1.9194 | 1.9119 | 1.9043 | 1.8967 | 1.8892 | 1.8816 | 1.8740 | 1.8665 |
| 0.0149 | 1.6346 |  |  |  |  |  |  |
| 21.6454 | 21.6447 | 21.6441 | 21.6438 | 21.6436 | 21.6436 | 1.6345 | 6272.8438 |
| 1.9194 | 1.9121 | 1.9047 | 1.8974 | 1.8900 | 1.8826 | 1.8753 | 1.8680 |
| 0.0149 | 1.6377 |  |  |  |  |  |  |
| 21.6865 | 21.6858 | 21.6853 | 21.6850 | 21.6848 | 21.6848 | 1.6376 | 6356.4814 |
| 1.9194 | 1.9123 | 1.9051 | 1.8980 | 1.8908 | 1.8837 | 1.8765 | 1.8694 |
| 0.0149 | 1.6407 |  |  |  |  |  |  |
| 21.7266 | 21.7259 | 21.7254 | 21.7250 | 21.7248 | 21.7248 | 1.6406 | 6440.1196 |
| 1.9194 | 1.9125 | 1.9055 | 1.8986 | 1.8916 | 1.8846 | 1.8777 | 1.8708 |
| 0.0150 | 1.6436 |  |  |  |  |  |  |


| 21.7655 | 21.7648 | 21.7643 | 21.7640 | 21.7638 | 21.7638 | 1.6435 | 6523.7573 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.9194 | 1.9127 | 1.9059 | 1.8991 | 1.8924 | 1.8856 | 1.8788 | 1.8721 |
| 0.0150 | 1.6465 |  |  |  |  |  |  |
| 21.8033 | 21.8027 | 21.8022 | 21.8018 | 21.8017 | 21.8017 | 1.6464 | 6607.3955 |
| 1.9194 | 1.9129 | 1.9063 | 1.8997 | 1.8931 | 1.8865 | 1.8800 | 1.8734 |
| 0.0150 | 1.6493 |  |  |  |  |  |  |
| 21.8401 | 21.8395 | 21.8390 | 21.8387 | 21.8385 | 21.8385 | 1.6492 | 6691.0332 |
| 1.9194 | 1.9130 | 1.9066 | 1.9002 | 1.8938 | 1.8874 | 1.8810 | 1.8746 |
| 0.0150 | 1.6520 |  |  |  |  |  |  |
| 21.8759 | 21.8753 | 21.8748 | 21.8745 | 21.8744 | 21.8744 | 1.6519 | 6774.6709 |
| 1.9194 | 1.9132 | 1.9070 | 1.9008 | 1.8945 | 1.8883 | 1.8821 | 1.8759 |
| 0.0150 | 1.6546 |  |  |  |  |  |  |
| 21.9107 | 21.9101 | 21.9097 | 21.9094 | 21.9092 | 21.9092 | 1.6545 | 6858.3091 |
| 1.9194 | 1.9134 | 1.9073 | 1.9013 | 1.8952 | 1.8891 | 1.8831 | 1.8770 |
| 0.0150 | 1.6572 |  |  |  |  |  |  |
| 21.9446 | 21.9440 | 21.9436 | 21.9433 | 21.9432 | 21.9432 | 1.6571 | 6941.9473 |
| 1.9194 | 1.9135 | 1.9076 | 1.9018 | 1.8959 | 1.8900 | 1.8841 | 1.8782 |
| 0.0150 | 1.6596 |  |  |  |  |  |  |
| 21.9776 | 21.9770 | 21.9766 | 21.9763 | 21.9762 | 21.9762 | 1.6596 | 7025.5850 |
| 1.9194 | 1.9137 | 1.9080 | 1.9022 | 1.8965 | 1.8908 | 1.8850 | 1.8793 |
| 0.0150 | 1.6621 |  |  |  |  |  |  |
| 22.0096 | 22.0091 | 22.0087 | 22.0084 | 22.0083 | 22.0083 | 1.6620 | 7109.2227 |
| 1.9194 | 1.9139 | 1.9083 | 1.9027 | 1.8971 | 1.8915 | 1.8860 | 1.8804 |
| 0.0150 | 1.6644 |  |  |  |  |  |  |
| 22.0408 | 22.0403 | 22.0399 | 22.0396 | 22.0395 | 22.0395 | 1.6644 | 7192.8604 |
| 1.9194 | 1.9140 | 1.9086 | 1.9031 | 1.8977 | 1.8923 | 1.8869 | 1.8814 |
| 0.0150 | 1.6667 |  |  |  |  |  |  |
| 22.0712 | 22.0707 | 22.0703 | 22.0700 | 22.0699 | 22.0699 | 1.6666 | 7276.4990 |
| 1.9194 | 1.9142 | 1.9089 | 1.9036 | 1.8983 | 1.8930 | 1.8877 | 1.8824 |
| 0.0150 | 1.6689 |  |  |  |  |  |  |
| 22.1008 | 22.1003 | 22.0999 | 22.0996 | 22.0995 | 22.0995 | 1.6689 | 7360.1367 |
| 1.9194 | 1.9143 | 1.9091 | 1.9040 | 1.8989 | 1.8937 | 1.8886 | 1.8834 |
| 0.0151 | 1.6711 |  |  |  |  |  |  |
| 22.1295 | 22.1291 | 22.1287 | 22.1284 | 22.1283 | 22.1283 | 1.6711 | 7443.7744 |
| 1.9194 | 1.9144 | 1.9094 | 1.9044 | 1.8994 | 1.8944 | 1.8894 | 1.8844 |
| 0.0151 | 1.6732 |  |  |  |  |  |  |
| 22.1575 | 22.1571 | 22.1567 | 22.1565 | 22.1564 | 22.1564 | 1.6732 | 7527.4121 |
| 1.9194 | 1.9146 | 1.9097 | 1.9048 | 1.8999 | 1.8951 | 1.8902 | 1.8853 |
| 0.0151 | 1.6753 |  |  |  |  |  |  |
| 22.1848 | 22.1843 | 22.1840 | 22.1838 | 22.1836 | 22.1836 | 1.6752 | 7611.0508 |
| 1.9194 | 1.9147 | 1.9099 | 1.9052 | 1.9004 | 1.8957 | 1.8910 | 1.8862 |
| 0.0151 | 1.6773 |  |  |  |  |  |  |
| 22.2113 | 22.2109 | 22.2106 | 22.2103 | 22.2102 | 22.2102 | 1.6772 | 7694.6885 |
| 1.9194 | 1.9148 | 1.9102 | 1.9056 | 1.9010 | 1.8963 | 1.8917 | 1.8871 |
| 0.0151 | 1.6792 |  |  |  |  |  |  |
| 22.2372 | 22.2367 | 22.2364 | 22.2362 | 22.2361 | 22.2361 | 1.6792 | 7778.3262 |
| 1.9194 | 1.9149 | 1.9104 | 1.9059 | 1.9014 | 1.8969 | 1.8924 | 1.8880 |
| 0.0151 | 1.6811 |  |  |  |  |  |  |
| 22.2623 | 22.2619 | 22.2616 | 22.2614 | 22.2613 | 22.2613 | 1.6811 | 7861.9639 |
| 1.9194 | 1.9151 | 1.9107 | 1.9063 | 1.9019 | 1.8975 | 1.8932 | 1.8888 |
| 0.0151 | 1.6830 |  |  |  |  |  |  |
| 22.2868 | 22.2864 | 22.2861 | 22.2859 | 22.2858 | 22.2858 | 1.6829 | 7945.6021 |
| 1.9194 | 1.9152 | 1.9109 | 1.9066 | 1.9024 | 1.8981 | 1.8938 | 1.8896 |
| 0.0151 | 1.6848 |  |  |  |  |  |  |
| 22.3107 | 22.3103 | 22.3100 | 22.3098 | 22.3097 | 22.3097 | 1.6847 | 8029.2402 |
| 1.9194 | 1.9153 | 1.9111 | 1.9070 | 1.9028 | 1.8987 | 1.8945 | 1.8904 |
| 0.0151 | 1.6866 |  |  |  |  |  |  |
| 22.3339 | 22.3335 | 22.3332 | 22.3330 | 22.3329 | 22.3329 | 1.6865 | 8112.8779 |
| 1.9194 | 1.9154 | 1.9114 | 1.9073 | 1.9033 | 1.8992 | 1.8952 | 1.8911 |
| 0.0151 | 1.6883 |  |  |  |  |  |  |


| 22.3565 | 22.3561 | 22.3558 | 22.3556 | 22.3555 | 22.3555 | 1.6882 | 8196.5156 |
| ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 1.9194 | 1.9155 | 1.9116 | 1.9076 | 1.9037 | 1.8997 | 1.8958 | 1.8919 |
| 0.0151 | 1.6899 |  |  |  |  |  |  |
| 22.3785 | 22.3782 | 22.3779 | 22.3777 | 22.3776 | 22.3776 | 1.6899 | 8280.1543 |
| 1.9194 | 1.9156 | 1.9118 | 1.9079 | 1.9041 | 1.9003 | 1.8964 | 1.8926 |
| 0.0151 | 1.6915 |  |  |  |  |  |  |
| 22.4000 | 22.3996 | 22.3994 | 22.3992 | 22.3991 | 22.3991 | 1.6915 | 8363.7920 |
| 1.9194 | 1.9157 | 1.9120 | 1.9082 | 1.9045 | 1.9008 | 1.8970 | 1.8933 |
| 0.0151 | 1.6931 |  |  |  |  |  |  |
| 22.4209 | 22.4205 | 22.4203 | 22.4201 | 22.4200 | 22.4200 | 1.6931 | 8447.4297 |
| 1.9194 | 1.9158 | 1.9122 | 1.9085 | 1.9049 | 1.9012 | 1.8976 | 1.8940 |
| 0.0151 | 1.6947 |  |  |  |  |  |  |
| 22.4412 | 22.4409 | 22.4406 | 22.4405 | 22.4404 | 22.4404 | 1.6946 | 8531.0674 |
| 1.9194 | 1.9159 | 1.9123 | 1.9088 | 1.9053 | 1.9017 | 1.8982 | 1.8946 |
| 0.0151 | 1.6962 |  |  |  |  |  |  |
| 22.4611 | 22.4607 | 22.4605 | 22.4603 | 22.4602 | 22.4602 | 1.6961 | 8614.7051 |
| 1.9194 | 1.9160 | 1.9125 | 1.9091 | 1.9056 | 1.9022 | 1.8987 | 1.8953 |
| 0.0151 | 1.6976 |  |  |  |  |  |  |
| 22.4804 | 22.4800 | 22.4798 | 22.4796 | 22.4795 | 22.4795 | 1.6976 | 8698.3438 |
| 1.9194 | 1.9161 | 1.9127 | 1.9093 | 1.9060 | 1.9026 | 1.8993 | 1.8959 |
| 0.0152 | 1.6990 |  |  |  |  |  |  |
| 22.4992 | 22.4989 | 22.4986 | 22.4985 | 22.4984 | 22.4984 | 1.6990 | 8781.9814 |
| 1.9194 | 1.9162 | 1.9129 | 1.9096 | 1.9063 | 1.9030 | 1.8998 | 1.8965 |
| 0.0152 | 1.7004 |  |  |  |  |  |  |
| 22.5175 | 22.5172 | 22.5170 | 22.5168 | 22.5167 | 22.5167 | 1.7004 | 8865.6191 |
| 1.9194 | 1.9163 | 1.9131 | 1.9099 | 1.9067 | 1.9035 | 1.9003 | 1.8971 |
| 0.0152 | 1.7018 |  |  |  |  |  |  |
| 22.5354 | 22.5351 | 22.5348 | 22.5347 | 22.5346 | 22.5346 | 1.7017 | 8949.2568 |
| 1.9194 | 1.9163 | 1.9132 | 1.9101 | 1.9070 | 1.9039 | 1.9008 | 1.8977 |
| 0.0152 | 1.7031 |  |  |  |  |  |  |
| 22.5528 | 22.5525 | 22.5522 | 22.5521 | 22.5520 | 22.5520 | 1.7030 | 9032.8945 |
| 1.9194 | 1.9164 | 1.9134 | 1.9103 | 1.9073 | 1.9043 | 1.9012 | 1.8982 |
| 0.0152 | 1.7044 |  |  |  |  |  |  |
| 22.5697 | 22.5694 | 22.5692 | 22.5691 | 22.5690 | 22.5690 | 1.7043 | 9116.5332 |
| 1.9194 | 1.9165 | 1.9135 | 1.9106 | 1.9076 | 1.9047 | 1.9017 | 1.8988 |
| 0.0152 | 1.7056 |  |  |  |  |  |  |
| 22.5862 | 22.5859 | 22.5857 | 22.5856 | 22.5855 | 22.5855 | 1.7056 | 9200.1709 |

All data are checked successfully :!! Re-check all data entered

Temperature of storage enviroment incelsius $\mathbf{- 2 5 . 0 0}$
Relative humidity of storage environment in $=90.00$
Absolute humidity of storage environment ingH20/gAir $=.0183$
Diffusion coefficient of packaging materialin $10^{\wedge}-7 \mathrm{~cm} 2 / \mathrm{sec}=0.020$
Henry constant of packaging material in (gH2O/cm^3 PKG)/(gH20/cm^3 Air) - 125.12 000
Thickness of packaging material in cm = 0.01140
Surface area of packaging material in cm^2 $=3.78000$
Volume of packaging material in $\mathrm{cm}^{\wedge} 3=0.80000$
Diffusion coefficient of product in $10^{\wedge}-5 \mathrm{~cm}^{\wedge} 2 / \mathrm{sec}=0.11790$
Initial moisture content in $\mathbf{g H 2 O} / \mathbf{1 0 0 g}$ dryproduct $=0.00$
Critical moisture content in $9 \mathrm{H} 2 \mathrm{O} / 100 \mathrm{~g}$ dryproduct $\mathbf{~} \mathbf{2} .00$
Dry weight of product in $g=0.40770$
Chemical reaction rate = 0.0
Chemical reaction order $=0.0$
$A w / M=-.1790 E+01 \lambda w^{\wedge} 2+0.1922 E+01 \lambda w+0.6400 E-01$
Radius of product in $\mathrm{cm}=0.50000$
Thickness of product (Only Plate shape) incm = 0.39200
Hit any key to continue.....
INITIAL CONCENTRATION

```
Concentration of outside environment (CE) = 0.01938 g/L
Concentration of outside surface of PKG(CLE) = 2.42433 g/L
Concentration of inside surface of PKG(CLH) = 0.00002 g/L
Concentration of headspace (CH) = 0.00000 g/L
Concentration of outside surface of product (CRH) = 0.00132 g/L
```

```
DIMENSSIONLESS CONSTANT
```

$\mathrm{Q}=0.1260 \mathrm{E}-02$
$\mathrm{G}=0.1700 \mathrm{E}-02$
$A 1=0.1815 E-04$
$\mathrm{B} 1=0.2127 \mathrm{E}-03$
$S=0.2215 E+01$
$X=0.9000 \mathrm{E}+03$
$=7$

Hit any key to continue ......

Enter the number of time to calculateconcentrations at once.
<NOTICE !!! It must be over 200 and be times of 200>

## 89

CONCENTRATON PROFILE IN PRODUCT
(Plate Shape)
Each step is 137000 . steps ( 84.3120 hrs )
< of the divided shell of product is
5

| CLE CRH | $\begin{aligned} & \text { CL1 } \\ & \text { CRI } \end{aligned}$ | $\begin{aligned} & \text { CL2 } \\ & \text { CR2 } \end{aligned}$ | $\begin{aligned} & \text { CL3 } \\ & \text { CR3 } \end{aligned}$ | $\begin{aligned} & \text { CL4 } \\ & \text { CR4 } \end{aligned}$ | $\begin{aligned} & \text { CLH } \\ & \text { CRC } \end{aligned}$ | $\begin{array}{r} \mathrm{CH} \\ \text { GAIN } \end{array}$ | $\begin{gathered} \text { Meq } \\ \text { TIME (hrs) } \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.0819 | 1.7395 | 1.3971 | 1.0549 | 0.7127 | 0.3707 | 0.0290 |
| 0.0002 | 0.1273 |  |  |  |  |  |  |
| 1.6856 | 1.6564 | 1.6346 | 1.6200 | 1.6127 | 1.6127 | 0.1234 | 84.3120 |
| 2.4243 | 2.0894 | 1.7545 | 1.4198 | 1.0852 | 0.7509 | 0.4169 | 0.0833 |
| 0.0007 | 0.2540 |  |  |  |  |  |  |
| 3.3635 | 3.3351 | 3.3137 | 3.2995 | 3.2924 | 3.2924 | 0.2502 | 168.6240 |
| 2.4243 | 2.1053 | 1.7863 | 1.4676 | 1.1493 | 0.8316 | 0.5145 | 0.1983 |
| 0.0016 | 0.3760 |  |  |  |  |  |  |
| 4.9788 | 4.9518 | 4.9316 | 4.9181 | 4.9114 | 4.9114 | 0.3724 | 252.9361 |
| 2.4243 | 2.1366 | 1.8492 | 1.5622 | 1.2758 | 0.9904 | 0.7060 | 0.4230 |
| 0.0034 | 0.4882 |  |  |  |  |  |  |
| 6.4646 | 6.4405 | 6.4224 | 6.4104 | 6.4044 | 6.4044 | 0.4850 | 337.2481 |
| 2.4243 | 2.1758 | 1.9276 | 1.6797 | 1.4326 | 1.1862 | 0.9410 | 0.6970 |
| 0.0056 | 0.5861 |  |  |  |  |  |  |
| 7.7616 | 7.7408 | 7.7252 | 7.7149 | 7.7097 | 7.7097 | 0.5834 | 421.5601 |
| 2.4243 | 2.2092 | 1.9943 | 1.7797 | 1.5656 | 1.3521 | 1.1396 | 0.9280 |
| 0.0074 | 0.6706 |  |  |  |  |  |  |
| 8.8809 | 8.8629 | 8.8493 | 8.8403 | 8.8358 | 8.8358 | 0.6683 | 505.8722 |
| 2.4243 | 2.2350 | 2.0457 | 1.8567 | 1.6681 | 1.4800 | 1.2926 | 1.1060 |
| 0.0088 | 0.7446 |  |  |  |  |  |  |
| 9.8605 | 9.8446 | 9.8327 | 9.8248 | 9.8208 | 9.8208 | 0.7425 | 590.1841 |
| 2.4243 | 2.2549 | 2.0856 | 1.9165 | 1.7477 | 1.5793 | 1.4114 | 1.2441 |
| 0.0099 | 0.8105 |  |  |  |  |  |  |
| 10.7325 | 10.7183 | 10.7076 | 10.7005 | 10.6969 | 10.6969 | 0.8086 | 674.4962 |
| 2.4243 | 2.2708 | 2.1173 | 1.9640 | 1.8109 | 1.6582 | 1.5059 | 1.3540 |
| 0.0108 | 0.8699 |  |  |  |  |  |  |
| 11.5196 | 11.5067 | 11.4970 | 11.4905 | 11.4873 | 11.4873 | 0.8682 | 758.8082 |
| 2.4243 | 2.2837 | 2.1431 | 2.0027 | 1.8625 | 1.7225 | 1.5829 | 1.4437 |
| 0.0115 | 0.9242 |  |  |  |  |  |  |
| 12.2381 | 12.2263 | 12.2174 | 12.2114 | 12.2085 | 12.2085 | 0.9226 | 843.1202 |
| 2.4243 | 2.2945 | 2.1646 | 2.0349 | 1.9054 | 1.7761 | 1.6471 | 1.5184 |
| 0.0121 | 0.9741 |  |  |  |  |  |  |
| 12.8999 | 12.8890 | 12.8808 | 12.8753 | 12.8725 | 12.8725 | 0.9727 | 927.4323 |
| 2.4243 | 2.3036 | 2.1829 | 2.0623 | 1.9418 | 1.8215 | 1.7015 | 1.5818 |
| 0.0126 | 1.0205 |  |  |  |  |  |  |
| 13.5140 | 13.5038 | 13.4961 | 13.4910 | 13.4885 | 13.4885 | 1.0192 | 1011.7443 |
| 2.4243 | 2.3114 | 2.1985 | 2.0858 | 1.9731 | 1.8606 | 1.7483 | 1.6363 |
| 0.0131 | 1.0638 |  |  |  |  |  |  |
| 14.0871 | 14.0776 | 14.0704 | 14.0657 | 14.0633 | 14.0633 | 1.0625 | 1096.0563 |
| 2.4243 | 2.3182 | 2.2122 | 2.1062 | 2.0004 | 1.8947 | 1.7891 | 1.6838 |
| 0.0135 | 1.1044 |  |  |  |  |  |  |
| 14.6248 | 14.6159 | 14.6091 | 14.6046 | 14.6024 | 14.6024 | 1.1032 | 1180.3683 |
| 2.4243 | 2.3243 | 2.2242 | 2.1243 | 2.0244 | 1.9246 | 1.8251 | 1.7257 |
| 0.0138 | 1.1427 |  |  |  |  |  |  |
| 15.1314 | 15.1229 | 15.1165 | 15.1123 | 15.1102 | 15.1102 | 1.1415 | 1264.6804 |
| 2.4243 | 2.3296 | 2.2349 | 2.1403 | 2.0457 | 1.9513 | 1.8570 | 1.7629 |
| 0.0141 | 1.1788 |  |  |  |  |  |  |
| 15.6103 | 15.6023 | 15.5963 | 15.5923 | 15.5903 | 15.5903 | 1.1778 | 1348.9923 |
| 2.4243 | 2.3344 | 2.2445 | 2.1546 | 2.0649 | 1.9752 | 1.8857 | 1.7963 |
| 0.0144 | 1.2131 |  |  |  |  |  |  |
| 16.0646 | 16.0570 | 16.0513 | 16.0475 | 16.0456 | 16.0456 | 1.2121 | 1433.3044 |
| 2.4243 | 2.3387 | 2.2531 | 2.1676 | 2.0821 | 1.9968 | 1.9115 | 1.8264 |


| 0.0146 | 1.2458 |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 16.4967 | 16.4894 | 16.4840 | 16.4804 | 16.4786 | 16.4786 | 1.2448 | 1517.6163 |
| 2.4243 | 2.3426 | 2.2610 | 2.1794 | 2.0978 | 2.0163 | 1.9350 | 1.8537 |
| 0.0148 | 1.2769 |  |  |  |  |  |  |
| 16.9087 | 16.9018 | 16.8966 | 16.8931 | 16.8914 | 16.8914 | 1.2759 | 1601.9285 |
| 2.4243 | 2.3462 | 2.2681 | 2.1901 | 2.1121 | 2.0342 | 1.9564 | 1.8787 |
| 0.0150 | 1.3066 |  |  |  |  |  |  |
| 17.3024 | 17.2957 | 17.2908 | 17.2875 | 17.2858 | 17.2858 | 1.3057 | 1686.2404 |
| 2.4243 | 2.3495 | 2.2747 | 2.1999 | 2.1252 | 2.0506 | 1.9760 | 1.9016 |
| 0.0152 | 1.3351 |  |  |  |  |  |  |
| 17.6793 | 17.6729 | 17.6682 | 17.6650 | 17.6634 | 17.6634 | 1.3342 | 1770.5525 |
| 2.4243 | 2.3525 | 2.2808 | 2.2090 | 2.1373 | 2.0657 | 1.9941 | 1.9227 |
| 0.0154 | 1.3624 |  |  |  |  |  |  |
| 18.0407 | 18.0346 | 18.0301 | 18.0270 | 18.0255 | 18.0255 | 1.3615 | 1854.8646 |
| 2.4243 | 2.3553 | 2.2863 | 2.2174 | 2.1485 | 2.0796 | 2.0109 | 1.9422 |
| 0.0155 | 1.3886 |  |  |  |  |  |  |
| 18.3880 | 18.3821 | 18.3777 | 18.3748 | 18.3733 | 18.3733 | 1.3878 | 1939.1765 |
| 2.4243 | 2.3579 | 2.2915 | 2.2252 | 2.1588 | 2.0926 | 2.0264 | 1.9603 |
| 0.0157 | 1.4138 |  |  |  |  |  |  |
| 18.7220 | 18.7164 | 18.7121 | 18.7093 | 18.7079 | 18.7079 | 1.4131 | 2023.4886 |
| 2.4243 | 2.3603 | 2.2964 | 2.2324 | 2.1685 | 2.1046 | 2.0408 | 1.9771 |
| 0.0158 | 1.4381 |  |  |  |  |  |  |
| 19.0437 | 19.0383 | 19.0342 | 19.0315 | 19.0302 | 19.0302 | 1.4374 | 2107.8005 |
| 2.4243 | 2.3626 | 2.3009 | 2.2392 | 2.1775 | 2.1159 | 2.0543 | 1.9929 |
| 0.0159 | 1.4615 |  |  |  |  |  |  |
| 19.3540 | 19.3488 | 19.3448 | 19.3422 | 19.3409 | 19.3409 | 1.4608 | 2192.1125 |
| 2.4243 | 2.3647 | 2.3051 | 2.2455 | 2.1859 | 2.1264 | 2.0670 | 2.0076 |
| 0.0160 | 1.4841 |  |  |  |  |  |  |
| 19.6536 | 19.6485 | 19.6447 | 19.6422 | 19.6409 | 19.6409 | 1.4835 | 2276.4248 |
| 2.4243 | 2.3667 | 2.3091 | 2.2514 | 2.1939 | 2.1363 | 2.0789 | 2.0214 |
| 0.0162 | 1.5060 |  |  |  |  |  |  |
| 19.9431 | 19.9382 | 19.9345 | 19.9321 | 19.9309 | 19.9309 | 1.5054 | 2360.7366 |
| 2.4243 | 2.3686 | 2.3128 | 2.2570 | 2.2013 | 2.1456 | 2.0900 | 2.0345 |
| 0.0163 | 1.5272 |  |  |  |  |  |  |
| 20.2232 | 20.2184 | 20.2149 | 20.2125 | 20.2113 | 20.2113 | 1.5265 | 2445.0486 |
| 2.4243 | 2.3703 | 2.3163 | 2.2623 | 2.2083 | 2.1544 | 2.1006 | 2.0467 |
| 0.0164 | 1.5476 |  |  |  |  |  |  |
| 20.4943 | 20.4897 | 20.4863 | 20.4840 | 20.4829 | 20.4829 | 1.5470 | 2529.3608 |
| 2.4243 | 2.3720 | 2.3196 | 2.2673 | 2.2150 | 2.1627 | 2.1105 | 2.0583 |
| 0.0165 | 1.5675 |  |  |  |  |  |  |
| 20.7571 | 20.7527 | 20.7493 | 20.7471 | 20.7460 | 20.7460 | 1.5669 | 2613.6729 |
| 2.4243 | 2.3735 | 2.3228 | 2.2720 | 2.2213 | 2.1706 | 2.1199 | 2.0693 |
| 0.0165 | 1.5867 |  |  |  |  |  |  |
| 21.0119 | 21.0076 | 21.0044 | 21.0022 | 21.0011 | 21.0011 | 1.5862 | 2697.9846 |
| 2.4243 | 2.3750 | 2.3257 | 2.2765 | 2.2272 | 2.1780 | 2.1288 | 2.0797 |
| 0.0166 | 1.6054 |  |  |  |  |  |  |
| 21.2592 | 21.2550 | 21.2519 | 21.2498 | 21.2487 | 21.2487 | 1.6048 | 2782.2966 |
| 2.4243 | 2.3765 | 2.3286 | 2.2807 | 2.2329 | 2.1851 | 2.1373 | 2.0896 |
| 0.0167 | 1.6235 |  |  |  |  |  |  |
| 21.4993 | 21.4953 | 21.4922 | 21.4902 | 21.4892 | 21.4892 | 1.6230 | 2866.6089 |
| 2.4243 | 2.3778 | 2.3313 | 2.2847 | 2.2383 | 2.1918 | 2.1454 | 2.0990 |
| 0.0168 | 1.6412 |  |  |  |  |  |  |
| 21.7327 | 21.7287 | 21.7258 | 21.7238 | 21.7228 | 21.7228 | 1.6406 | 2950.9209 |
| 2.4243 | 2.3791 | 2.3338 | 2.2886 | 2.2434 | 2.1982 | 2.1530 | 2.1079 |
| 0.0168 | 1.6583 |  |  |  |  |  |  |
| 21.9596 | 21.9557 | 21.9528 | 21.9509 | 21.9499 | 21.9499 | 1.6578 | 3035.2327 |
| 2.4243 | 2.3803 | 2.3363 | 2.2923 | 2.2483 | 2.2043 | 2.1604 | 2.1165 |
| 0.0169 | 1.6750 |  |  |  |  |  |  |
| 22.1803 | 22.1765 | 22.1737 | 22.1718 | 22.1709 | 22.1709 | 1.6745 | 3119.5449 |
| 2.4243 | 2.3815 | 2.3386 | 2.2958 | 2.2529 | 2.2101 | 2.1674 | 2.1246 |


| 0.0170 | 1.6912 |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 22.3951 | 22.3914 | 22.3887 | 22.3869 | 22.3860 | 22.3860 | 1.6907 | 3203.8569 |
| 2.4243 | 2.3826 | 2.3408 | 2.2991 | 2.2574 | 2.2157 | 2.1740 | 2.1324 |
| 0.0170 | 1.7070 |  |  |  |  |  |  |
| 22.6043 | 22.6008 | 22.5981 | 22.5963 | 22.5954 | 22.5954 | 1.7065 | 3288.1689 |
| 2.4243 | 2.3836 | 2.3430 | 2.3023 | 2.2616 | 2.2210 | 2.1804 | 2.1399 |
| 0.0171 | 1.7224 |  |  |  |  |  |  |
| 22.8081 | 22.8047 | 22.8021 | 22.8003 | 22.7995 | 22.7995 | 1.7219 | 3372.4807 |
| 2.4243 | 2.3847 | 2.3450 | 2.3054 | 2.2657 | 2.2261 | 2.1866 | 2.1470 |
| 0.0172 | 1.7374 |  |  |  |  |  |  |
| 23.0068 | 23.0034 | 23.0009 | 22.9992 | 22.9984 | 22.9984 | 1.7369 | 3456.7930 |
| 2.4243 | 2.3857 | 2.3470 | 2.3083 | 2.2697 | 2.2310 | 2.1924 | 2.1539 |
| 0.0172 | 1.7520 |  |  |  |  |  |  |
| 23.2006 | 23.1973 | 23.1948 | 23.1932 | 23.1923 | 23.1923 | 1.7516 | 3541.1050 |
| 2.4243 | 2.3866 | 2.3489 | 2.3111 | 2.2734 | 2.2357 | 2.1981 | 2.1604 |
| 0.0173 | 1.7663 |  |  |  |  |  |  |
| 23.3896 | 23.3864 | 23.3839 | 23.3823 | 23.3815 | 23.3815 | 1.7658 | 3625.4170 |
| 2.4243 | 2.3875 | 2.3507 | 2.3138 | 2.2770 | 2.2402 | 2.2035 | 2.1667 |
| 0.0173 | 1.7802 |  |  |  |  |  |  |
| 23.5740 | 23.5709 | 23.5685 | 23.5670 | 23.5662 | 23.5662 | 1.7798 | 3709.7292 |
| 2.4243 | 2.3884 | 2.3524 | 2.3164 | 2.2805 | 2.2446 | 2.2087 | 2.1728 |
| 0.0174 | 1.7938 |  |  |  |  |  |  |
| 23.7541 | 23.7510 | 23.7488 | 23.7472 | 23.7465 | 23.7465 | 1.7934 | 3794.0410 |
| 2.4243 | 2.3892 | 2.3541 | 2.3190 | 2.2838 | 2.2488 | 2.2137 | 2.1787 |
| 0.0174 | 1.8071 |  |  |  |  |  |  |
| 23.9300 | 23.9270 | 23.9248 | 23.9233 | 23.9225 | 23.9225 | 1.8067 | 3878.3530 |
| 2.4243 | 2.3900 | 2.3557 | 2.3214 | 2.2871 | 2.2528 | 2.2185 | 2.1843 |
| 0.0175 | 1.8201 |  |  |  |  |  |  |
| 24.1018 | 24.0989 | 24.0967 | 24.0952 | 24.0945 | 24.0945 | 1.8197 | 3962.6653 |
| 2.4243 | 2.3908 | 2.3572 | 2.3237 | 2.2902 | 2.2567 | 2.2232 | 2.1897 |
| 0.0175 | 1.8327 |  |  |  |  |  |  |
| 24.2697 | 24.2669 | 24.2647 | 24.2633 | 24.2626 | 24.2626 | 1.8324 | 4046.9773 |
| 2.4243 | 2.3915 | 2.3587 | 2.3259 | 2.2932 | 2.2604 | 2.2277 | 2.1950 |
| 0.0175 | 1.8451 |  |  |  |  |  |  |
| 24.4339 | 24.4311 | 24.4290 | 24.4276 | 24.4269 | 24.4269 | 1.8448 | 4131.2891 |
| 2.4243 | 2.3923 | 2.3602 | 2.3281 | 2.2961 | 2.2640 | 2.2320 | 2.2000 |
| 0.0176 | 1.8573 |  |  |  |  |  |  |
| 24.5944 | 24.5917 | 24.5896 | 24.5883 | 24.5876 | 24.5876 | 1.8569 | 4215.6011 |
| 2.4243 | 2.3930 | 2.3616 | 2.3302 | 2.2988 | 2.2675 | 2.2362 | 2.2049 |
| 0.0176 | 1.8691 |  |  |  |  |  |  |
| 24.7514 | 24.7488 | 24.7468 | 24.7454 | 24.7447 | 24.7447 | 1.8688 | 4299.9136 |
| 2.4243 | 2.3936 | 2.3629 | 2.3322 | 2.3015 | 2.2709 | 2.2402 | 2.2096 |
| 0.0177 | 1.8807 |  |  |  |  |  |  |
| 24.9051 | 24.9024 | 24.9005 | 24.8992 | 24.8985 | 24.8985 | 1.8804 | 4384.2251 |
| 2.4243 | 2.3943 | 2.3642 | 2.3342 | 2.3042 | 2.2741 | 2.2441 | 2.2142 |
| 0.0177 | 1.8921 |  |  |  |  |  |  |
| 25.0554 | 25.0528 | 25.0509 | 25.0496 | 25.0490 | 25.0490 | 1.8917 | 4468.5371 |
| 2.4243 | 2.3949 | 2.3655 | 2.3361 | 2.3067 | 2.2773 | 2.2479 | 2.2186 |
| 0.0177 | 1.9032 |  |  |  |  |  |  |
| 25.2026 | 25.2001 | 25.1982 | 25.1969 | 25.1963 | 25.1963 | 1.9029 | 4552.8496 |
| 2.4243 | 2.3955 | 2.3667 | 2.3379 | 2.3091 | 2.2803 | 2.2516 | 2.2228 |
| 0.0178 | 1.9141 |  |  |  |  |  |  |
| 25.3467 | 25.3442 | 25.3424 | 25.3412 | 25.3406 | 25.3406 | 1.9137 | 4637.1616 |
| 2.4243 | 2.3961 | 2.3679 | 2.3397 | 2.3115 | 2.2833 | 2.2551 | 2.2270 |
| 0.0178 | 1.9247 |  |  |  |  |  |  |
| 25.4878 | 25.4854 | 25.4836 | 25.4824 | 25.4818 | 25.4818 | 1.9244 | 4721.4731 |
| 2.4243 | 2.3967 | 2.3690 | 2.3414 | 2.3138 | 2.2862 | 2.2586 | 2.2310 |
| 0.0178 | 1.9352 |  |  |  |  |  |  |
| 25.6261 | 25.6237 | 25.6220 | 25.6208 | 25.6202 | 25.6202 | 1.9349 | 4805.7856 |
| 2.4243 | 2.3972 | 2.3702 | 2.3431 | 2.3160 | 2.2889 | 2.2619 | 2.2349 |

$92$


All data are checked successfully !!!
Re-check all data entered

```
Temperature of storage environment incelsius \(\mathbf{= 2 5} .00\)
Relative humidity of storage environment in \(=80.00\)
Absolute humidity of storage environment ingH20/gAir \(=.0163\)
Diffusion coefficient of packaging materialin \(10^{\wedge}-7 \mathrm{~cm} \wedge 2 / \mathrm{sec}=0.020\)
Henry constant of packaging material in (gH2O/cm^3 PKG)/(gH2O/cm^3 Air) - 125.12
000
Thickness of packaging material in \(\mathrm{cm}=0.02300\)
Surface area of packaging material in \(\mathrm{cm}^{\wedge} 2=3.78000\)
Volume of packaging material in \(\mathrm{cm}^{\wedge} 3=0.80000\)
Diffusion coefficient of product in \(10^{\wedge}-5 \mathrm{~cm} \wedge 2 / \mathrm{sec}=0.11790\)
Initial moisture content in \(\mathrm{gH} 2 \mathrm{O} / 100 \mathrm{~g}\) dryproduct \(=0.00\)
Critical moisture content in \(\mathbf{g H 2 O / 1 0 0 g}\) dryproduct \(=2.00\)
ury weight of product in \(g=0.40770\)
Chemical reaction rate \(=0.0\)
Chemical reaction order \(=0.0\)
Aw/Ms-.1790E+01 Aw^2 \(+0.1922 E+01 \mathrm{Aw}+0.6400 \mathrm{E}-01\)
Radius of product in \(\mathrm{cm}=0.50000\)
Thickness of product (Only Plate shape) incm = 0.39200
Hit any key to continue.....
```


## INITIAL CONCENTRATION



## dimenssionless constant

```
Q=0.1420E-02
G=0.1520E-02
A1=0.1822E-04
B1=0.1902E-03
S=0.1981E+01
X=0.9000E+03
    = 14
```


Hit any key to continue ......

Enter the number of time to calculateconcentrations at once.
<NOTICE !!! It must be over 200 and be times of 200>

|  | Each step is < of the di |  | te Shap 152000 . ded shel | teps 1 of prod | $\begin{aligned} & 6379 \mathrm{hrs} \\ & \text { it is } \end{aligned}$ | 5 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| CLE | CL1 | CL2 | CL3 | CL4 | CLH | CH | Meq |
| CRH | CR1 | CR2 | CR3 | CR4 | CRC | GAIN | TIME (hrs) |
| 1.9194 | 1.7828 | 1.6462 | 1.5096 | 1.3730 | 1.2365 | 1.0999 | 0.9634 |
| 0.8269 | 0.6904 | 0.5540 | 0.4175 | 0.2812 | 0.1449 | 0.0086 | 0.0001 |
| 0.0504 |  |  |  |  |  |  |  |
| 0.6676 | 0.6545 | 0.6448 | 0.6382 | 0.6350 | 0.6350 | 0.0487 | 83.6379 |
| 1.9194 | 1.7837 | 1.6479 | 1.5122 | 1.3764 | 1.2407 | 1.1050 | 0.9693 |
| 0.8337 | 0.6980 | 0.5625 | 0.4269 | 0.2915 | 0.1560 | 0.0207 | 0.0002 |
| 0.1071 |  |  |  |  |  |  |  |
| 1.4189 | 1.4059 | 1.3962 | 1.3897 | 1.3865 | 1.3865 | 0.1054 | 167.2758 |
| 1.9194 | 1.7848 | 1.6501 | 1.5154 | 1.3807 | 1.2461 | 1.1115 | 0.9769 |
| 0.8424 | 0.7079 | 0.5735 | 0.4391 | 0.3048 | 0.1705 | 0.0364 | 0.0003 |
| 0.1634 |  |  |  |  |  |  |  |
| 2.1642 | 2.1514 | 2.1417 | 2.1353 | 2.1321 | 2.1321 | 0.1617 | 250.9138 |
| 1.9194 | 1.7862 | 1.6529 | 1.5197 | 1.3864 | 1.2533 | 1.1201 | 0.9870 |
| 0.8539 | 0.7209 | 0.5880 | 0.4552 | 0.3224 | 0.1898 | 0.0572 | 0.0005 |
| 0.2191 |  |  |  |  |  |  |  |
| 2.9017 | 2.8890 | 2.8795 | 2.8731 | 2.8700 | 2.8700 | 0.2174 | 334.5517 |
| 1.9194 | 1.7881 | 1.6568 | 1.5255 | 1.3942 | 1.2630 | 1.1318 | 1.0007 |
| 0.8697 | 0.7388 | 0.6079 | 0.4772 | 0.3466 | 0.2161 | 0.0857 | 0.0007 |
| 0.2740 |  |  |  |  |  |  |  |
| 3.6285 | 3.6160 | 3.6067 | 3.6004 | 3.5973 | 3.5973 | 0.2724 | 418.1896 |
| 1.9194 | 1.7908 | 1.6622 | 1.5336 | 1.4051 | 1.2766 | 1.1482 | 1.0199 |
| 0.8917 | 0.7636 | 0.6357 | 0.5079 | 0.3803 | 0.2528 | 0.1256 | 0.0010 |
| 0.3278 |  |  |  |  |  |  |  |
| 4.3404 | 4.3282 | 4.3191 | 4.3130 | 4.3100 | 4.3100 | 0.3262 | 501.8275 |
| 1.9194 | 1.7946 | 1.6698 | 1.5451 | 1.4204 | 1.2958 | 1.1713 | 1.0469 |
| 0.9227 | 0.7986 | 0.6748 | 0.5511 | 0.4277 | 0.3045 | 0.1816 | 0.0015 |
| 0.3799 |  |  |  |  |  |  |  |
| 5.0314 | 5.0196 | 5.0108 | 5.0049 | 5.0020 | 5.0020 | 0.3784 | 585.4654 |
| 1.9194 | 1.7998 | 1.6803 | 1.5607 | 1.4413 | 1.3220 | 1.2028 | 1.0838 |
| 0.9649 | 0.8463 | 0.7280 | 0.6099 | 0.4921 | 0.3747 | 0.2576 | 0.0021 |
| 0.4300 |  |  |  |  |  |  |  |
| 5.6936 | 5.6824 | 5.6740 | 5.6684 | 5.6656 | 5.6656 | 0.4285 | 669.1033 |
| 1.9194 | 1.8064 | 1.6934 | 1.5805 | 1.4677 | 1.3549 | 1.2424 | 1.1301 |
| 1.0180 | 0.9061 | 0.7946 | 0.6834 | 0.5725 | 0.4621 | 0.3521 | 0.0028 |
| 0.4772 |  |  |  |  |  |  |  |
| 6.3194 | 6.3089 | 6.3010 | 6.2957 | 6.2931 | 6.2931 | 0.4758 | 752.7413 |
| 1.9194 | 1.8138 | 1.7082 | 1.6027 | 1.4972 | 1.3919 | 1.2868 | 1.1819 |
| 1.0773 | 0.9729 | 0.8688 | 0.7651 | 0.6617 | 0.5588 | 0.4564 | 0.0036 |
| 0.5214 |  |  |  |  |  |  |  |
| 6.9042 | 6.8944 | 6.8871 | 6.8822 | 6.8798 | 6.8798 | 0.5201 | 836.3792 |
| 1.9194 | 1.8213 | 1.7231 | 1.6250 | 1.5271 | 1.4292 | 1.3316 | 1.2341 |
| 1.1369 | 1.0399 | 0.9432 | 0.8469 | 0.7510 | 0.6554 | 0.5603 | 0.0045 |
| 0.5624 |  |  |  |  |  |  |  |
| 7.4476 | 7.4386 | 7.4317 | 7.4272 | 7.4249 | 7.4249 | 0.5612 | 920.0171 |
| 1.9194 | 1.8283 | 1.7372 | 1.6461 | 1.5551 | 1.4643 | 1.3736 | 1.2831 |
| 1.1928 | 1.1027 | 1.0130 | 0.9235 | 0.8344 | 0.7456 | 0.6573 | 0.0053 |
| 0.6005 |  |  |  |  |  |  |  |
| 7.9521 | 7.9437 | 7.9374 | 7.9331 | 7.9310 | 7.9310 | 0.5994 | 1003.6550 |
| 1.9194 | 1.8346 | 1.7499 | 1.6652 | 1.5805 | 1.4960 | 1.4116 | 1.3274 |
| 1.2434 | 1.1596 | 1.0760 | 0.9928 | 0.9098 | 0.8271 | 0.7448 | 0.0060 |
| 0.6359 |  |  |  |  |  |  |  |
| 8.4214 | 8.4135 | 8.4076 | 8.4037 | 8.4017 | 8.4017 | 0.6349 | 1087.2930 |
| 1.9194 | 1.8403 | 1.7612 | 1.6822 | 1.6032 | 1.5243 | 1.4455 | 1.3669 |

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| 1.2885 | 1.2102 | 1.1322 | 1.0545 | 0.9769 | 0.8997 | 0.8228 | 0.0066 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0.6690 |  |  |  |  |  |  |  |
| 8.8593 | 8.8519 | 8.8464 | 8.8427 | 8.8409 | 8.8409 | 0.6680 | 1170.9308 |
| 1.9194 | 1.8454 | 1.7713 | 1.6972 | 1.6233 | 1.5494 | 1.4756 | 1.4020 |
| 1.3285 | 1.2552 | 1.1821 | 1.1092 | 1.0366 | 0.9642 | 0.8920 | 0.0071 |
| 0.7000 |  |  |  |  |  |  |  |
| 9.2693 | 9.2624 | 9.2572 | 9.2538 | 9.2521 | 9.2521 | 0.6991 | 1254.5687 |
| 1.9194 | 1.8498 | 1.7802 | 1.7107 | 1.6412 | 1.5717 | 1.5024 | 1.4332 |
| 1.3641 | 1.2952 | 1.2264 | 1.1579 | 1.0895 | 1.0214 | 0.9536 | 0.0076 |
| 0.7291 |  |  |  |  |  |  |  |
| 9.6545 | 9.6481 | 9.6432 | 9.6399 | 9.6383 | 9.6383 | 0.7282 | 1338.2067 |
| 1.9194 | 1.8538 | 1.7882 | 1.7226 | 1.6571 | 1.5916 | 1.5263 | 1.4610 |
| 1.3958 | 1.3308 | 1.2660 | 1.2013 | 1.1368 | 1.0725 | 1.0085 | 0.0081 |
| 0.7565 |  |  |  |  |  |  |  |
| 10.0177 | 10.0116 | 10.0070 | 10.0040 | 10.0024 | 10.0024 | 0.7557 | 1421.8446 |
| 1.9194 | 1.8574 | 1.7953 | 1.7333 | 1.6714 | 1.6095 | 1.5476 | 1.4859 |
| 1.4243 | 1.3628 | 1.3014 | 1.2402 | 1.1792 | 1.1184 | 1.0577 | 0.0085 |
| 0.7824 |  |  |  |  |  |  |  |
| 10.3612 | 10.3554 | 10.3510 | 10.3481 | 10.3467 | 10.3467 | 0.7817 | 1505.4825 |
| 1.9194 | 1.8606 | 1.8018 | 1.7430 | 1.6842 | 1.6255 | 1.5669 | 1.5083 |
| 1.4499 | 1.3916 | 1.3334 | 1.2753 | 1.2174 | 1.1596 | 1.1021 | 0.0088 |
| 0.8070 |  |  |  |  |  |  |  |
| 10.6868 | 10.6813 | 10.6771 | 10.6744 | 10.6730 | 10.6730 | 0.8063 | 1589.1204 |
| 1.9194 | 1.8635 | 1.8076 | 1.7517 | 1.6959 | 1.6401 | 1.5843 | 1.5287 |
| 1.4731 | 1.4176 | 1.3623 | 1.3070 | 1.2520 | 1.1970 | 1.1423 | 0.0091 |
| 0.8304 |  |  |  |  |  |  |  |
| 10.9963 | 10.9910 | 10.9871 | 10.9845 | 10.9832 | 10.9832 | 0.8297 | 1672.7583 |
| 1.9194 | 1.8662 | 1.8129 | 1.7597 | 1.7064 | 1.6533 | 1.6002 | 1.5471 |
| 1.4942 | 1.4413 | 1.3886 | 1.3359 | 1.2834 | 1.2310 | 1.1788 | 0.0094 |
| 0.8527 |  |  |  |  |  |  |  |
| 11.2911 | 11.2861 | 11.2824 | 11.2799 | 11.2786 | 11.2786 | 0.8520 | 1756.3962 |
| 1.9194 | 1.8686 | 1.8177 | 1.7669 | 1.7161 | 1.6654 | 1.6146 | 1.5640 |
| 1.5134 | 1.4630 | 1.4126 | 1.3623 | 1.3122 | 1.2621 | 1.2122 | 0.0097 |
| 0.8739 |  |  |  |  |  |  |  |
| 11.5726 | 11.5678 | 11.5642 | 11.5618 | 11.5606 | 11.5606 | 0.8733 | 1840.0342 |
| 1.9194 | 1.8708 | 1.8222 | 1.7736 | 1.7250 | 1.6764 | 1.6279 | 1.5795 |
| 1.5311 | 1.4828 | 1.4346 | 1.3865 | 1.3385 | 1.2907 | 1.2429 | 0.0099 |
| 0.8942 |  |  |  |  |  |  |  |
| 11.8417 | 11.8372 | 11.8337 | 11.8315 | 11.8303 | 11.8303 | 0.8936 | 1923.6721 |
| 1.9194 | 1.8728 | 1.8263 | 1.7797 | 1.7331 | 1.6866 | 1.6402 | 1.5938 |
| 1.5474 | 1.5011 | 1.4549 | 1.4088 | 1.3628 | 1.3169 | 1.2712 | 0.0102 |
| 0.9137 |  |  |  |  |  |  |  |
| 12.0996 | 12.0952 | 12.0919 | 12.0898 | 12.0887 | 12.0887 | 0.9131 | 2007.3101 |
| 1.9194 | 1.8747 | 1.8300 | 1.7853 | 1.7407 | 1.6961 | 1.6515 | 1.6069 |
| 1.5625 | 1.5181 | 1.4737 | 1.4295 | 1.3853 | 1.3413 | 1.2973 | 0.0104 |
| 0.9324 |  |  |  |  |  |  |  |
| 12.3470 | 12.3428 | 12.3397 | 12.3376 | 12.3365 | 12.3365 | 0.9318 | 2090.9480 |
| 1.9194 | 1.8765 | 1.8335 | 1.7906 | 1.7477 | 1.7048 | 1.6620 | 1.6192 |
| 1.5764 | 1.5337 | 1.4911 | 1.4486 | 1.4062 | 1.3638 | 1.3216 | 0.0106 |
| 0.9503 |  |  |  |  |  |  |  |
| 12.5848 | 12.5807 | 12.5777 | 12.5757 | 12.5747 | 12.5747 | 0.9498 | 2174.5859 |
| 1.9194 | 1.8781 | 1.8368 | 1.7955 | 1.7542 | 1.7129 | 1.6717 | 1.6305 |
| 1.5894 | 1.5483 | 1.5073 | 1.4664 | 1.4256 | 1.3848 | 1.3441 | 0.0107 |
| 0.9676 |  |  |  |  |  |  |  |
| 12.8135 | 12.8096 | 12.8067 | 12.8047 | 12.8037 | 12.8037 | 0.9671 | 2258.2236 |
| 1.9194 | 1.8796 | 1.8398 | 1.8000 | 1.7603 | 1.7205 | 1.6808 | 1.6411 |
| 1.6015 | 1.5620 | 1.5224 | 1.4830 | 1.4436 | 1.4044 | 1.3652 | 0.0109 |
| 0.9842 |  |  |  |  |  |  |  |
| 13.0338 | 13.0300 | 13.0272 | 13.0253 | 13.0244 | 13.0244 | 0.9838 | 2341.8616 |
| 1.9194 | 1.8811 | 1.8427 | 1.8043 | 1.7659 | 1.7276 | 1.6893 | 1.6511 |


| 1.6129 | 1.5747 | 1.5366 | 1.4985 | 1.4606 | 1.4227 | 1.3849 | 0.0111 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.0003 |  |  |  |  |  |  |  |
| 13.2462 | 13.2426 | 13.2399 | 13.2381 | 13.2372 | 13.2372 | 0.9998 | 2425.4995 |
| 1.9194 | 1.8824 | 1.8453 | 1.8083 | 1.7713 | 1.7343 | 1.6973 | 1.6604 |
| 1.6235 | 1.5866 | 1.5498 | 1.5131 | 1.4764 | 1.4399 | 1.4033 | 0.0112 |
| 1.0158 |  |  |  |  |  |  |  |
| 13.4513 | 13.4478 | 13.4452 | 13.4434 | 13.4426 | 13.4426 | 1.0153 | 2509.1375 |
| 1.9194 | 1.8836 | 1.8478 | 1.8120 | 1.7763 | 1.7405 | 1.7048 | 1.6691 |
| 1.6335 | 1.5979 | 1.5623 | 1.5268 | 1.4914 | 1.4560 | 1.4207 | 0.0114 |
| 1.0307 |  |  |  |  |  |  |  |
| 13.6494 | 13.6461 | 13.6435 | 13.6418 | 13.6410 | 13.6410 | 1.0303 | 2592.7754 |
| 1.9194 | 1.8848 | 1.8502 | 1.8156 | 1.7810 | 1.7464 | 1.7119 | 1.6773 |
| 1.6429 | 1.6084 | 1.5740 | 1.5397 | 1.5054 | 1.4712 | 1.4371 | 0.0115 |
| 1.0452 |  |  |  |  |  |  |  |
| 13.8411 | 13.8378 | 13.8353 | 13.8337 | 13.8329 | 13.8329 | 1.0448 | 2676.4133 |
| 1.9194 | 1.8859 | 1.8524 | 1.8189 | 1.7854 | 1.7520 | 1.7185 | 1.6851 |
| 1.6517 | 1.6184 | 1.5851 | 1.5519 | 1.5187 | 1.4856 | 1.4525 | 0.0116 |
| 1.0592 |  |  |  |  |  |  |  |
| 14.0265 | 14.0234 | 14.0210 | 14.0194 | 14.0186 | 14.0186 | 1.0588 | 2760.0510 |
| 1.9194 | 1.8870 | 1.8545 | 1.8221 | 1.7896 | 1.7572 | 1.7248 | 1.6925 |
| 1.6601 | 1.6278 | 1.5956 | 1.5634 | 1.5312 | 1.4991 | 1.4671 | 0.0117 |
| 1.0728 |  |  |  |  |  |  |  |
| 14.2062 | 14.2031 | 14.2008 | 14.1993 | 14.1985 | 14.1985 | 1.0724 | 2843.6892 |
| 1.9194 | 1.8880 | 1.8565 | 1.8251 | 1.7936 | 1.7622 | 1.7308 | 1.6994 |
| 1.6681 | 1.6368 | 1.6055 | 1.5743 | 1.5431 | 1.5120 | 1.4809 | 0.0118 |
| 1.0859 |  |  |  |  |  |  |  |
| 14.3803 | 14.3774 | 14.3751 | 14.3736 | 14.3729 | 14.3729 | 1.0855 | 2927.3269 |
| 1.9194 | 1.8889 | 1.8584 | 1.8279 | 1.7974 | 1.7669 | 1.7364 | 1.7060 |
| 1.6756 | 1.6452 | 1.6149 | 1.5846 | 1.5544 | 1.5242 | 1.4940 | 0.0119 |
| 1.0987 |  |  |  |  |  |  |  |
| 14.5492 | 14.5464 | 14.5442 | 14.5428 | 14.5420 | 14.5420 | 1.0983 | 3010.9651 |
| 1.9194 | 1.8898 | 1.8602 | 1.8306 | 1.8010 | 1.7714 | 1.7418 | 1.7123 |
| 1.6828 | 1.6533 | 1.6238 | 1.5944 | 1.5650 | 1.5357 | 1.5065 | 0.0120 |
| 1.1111 |  |  |  |  |  |  |  |
| 14.7132 | 14.7104 | 14.7083 | 14.7069 | 14.7062 | 14.7062 | 1.1107 | 3094.6028 |
| 1.9194 | 1.8907 | 1.8619 | 1.8331 | 1.8044 | 1.7756 | 1.7469 | 1.7182 |
| 1.6896 | 1.6609 | 1.6323 | 1.6038 | 1.5752 | 1.5467 | 1.5183 | 0.0121 |
| 1.1231 |  |  |  |  |  |  |  |
| 14.8724 | 14.8697 | 14.8677 | 14.8663 | 14.8656 | 14.8656 | 1.1227 | 3178.2407 |
| 1.9194 | 1.8915 | 1.8635 | 1.8356 | 1.8076 | 1.7797 | 1.7518 | 1.7239 |
| 1.6960 | 1.6682 | 1.6404 | 1.6126 | 1.5849 | 1.5572 | 1.5296 | 0.0122 |
| 1.1348 |  |  |  |  |  |  |  |
| 15.0272 | 15.0245 | 15.0226 | 15.0212 | 15.0206 | 15.0206 | 1.1344 | 3261.8787 |
| 1.9194 | 1.8923 | 1.8651 | 1.8379 | 1.8107 | 1.7836 | 1.7564 | 1.7293 |
| 1.7022 | 1.6752 | 1.6481 | 1.6211 | 1.5942 | 1.5673 | 1.5404 | 0.0123 |
| 1.1461 |  |  |  |  |  |  |  |
| 15.1777 | 15.1751 | 15.1732 | 15.1719 | 15.1712 | 15.1712 | 1.1458 | 3345.5166 |
| 1.9194 | 1.8930 | 1.8666 | 1.8401 | 1.8137 | 1.7873 | 1.7609 | 1.7345 |
| 1.7081 | 1.6818 | 1.6555 | 1.6292 | 1.6030 | 1.5768 | 1.5507 | 0.0124 |
| 1.1572 |  |  |  |  |  |  |  |
| 15.3240 | 15.3215 | 15.3196 | 15.3184 | 15.3178 | 15.3178 | 1.1569 | 3429.1545 |
| 1.9194 | 1.8937 | 1.8680 | 1.8422 | 1.8165 | 1.7908 | 1.7651 | 1.7394 |
| 1.7138 | 1.6881 | 1.6625 | 1.6370 | 1.6114 | 1.5859 | 1.5605 | 0.0125 |
| 1.1680 |  |  |  |  |  |  |  |
| 15.4665 | 15.4640 | 15.4622 | 15.4610 | 15.4604 | 15.4604 | 1.1676 | 3512.7925 |
| 1.9194 | 1.8944 | 1.8693 | 1.8443 | 1.8192 | 1.7942 | 1.7692 | 1.7442 |
| 1.7192 | 1.6942 | 1.6693 | 1.6444 | 1.6195 | 1.5947 | 1.5699 | 0.0125 |
| 1.1784 |  |  |  |  |  |  |  |
| 15.6052 | 15.6028 | 15.6010 | 15.5998 | 15.5992 | 15.5992 | 1.1781 | 3596.4302 |
| 1.9194 | 1.8950 | 1.8706 | 1.8462 | 1.8218 | 1.7974 | 1.7730 | 1.7487 |


| 1.7243 | 1.7000 | 1.6757 | 1.6515 | 1.6273 | 1.6031 | 1.5789 | 0.0126 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.1886 |  |  |  |  |  |  |  |
| 15.7403 | 15.7380 | 15.7363 | 15.7351 | 15.7345 | 15.7345 | 1.1883 | 3680.0684 |
| 1.9194 | 1.8957 | 1.8719 | 1.8481 | 1.8243 | 1.8005 | 1.7768 | 1.7530 |
| 1.7293 | 1.7056 | 1.6819 | 1.6583 | 1.6347 | 1.6111 | 1.5876 | 0.0127 |
| 1.1986 |  |  |  |  |  |  |  |
| 15.8720 | 15.8697 | 15.8680 | 15.8669 | 15.8664 | 15.8664 | 1.1983 | 3763.7061 |
| 1.9194 | 1.8962 | 1.8731 | 1.8499 | 1.8267 | 1.8035 | 1.7803 | 1.7572 |
| 1.7341 | 1.7110 | 1.6879 | 1.6648 | 1.6418 | 1.6188 | 1.5959 | 0.0128 |
| 1.2083 |  |  |  |  |  |  |  |
| 16.0004 | 15.9982 | 15.9965 | 15.9954 | 15.9949 | 15.9949 | 1.2080 | 3847.3442 |
| 1.9194 | 1.8968 | 1.8742 | 1.8516 | 1.8290 | 1.8064 | 1.7838 | 1.7612 |
| 1.7386 | 1.7161 | 1.6936 | 1.6711 | 1.6487 | 1.6262 | 1.6038 | 0.0128 |
| 1.2177 |  |  |  |  |  |  |  |
| 16.1256 | 16.1234 | 16.1218 | 16.1208 | 16.1202 | 16.1202 | 1.2174 | 3930.9819 |
| 1.9194 | 1.8974 | 1.8753 | 1.8532 | 1.8312 | 1.8091 | 1.7871 | 1.7650 |
| 1.7430 | 1.7211 | 1.6991 | 1.6772 | 1.6552 | 1.6334 | 1.6115 | 0.0129 |
| 1.2270 |  |  |  |  |  |  |  |
| 16.2477 | 16.2457 | 16.2441 | 16.2430 | 16.2425 | 16.2425 | 1.2267 | 4014.6201 |
| 1.9194 | 1.8979 | 1.8764 | 1.8548 | 1.8333 | 1.8118 | 1.7903 | 1.7688 |
| 1.7473 | 1.7258 | 1.7044 | 1.6830 | 1.6616 | 1.6402 | 1.6189 | 0.0129 |
| 1.2360 |  |  |  |  |  |  |  |
| 16.3670 | 16.3649 | 16.3634 | 16.3624 | 16.3619 | 16.3619 | 1.2357 | 4098.2578 |
| 1.9194 | 1.8984 | 1.8774 | 1.8563 | 1.8353 | 1.8143 | 1.7933 | 1.7723 |
| 1.7513 | 1.7304 | 1.7095 | 1.6886 | 1.6677 | 1.6468 | 1.6260 | 0.0130 |
| 1.2447 |  |  |  |  |  |  |  |
| 16.4834 | 16.4814 | 16.4799 | 16.4789 | 16.4784 | 16.4784 | 1.2445 | 4181.8960 |
| 1.9194 | 1.8989 | 1.8784 | 1.8578 | 1.8373 | 1.8168 | 1.7963 | 1.7758 |
| 1.7553 | 1.7348 | 1.7144 | 1.6939 | 1.6735 | 1.6532 | 1.6328 | 0.0131 |
| 1.2533 |  |  |  |  |  |  |  |
| 16.5971 | 16.5951 | 16.5937 | 16.5927 | 16.5922 | 16.5922 | 1.2531 | 4265.5337 |
| 1.9194 | 1.8994 | 1.8793 | 1.8592 | 1.8392 | 1.8191 | 1.7991 | 1.7791 |
| 1.7591 | 1.7391 | 1.7191 | 1.6991 | 1.6792 | 1.6593 | 1.6394 | 0.0131 |
| 1.2617 |  |  |  |  |  |  |  |
| 16.7081 | 16.7062 | 16.7048 | 16.7039 | 16.7034 | 16.7034 | 1.2615 | 4349.1719 |
| 1.9194 | 1.8998 | 1.8802 | 1.8606 | 1.8410 | 1.8214 | 1.8018 | 1.7823 |
| 1.7627 | 1.7432 | 1.7237 | 1.7042 | 1.6847 | 1.6652 | 1.6458 | 0.0132 |
| 1.2699 |  |  |  |  |  |  |  |
| 16.8167 | 16.8148 | 16.8134 | 16.8125 | 16.8120 | 16.8120 | 1.2697 | 4432.8096 |
| 1.9194 | 1.9003 | 1.8811 | 1.8619 | 1.8428 | 1.8236 | 1.8045 | 1.7854 |
| 1.7662 | 1.7471 | 1.7281 | 1.7090 | 1.6900 | 1.6709 | 1.6520 | 0.0132 |
| 1.2779 |  |  |  |  |  |  |  |
| 16.9228 | 16.9209 | 16.9196 | 16.9187 | 16.9182 | 16.9182 | 1.2777 | 4516.4473 |
| 1.9194 | 1.9007 | 1.8820 | 1.8632 | 1.8445 | 1.8258 | 1.8070 | 1.7883 |
| 1.7697 | 1.7510 | 1.7323 | 1.7137 | 1.6951 | 1.6765 | 1.6579 | 0.0133 |
| 1.2858 |  |  |  |  |  |  |  |
| 17.0265 | 17.0247 | 17.0234 | 17.0225 | 17.0220 | 17.0220 | 1.2855 | 4600.0854 |
| 1.9194 | 1.9011 | 1.8828 | 1.8645 | 1.8461 | 1.8278 | 1.8095 | 1.7912 |
| 1.7729 | 1.7547 | 1.7364 | 1.7182 | 1.7000 | 1.6818 | 1.6636 | 0.0133 |
| 1.2934 |  |  |  |  |  |  |  |
| 17.1279 | 17.1262 | 17.1249 | 17.1240 | 17.1236 | 17.1236 | 1.2932 | 4683.7231 |
| 1.9194 | 1.9015 | 1.8836 | 1.8657 | 1.8477 | 1.8298 | 1.8119 | 1.7940 |
| 1.7761 | 1.7583 | 1.7404 | 1.7226 | 1.7048 | 1.6870 | 1.6692 | 0.0133 |
| 1.3009 |  |  |  |  |  |  |  |
| 17.2272 | 17.2255 | 17.2242 | 17.2233 | 17.2229 | 17.2229 | 1.3007 | 4767.3613 |
| 1.9194 | 1.9019 | 1.8844 | 1.8668 | 1.8493 | 1.8317 | 1.8142 | 1.7967 |
| 1.7792 | 1.7617 | 1.7443 | 1.7268 | 1.7094 | 1.6920 | 1.6746 | 0.0134 |
| 1.3082 |  |  |  |  |  |  |  |
| 17.3243 | 17.3226 | 17.3214 | 17.3205 | 17.3201 | 17.3201 | 1.3080 | 4850.9990 |
| 1.9194 | 1.9023 | 1.8851 | 1.8679 | 1.8508 | 1.8336 | 1.8165 | 1.7993 |

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| 1.7822 | 1.7651 | 1.7480 | 1.7309 | 1.7138 | 1.6968 | 1.6798 | 0.0134 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.3154 |  |  |  |  |  |  |  |
| 17.4193 | 17.4177 | 17.4165 | 17.4156 | 17.4152 | 17.4152 | 1.3152 | 4934.6372 |
| 1.9194 | 1.9026 | 1.8858 | 1.8690 | 1.8522 | 1.8354 | 1.8186 | 1.8019 |
| 1.7851 | 1.7683 | 1.7516 | 1.7349 | 1.7182 | 1.7015 | 1.6848 | 0.0135 |
| 1.3224 |  |  |  |  |  |  |  |
| 17.5123 | 17.5107 | 17.5095 | 17.5087 | 17.5083 | 17.5083 | 1.3222 | 5018.2749 |
| 1.9194 | 1.9030 | 1.8865 | 1.8701 | 1.8536 | 1.8372 | 1.8207 | 1.8043 |
| 1.7879 | 1.7715 | 1.7551 | 1.7387 | 1.7224 | 1.7060 | 1.6897 | 0.0135 |
| 1.3293 |  |  |  |  |  |  |  |
| 17.6034 | 17.6019 | 17.6007 | 17.5999 | 17.5995 | 17.5995 | 1.3291 | 5101.9126 |
| 1.9194 | 1.9033 | 1.8872 | 1.8711 | 1.8550 | 1.8389 | 1.8228 | 1.8067 |
| 1.7906 | 1.7746 | 1.7585 | 1.7425 | 1.7264 | 1.7104 | 1.6945 | 0.0135 |
| 1.3361 |  |  |  |  |  |  |  |
| 17.6926 | 17.6911 | 17.6899 | 17.6892 | 17.6888 | 17.6888 | 1.3359 | 5185.5508 |
| 1.9194 | 1.9037 | 1.8879 | 1.8721 | 1.8563 | 1.8405 | 1.8248 | 1.8090 |
| 1.7933 | 1.7775 | 1.7618 | 1.7461 | 1.7304 | 1.7147 | 1.6991 | 0.0136 |
| 1.3427 |  |  |  |  |  |  |  |
| 17.7800 | 17.7785 | 17.7774 | 17.7766 | 17.7762 | 17.7762 | 1.3425 | 5269.1890 |
| 1.9194 | 1.9040 | 1.8885 | 1.8730 | 1.8576 | 1.8421 | 1.8267 | 1.8112 |
| 1.7958 | 1.7804 | 1.7650 | 1.7496 | 1.7342 | 1.7189 | 1.7035 | 0.0136 |
| 1.3491 |  |  |  |  |  |  |  |
| 17.8656 | 17.8641 | 17.8630 | 17.8623 | 17.8619 | 17.8619 | 1.3489 | 5352.8267 |
| 1.9194 | 1.9043 | 1.8891 | 1.8740 | 1.8588 | 1.8437 | 1.8285 | 1.8134 |
| 1.7983 | 1.7832 | 1.7681 | 1.7530 | 1.7380 | 1.7229 | 1.7079 | 0.0136 |
| 1.3555 |  |  |  |  |  |  |  |
| 17.9495 | 17.9480 | 17.9470 | 17.9462 | 17.9459 | 17.9459 | 1.3553 | 5436.4644 |
| 1.9194 | 1.9046 | 1.8897 | 1.8749 | 1.8600 | 1.8452 | 1.8304 | 1.8155 |
| 1.8007 | 1.7859 | 1.7711 | 1.7563 | 1.7416 | 1.7268 | 1.7121 | 0.0137 |
| 1.3617 |  |  |  |  |  |  |  |
| 18.0317 | 18.0303 | 18.0292 | 18.0285 | 18.0282 | 18.0282 | 1.3615 | 5520.1021 |
| 1.9194 | 1.9049 | 1.8903 | 1.8758 | 1.8612 | 1.8467 | 1.8321 | 1.8176 |
| 1.8031 | 1.7885 | 1.7740 | 1.7596 | 1.7451 | 1.7306 | 1.7162 | 0.0137 |
| 1.3678 |  |  |  |  |  |  |  |
| 18.1123 | 18.1109 | 18.1099 | 18.1092 | 18.1088 | 18.1088 | 1.3676 | 5603.7407 |
| 1.9194 | 1.9052 | 1.8909 | 1.8766 | 1.8624 | 1.8481 | 1.8338 | 1.8196 |
| 1.8053 | 1.7911 | 1.7769 | 1.7627 | 1.7485 | 1.7343 | 1.7202 | 0.0137 |
| 1.3737 |  |  |  |  |  |  |  |
| 18.1913 | 18.1899 | 18.1889 | 18.1882 | 18.1879 | 18.1879 | 1.3735 | 5687.3784 |
| 1.9194 | 1.9054 | 1.8915 | 1.8775 | 1.8635 | 1.8495 | 1.8355 | 1.8215 |
| 1.8076 | 1.7936 | 1.7797 | 1.7657 | 1.7518 | 1.7379 | 1.7240 | 0.0138 |
| 1.3796 |  |  |  |  |  |  |  |
| 18.2687 | 18.2674 | 18.2664 | 18.2658 | 18.2654 | 18.2654 | 1.3794 | 5771.0161 |
| 1.9194 | 1.9057 | 1.8920 | 1.8783 | 1.8645 | 1.8508 | 1.8371 | 1.8234 |
| 1.8097 | 1.7960 | 1.7824 | 1.7687 | 1.7550 | 1.7414 | 1.7278 | 0.0138 |
| 1.3853 |  |  |  |  |  |  |  |
| 18.3447 | 18.3434 | 18.3424 | 18.3418 | 18.3415 | 18.3415 | 1.3851 | 5854.6538 |
| 1.9194 | 1.9060 | 1.8925 | 1.8791 | 1.8656 | 1.8521 | 1.8387 | 1.8252 |
| 1.8118 | 1.7984 | 1.7850 | 1.7716 | 1.7582 | 1.7448 | 1.7315 | 0.0138 |
| 1.3909 |  |  |  |  |  |  |  |
| 18.4192 | 18.4180 | 18.4170 | 18.4164 | 18.4160 | 18.4160 | 1.3908 | 5938.2920 |
| 1.9194 | 1.9062 | 1.8930 | 1.8798 | 1.8666 | 1.8534 | 1.8402 | 1.8270 |
| 1.8139 | 1.8007 | 1.7875 | 1.7744 | 1.7612 | 1.7481 | 1.7350 | 0.0139 |
| 1.3965 |  |  |  |  |  |  |  |
| 18.4923 | 18.4911 | 18.4902 | 18.4895 | 18.4892 | 18.4892 | 1.3963 | 6021.9302 |
| 1.9194 | 1.9065 | 1.8935 | 1.8806 | 1.8676 | 1.8547 | 1.8417 | 1.8288 |
| 1.8158 | 1.8029 | 1.7900 | 1.7771 | 1.7642 | 1.7513 | 1.7385 | 0.0139 |
| 1.4019 0.0139 |  |  |  |  |  |  |  |
| 18.5641 | 18.5628 | 18.5619 | 18.5613 | 18.5610 | 18.5610 | 1.4017 | 6105.5679 |
| 1.9194 | 1.9067 | 1.8940 | 1.8813 | 1.8686 | 1.8559 | 1.8432 | 1.8305 |


| 1.8178 | 1.8051 | 1.7924 | 1.7798 | 1.7671 | 1.7545 | 1.7419 | 0.0139 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.4072 |  |  |  |  |  |  |  |
| 18.6345 | 18.6333 | 18.6323 | 18.6317 | 18.6314 | 18.6314 | 1.4070 | 6189.2056 |
| 1.9194 | 1.9070 | 1.8945 | 1.8820 | 1.8695 | 1.8571 | 1.8446 | 1.8321 |
| 1.8197 | 1.8072 | 1.7948 | 1.7824 | 1.7700 | 1.7576 | 1.7452 | 0.0139 |
| 1.4124 |  |  |  |  |  |  |  |
| 18.7035 | 18.7024 | 18.7015 | 18.7009 | 18.7006 | 18.7006 | 1.4122 | 6272.8438 |
| 1.9194 | 1.9072 | 1.8949 | 1.8827 | 1.8704 | 1.8582 | 1.8460 | 1.8337 |
| 1.8215 | 1.8093 | 1.7971 | 1.7849 | 1.7727 | 1.7605 | 1.7484 | 0.0140 |
| 1.4175 |  |  |  |  |  |  |  |
| 18.7713 | 18.7702 | 18.7693 | 18.7687 | 18.7684 | 18.7684 | 1.4174 | 6356.4814 |
| 1.9194 | 1.9074 | 1.8954 | 1.8834 | 1.8713 | 1.8593 | 1.8473 | 1.8353 |
| 1.8233 | 1.8113 | 1.7993 | 1.7874 | 1.7754 | 1.7634 | 1.7515 | 0.0140 |
| 1.4226 |  |  |  |  |  |  |  |
| 18.8379 | 18.8368 | 18.8359 | 18.8353 | 18.8351 | 18.8351 | 1.4224 | 6440.1196 |
| 1.9194 | 1.9076 | 1.8958 | 1.8840 | 1.8722 | 1.8604 | 1.8486 | 1.8368 |
| 1.8251 | 1.8133 | 1.8015 | 1.7898 | 1.7780 | 1.7663 | 1.7546 | 0.0140 |
| 1.4275 |  |  |  |  |  |  |  |
| 18.9033 | 18.9021 | 18.9013 | 18.9007 | 18.9005 | 18.9005 | 1.4273 | 6523.7573 |
| 1.9194 | 1.9079 | 1.8963 | 1.8847 | 1.8731 | 1.8615 | 1.8499 | 1.8383 |
| 1.8268 | 1.8152 | 1.8036 | 1.7921 | 1.7806 | 1.7690 | 1.7575 | 0.0140 |
| 1.4323 |  |  |  |  |  |  |  |
| 18.9674 | 18.9663 | 18.9655 | 18.9650 | 18.9647 | 18.9647 | 1.4322 | 6607.3955 |
| 1.9194 | 1.9081 | 1.8967 | 1.8853 | 1.8739 | 1.8625 | 1.8512 | 1.8398 |
| 1.8284 | 1.8171 | 1.8057 | 1.7944 | 1.7831 | 1.7717 | 1.7604 | 0.0141 |
| 1.4371 |  |  |  |  |  |  |  |
| 19.0304 | 19.0294 | 19.0286 | 19.0280 | 19.0277 | 19.0277 | 1.4369 | 6691.0332 |
| 1.9194 | 1.9083 | 1.8971 | 1.8859 | 1.8747 | 1.8635 | 1.8524 | 1.8412 |
| 1.8300 | 1.8189 | 1.8078 | 1.7966 | 1.7855 | 1.7744 | 1.7633 | 0.0141 |
| 1.4418 |  |  |  |  |  |  |  |
| 19.0923 | 19.0913 | 19.0905 | 19.0899 | 19.0897 | 19.0897 | 1.4416 | 6774.6709 |
| 1.9194 | 1.9085 | 1.8975 | 1.8865 | 1.8755 | 1.8645 | 1.8536 | 1.8426 |
| 1.8316 | 1.8207 | 1.8097 | 1.7988 | 1.7879 | 1.7770 | 1.7660 | 0.0141 |
| 1.4464 |  |  |  |  |  |  |  |
| 19.1531 | 19.1521 | 19.1513 | 19.1508 | 19.1505 | 19.1505 | 1.4462 | 6858.3091 |
| 1.9194 | 1.9087 | 1.8979 | 1.8871 | 1.8763 | 1.8655 | 1.8547 | 1.8439 |
| 1.8332 | 1.8224 | 1.8117 | 1.8009 | 1.7902 | 1.7795 | 1.7688 | 0.0141 |
| 1.4509 |  |  |  |  |  |  |  |
| 19.2129 | 19.2118 | 19.2111 | 19.2105 | 19.2103 | 19.2103 | 1.4507 | 6941.9473 |
| 1.9194 | 1.9088 | 1.8982 | 1.8876 | 1.8770 | 1.8664 | 1.8559 | 1.8453 |
| 1.8347 | 1.8241 | 1.8136 | 1.8030 | 1.7925 | 1.7819 | 1.7714 | 0.0142 |
| 1.4553 |  |  |  |  |  |  |  |
| 19.2715 | 19.2705 | 19.2698 | 19.2693 | 19.2690 | 19.2690 | 1.4552 | 7025.5850 |
| 1.9194 | 1.9090 | 1.8986 | 1.8882 | 1.8778 | 1.8674 | 1.8570 | 1.8466 |
| 1.8362 | 1.8258 | 1.8154 | 1.8050 | 1.7947 | 1.7843 | 1.7740 | 0.0142 |
| 1.4596 |  |  |  |  |  |  |  |
| 19.3292 | 19.3282 | 19.3275 | 19.3270 | 19.3267 | 19.3267 | 1.4595 | 7109.2227 |
| 1.9194 | 1.9092 | 1.8990 | 1.8887 | 1.8785 | 1.8683 | 1.8580 | 1.8478 |
| 1.8376 | 1.8274 | 1.8172 | 1.8070 | 1.7968 | 1.7867 | 1.7765 | 0.0142 |
| 1.4639 |  |  |  |  |  |  |  |
| 19.3858 | 19.3849 | 19.3841 | 19.3836 | 19.3834 | 19.3834 | 1.4638 | 7192.8604 |
| 1.9194 | 1.9094 | 1.8993 | 1.8893 | 1.8792 | 1.8692 | 1.8591 | 1.8491 |
| 1.8390 | 1.8290 | 1.8190 | 1.8089 | 1.7989 | 1.7889 | 1.7789 | 0.0142 |
| 1.4681 |  |  |  |  |  |  |  |
| 19.4415 | 19.4406 | 19.4398 | 19.4394 | 19.4391 | 19.4391 | 1.4680 | 7276.4990 |
| 1.9194 | 1.9096 | 1.8997 | 1.8898 | 1.8799 | 1.8700 | 1.8601 | 1.8503 |
| 1.8404 | 1.8305 | 1.8207 | 1.8108 | 1.8010 | 1.7912 | 1.7814 | 0.0142 |
| 1.4723 |  |  |  |  |  |  |  |
| 19.4962 | 19.4953 | 19.4946 | 19.4941 | 19.4939 | 19.4939 | 1.4721 | 7360.1367 |
| 1.9194 | 1.9097 | 1.9000 | 1.8903 | 1.8806 | 1.8709 | 1.8612 | 1.8514 |


| 1.8417 | 1.8321 | 1.8224 | 1.8127 | 1.8030 | 1.7934 | 1.7837 | 0.0143 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.4763 |  |  |  |  |  |  |  |
| 19.5500 | 19.5491 | 19.5484 | 19.5479 | 19.5477 | 19.5477 | 1.4762 | 7443.7744 |
| 1.9194 | 1.9099 | 1.9003 | 1.8908 | 1.8812 | 1.8717 | 1.8621 | 1.8526 |
| 1.8431 | 1.8335 | 1.8240 | 1.8145 | 1.8050 | 1.7955 | 1.7860 | 0.0143 |
| 1.4803 |  |  |  |  |  |  |  |
| 19.6029 | 19.6020 | 19.6013 | 19.6009 | 19.6006 | 19.6006 | 1.4802 | 7527.4121 |
| 1.9194 | 1.9101 | 1.9007 | 1.8913 | 1.8819 | 1.8725 | 1.8631 | 1.8537 |
| 1.8444 | 1.8350 | 1.8256 | 1.8163 | 1.8069 | 1.7976 | 1.7883 | 0.0143 |
| 1.4842 |  |  |  |  |  |  |  |
| 19.6549 | 19.6540 | 19.6533 | 19.6529 | 19.6527 | 19.6527 | 1.4841 | 7611.0508 |
| 1.9194 | 1.9102 | 1.9010 | 1.8917 | 1.8825 | 1.8733 | 1.8641 | 1.8548 |
| 1.8456 | 1.8364 | 1.8272 | 1.8180 | 1.8088 | 1.7996 | 1.7905 | 0.0143 |
| 1.4881 |  |  |  |  |  |  |  |
| 19.7060 | 19.7051 | 19.7045 | 19.7040 | 19.7038 | 19.7038 | 1.4880 | 7694.6885 |
| 1.9194 | 1.9104 | 1.9013 | 1.8922 | 1.8831 | 1.8740 | 1.8650 | 1.8559 |
| 1.8468 | 1.8378 | 1.8287 | 1.8197 | 1.8107 | 1.8016 | 1.7926 | 0.0143 |
| 1.4919 |  |  |  |  |  |  |  |
| 19.7563 | 19.7554 | 19.7548 | 19.7543 | 19.7541 | 19.7541 | 1.4918 | 7778.3262 |
| 1.9194 | 1.9105 | 1.9016 | 1.8927 | 1.8837 | 1.8748 | 1.8659 | 1.8570 |
| 1.8481 | 1.8391 | 1.8302 | 1.8214 | 1.8125 | 1.8036 | 1.7947 | 0.0143 |
| 1.4956 |  |  |  |  |  |  |  |
| 19.8057 | 19.8048 | 19.8042 | 19.8038 | 19.8036 | 19.8036 | 1.4955 | 7861.9639 |
| 1.9194 | 1.9107 | 1.9019 | 1.8931 | 1.8843 | 1.8755 | 1.8668 | 1.8580 |
| 1.8492 | 1.8405 | 1.8317 | 1.8230 | 1.8142 | 1.8055 | 1.7968 | 0.0144 |
| 1.4993 |  |  |  |  |  |  |  |
| 19.8543 | 19.8535 | 19.8528 | 19.8524 | 19.8522 | 19.8522 | 1.4992 | 7945.6021 |
| 1.9194 | 1.9108 | 1.9022 | 1.8935 | 1.8849 | 1.8763 | 1.8676 | 1.8590 |
| 1.8504 | 1.8418 | 1.8332 | 1.8246 | 1.8160 | 1.8074 | 1.7988 | 0.0144 |
| 1.5029 |  |  |  |  |  |  |  |
| 19.9021 | 19.9013 | 19.9007 | 19.9002 | 19.9000 | 19.9000 | 1.5028 | 8029.2402 |
| 1.9194 | 1.9110 | 1.9025 | 1.8940 | 1.8855 | 1.8770 | 1.8685 | 1.8600 |
| 1.8515 | 1.8430 | 1.8346 | 1.8261 | 1.8177 | 1.8092 | 1.8008 | 0.0144 |
| 1.5065 |  |  |  |  |  |  |  |
| 19.9491 | 19.9483 | 19.9477 | 19.9473 | 19.9471 | 19.9471 | 1.5064 | 8112.8779 |
| 1.9194 | 1.9111 | 1.9027 | 1.8944 | 1.8860 | 1.8777 | 1.8693 | 1.8610 |
| 1.8526 | 1.8443 | 1.8360 | 1.8276 | 1.8193 | 1.8110 | 1.8027 | 0.0144 |
| 1.5100 |  |  |  |  |  |  |  |
| 19.9954 | 19.9946 | 19.9940 | 19.9936 | 19.9934 | 19.9934 | 1.5099 | 8196.5156 |
| 1.9194 | 1.9112 | 1.9030 | 1.8948 | 1.8866 | 1.8783 | 1.8701 | 1.8619 |
| 1.8537 | 1.8455 | 1.8373 | 1.8291 | 1.8210 | 1.8128 | 1.8046 | 0.0144 |
| 1.5134 |  |  |  |  |  |  |  |
| 20.0409 | 20.0401 | 20.0395 | 20.0391 | 20.0389 | 20.0389 | 1.5133 | 8280.1543 |
| 1.9194 | 1.9114 | 1.9033 | 1.8952 | 1.8871 | 1.8790 | 1.8709 | 1.8629 |
| 1.8548 | 1.8467 | 1.8386 | 1.8306 | 1.8225 | 1.8145 | 1.8065 | 0.0144 |
| 1.5168 |  |  |  |  |  |  |  |
| 20.0856 | 20.0849 | 20.0843 | 20.0839 | 20.0837 | 20.0837 | 1.5167 | 8363.7920 |
| 1.9194 | 1.9115 | 1.9035 | 1.8956 | 1.8876 | 1.8797 | 1.8717 | 1.8638 |
| 1.8558 | 1.8479 | 1.8400 | 1.8320 | 1.8241 | 1.8162 | 1.8083 | 0.0145 |
| 1.5201 |  |  |  |  |  |  |  |
| 20.1297 | 20.1289 | 20.1284 | 20.1280 | 20.1278 | 20.1278 | 1.5200 | 8447.4297 |
| 1.9194 | 1.9116 | 1.9038 | 1.8960 | 1.8881 | 1.8803 | 1.8725 | 1.8647 |
| 1.8568 | 1.8490 | 1.8412 | 1.8334 | 1.8256 | 1.8178 | 1.8101 | 0.0145 |
| 1.5234 |  |  |  |  |  |  |  |
| 20.1730 | 20.1723 | 20.1717 | 20.1713 | 20.1712 | 20.1712 | 1.5233 | 8531.0674 |
| 1.9194 | 1.9117 | 1.9040 | 1.8963 | 1.8886 | 1.8809 | 1.8732 | 1.8655 |
| 1.8578 | 1.8502 | 1.8425 | 1.8348 | 1.8271 | 1.8195 | 1.8118 | 0.0145 |
| 1.5266 |  |  |  |  |  |  |  |
| 20.2157 | 20.2149 | 20.2144 | 20.2140 | 20.2138 | 20.2138 | 1.5265 | 8614.7051 |
| 1.9194 | 1.9119 | 1.9043 | 1.8967 | 1.8891 | 1.8815 | 1.8740 | 1.8664 |

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| 1.8588 | 1.8513 | 1.8437 | 1.8361 | 1.8286 | 1.8211 | 1.8135 | 0.0145 |
| ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 1.5298 |  |  |  |  |  |  |  |
| 20.2576 | 20.2569 | 20.2564 | 20.2560 | 20.2558 | 20.2558 | 1.5297 | 8698.3438 |
| 1.9194 | 1.9120 | 1.9045 | 1.8971 | 1.8896 | 1.8821 | 1.8747 | 1.8672 |
| 1.8598 | 1.8523 | 1.8449 | 1.8375 | 1.8300 | 1.8226 | 1.8152 | 0.0145 |
| 1.5329 |  |  |  |  |  |  |  |
| 20.2989 | 20.2982 | 20.2977 | 20.2973 | 20.2972 | 20.2972 | 1.5328 | 8781.9814 |
| 1.9194 | 1.9121 | 1.9048 | 1.8974 | 1.8901 | 1.8827 | 1.8754 | 1.8681 |
| 1.8607 | 1.8534 | 1.8461 | 1.8388 | 1.8314 | 1.8241 | 1.8168 | 0.0145 |
| 1.5360 |  |  |  |  |  |  |  |
| 20.3396 | 20.3389 | 20.3384 | 20.3380 | 20.3378 | 20.3378 | 1.5359 | 8865.6191 |
| 1.9194 | 1.9122 | 1.9050 | 1.8978 | 1.8905 | 1.8833 | 1.8761 | 1.8689 |
| 1.8616 | 1.8544 | 1.8472 | 1.8400 | 1.8328 | 1.8256 | 1.8185 | 0.0145 |
| 1.5390 |  |  |  |  |  |  |  |
| 20.3796 | 20.3789 | 20.3784 | 20.3780 | 20.3779 | 20.3779 | 1.5389 | 8949.2568 |
| 1.9194 | 1.9123 | 1.9052 | 1.8981 | 1.8910 | 1.8839 | 1.8768 | 1.8697 |
| 1.8626 | 1.8555 | 1.8484 | 1.8413 | 1.8342 | 1.8271 | 1.8200 | 0.0145 |
| 1.5419 |  |  |  |  |  |  |  |
| 20.4190 | 20.4183 | 20.4178 | 20.4175 | 20.4173 | 20.4173 | 1.5419 | 9032.8945 |
| 1.9194 | 1.9124 | 1.9054 | 1.8984 | 1.8914 | 1.8844 | 1.8774 | 1.8704 |
| 1.8634 | 1.8565 | 1.8495 | 1.8425 | 1.8355 | 1.8286 | 1.8216 | 0.0146 |
| 1.5449 |  |  |  |  |  |  |  |
| 20.4577 | 20.4571 | 20.4566 | 20.4562 | 20.4561 | 20.4561 | 1.5448 | 9116.5332 |
| 1.9194 | 1.9126 | 1.9057 | 1.8988 | 1.8919 | 1.8850 | 1.8781 | 1.8712 |
| 1.8643 | 1.8574 | 1.8506 | 1.8437 | 1.8368 | 1.8300 | 1.8231 | 0.0146 |
| 1.5478 |  |  |  |  |  |  |  |
| 20.4959 | 20.4953 | 20.4948 | 20.4944 | 20.4943 | 20.4943 | 1.5477 | 9200.1709 |

All data are checked successfully !!!
Re-check all data entered

```
Temperature of storage environment incelsius \(\mathbf{= 2 5 . 0 0}\)
Relative humidity of storage environment in \(=90.00\)
Absolute humidity of storage environment ingH20/gAir \(=.0183\)
Diffusion coefficient of packaging materialin \(10^{\wedge}-7 \mathrm{~cm} \wedge 2 / \mathrm{sec}=0.020\)
Henry constant of packaging material in (gH2O/cm^3 PKG)/(gH2O/cm^3 Air)=125.12 000
Thickness of packaging material in \(\mathrm{cm}=0.02300\)
Surface area of packaging material in cm^2 - 3.78000
Volume of packaging material in \(\mathrm{cm}^{\wedge} 3=0.80000\)
Diffusion coefficient of product in \(10^{\wedge}-5 \mathrm{~cm} \wedge 2 / \mathrm{sec}=0.11790\)
Initial moisture content in \(\mathbf{g H 2 O} / 100 \mathrm{~g}\) dryproduct \(=0.00\)
Critical moisture content in \(\mathbf{g H 2 0 / 1 0 0 g}\) dryproduct \(\mathbf{~} 2.00\)
Dry weight of product in \(g=0.40770\)
Chemical reaction rate \(=0.0\)
Chemical reaction order \(=0.0\)
\(A w / M=-1790 \mathrm{E}+01 \mathrm{Aw}\) ^2 \(+0.1922 \mathrm{E}+01 \mathrm{Aw}+0.6400 \mathrm{E}-01\)
Radius of product in \(\mathrm{cm}=0.50000\)
Thickness of product (Only Plate shape) incm - 0.39200
Hit any key to continue.....
INITIAL CONCENTRATION
```

```
Concentration of outside environment (CE) = 0.01938 g/L
```

Concentration of outside environment (CE) = 0.01938 g/L
Concentration of outside surface of PKG(CLE) = 2.42433 g/L
Concentration of outside surface of PKG(CLE) = 2.42433 g/L
Concentration of inside surface of PKG(CLH) = 0.00002 g/L
Concentration of inside surface of PKG(CLH) = 0.00002 g/L
Concentration of headspace (CH) = 0.00000 g/L
Concentration of headspace (CH) = 0.00000 g/L
Concentration of outside surface of product (CRH) = 0.00132 g/L

```
Concentration of outside surface of product (CRH) = 0.00132 g/L
```


## dIMENSSIONLESS CONSTANT

```
Q=0.1260E-02
G=0.1700E-02
```

A1-0.1815E-04
B1=0.2127E-03
$S=0.2215 E+01$
$X=0.9000 E+03$
$=13$


Hit any key to continue ......
Enter the number of time to calculateconcentrations at once.
<NOTICE !!! It must be over 200 and be times of 200>
(Plate Shape)
Each step is 137000 . steps ( 84.3120 hrs )
< of the divided shell of product is
5

| CLE CRH | $\begin{aligned} & \text { CL1 } \\ & \text { CR1 } \end{aligned}$ | $\begin{aligned} & \mathrm{CL} 2 \\ & \mathrm{CR} 2 \end{aligned}$ | $\begin{aligned} & \text { CL3 } \\ & \text { CR3 } \end{aligned}$ | CL4 CR4 | CRH | $\begin{array}{r} \mathrm{CH} \\ \text { GAIN } \end{array}$ | $\begin{gathered} \text { Meq } \\ \text { TIME (hrs) } \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.2386 | 2.0528 | 1.8670 | 1.6813 | 1.4956 | 1.3099 | 1.1243 |
| 0.9387 | 0.7532 | 0.5678 | 0.3824 | 0.1971 | 0.0118 | 0.0001 | 0.0607 |
| 0.8037 | 0.7879 | 0.7761 | 0.7682 | 0.7642 | 0.7642 | 0.0586 | 84.3120 |
| 2.4243 | 2.2399 | 2.0554 | 1.8710 | 1.6866 | 1.5023 | 1.3179 | 1.1337 |
| 0.9495 | 0.7653 | 0.5813 | 0.3973 | 0.2135 | 0.0297 | 0.0002 | 0.1299 |
| 1.7200 | 1.7043 | 1.6925 | 1.6847 | 1.6808 | 1.6808 | 0.1278 | 168.6240 |
| 2.4243 | 2.2417 | 2.0591 | 1.8765 | 1.6939 | 1.5114 | 1.3289 | 1.1466 |
| 0.9643 | 0.7821 | 0.6000 | 0.4181 | 0.2363 | 0.0546 | 0.0004 | 0.1984 |
| 2.6272 | 2.6117 | 2.6001 | 2.5923 | 2.5884 | 2.5884 | 0.1963 | 252.9361 |
| 2.4243 | 2.2443 | 2.0643 | 1.8843 | 1.7044 | 1.5246 | 1.3448 | 1.1652 |
| 0.9857 | 0.8063 | 0.6271 | 0.4481 | 0.2693 | 0.0908 | 0.0007 | 0.2659 |
| 3.5213 | 3.5061 | 3.4947 | 3.4871 | 3.4833 | 3.4833 | 0.2639 | 337.2481 |
| 2.4243 | 2.2482 | 2.0721 | 1.8961 | 1.7202 | 1.5443 | 1.3687 | 1.1931 |
| 1.0178 | 0.8427 | 0.6679 | 0.4933 | 0.3191 | 0.1452 | 0.0012 | 0.3320 |
| 4.3960 | 4.3811 | 4.3700 | 4.3626 | 4.3589 | 4.3589 | 0.3300 | 421.5601 |
| 2.4243 | 2.2542 | 2.0841 | 1.9141 | 1.7442 | 1.5744 | 1.4049 | 1.2357 |
| 1.0667 | 0.8981 | 0.7299 | 0.5621 | 0.3947 | 0.2280 | 0.0018 | 0.3958 |
| 5.2408 | 5.2266 | 5.2160 | 5.2088 | 5.2053 | 5.2053 | 0.3939 | 505.8722 |
| 2.4243 | 2.2628 | 2.1013 | 1.9399 | 1.7788 | 1.6178 | 1.4571 | 1.2968 |
| 1.1369 | 0.9774 | 0.8185 | 0.6601 | 0.5024 | 0.3455 | 0.0028 | 0.4563 |
| 6.0426 | 6.0292 | 6.0192 | 6.0125 | 6.0092 | 6.0092 | 0.4545 | 590.1841 |
| 2.4243 | 2.2736 | 2.1229 | 1.9723 | 1.8220 | 1.6719 | 1.5221 | 1.3728 |
| 1.2239 | 1.0755 | 0.9277 | 0.7806 | 0.6342 | 0.4886 | 0.0039 | 0.5128 |
| 6.7904 | 6.7780 | 6.7687 | 6.7625 | 6.7594 | 6.7594 | 0.5111 | 674.4962 |
| 2.4243 | 2.2850 | 2.1457 | 2.0065 | 1.8676 | 1.7289 | 1.5905 | 1.4525 |
| 1.3150 | 1.1780 | 1.0415 | 0.9057 | 0.7706 | 0.6363 | 0.0051 | 0.5649 |
| 7.4812 | 7.4698 | 7.4612 | 7.4555 | 7.4526 | 7.4526 | 0.5634 | 758.8082 |
| 2.4243 | 2.2957 | 2.1671 | 2.0387 | 1.9104 | 1.7823 | 1.6546 | 1.5271 |
| 1.4001 | 1.2736 | 1.1476 | 1.0222 | 0.8974 | 0.7733 | 0.0062 | 0.6131 |
| 8.1188 | 8.1082 | 8.1003 | 8.0950 | 8.0924 | 8.0924 | 0.6117 | 843.1202 |
| 2.4243 | 2.3052 | 2.1861 | 2.0672 | 1.9483 | 1.8297 | 1.7114 | 1.5933 |
| 1.4756 | 1.3584 | 1.2415 | 1.1252 | 1.0095 | 0.8943 | 0.0071 | 0.6577 |
| 8.7092 | 8.6994 | 8.6920 | 8.6871 | 8.6847 | 8.6847 | 0.6564 | 927.4323 |
| 2.4243 | 2.3135 | 2.2027 | 2.0920 | 1.9814 | 1.8710 | 1.7608 | 1.6509 |
| 1.5413 | 1.4321 | 1.3233 | 1.2149 | 1.1069 | 0.9995 | 0.0080 | 0.6992 |
| 9.2586 | 9.2495 | 9.2426 | 9.2381 | 9.2358 | 9.2358 | 0.6980 | 1011.7443 |
| 2.4243 | 2.3207 | 2.2171 | 2.1135 | 2.0101 | 1.9069 | 1.8038 | 1.7010 |
| 1.5984 | 1.4962 | 1.3942 | 1.2927 | 1.1916 | 1.0910 | 0.0087 | 0.7380 |
| 9.7725 | 9.7639 | 9.7575 | 9.7532 | 9.7511 | 9.7511 | 0.7368 | 1096.0563 |
| 2.4243 | 2.3270 | 2.2296 | 2.1323 | 2.0352 | 1.9381 | 1.8413 | 1.7446 |
| 1.6482 | 1.5520 | 1.4562 | 1.3607 | 1.2655 | 1.1708 | 0.0094 | 0.7744 |
| 10.2553 | 10.2473 | 10.2412 | 10.2372 | 10.2352 | 10.2352 | 0.7734 | 1180.3683 |
| 2.4243 | 2.3325 | 2.2406 | 2.1489 | 2.0572 | 1.9656 | 1.8742 | 1.7829 |
| 1.6919 | 1.6011 | 1.5106 | 1.4204 | 1.3304 | 1.2409 | 0.0099 | 0.8088 |
| 10.7109 | 10.7033 | 10.6976 | 10.6938 | 10.6919 | 10.6919 | 0.8078 | 1264.6804 |
| 2.4243 | 2.3373 | 2.2504 | 2.1634 | 2.0766 | 1.9899 | 1.9033 | 1.8168 |
| 1.7306 | 1.6445 | 1.5587 | 1.4732 | 1.3879 | 1.3030 | 0.0104 | 0.8414 |
| 11.1424 | 11.1352 | 11.1298 | 11.1261 | 11.1243 | 11.1243 | 0.8405 | 1348.9923 |
| 2.4243 | 2.3417 | 2.2590 | 2.1764 | 2.0939 | 2.0115 | 1.9292 | 1.8470 |
| 1.7650 | 1.6832 | 1.6016 | 1.5203 | 1.4392 | 1.3583 | 0.0109 | 0.8724 |
| 11.5525 | 11.5456 | 11.5404 | 11.5370 | 11.5353 | 11.5353 | 0.8715 | 1433.3044 |
| 2.4243 | 2.3456 | 2.2668 | 2.1881 | 2.1095 | 2.0309 | 1.9525 | 1.8741 |
| 1.7960 | 1.7179 | 1.6401 | 1.5625 | 1.4852 | 1.4080 | 0.0113 | 0.9019 |


| 32 | 11.9367 | 17 | 11.9285 | 11.9268 | 11.9268 | 9010 | 63 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.3491 | 2.2738 | 2.1986 | 2.1235 | 2.0484 | 1.9734 | 1.8986 |
| 1.8239 | 1.7493 | 1.6749 | 1.6007 | 1.5267 | 1.4529 | 0.0116 | 0.9301 |
| 12.3166 | 12.3104 | 12.3057 | 12.3025 | 12.3009 | 12.3009 | 0.9293 | 1601.9285 |
| 2.4243 | 2.3523 | 2.2802 | 2.2082 | 2.1362 | 2.0643 | 1.9925 | 1.9208 |
| 1.8492 | 1.7778 | 1.7065 | 1.6354 | 1.5644 | 1.4937 | 0.0119 | 0.9571 |
| 12.6743 | 12.6682 | 12.6637 | 12.6607 | 12.6592 | 12.6592 | 0.9563 | 1686.2404 |
| 2.4243 | 2.3552 | 2.2860 | 2.2169 | 2.1478 | 2.0788 | 2.0099 | 1.9410 |
| 1.8723 | 1.8037 | 1.7353 | 1.6670 | 1.5989 | 1.5310 | 0.0122 | 0.9830 |
| 13.0175 | 13.0117 | 13.0074 | 13.0045 | 13.0030 | 13.0030 | 0.9823 | 1770.5525 |
| 2.4243 | 2.3578 | 2.2913 | 2.2249 | 2.1585 | 2.0921 | 2.0258 | 1.9596 |
| 1.8935 | 1.8275 | 1.7617 | 1.6960 | 1.6305 | 1.5651 | 0.0125 | 1.0079 |
| 13.3475 | 13.3420 | 13.3378 | 13.3350 | 13.3336 | 13.3336 | 1.0072 | 1854.8646 |
| 2.4243 | 2.3603 | 2.2962 | 2.2322 | 2.1683 | 2.1043 | 2.0405 | 1.9767 |
| 1.9130 | 1.8495 | 1.7860 | 1.7227 | 1.6596 | 1.5966 | 0.0128 | 1.0319 |
| 13.6654 | 13.6601 | 13.6560 | 13.6533 | 13.6520 | 13.6520 | 1.0312 | 1939.1765 |
| 2.4243 | 2.3625 | 2.3008 | 2.2390 | 2.1773 | 2.1156 | 2.0540 | 1.9925 |
| 1.9311 | 1.8698 | 1.8085 | 1.7474 | 1.6865 | 1.6257 | 0.0130 | 1.0551 |
| 13.9721 | 13.9669 | 13.9630 | 13.9604 | 13.9591 | 13.9591 | 1.0544 | 2023.4886 |
| 2.4243 | 2.3646 | 2.3050 | 2.2453 | 2.1857 | 2.1261 | 2.0666 | 2.0072 |
| 1.9478 | 1.8886 | 1.8294 | 1.7704 | 1.7114 | 1.6527 | 0.0132 | 1.0775 |
| 14.2683 | 14.2633 | 14.2595 | 14.2570 | 14.2558 | 14.2558 | 1.0768 | 2107.8005 |
| 2.4243 | 2.3666 | 2.3089 | 2.2512 | 2.1935 | 2.1359 | 2.0783 | 2.0208 |
| 1.9634 | 1.9061 | 1.8488 | 1.7917 | 1.7347 | 1.6778 | 0.0134 | 1.0991 |
| 14.5548 | 14.5500 | 14.5464 | 14.5439 | 14.5427 | 14.5427 | 1.0985 | 2192.1125 |
| 2.4243 | 2.3684 | 2.3125 | 2.2567 | 2.2008 | 2.1450 | 2.0893 | 2.0336 |
| 1.9780 | 1.9224 | 1.8670 | 1.8116 | 1.7564 | 1.7013 | 0.0136 | 1.1201 |
| 14.8323 | 14.8276 | 14.8241 | 14.8218 | 14.8206 | 14.8206 | 1.1194 | 2276.4248 |
| 2.4243 | 2.3701 | 2.3160 | 2.2618 | 2.2077 | 2.1536 | 2.0995 | 2.0455 |
| 1.9916 | 1.9377 | 1.8840 | 1.8303 | 1.7767 | 1.7233 | 0.0138 | 1.1404 |
| 15.1013 | 15.0968 | 15.0934 | 15.0911 | 15.0899 | 15.0899 | 1.1398 | 2360.7366 |
| 2.4243 | 2.3717 | 2.3192 | 2.2666 | 2.2141 | 2.1616 | 2.1091 | 2.0567 |
| 2.0044 | 1.9521 | 1.8999 | 1.8478 | 1.7958 | 1.7439 | 0.0139 | 1.1601 |
| 15.3624 | 15.3580 | 15.3546 | 15.3524 | 15.3513 | 15.3513 | 1.1595 | 445.0486 |
| 2.4243 | 2.3733 | 2.3222 | 2.2711 | 2.2201 | 2.1691 | 2.1181 | 2.0672 |
| 2.0164 | 1.9656 | 1.9149 | 1.8643 | 1.8138 | 1.7633 | 0.0141 | 1.1792 |
| 15.6159 | 15.6117 | 15.6084 | 15.6063 | 15.6052 | 15.6052 | 1.1787 | 2529.3608 |
| 2.4243 | 2.3747 | 2.3250 | 2.2754 | 2.2258 | 2.1762 | 2.1267 | 2.0772 |
| 2.0277 | 1.9784 | 1.9291 | 1.8798 | 1.8307 | 1.7817 | 0.0142 | 1.1979 |
| 15.8625 | 15.8583 | 15.8552 | 15.8531 | 15.8520 | 15.8520 | 1.1973 | 2613.6729 |
| 2.4243 | 2.3760 | 2.3277 | 2.2794 | 2.2311 | 2.1829 | 2.1347 | 2.0865 |
| 2.0384 | 1.9904 | 1.9424 | 1.8945 | 1.8467 | 1.7990 | 0.0144 | 1.2160 |
| 16.1023 | 16.0982 | 16.0952 | 16.0932 | 16.0921 | 16.0921 | 1.2154 | 2697.9846 |
| 2.4243 | 2.3773 | 2.3303 | 2.2832 | 2.2362 | 2.1893 | 2.1423 | 2.0954 |
| 2.0486 | 2.0018 | 1.9551 | 1.9084 | 1.8619 | 1.8154 | 0.0145 | 1.2336 |
| 16.3359 | 16.3319 | 16.3289 | 16.3269 | 16.3260 | 16.3260 | 1.2331 | 2782.2966 |
| 2.4243 | 2.3785 | 2.3327 | 2.2868 | 2.2411 | 2.1953 | 2.1495 | 2.1039 |
| 2.0582 | 2.0126 | 1.9671 | 1.9216 | 1.8762 | 1.8309 | 0.0146 | 1.2508 |
| 16.5634 | 16.5596 | 16.5567 | 16.5547 | 16.5538 | 16.5538 | 1.2503 | 2866.6089 |
| 2.4243 | 2.3796 | 2.3350 | 2.2903 | 2.2456 | 2.2010 | 2.1564 | 2.1119 |
| 2.0673 | 2.0229 | 1.9785 | 1.9341 | 1.8899 | 1.8457 | 0.0148 | 1.2675 |
| 16.7853 | 16.7815 | 16.7787 | 16.7768 | 16.7759 | 16.7759 | 1.2670 | 2950.9209 |
| 2.4243 | 2.3807 | 2.3371 | 2.2936 | 2.2500 | 2.2064 | 2.1629 | 2.1195 |
| 2.0760 | 2.0327 | 1.9893 | 1.9461 | 1.9029 | 1.8597 | 0.0149 | 1.2839 |
| 17.0018 | 16.9981 | 16.9953 | 16.9935 | 16.9926 | 16.9926 | 1.2834 | 3035.2327 |
| 2.4243 | 2.3818 | 2.3392 | 2.2967 | 2.2541 | 2.2116 | 2.1692 | 2.1267 |
| 2.0843 | 2.0420 | 1.9997 | 1.9574 | 1.9152 | 1.8731 | 0.0150 | 1.2999 |
| 17.2131 | 17.2095 | 17.2068 | 17.2050 | 17.2041 | 17.2041 | 1.2994 | 3119.5449 |
| 2.4243 | 2.3828 | 2.3412 | 2.2996 | 2.2581 | 2.2166 | 2.1751 | 2.1336 |
| 2.0922 | 2.0508 | 2.0095 | 1.9683 | 1.9270 | 1.8859 | 0.0151 | 1.3154 |

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| 17.4195 | 17.4160 | 17.4134 | 17.4116 | 17.4107 | 17.4107 | 1.3150 | 3203.8569 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.3837 | 2.3431 | 2.3025 | 2.2619 | 2.2213 | 2.1808 | 2.1402 |
| 2.0998 | 2.0593 | 2.0189 | 1.9786 | 1.9383 | 1.8981 | 0.0152 | 1.3307 |
| 17.6212 | 17.6178 | 17.6152 | 17.6135 | 17.6126 | 17.6126 | 1.3302 | 3288.1689 |
| 2.4243 | 2.3846 | 2.3449 | 2.3052 | 2.2655 | 2.2258 | 2.1862 | 2.1466 |
| 2.1070 | 2.0674 | 2.0280 | 1.9885 | 1.9491 | 1.9098 | 0.0153 | 1.3456 |
| 17.8184 | 17.8151 | 17.8126 | 17.8109 | 17.8100 | 17.8100 | 1.3451 | 3372.4807 |
| 2.4243 | 2.3855 | 2.3466 | 2.3078 | 2.2690 | 2.2302 | 2.1914 | 2.1526 |
| 2.1139 | 2.0752 | 2.0366 | 1.9980 | 1.9595 | 1.9210 | 0.0154 | 1.3601 |
| 18.0113 | 18.0081 | 18.0056 | 18.0040 | 18.0031 | 18.0031 | 1.3597 | 56.7930 |
| 2.4243 | 2.3863 | 2.3483 | 2.3103 | 2.2723 | 2.2343 | 2.1963 | 2.1584 |
| 2.1205 | 2.0827 | 2.0449 | 2.0071 | 1.9694 | 1.9317 | 0.0154 | 1.3744 |
| 18.2001 | 18.1969 | 18.1945 | 18.1929 | 18.1921 | 18.1921 | 1.3740 | 3541.1050 |
| 2.4243 | 2.3871 | 2.3499 | 2.3127 | 2.2755 | 2.2383 | 2.2011 | 2.1640 |
| 2.1269 | 2.0898 | 2.0528 | 2.0158 | 1.9789 | 1.9420 | 0.0155 | 1.3883 |
| 18.3850 | 18.3818 | 18.3795 | 18.3779 | 18.3771 | 18.3771 | 1.3879 | 625.4170 |
| 2.4243 | 2.3879 | 2.3514 | 2.3150 | 2.2785 | 2.2421 | 2.2057 | 2.1693 |
| 2.1330 | 2.0967 | 2.0604 | 2.0242 | 1.9880 | 1.9519 | 0.0156 | 1.4020 |
| 18.5660 | 18.5629 | 18.5606 | 18.5591 | 18.5583 | 18.5583 | 1.4016 | 709.7292 |
| 2.4243 | 2.3886 | 2.3529 | 2.3172 | 2.2815 | 2.2458 | 2.2101 | 2.1745 |
| 2.1389 | 2.1033 | 2.0678 | 2.0323 | 1.9968 | 1.9614 | 0.0157 | 1.4154 |
| 18.7434 | 18.7404 | 18.7381 | 18.7366 | 18.7359 | 18.7359 | 1.4150 | 94.0410 |
| 2.4243 | 2.3893 | 2.3543 | 2.3193 | 2.2843 | 2.2493 | 2.2144 | 2.1794 |
| 2.1445 | 2.1097 | 2.0748 | 2.0400 | 2.0053 | 1.9706 | 0.0157 | 1.4285 |
| 18.9173 | 18.9143 | 18.9121 | 18.9106 | 18.9099 | 18.9099 | 1.4282 | 78.3530 |
| 2.4243 | 2.3900 | 2.3557 | 2.3213 | 2.2870 | 2.2527 | 2.2185 | 2.1842 |
| 2.1500 | 2.1158 | 2.0816 | 2.0475 | 2.0134 | 1.9794 | 0.0158 | 1.4414 |
| 19.0878 | 19.0849 | 19.0827 | 19.0812 | 19.0805 | 19.0805 | 1.4410 | 962.6653 |
| 2.4243 | 2.3907 | 2.3570 | 2.3233 | 2.2897 | 2.2560 | 2.2224 | 2.1888 |
| 2.1552 | 2.1217 | 2.0882 | 2.0547 | 2.0213 | 1.9879 | 0.0159 | 1.4540 |
| 19.2550 | 19.2521 | 19.2500 | 19.2486 | 19.2479 | 19.2479 | 1.4537 | 046.9773 |
| 2.4243 | 2.3913 | 2.3583 | 2.3252 | 2.2922 | 2.2592 | 2.2262 | 2.1932 |
| 2.1603 | 2.1274 | 2.0945 | 2.0617 | 2.0289 | 1.9961 | 0.0160 | 1.4664 |
| 19.4190 | 19.4163 | 19.4142 | 19.4128 | 19.4121 | 19.4121 | 1.4661 | 131.2891 |
| 2.4243 | 2.3919 | 2.3595 | 2.3271 | 2.2947 | 2.2623 | 2.2299 | 2.1975 |
| 2.1652 | 2.1329 | 2.1006 | 2.0684 | 2.0362 | 2.0040 | 0.0160 | 1.4786 |
| 19.5801 | 19.5773 | 19.5753 | 19.5739 | 19.5732 | 19.5732 | 1.4782 | 4215.6011 |
| 2.4243 | 2.3925 | 2.3607 | 2.3288 | 2.2970 | 2.2652 | 2.2334 | 2.2017 |
| 2.1699 | 2.1382 | 2.1065 | 2.0749 | 2.0433 | 2.0117 | 0.0161 | 1.4905 |
| 19.7382 | 19.7355 | 19.7334 | 19.7321 | 19.7314 | 19.7314 | 1.4902 | 4299.9136 |
| 2.4243 | 2.3931 | 2.3618 | 2.3306 | 2.2993 | 2.2681 | 2.2369 | 2.2057 |
| 2.1745 | 2.1434 | 2.1122 | 2.0812 | 2.0501 | 2.0191 | 0.0161 | 1.5023 |
| 19.8934 | 19.8907 | 19.8888 | 19.8874 | 19.8868 | 19.8868 | 1.5019 | 4384.2251 |
| 2.4243 | 2.3936 | 2.3629 | 2.3322 | 2.3015 | 2.2709 | 2.2402 | 2.2095 |
| 2.1789 | 2.1483 | 2.1178 | 2.0872 | 2.0567 | 2.0263 | 0.0162 | 1.5138 |
| 20.0459 | 20.0433 | 20.0413 | 20.0400 | 20.0394 | 20.0394 | 1.5134 | 4468.5371 |
| 2.4243 | 2.3942 | 2.3640 | 2.3338 | 2.3037 | 2.2735 | 2.2434 | 2.2133 |
| 2.1832 | 2.1531 | 2.1231 | 2.0931 | 2.0631 | 2.0332 | 0.0163 | 1.5251 |
| 20.1957 | 20.1932 | 20.1912 | 20.1900 | 20.1893 | 20.1893 | 1.5247 | 4552.8496 |
| 2.4243 | 2.3947 | 2.3650 | 2.3354 | 2.3058 | 2.2761 | 2.2465 | 2.2169 |
| 2.1874 | 2.1578 | 2.1283 | 2.0988 | 2.0693 | 2.0399 | 0.0163 | 1.5362 |
| 20.3429 | 20.3404 | 20.3386 | 20.3373 | 20.3367 | 20.3367 | 1.5359 | 4637.1616 |
| 2.4243 | 2.3952 | 2.3660 | 2.3369 | 2.3078 | 2.2786 | 2.2495 | 2.2205 |
| 2.1914 | 2.1623 | 2.1333 | 2.1043 | 2.0754 | 2.0464 | 0.0164 | 1.5471 |
| 20.4877 | 20.4852 | 20.4834 | 20.4821 | 20.4815 | 20.4815 | 1.5468 | 4721.4731 |
| 2.4243 | 2.3957 | 2.3670 | 2.3384 | 2.3097 | 2.2811 | 2.2525 | 2.2239 |
| 2.1953 | 2.1667 | 2.1382 | 2.1097 | 2.0812 | 2.0528 | 0.0164 | 1.5579 |
| 20.6300 | 20.6276 | 20.6258 | 20.6246 | 20.6240 | 20.6240 | 1.5576 | 4805.7856 |
| 2.4243 | 2.3961 | 2.3680 | 2.3398 | 2.3116 | 2.2835 | 2.2553 | 2.2272 |
| 2.1991 | 2.1710 | 2.1429 | 2.1149 | 2.0869 | 2.0589 | 0.0165 | 1.5685 |


| 20.7700 | 20.7676 | 20.7658 | 20.7646 | 20.7640 | 20.7640 | 1.5681 | 4890.0972 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.3966 | 2.3689 | 2.3412 | 2.3135 | 2.2858 | 2.2581 | 2.2304 |
| 2.2027 | 2.1751 | 2.1475 | 2.1199 | 2.0924 | 2.0649 | 0.0165 | 1.5788 |
| 20.9077 | 20.9053 | 20.9036 | 20.9024 | 20.9018 | 20.9018 | 1.5785 | 4974.4097 |
| 2.4243 | 2.3971 | 2.3698 | 2.3425 | 2.3152 | 2.2880 | 2.2607 | 2.2335 |
| 2.2063 | 2.1791 | 2.1520 | 2.1248 | 2.0977 | 2.0706 | 0.0165 | 1.5891 |
| 21.0431 | 21.0408 | 21.0391 | 21.0379 | 21.0374 | 21.0374 | 1.58888 | 5058.7217 |
| 2.4243 | 2.3975 | 2.3706 | 2.3438 | 2.3170 | 2.2902 | 2.2634 | 2.2366 |
| 2.2098 | 2.1830 | 2.1563 | 2.1296 | 2.1029 | 2.0763 | 0.0166 | 1.5991 |
| 21.1764 | 21.1742 | 21.1725 | 21.1713 | 21.1708 | 21.1708 | 1.5988 | 143.0332 |
| 2.4243 | 2.3979 | 2.3715 | 2.3451 | 2.3187 | 2.2923 | 2.2659 | 2.2395 |
| 2.2132 | 2.1868 | 2.1605 | 2.1342 | 2.1080 | 2.0817 | 0.0166 | 1.6091 |
| 21.3076 | 21.3054 | 21.3037 | 21.3026 | 21.3021 | 21.3021 | 1.6088 | 5227.3457 |
| 2.4243 | 2.3983 | 2.3723 | 2.3463 | 2.3203 | 2.2943 | 2.2683 | 2.2424 |
| 2.2164 | 2.1905 | 2.1646 | 2.1387 | 2.1129 | 2.0870 | 0.0167 | 1.6188 |
| 21.4368 | 21.4346 | 21.4330 | 21.4319 | 21.4313 | 21.4313 | 1.6185 | 5311.6577 |
| 2.4243 | 2.3987 | 2.3731 | 2.3475 | 2.3219 | 2.2963 | 2.2707 | 2.2452 |
| 2.2196 | 2.1941 | 2.1686 | 2.1431 | 2.1177 | 2.0922 | 0.0167 | 1.6284 |
| 21.5640 | 21.5618 | 21.5602 | 21.5591 | 21.5586 | 21.5586 | 1.6281 | 395.9692 |
| 2.4243 | 2.3991 | 2.3739 | 2.3487 | 2.3235 | 2.2983 | 2.2731 | 2.2479 |
| 2.2227 | 2.1976 | 2.1725 | 2.1474 | 2.1223 | 2.0973 | 0.0168 | 1.6379 |
| 21.6893 | 21.6871 | 21.6855 | 21.6844 | 21.6839 | 21.6839 | 1.6376 | 5480.2817 |
| 2.4243 | 2.3995 | 2.3747 | 2.3498 | 2.3250 | 2.3002 | 2.2754 | 2.2506 |
| 2.2258 | 2.2010 | 2.1763 | 2.1515 | 2.1268 | 2.1022 | 0.0168 | 1.6472 |
| 21.8126 | 21.8105 | 21.8089 | 21.8079 | 21.8074 | 21.8074 | 1.6469 | 5564.5933 |
| 2.4243 | 2.3999 | 2.3754 | 2.3509 | 2.3265 | 2.3020 | 2.2776 | 2.2531 |
| 2.2287 | 2.2043 | 2.1799 | 2.1556 | 2.1313 | 2.1069 | 0.0168 | 1.6564 |
| 21.9342 | 21.9321 | 21.9305 | 21.9295 | 21.9290 | 21.9290 | 1.6561 | 5648.9058 |
| 2.4243 | 2.4002 | 2.3761 | 2.3520 | 2.3279 | 2.3038 | 2.2797 | 2.2557 |
| 2.2316 | 2.2076 | 2.1835 | 2.1595 | 2.1356 | 2.1116 | 0.0169 | 1.6654 |
| 22.0539 | 22.0519 | 22.0503 | 22.0493 | 22.0488 | 22.0488 | 1.6651 | 5733.2178 |
| 2.4243 | 2.4006 | 2.3768 | 2.3531 | 2.3293 | 2.3056 | 2.2818 | 2.2581 |
| 2.2344 | 2.2107 | 2.1870 | 2.1634 | 2.1398 | 2.1162 | 0.0169 | 1.6743 |
| 22.1719 | 22.1699 | 22.1684 | 22.1674 | 22.1669 | 22.1669 | 1.6741 | 5817.5293 |
| 2.4243 | 2.4009 | 2.3775 | 2.3541 | 2.3307 | 2.3073 | 2.2839 | 2.2605 |
| 2.2371 | 2.2138 | 2.1905 | 2.1671 | 2.1439 | 2.1206 | 0.0169 | 1.6831 |
| 22.2882 | 22.2862 | 22.2847 | 22.2838 | 22.2833 | 22.2833 | 1.6828 | 5901.8418 |
| 2.4243 | 2.4012 | 2.3782 | 2.3551 | 2.3320 | 2.3089 | 2.2859 | 2.2628 |
| 2.2398 | 2.2168 | 2.1938 | 2.1708 | 2.1479 | 2.1249 | 0.0170 | 1.6918 |
| 22.4029 | 22.4009 | 22.3994 | 22.3985 | 22.3980 | 22.3980 | 1.6915 | 5986.1538 |
| 2.4243 | 2.4016 | 2.3788 | 2.3561 | 2.3333 | 2.3106 | 2.2878 | 2.2651 |
| 2.2424 | 2.2197 | 2.1970 | 2.1744 | 2.1518 | 2.1291 | 0.0170 | 1.7003 |
| 22.5159 | 22.5140 | 22.5125 | 22.5116 | 22.5111 | 22.5111 | 1.7000 | 6070.4653 |
| 2.4243 | 2.4019 | 2.3795 | 2.3570 | 2.3346 | 2.3122 | 2.2898 | 2.2673 |
| 2.2450 | 2.2226 | 2.2002 | 2.1779 | 2.1556 | 2.1333 | 0.0170 | 1.7087 |
| 22.6273 | 22.6254 | 22.6240 | 22.6231 | 22.6226 | 22.6226 | 1.7085 | 6154.7778 |
| 2.4243 | 2.4022 | 2.3801 | 2.3580 | 2.3358 | 2.3137 | 2.2916 | 2.2695 |
| 2.2474 | 2.2254 | 2.2033 | 2.1813 | 2.1593 | 2.1373 | 0.0171 | 1.7170 |
| 22.7372 | 22.7354 | 22.7340 | 22.7330 | 22.7326 | 22.7326 | 1.7168 | 6239.0898 |
| 2.4243 | 2.4025 | 2.3807 | 2.3589 | 2.3370 | 2.3152 | 2.2934 | 2.2716 |
| 2.2499 | 2.2281 | 2.2064 | 2.1846 | 2.1629 | 2.1412 | 0.0171 | 1.7252 |
| 22.8456 | 22.8438 | 22.8424 | 22.8415 | 22.8410 | 22.8410 | 1.7250 | 6323.4019 |
| 2.4243 | 2.4028 | 2.3813 | 2.3598 | 2.3382 | 2.3167 | 2.2952 | 2.2737 |
| 2.2522 | 2.2308 | 2.2093 | 2.1879 | 2.1665 | 2.1451 | 0.0171 | 1.7333 |
| 22.9526 | 22.9507 | 22.9494 | 22.9484 | 22.9480 | 22.9480 | 1.7330 | 6407.7139 |
| 2.4243 | 2.4031 | 2.3819 | 2.3606 | 2.3394 | 2.3182 | 2.2970 | 2.2758 |
| 2.2546 | 2.2334 | 2.2122 | 2.1911 | 2.1699 | 2.1488 | 0.0172 | 1.7412 |
| 23.0580 | 23.0562 | 23.0549 | 23.0540 | 23.0535 | 23.0535 | 1.7410 | 6492.0259 |
| 2.4243 | 2.4034 | 2.3824 | 2.3615 | 2.3405 | 2.3196 | 2.2987 | 2.2777 |
| 2.2568 | 2.2359 | 2.2150 | 2.1942 | 2.1733 | 2.1525 | 0.0172 | 1.7491 |


| 23.1621 | 23.1603 | 23.1590 | 23.1581 | 23.1577 | 23.1577 | 1.7489 | 6576.3379 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.4037 | 2.3830 | 2.3623 | 2.3416 | 2.3210 | 2.3003 | 2.2797 |
| 2.2590 | 2.2384 | 2.2178 | 2.1972 | 2.1767 | 2.1561 | 0.0172 | 1.7568 |
| 23.2648 | 23.2630 | 23.2617 | 23.2608 | 23.2604 | 23.2604 | 1.7566 | 6660.6499 |
| 2.4243 | 2.4039 | 2.3835 | 2.3631 | 2.3427 | 2.3223 | 2.3020 | 2.2816 |
| 2.2612 | 2.2409 | 2.2205 | 2.2002 | 2.1799 | 2.1596 | 0.0173 | 1.7645 |
| 23.3661 | 23.3644 | 23.3631 | 23.3622 | 23.3618 | 23.3618 | 1.7643 | 6744.9614 |
| 2.4243 | 2.4042 | 2.3841 | 2.3639 | 2.3438 | 2.3237 | 2.3035 | 2.2834 |
| 2.2633 | 2.2433 | 2.2232 | 2.2031 | 2.1831 | 2.1631 | 0.0173 | 1.7721 |
| 23.4662 | 23.4644 | 23.4632 | 23.4623 | 23.4619 | 23.4619 | 1.7718 | 6829.2739 |
| 2.4243 | 2.4045 | 2.3846 | 2.3647 | 2.3448 | 2.3250 | 2.3051 | 2.2853 |
| 2.2654 | 2.2456 | 2.2258 | 2.2060 | 2.1862 | 2.1664 | 0.0173 | 1.7795 |
| 23.5649 | 23.5632 | 23.5619 | 23.5611 | 23.5607 | 23.5607 | 1.7793 | 6913.5859 |
| 2.4243 | 2.4047 | 2.3851 | 2.3655 | 2.3458 | 2.3262 | 2.3066 | 2.2870 |
| 2.2675 | 2.2479 | 2.2283 | 2.2088 | 2.1892 | 2.1697 | 0.0173 | 1.7869 |
| 23.6624 | 23.6607 | 23.6594 | 23.6586 | 23.6582 | 23.6582 | 1.7867 | 97.8979 |
| 2.4243 | 2.4050 | 2.3856 | 2.3662 | 2.3468 | 2.3275 | 2.3081 | 2.2888 |
| 2.2694 | 2.2501 | 2.2308 | 2.2115 | 2.1922 | 2.1730 | 0.0174 | 1.7941 |
| 23.7586 | 23.7569 | 23.7557 | 23.7549 | 23.7545 | 23.7545 | 1.7939 | 7082.2100 |
| 2.4243 | 2.4052 | 2.3861 | 2.3669 | 2.3478 | 2.3287 | 2.3096 | 2.2905 |
| 2.2714 | 2.2523 | 2.2333 | 2.2142 | 2.1952 | 2.1761 | 0.0174 | 1.8013 |
| 23.8536 | 23.8520 | 23.8508 | 23.8499 | 23.8495 | 23.8495 | 1.8011 | 166.5225 |
| 2.4243 | 2.4054 | 2.3866 | 2.3677 | 2.3488 | 2.3299 | 2.3110 | 2.2922 |
| 2.2733 | 2.2545 | 2.2356 | 2.2168 | 2.1980 | 2.1792 | 0.0174 | 1.8084 |
| 23.9474 | 23.9458 | 23.9446 | 23.9438 | 23.9434 | 23.9434 | 1.8082 | 50.8340 |
| 2.4243 | 2.4057 | 2.3870 | 2.3684 | 2.3497 | 2.3311 | 2.3124 | 2.2938 |
| 2.2752 | 2.2566 | 2.2380 | 2.2194 | 2.2008 | 2.1823 | 0.0174 | 1.8154 |
| 24.0401 | 24.0385 | 24.0373 | 24.0365 | 24.0361 | 24.0361 | 1.8152 | 7335.1460 |
| 2.4243 | 2.4059 | 2.3875 | 2.3691 | 2.3506 | 2.3322 | 2.3138 | 2.2954 |
| 2.2770 | 2.2587 | 2.2403 | 2.2219 | 2.2036 | 2.1853 | 0.0175 | 1.8223 |
| 24.1316 | 24.1300 | 24.1288 | 24.1281 | 24.1277 | 24.1277 | 1.8221 | 7419.4585 |
| 2.4243 | 2.4061 | 2.3879 | 2.3697 | 2.3515 | 2.3334 | 2.3152 | 2.2970 |
| 2.2788 | 2.2607 | 2.2425 | 2.2244 | 2.2063 | 2.1882 | 0.0175 | 1.8291 |
| 24.2220 | 24.2204 | 24.2193 | 24.2185 | 24.2181 | 24.2181 | 1.8289 | 7503.7700 |
| 2.4243 | 2.4064 | 2.3884 | 2.3704 | 2.3524 | 2.3345 | 2.3165 | 2.2985 |
| 2.2806 | 2.2627 | 2.2447 | 2.2268 | 2.2089 | 2.1911 | 0.0175 | 1.8359 |
| 24.3113 | 24.3098 | 24.3086 | 24.3078 | 24.3075 | 24.3075 | 1.8357 | 7588.0820 |
| 2.4243 | 2.4066 | 2.3888 | 2.3711 | 2.3533 | 2.3355 | 2.3178 | 2.3001 |
| 2.2823 | 2.2646 | 2.2469 | 2.2292 | 2.2115 | 2.1939 | 0.0175 | 1.8425 |
| 24.3995 | 24.3980 | 24.3969 | 24.3961 | 24.3957 | 24.3957 | 1.8423 | 672.3945 |
| 2.4243 | 2.4068 | 2.3892 | 2.3717 | 2.3541 | 2.3366 | 2.3191 | 2.3016 |
| 2.2840 | 2.2665 | 2.2490 | 2.2316 | 2.2141 | 2.1966 | 0.0176 | 1.8491 |
| 24.4867 | 24.4852 | 24.4841 | 24.4833 | 24.4829 | 24.4829 | 1.8489 | 756.7061 |
| 2.4243 | 2.4070 | 2.3897 | 2.3723 | 2.3550 | 2.3377 | 2.3203 | 2.3030 |
| 2.2857 | 2.2684 | 2.2511 | 2.2338 | 2.2166 | 2.1993 | 0.0176 | 1.8556 |
| 24.5728 | 24.5713 | 24.5702 | 24.5695 | 24.5691 | 24.5691 | 1.8554 | 7841.0186 |
| 2.4243 | 2.4072 | 2.3901 | 2.3729 | 2.3558 | 2.3387 | 2.3216 | 2.3044 |
| 2.2873 | 2.2702 | 2.2532 | 2.2361 | 2.2190 | 2.2020 | 0.0176 | 1.8620 |
| 24.6579 | 24.6564 | 24.6553 | 24.6546 | 24.6543 | 24.6543 | 1.8619 | 7925.3306 |
| 2.4243 | 2.4074 | 2.3905 | 2.3735 | 2.3566 | 2.3397 | 2.3228 | 2.3059 |
| 2.2889 | 2.2721 | 2.2552 | 2.2383 | 2.2214 | 2.2046 | 0.0176 | 1.8684 |
| 24.7420 | 24.7406 | 24.7395 | 24.7388 | 24.7384 | 24.7384 | 1.8682 | 8009.6421 |
| 2.4243 | 2.4076 | 2.3909 | 2.3741 | 2.3574 | 2.3407 | 2.3239 | 2.3072 |
| 2.2905 | 2.2738 | 2.2571 | 2.2405 | 2.2238 | 2.2072 | 0.0176 | 1.8747 |
| 24.8251 | 24.8237 | 24.8226 | 24.8219 | 24.8216 | 24.8216 | 1.8745 | 8093.9546 |
| 2.4243 | 2.4078 | 2.3912 | 2.3747 | 2.3582 | 2.3416 | 2.3251 | 2.3086 |
| 2.2921 | 2.2756 | 2.2591 | 2.2426 | 2.2261 | 2.2097 | 0.0177 | 1.8809 |
| 24.9073 | 24.9059 | 24.9048 | 24.9041 | 24.9038 | 24.9038 | 1.8807 | 8178.2661 |
| 2.4243 | 2.4080 | 2.3916 | 2.3753 | 2.3589 | 2.3426 | 2.3263 | 2.3099 |
| 2.2936 | 2.2773 | 2.2610 | 2.2447 | 2.2284 | 2.2121 | 0.0177 | 1.8870 |

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| 24.9885 | 24.9871 | 24.9861 | 24.9854 | 24.9850 | 24.9850 | 1.8868 | 62.5781 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2.4243 | 2.4082 | 2.3920 | 2.3758 | 2.3597 | 2.3435 | 2.3274 | 2.3112 |
| 2.2951 | 2.2790 | 2.2629 | 2.2467 | 2.2306 | 2.2146 | 0.0177 | 1.8931 |
| 25.0688 | 25.0674 | 25.0664 | 25.0657 | 25.0654 | 25.0654 | 1.8929 | 8346.8906 |
| 2.4243 | 2.4084 | 2.3924 | 2.3764 | 2.3604 | 2.3444 | 2.3285 | 2.3125 |
| 2.2966 | 2.2806 | 2.2647 | 2.2488 | 2.2328 | 2.2169 | 0.0177 | 1.8991 |
| 25.1482 | 25.1468 | 25.1458 | 25.1451 | 25.1448 | 25.1448 | 1.8989 | 31.2021 |
| 2.4243 | 2.4085 | 2.3927 | 2.3769 | 2.3611 | 2.3453 | 2.3296 | 2.3138 |
| 2.2980 | 2.2822 | 2.2665 | 2.2507 | 2.2350 | 2.2193 | 0.0177 | 1.9050 |
| 25.2266 | 25.2253 | 25.2243 | 25.2236 | 25.2233 | 25.2233 | 1.9048 | 5.5146 |
| 2.4243 | 2.4087 | 2.3931 | 2.3775 | 2.3618 | 2.3462 | 2.3306 | 2.3150 |
| 2.2994 | 2.2838 | 2.2683 | 2.2527 | 2.2371 | 2.2216 | 0.0178 | 1.9109 |
| 25.3042 | 25.3029 | 25.3019 | 25.3013 | 25.3009 | 25.3009 | 1.9107 | 99.8271 |
| 2.4243 | 2.4089 | 2.3934 | 2.3780 | 2.3625 | 2.3471 | 2.3317 | 2.3162 |
| 2.3008 | 2.2854 | 2.2700 | 2.2546 | 2.2392 | 2.2239 | 0.0178 | 1.9167 |
| 25.3810 | 25.3797 | 25.3787 | 25.3780 | 25.3777 | 25.3777 | 1.9165 | 8684.1387 |
| 2.4243 | 2.4091 | 2.3938 | 2.3785 | 2.3632 | 2.3480 | 2.3327 | 2.3174 |
| 2.3022 | 2.2870 | 2.2717 | 2.2565 | 2.2413 | 2.2261 | 0.0178 | 1.9224 |
| 25.4569 | 25.4556 | 25.4546 | 25.4539 | 25.4536 | 25.4536 | 1.9222 | 8768.4502 |
| 2.4243 | 2.4092 | 2.3941 | 2.3790 | 2.3639 | 2.3488 | 2.3337 | 2.3186 |
| 2.3035 | 2.2885 | 2.2734 | 2.2583 | 2.2433 | 2.2283 | 0.0178 | 1.9280 |
| 25.5319 | 25.5306 | 25.5297 | 25.5290 | 25.5287 | 25.5287 | 1.9279 | 852.7627 |
| 2.4243 | 2.4094 | 2.3944 | 2.3795 | 2.3646 | 2.3496 | 2.3347 | 2.3198 |
| 2.3049 | 2.2900 | 2.2751 | 2.2602 | 2.2453 | 2.2304 | 0.0178 | 1.9337 |
| 25.6061 | 25.6048 | 25.6039 | 25.6033 | 25.6029 | 25.6029 | 1.9335 | 937.0742 |
| 2.4243 | 2.4096 | 2.3948 | 2.3800 | 2.3652 | 2.3505 | 2.3357 | 2.3209 |
| 2.3062 | 2.2914 | 2.2767 | 2.2620 | 2.2472 | 2.2325 | 0.0178 | 1.9392 |
| 25.6795 | 25.6783 | 25.6773 | 25.6767 | 25.6764 | 25.6764 | 1.9390 | 9021.3867 |
| 2.4243 | 2.4097 | 2.3951 | 2.3805 | 2.3659 | 2.3513 | 2.3366 | 2.3220 |
| 2.3075 | 2.2929 | 2.2783 | 2.2637 | 2.2492 | 2.2346 | 0.0179 | 1.9447 |
| 25.7521 | 25.7509 | 25.7500 | 25.7493 | 25.7490 | 25.7490 | 1.9445 | 9105.6992 |
| 2.4243 | 2.4099 | 2.3954 | 2.3810 | 2.3665 | 2.3520 | 2.3376 | 2.3232 |
| 2.3087 | 2.2943 | 2.2799 | 2.2654 | 2.2510 | 2.2367 | 0.0179 | 1.9501 |
| 25.8240 | 25.8227 | 25.8218 | 25.8212 | 25.8209 | 25.8209 | 1.9499 | 9190.0107 |
| 2.4243 | 2.4100 | 2.3957 | 2.3814 | 2.3671 | 2.3528 | 2.3385 | 2.3242 |
| 2.3100 | 2.2957 | 2.2814 | 2.2672 | 2.2529 | 2.2387 | 0.0179 | 1.9555 |
| 25.8950 | 25.8938 | 25.8929 | 25.8923 | 25.8920 | 25.8920 | 1.9553 | 9274.3232 |
| 2.4243 | 2.4102 | 2.3960 | 2.3819 | 2.3677 | 2.3536 | 2.3394 | 2.3253 |
| 2.3112 | 2.2971 | 2.2829 | 2.2688 | 2.2547 | 2.2407 | 0.0179 | 1.9608 |
| 25.9653 | 25.9641 | 25.9632 | 25.9626 | 25.9623 | 25.9623 | 1.9606 | 9358.6348 |
| 2.4243 | 2.4103 | 2.3963 | 2.3823 | 2.3683 | 2.3543 | 2.3403 | 2.3264 |
| 2.3124 | 2.2984 | 2.2844 | 2.2705 | 2.2565 | 2.2426 | 0.0179 | 1.9660 |
| 26.0349 | 26.0337 | 26.0328 | 26.0322 | 26.0319 | 26.0319 | 1.9659 | 9442.9463 |
| 2.4243 | 2.4105 | 2.3966 | 2.3828 | 2.3689 | 2.3551 | 2.3412 | 2.3274 |
| 2.3136 | 2.2997 | 2.2859 | 2.2721 | 2.2583 | 2.2445 | 0.0179 | 1.9712 |
| 26.1037 | 26.1025 | 26.1016 | 26.1010 | 26.1007 | 26.1007 | 1.9711 | 9527.2588 |
| 2.4243 | 2.4106 | 2.3969 | 2.3832 | 2.3695 | 2.3558 | 2.3421 | 2.3284 |
| 2.3147 | 2.3010 | 2.2874 | 2.2737 | 2.2601 | 2.2464 | 0.0180 | 1.9764 |
| 26.1718 | 26.1706 | 26.1697 | 26.1692 | 26.1689 | 26.1689 | 1.9762 | 9611.5713 |
| 2.4243 | 2.4108 | 2.3972 | 2.3836 | 2.3701 | 2.3565 | 2.3430 | 2.3294 |
| 2.3159 | 2.3023 | 2.2888 | 2.2753 | 2.2618 | 2.2483 | 0.0180 | 1.9815 |
| 26.2392 | 26.2380 | 26.2371 | 26.2366 | 26.2363 | 26.2363 | 1.9813 | 9695.8838 |
| 2.4243 | 2.4109 | 2.3975 | 2.3841 | 2.3706 | 2.3572 | 2.3438 | 2.3304 |
| 2.3170 | 2.3036 | 2.2902 | 2.2768 | 2.2635 | 2.2501 | 0.0180 | 1.9865 |
| 26.3058 | 26.3047 | 26.3038 | 26.3033 | 26.3030 | 26.3030 | 1.9863 | 9780.1943 |
| 2.4243 | 2.4110 | 2.3978 | 2.3845 | 2.3712 | 2.3579 | 2.3446 | 2.3314 |
| 2.3181 | 2.3049 | 2.2916 | 2.2784 | 2.2651 | 2.2519 | 0.0180 | 1.9915 |
| 26.3718 | 26.3707 | 26.3699 | 26.3693 | 26.3690 | 26.3690 | 1.9913 | 9864.5068 |
| 2.4243 | 2.4112 | 2.3980 | 2.3849 | 2.3717 | 2.3586 | 2.3455 | 2.3323 |
| 2.3192 | 2.3061 | 2.2930 | 2.2799 | 2.2668 | 2.2537 | 0.018 | 1.9964 |

```
    1 0 9
26.4371 26.4360 26.4352 26.4346 26.4343 26.4343 1.9963 9948.8193
    SHELF-LIFE OF THIS PRODUCT IS 10013.31445hrs
```

FORTRAN STOP

## APPENDIX B

## APPENDIX B

Sorption Experiment of Deltasone Tablet

Table 11. Summary of sorption experiments of 20 mg Deltasone tablet at $25.0^{\circ} \mathrm{C}$

| Test Number | Experimental Test | Relative Humidity <br> Range (\%) |
| :---: | :---: | :---: |
| 1 | SORP B1 | $0-11.50$ |
| 2 | SORP B2 | $11.50-15.25$ |
| 3 | SORP C1 | $15.75-23.20$ |
| 4 | SORP C2 | $23.20-27$ |
| 5 | SORP C3a | $27.50-34.50$ |
| 6 | SORP C3b | $36-40$ |
| 7 | SORP C5 | $40.75-48.80$ |
| 8 | SORP 6C | $48.85-60.35$ |
| 9 | SORP 7Ca | $60.70-66$ |
| 10 | SORP 7Cb | $66-73.40$ |
| 11 | SORP C8 | $72.25-77.75$ |
| 12 | SORP C9 | $77.90-82.45$ |
| 13 | SORP 10 | $82.05-87.30$ |
| 14 | SORP 13 | $86.70-91.70$ |

Table 12. Moisture sorption isotherm data for Deltasone tablet at $25.0^{\circ} \mathrm{C}$

| A | Absolute <br> Tablet Weight <br> $(\mathrm{mg})$ | Tablet Weight <br> Change <br> (mg) | EMC <br> (g H2O/100 g <br> dry product) |
| :---: | :---: | :---: | :---: |
| 0 | 407.7421 | 0 | 0 |
| 0.115 | 409.2698 | 1.5277 | 0.375 |
| 0.153 | 409.35 | 1.6079 | 0.394 |
| 0.232 | 409.8798 | 2.1377 | 0.524 |
| 0.27 | 410.36 | 2.6179 | 0.642 |
| 0.345 | 410.593 | 2.8509 | 0.699 |
| 0.4 | 410.7729 | 3.0308 | 0.743 |
| 0.488 | 411.5429 | 3.8008 | 0.932 |
| 0.604 | 412.0246 | 4.2825 | 1.05 |
| 0.66 | 412.7226 | 4.9805 | 1.221 |
| 0.734 | 413.3085 | 5.5664 | 1.365 |
| 0.778 | 414.2913 | 6.5492 | 1.606 |
| 0.825 | 415.5057 | 7.7636 | 1.904 |
| 0.873 | 415.7983 | 8.0562 | 1.976 |
| 0.917 | 422.0713 | 14.3292 | 3.514 |

$A_{\mu}=$ Water activity
EMC = Equilibrium Moisture Content

Table 13. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $0-11.50 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \\ \hline \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{+} / M_{0} \\ & \hline \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ \mathrm{M}_{\mathrm{L}} / \mathrm{M}_{0} \\ \hline \end{gathered}$ | $\begin{gathered} \mathrm{T}_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.52 | 0.090486 |
| 1 | 0.427244 | 0.397925 | 1.54 | 0.089439 |
| 2 | 0.63193 | 0.540453 | 1.58 | 0.087708 |
| 3 | 0.73483 | 0.653264 | 1.62 | 0.086465 |
| 4 | 0.785625 | 0.738693 | 1.66 | 0.085695 |
| 5 | 0.819533 | 0.803099 | 1.70 | 0.085376 |
| 6 | 0.842836 | 0.851632 | 1.71 | 0.085365 |
| 7 | 0.859789 | 0.888202 | 1.72 | 0.085381 |
| 8 | 0.873208 | 0.915759 | 1.73 | 0.085422 |
| 9 | 0.883943 | 0.936523 | 1.74 | 0.085491 |
| 10 | 0.893042 | 0.952169 | 1.75 | 0.085587 |
| 11 | 0.900242 | 0.963959 | 1.76 | 0.085711 |
| 12 | 0.906592 | 0.972842 |  |  |
| 13 | 0.911828 | 0.979536 |  |  |
| 14 | 0.91641 | 0.98458 |  |  |
| 15 | 0.920665 | 0.988381 | Diffusion |  |
| 16 | 0.923545 | 0.991245 | Coeff. = |  |
| 17 | 0.924789 | 0.993403 | 0.004404 |  |
| 18 | 0.925313 | 0.995029 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 19 | 0.923807 | 0.996254 |  |  |
| 20 | 0.931138 | 0.997178 |  |  |
| 21 | 0.948616 | 0.997873 |  |  |
| 22 | 0.955227 | 0.998397 |  |  |
| 23 | 0.960136 | 0.998792 |  |  |
| 24 | 0.96354 | 0.99909 |  |  |
| 25 | 0.967467 | 0.999314 |  |  |
| 26 | 0.973555 | 0.999483 |  |  |
| 27 | 0.975453 | 0.999611 |  |  |
| 28 | 0.976239 | 0.999707 |  |  |
| 29 | 0.979577 | 0.999779 |  |  |
| 30 | 0.979053 | 0.999833 |  |  |
| 31 | 0.980101 | 0.999875 |  |  |
| 32 | 0.981606 | 0.999905 |  |  |
| 33 | 0.984094 | 0.999929 |  |  |
| 34 | 0.987039 | 0.999946 |  |  |
| 35 | 0.990116 | 0.99996 |  |  |
| 36 | 0.992996 | 0.99997 |  |  |
| 37 | 0.995352 | 0.999977 |  |  |
| 38 | 0.997185 | 0.999983 |  |  |
| 39 | 0.998756 | 0.999987 |  |  |
| 40 | 1 | 0.99999 |  |  |
| 40.75 | 1 | 0.999992 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 25. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $0-11.50 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ (SORP B1)


Figure 26. Experimental sorption of tablet at 11.50-15.25\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP B2)


Figure 27. Experimental sorption of tablet at 15.75-23.20\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP Cl)


Figure 28. Experimental tablet weight gain at 23.20-27\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP C2)


Figure 29. Experimental sorption of tablet at 27.50-34.50\% R.H., 25.0 ${ }^{\circ}$ C (SORP C3a)

Table 14. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $36-40 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{+} / M_{o} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{+} / M_{0} \end{gathered}$ | $\begin{gathered} \mathrm{T}_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 2.10 | 0.761768 |
| 0.25 | 0.00603 | 0.299699 | 2.20 | 0.721648 |
| 0.5 | 0.022111 | 0.31119 | 2.30 | 0.695722 |
| 0.75 | 0.052261 | 0.330029 | 2.40 | 0.682854 |
| 1 | 0.088442 | 0.353041 | 2.45 | 0.68094 |
| 1.25 | 0.139698 | 0.378209 | 2.46 | 0.680894 |
| 1.5 | 0.18392 | 0.404266 | 2.47 | 0.680961 |
| 1.75 | 0.237186 | 0.430419 | 2.48 | 0.681131 |
| 2 | 0.281407 | 0.456183 |  |  |
| 2.25 | 0.333668 | 0.481267 |  |  |
| 2.5 | 0.38191 | 0.505505 |  |  |
| 2.75 | 0.435176 | 0.528809 |  |  |
| 3 | 0.478392 | 0.551144 |  |  |
| 3.25 | 0.514573 | 0.572502 |  |  |
| 3.5 | 0.539698 | 0.592896 |  |  |
| 3.75 | 0.560804 | 0.612352 |  |  |
| 4 | 0.584925 | 0.630899 |  |  |
| 4.25 | 0.60804 | 0.648573 | Coeff. $=$ |  |
| 4.5 | 0.634171 | 0.66541 | 0.003061 |  |
| 4.75 | 0.660302 | 0.681446 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 5 | 0.681407 | 0.696717 |  |  |
| 5.25 | 0.702513 | 0.711258 |  |  |
| 5.5 | 0.731658 | 0.725104 |  |  |
| 5.75 | 0.751759 | 0.738286 |  |  |
| 6 | 0.769849 | 0.750837 |  |  |
| 6.25 | 0.78995 | 0.762787 |  |  |
| 6.5 | 0.80804 | 0.774164 |  |  |
| 6.75 | 0.826131 | 0.784995 |  |  |
| 7 | 0.842211 | 0.795307 |  |  |
| 7.25 | 0.861307 | 0.805124 |  |  |
| 7.5 | 0.870352 | 0.814471 |  |  |
| 7.75 | 0.881407 | 0.823369 |  |  |
| 8 | 0.895477 | 0.831841 |  |  |
| 8.25 | 0.911558 | 0.839906 |  |  |
| 8.5 | 0.923618 | 0.847585 |  |  |
| 8.75 | 0.934673 | 0.854895 |  |  |
| 9 | 0.950754 | 0.861855 |  |  |
| 9.25 | 0.956784 | 0.86848 |  |  |
| 9.5 | 0.970854 | 0.874788 |  |  |
| 9.75 | 0.975879 | 0.880794 |  |  |
| 10 | 0.972864 | 0.886511 |  |  |
| 10.25 | 0.978894 | 0.891954 |  |  |
| 10.5 | 0.98191 | 0.897137 |  |  |
| 10.75 | 0.988945 | 0.90207 |  |  |
| 11 11.25 | 1.001005 1.001005 | 0.906767 0.911239 |  |  |
| 11.5 |  | 0.915496 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


- Experimental __ Calculated

Figure 30. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $36-40 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ (SORP C3b)

Table 15. Comparison of experimental and calculated $M_{r} / M_{s}$ for tablet at 40.75-48.80\% R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{t} / M_{\infty} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{t} / M_{0} \end{gathered}$ | $\begin{gathered} \mathbf{T}_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 3.30 | 0.08315 |
| 1 | 0.27509 | 0.326579 | 3.40 | 0.081304 |
| 2 | 0.481551 | 0.39566 | 3.46 | 0.080946 |
| 3 | 0.573439 | 0.468999 | 3.47 | 0.080942 |
| 4 | 0.629289 | 0.536574 | 3.48 | 0.080951 |
| 5 | 0.668916 | 0.596435 | 3.49 | 0.080981 |
| 6 | 0.701795 | 0.648815 | 3.50 | 0.081021 |
| 7 | 0.728643 | 0.694469 |  |  |
| 8 | 0.753625 | 0.734208 |  |  |
| 9 | 0.775879 | 0.768785 |  |  |
| 10 | 0.799569 | 0.798865 | Diffusion |  |
| 11 | 0.819239 | 0.825032 | Coeff. = |  |
| 12 | 0.837904 | 0.847795 | 0.002170 |  |
| 13 | 0.861307 | 0.867597 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 14 | 0.86748 | 0.884822 |  |  |
| 15 | 0.865757 | 0.899807 |  |  |
| 16 | 0.854559 | 0.912842 |  |  |
| 17 | 0.856138 | 0.924181 |  |  |
| 18 | 0.870065 | 0.934045 |  |  |
| 19 | 0.884566 | 0.942626 |  |  |
| 20 | 0.896482 | 0.95009 |  |  |
| 21 | 0.903087 | 0.956583 |  |  |
| 22 | 0.909404 | 0.962232 |  |  |
| 23 | 0.916296 | 0.967145 |  |  |
| 24 | 0.922757 | 0.97142 |  |  |
| 25 | 0.927638 | 0.975138 |  |  |
| 26 | 0.933094 | 0.978372 |  |  |
| 27 | 0.938406 | 0.981186 |  |  |
| 28 | 0.943862 | 0.983634 |  |  |
| 29 | 0.950179 | 0.985763 |  |  |
| 30 | 0.956927 | 0.987615 |  |  |
| 31 | 0.964393 | 0.989227 |  |  |
| 32 | 0.971285 | 0.990628 |  |  |
| 33 | 0.979469 | 0.991847 |  |  |
| 34 | 0.986648 | 0.992908 |  |  |
| 35 | 0.996698 | 0.993831 |  |  |
| 35.5 | 1 | 0.994246 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 31. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at 40.75-48.80\% R.H. and $25.0^{\circ} \mathrm{C}$ (SORP C5)


Figure 32. Experimental sorption of tablet at 48.85-60.35\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP 6C)

Table 16. Comparison of experimental and calculated $M_{0} / M_{0}$ for tablet at $60.70-66 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{+} / M_{0} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{+} / M_{0} \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.60 | 0.164457 |
| 0.5 | 0.00294 | 0.32929 | 1.64 | 0.16293 |
| 1 | 0.191102 | 0.402445 | 1.65 | 0.16278 |
| 1.5 | 0.407291 | 0.478689 | 1.66 | 0.162713 |
| 2 | 0.542728 | 0.548098 | 1.67 | 0.162736 |
| 2.5 | 0.633281 | 0.609038 | 1.68 | 0.162847 |
| 3 | 0.696394 | 0.661967 | 1.70 | 0.16333 |
| 3.5 | 0.742062 | 0.707786 |  |  |
| 4 | 0.776362 | 0.74741 |  |  |
| 4.5 | 0.804194 | 0.781665 |  |  |
| 5 | 0.828499 | 0.811275 | Diffusion |  |
| 5.5 | 0.849667 | 0.83687 | Coeff. $=$ |  |
| 6 | 0.868091 | 0.858994 | 0.004536 |  |
| 6.5 | 0.884555 | 0.878117 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 7 | 0.899647 | 0.894647 |  |  |
| 7.5 | 0.912191 | 0.908935 |  |  |
| 8 | 0.924735 | 0.921286 |  |  |
| 8.5 | 0.935711 | 0.931961 |  |  |
| 9 | 0.945708 | 0.941189 |  |  |
| 9.5 | 0.957076 | 0.949165 |  |  |
| 10 | 0.966484 | 0.956059 |  |  |
| 10.5 | 0.97452 | 0.962018 |  |  |
| 11 | 0.982556 | 0.96717 |  |  |
| 11.5 | 0.988436 | 0.971622 |  |  |
| 12 | 0.989808 | 0.975471 |  |  |
| 12.5 | 0.988044 | 0.978797 |  |  |
| 13 | 0.988044 | 0.981673 |  |  |
| 13.5 | 0.990004 | 0.984158 |  |  |
| 14 | 0.996472 | 0.986307 |  |  |
| 14.5 | 1 | 0.988164 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 33. Comparison of experimental and calculated $M_{t} / M_{*}$ for tablet at $60.70-66 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ (SORP 7 Ca )

Table 17. Comparison of experimental and calculated $M_{*} / M_{0}$ for tablet at $66-73.40 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | Exp. $M_{+} / M_{0}$ | Calculated $M_{2} / M_{0}$ | $\begin{gathered} \mathrm{T}_{1 / 2} \\ \text { (hours) } \\ \hline \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.27 | 0.2142 |
| 0.25 | 0.003256 | 0.309764 | 1.28 | 0.213818 |
| 0.5 | 0.092716 | 0.34859 | 1.29 | 0.213665 |
| 0.75 | 0.224507 | 0.397027 | 1.30 | 0.213742 |
| 1 | 0.341902 | 0.446755 | 1.36 | 0.218822 |
| 1.25 | 0.435476 | 0.494451 | 1.40 | 0.226393 |
| 1.5 | 0.511397 | 0.538918 | 1.43 | 0.234163 |
| 1.75 | 0.572408 | 0.579853 | 1.46 | 0.243604 |
| 2 | 0.622451 | 0.617315 |  |  |
| 2.25 | 0.665124 | 0.651507 |  |  |
| 2.5 | 0.701971 | 0.682674 |  |  |
| 2.75 | 0.732648 | 0.711067 |  |  |
| 3 | 0.75904 | 0.736924 | Diffusion |  |
| 3.25 | 0.782519 | 0.76047 | Coeff. $=$ |  |
| 3.5 | 0.802742 | 0.78191 | 0.005837 |  |
| 3.75 | 0.81988 | 0.801431 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 4 | 0.836675 | 0.819205 |  |  |
| 4.25 | 0.850386 | 0.835388 |  |  |
| 4.5 | 0.864096 | 0.850122 |  |  |
| 4.75 | 0.876435 | 0.863538 |  |  |
| 5 | 0.887746 | 0.875753 |  |  |
| 5.25 | 0.898543 | 0.886874 |  |  |
| 5.5 | 0.907798 | 0.897 |  |  |
| 5.75 | 0.917224 | 0.90622 |  |  |
| 6 | 0.924764 | 0.914614 |  |  |
| 6.25 | 0.931962 | 0.922257 |  |  |
| 6.5 | 0.938646 | 0.929216 |  |  |
| 6.75 | 0.944987 | 0.935552 |  |  |
| 7 | 0.951157 | 0.941321 |  |  |
| 7.25 | 0.956641 | 0.946573 |  |  |
| 7.5 | 0.962639 | 0.951355 |  |  |
| 7.75 | 0.967952 | 0.95571 |  |  |
| 8 | 0.973093 | 0.959674 |  |  |
| 8.25 | 0.978406 | 0.963284 |  |  |
| 8.5 | 0.982862 | 0.96657 |  |  |
| 8.75 | 0.987318 | 0.969563 |  |  |
| 9 | 0.991945 | 0.972287 |  |  |
| 9.25 | 0.995716 | 0.974768 |  |  |
| 9.5 | 0.998972 | 0.977026 |  |  |
| 9.75 | 1.001371 | 0.979083 |  |  |
| 10 | 1.002742 | 0.980955 |  |  |
| 10.25 | 0.991602 | 0.98266 |  |  |
| 10.5 | 1.002913 | 0.984212 |  |  |
| 10.75 | 1.002057 | 0.985625 |  |  |
| 11 | 1 | 0.986912 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 34. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at 66 - 73.40\% R.H. and 25.0 ${ }^{\circ} \mathrm{C}$ (SORP 7Cb)

Table 18. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $72.25-77.75 \% \mathrm{R} . \mathrm{H}$. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| Time (hours) | $\begin{aligned} & \operatorname{Exp}_{0} \\ & M_{+} / M_{0} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{+} / M_{0} \\ \hline \hline \end{gathered}$ | $\begin{gathered} \mathrm{T}_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.60 | 0.051542 |
| 0.5 | 0.126425 | 0.329647 | 1.64 | 0.050668 |
| 1 | 0.332308 | 0.403324 | 1.65 | 0.050656 |
| 1.5 | 0.47819 | 0.479935 | 1.66 | 0.050726 |
| 2 | 0.569321 | 0.549571 | 1.68 | 0.051105 |
| 2.5 | 0.637466 | 0.610642 | 1.70 | 0.051804 |
| 3 | 0.691493 | 0.663634 | 1.72 | 0.052799 |
| 3.5 | 0.733032 | 0.709468 |  |  |
| 4 | 0.768597 | 0.749071 |  |  |
| 4.5 | 0.800271 | 0.783279 |  |  |
| 5 | 0.823077 | 0.812825 | Diffusion |  |
| 5.5 | 0.842896 | 0.838344 | Coeff. $=$ |  |
| 6 | 0.85991 | 0.860383 | 0.004564 |  |
| 6.5 | 0.874299 | 0.879417 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 7 | 0.886787 | 0.895857 |  |  |
| 7.5 | 0.897738 | 0.910055 |  |  |
| 8 | 0.907692 | 0.922318 |  |  |
| 8.5 | 0.920271 | 0.932908 |  |  |
| 9 | 0.93276 | 0.942055 |  |  |
| 9.5 | 0.942443 | 0.949955 |  |  |
| 10 | 0.949955 | 0.956778 |  |  |
| 10.5 | 0.95629 | 0.962671 |  |  |
| 11 | 0.9619 | 0.96776 |  |  |
| 11.5 | 0.967149 | 0.972155 |  |  |
| 12 | 0.971222 | 0.975952 |  |  |
| 12.5 | 0.975837 | 0.97923 |  |  |
| 13 | 0.979457 | 0.982062 |  |  |
| 13.5 | 0.982624 | 0.984507 |  |  |
| 14 | 0.985068 | 0.98662 |  |  |
| 14.5 | 0.987692 | 0.988444 |  |  |
| 15 | 0.990407 | 0.990019 |  |  |
| 15.5 | 0.992489 | 0.99138 |  |  |
| 16 | 0.994842 | 0.992555 |  |  |
| 16.5 | 0.997014 | 0.99357 |  |  |
| 17 | 0.999548 | 0.994447 |  |  |
| 17.5 | 1.001448 | 0.995204 |  |  |
| 17.75 | 1 | 0.995543 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 35. Experimental sorption of tablet at 72.25-77.75\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP C8)

Table 19. Comparison of experimental and calculated $M_{t} / M_{0}$ for tablet at $77.90-82.45 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{t} / M_{0} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{t} / M_{0} \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \\ \hline \end{gathered}$ | $\begin{aligned} & \text { Sum of } \\ & \text { diff. } \end{aligned}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.25 | 0.074536 |
| 0.5 | 0.191391 | 0.347156 | 1.30 | 0.0726 |
| 1 | 0.337666 | 0.443662 | 1.31 | 0.072598 |
| 1.5 | 0.453808 | 0.534866 | 1.32 | 0.072723 |
| 2 | 0.557202 | 0.61278 | 1.35 | 0.073829 |
| 2.5 | 0.645778 | 0.677956 | 1.40 | 0.078014 |
| 3 | 0.720778 | 0.732221 | 1.45 | 0.084958 |
| 3.5 | 0.782368 | 0.777354 | 1.50 | 0.094519 |
| 4 | 0.831871 | 0.814882 |  |  |
| 4.5 | 0.871109 | 0.846085 |  |  |
| 5 | 0.90505 | 0.872028 |  |  |
| 5.5 | 0.932781 | 0.893599 | Diffusion |  |
| 6 | 0.953808 | 0.911533 | Coeff. $=$ |  |
| 6.5 | 0.969619 | 0.926445 | 0.005748 |  |
| 7 | 0.981043 | 0.938843 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 7.5 | 0.991142 | 0.949152 |  |  |
| 8 | 0.999338 | 0.957723 |  |  |
| 8.5 | 1.004636 | 0.964849 |  |  |
| 9 | 1.008692 | 0.970774 |  |  |
| 9.5 | 1.012169 | 0.9757 |  |  |
| 10 | 1.015563 | 0.979796 |  |  |
| 10.5 | 1.019123 | 0.983201 |  |  |
| 11 | 1.021689 | 0.986033 |  |  |
| 11.5 | 1.023179 | 0.988387 |  |  |
| 12 | 1.024338 | 0.990345 |  |  |
| 12.5 | 1.022599 | 0.991972 |  |  |
| 13 | 1.020033 | 0.993325 |  |  |
| 13.5 | 1.017881 | 0.99445 |  |  |
| 14 | 1.015811 | 0.995386 |  |  |
| 14.5 | 1.013162 | 0.996164 |  |  |
| 15 | 1.009272 | 0.99681 |  |  |
| 15.5 | 1.007036 | 0.997348 |  |  |
| 16 | 1.004884 | 0.997795 |  |  |
| 16.5 | 1.00207 | 0.998167 |  |  |
| 16.75 | 1 | 0.998328 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 36. Comparison of experimental and calculated $M_{t} / M_{\infty}$ for tablet at 77.90-82.45\% R.H. and 25.0 ${ }^{\circ} \mathrm{C}$ (SORP C9)

Table 20. Comparison of experimental and calculated $M_{t} / M_{\infty}$ for tablet at $82.05-87.30 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{+} / M_{0} \\ & \hline \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{t} / M_{0} \end{gathered}$ | $\begin{gathered} \mathrm{T}_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 2.08 | 0.038614 |
| 1 | 0.215121 | 0.37013 | 2.09 | 0.038574 |
| 2 | 0.439014 | 0.490327 | 2.10 | 0.038571 |
| 3 | 0.577833 | 0.593975 | 2.11 | 0.038603 |
| 4 | 0.670774 | 0.677335 | 2.15 | 0.039101 |
| 5 | 0.741994 | 0.74368 | 2.20 | 0.040502 |
| 6 | 0.799151 | 0.796395 | 2.25 | 0.042795 |
| 7 | 0.845725 | 0.838271 | 2.30 | 0.045849 |
| 8 | 0.883111 | 0.871534 |  |  |
| 9 | 0.913464 | 0.897956 |  |  |
| 10 | 0.938179 | 0.918944 |  |  |
| 11 | 0.959343 | 0.935615 | Diffusion |  |
| 12 | 0.975494 | 0.948857 | Coeff. = |  |
| 13 | 0.989 | 0.959376 | 0.003585 |  |
| 14 | 0.999582 | 0.967731 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 15 | 1.004107 | 0.974368 |  |  |
| 16 | 1.006892 | 0.97964 |  |  |
| 17 | 1.007449 | 0.983827 |  |  |
| 18 | 1.007519 | 0.987153 |  |  |
| 19 | 1.007937 | 0.989796 |  |  |
| 20 | 1.009816 | 0.991894 |  |  |
| 21 | 1.012531 | 0.993561 |  |  |
| 22 | 1.013854 | 0.994886 |  |  |
| 23 | 1.015664 | 0.995938 |  |  |
| 24 | 1.020955 | 0.996773 |  |  |
| 25 | 1.024854 | 0.997437 |  |  |
| 26 | 1.02374 | 0.997964 |  |  |
| 27 | 1.021791 | 0.998383 |  |  |
| 28 | 1.01817 | 0.998715 |  |  |
| 29 | 1.013436 | 0.99898 |  |  |
| 30 | 1.008911 | 0.999189 |  |  |
| 31 | 1.005569 | 0.999356 |  |  |
| 32 | 1.001184 | 0.999489 |  |  |
| 32.25 | 1 | 0.999517 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.

. Experimental __Calculated

Figure 37. Comparison of experimental and calculated $M_{t} / M_{\infty}$ for tablet at 82.05-87.30\% R.H. and $25.0^{\circ} \mathrm{C}$ (SORP 10)


Figure 38. Experimental sorption of tablet at 86.70-91.70\% R.H., 25.0 ${ }^{\circ}$ C (SORP 13)

## APPENDIX C

## APPENDIX C

Sorption Experiment of PVC Film

Table 21. Summary of sorption experiments of PVC film at

| Test Number | Experimental Test | Relative Humidity <br> Range (\%) |
| :---: | :---: | :---: |
| 1 | SORP P1 | $0-26.90$ |
| 2 | SORP P2 | $26.65-43.50$ |
| 3 | SORP P3 | $43.50-58.20$ |
| 4 | SORP P4 | $58.20-77$ |

Table 22. Moisture sorption isotherm data for PVC film at $25.0^{\circ} \mathrm{C}$

| $A_{W}$ | Absolute <br> Film <br> Weight <br> (mg) | Film <br> Weight <br> Change <br> (mg) | EMC <br> (g H2O/ <br> 100 g dry <br> product) | Calc. EMC <br> (g H2O/ <br> 100 g dry <br> product) |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 193.9691 | 0 | 0 | 0 |
| 0.269 | 194.0393 | 0.0702 | 0.036 | 0.046 |
| 0.435 | 194.1173 | 0.1482 | 0.076 | 0.074 |
| 0.582 | 194.1622 | 0.1931 | 0.1 | 0.099 |
| 0.77 | 194.2264 | 0.2573 | 0.133 | 0.131 |

$A_{y}=$ Water activity
EMC = Equilibrium Moisture Content
Calc. = Calculated

Table 23. Comparison of experimental and calculated $M_{1} / M_{0}$ for PVC film at $0-26.90 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{t} / M_{o} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ \text { M./M } \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 0.74 | 0.040469 |
| 0.5 | 0.373219 | 0.39354 | 0.80 | 0.03044 |
| 1 | 0.586895 | 0.532911 | 0.82 | 0.029135 |
| 1.5 | 0.696581 | 0.644594 | 0.84 | 0.027906 |
| 2 | 0.762108 | 0.729935 | 0.86 | 0.027173 |
| 2.5 | 0.806268 | 0.794814 | 0.87 | 0.026994 |
| 3 | 0.847578 | 0.844109 | 0.88 | 0.026993 |
| 3.5 | 0.873219 | 0.881561 | 0.89 | 0.02709 |
| 4 | 0.894587 | 0.910016 | 0.90 | 0.02729 |
| 4.5 | 0.908832 | 0.931635 |  |  |
| 5 | 0.911681 | 0.948059 |  |  |
| 5.5 | 0.924501 | 0.960538 |  |  |
| 6 | 0.930199 | 0.970019 | Diffusion |  |
| 6.5 | 0.935897 | 0.977222 | Coeff. $=$ |  |
| 7 | 0.935897 | 0.982694 | 2.01 E-05 |  |
| 7.5 | 0.950142 | 0.986852 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 8 | 0.951567 | 0.990011 |  |  |
| 8.5 | 0.954416 | 0.992411 |  |  |
| 9 | 0.958689 | 0.994234 |  |  |
| 9.5 | 0.960114 | 0.995619 |  |  |
| 10 | 0.962963 | 0.996672 |  |  |
| 10.5 | 0.972934 | 0.997471 |  |  |
| 11 | 0.974359 | 0.998079 |  |  |
| 11.5 | 0.977208 | 0.99854 |  |  |
| 12 | 0.981481 | 0.998891 |  |  |
| 12.5 | 0.987179 | 0.999157 |  |  |
| 13 | 0.992877 | 0.99936 |  |  |
| 13.5 | 0.994302 | 0.999514 |  |  |
| 14 | 0.998575 | 0.999631 |  |  |
| 14.5 | 0.994302 | 0.999719 |  |  |
| 15 | 1.002849 | 0.999787 |  |  |
| 15.5 | 1.005698 | 0.999838 |  |  |
| 16 | 1.008547 | 0.999877 |  |  |
| 16.5 | 1.012821 | 0.999906 |  |  |
| 17 | 1.014245 | 0.999929 |  |  |
| 17.5 | 1.01567 | 0.999946 |  |  |
| 18 | 1.004274 | 0.999959 |  |  |
| 18.5 | 1 | 0.999969 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 39. Comparison of experimental and calculated $M_{t} / M_{-}$for PVC film at 0 - $26.90 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ (SORP P1)


Figure 40. Experimental sorption of PVC film at 26.65-43.50\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP P2)


Figure 41. Experimental sorption of PVC film at 43.50-58.20\% R.H., 25.0 ${ }^{\circ} \mathrm{C}$ (SORP P3)

Table 24. Comparison of experimental and calculated $M_{t} / M_{0}$ for PVC film at $58.20-77 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| Time <br> (hours) | $\operatorname{Exp}_{M_{t} / M_{\infty}}$ | $\begin{gathered} \text { Calculated } \\ M_{+} / M_{0} \\ \hline \hline \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 1.05 | 0.048983 |
| 0.5 | 0.203288 | 0.365588 | 1.06 | 0.048705 |
| 1 | 0.439462 | 0.48154 | 1.07 | 0.048296 |
| 1.5 | 0.596413 | 0.583157 | 1.08 | 0.048169 |
| 2 | 0.699552 | 0.665774 | 1.09 | 0.048075 |
| 2.5 | 0.769806 | 0.73214 | 1.10 | 0.048112 |
| 3 | 0.814649 | 0.785346 | 1.14 | 0.049606 |
| 3.5 | 0.849028 | 0.827985 |  |  |
| 4 | 0.877429 | 0.862155 |  |  |
| 4.5 | 0.896861 | 0.889537 |  |  |
| 5 | 0.910314 | 0.91148 |  |  |
| 5.5 | 0.920777 | 0.929064 |  |  |
| 6 | 0.932735 | 0.943155 |  |  |
| 6.5 | 0.93722 | 0.954447 |  |  |
| 7 | 0.944694 | 0.963496 |  |  |
| 7.5 | 0.947683 | 0.970747 |  |  |
| 8 | 0.949178 | 0.976558 | Diffusion |  |
| 8.5 | 0.950673 | 0.981215 | Coeff. = |  |
| 9 | 0.964126 | 0.984946 | 1.62 E -05 |  |
| 9.5 | 0.971599 | 0.987937 | $\mathrm{Cm}^{2} / \mathrm{hour}$ |  |
| 10 | 0.980568 | 0.990333 |  |  |
| 10.5 | 0.979073 | 0.992253 |  |  |
| 11 | 0.980568 | 0.993792 |  |  |
| 11.5 | 0.989537 | 0.995025 |  |  |
| 12 | 0.995516 | 0.996013 |  |  |
| 12.5 | 1.00299 | 0.996805 |  |  |
| 13 | 1.008969 | 0.99744 |  |  |
| 13.5 | 1.017937 | 0.997949 |  |  |
| 14 | 1.025411 | 0.998356 |  |  |
| 14.5 | 1.029895 | 0.998683 |  |  |
| 15 | 1.035874 | 0.998944 |  |  |
| 15.5 | 1.037369 | 0.999154 |  |  |
| 16 | 1.037369 | 0.999322 |  |  |
| 16.5 | 1.037369 | 0.999457 |  |  |
| 17 | 1.037369 | 0.999565 |  |  |
| 17.5 | 1.028401 | 0.999651 |  |  |
| 18 | 1.019432 | 0.99972 |  |  |
| 18.5 | 1.010463 | 0.999776 |  |  |
| 19 | 1.010463 | 0.99982 |  |  |
| 19.5 | 1.007474 | 0.999856 |  |  |
| 20 | 1.00299 | 0.999885 |  |  |
| 20.5 | 1.007474 | 0.999908 |  |  |
| 21 | 1.004484 | 0.999926 |  |  |
| 21.5 | 1.001495 | 0.999941 |  |  |
| 22 | 1.008969 | 0.999952 |  |  |
| 22.5 | 1.014948 | 0.999962 |  |  |
| 23 | 1.010463 | 0.999969 |  |  |
| 23.5 | 1 | 0.999976 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 42. Experimental sorption of PVC film at 58.20-77\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP P4)

## APPENDIX D

## APPENDIX D

## Sorption Experiment of Aclar Film

Table 25. Summary of sorption experiments of Aclar film at

| Test Number | Experimental Test | Relative Humidity <br> Range (\%) |
| :---: | :---: | :---: |
| 1 | SORP L2 | $0-27.35$ |
| 2 | SORP L4 | $27.35-43.50$ |
| 3 | SORP L6 | $43.50-58$ |
| 4 | SORP L7 | $58-74.45$ |

Table 26. Moisture sorption isotherm data for Aclar film at $25.0^{\circ} \mathrm{C}$

| $A_{w}$ | $\begin{aligned} & \text { Absolute } \\ & \text { Film } \\ & \text { Weight } \\ & \text { (mg) } \\ & \hline \end{aligned}$ | Film <br> Weight <br> Change <br> (mg) | $\begin{gathered} \text { EMC } \\ \left(\mathrm{g} \mathrm{H} \mathrm{H}_{2} \mathrm{O} /\right. \\ 100 \mathrm{~g} \text { dry } \\ \text { product) } \end{gathered}$ | Calc. EMC ( $\mathrm{g} \mathrm{H}_{2} \mathrm{O}$ ) 100 g dry product) |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 50.7371 | 0 | 0 | 0.003 |
| 0.274 | 50.7649 | 0.0278 | 0.055 | 0.054 |
| 0.435 | 50.7797 | 0.0426 | 0.084 | 0.083 |
| 0.58 | 50.7983 | 0.0612 | 0.121 | 0.11 |
| 0.745 | 50.8034 | 0.0663 | 0.131 | 0.14 |

$A_{M}=$ Water activity
EMC = Equilibrium Moisture Content
Calc. = Calculated


Figure 43. Experimental sorption of Aclar film at 0 - 27.35\% R.H., 25.0 ${ }^{\circ}$ C (SORP L2)

Table 27. Comparison of experimental and calculated $M_{\alpha} / M_{0}$ for Aclar film at 27.35-43.50\% R.H. and 25.0 ${ }^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{+} / M_{+} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ \mathrm{M}_{+} / \mathrm{M}_{0} \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 0.50 | 0.089474 |
| 0.25 | 0.422857 | 0.348129 | 0.52 | 0.077926 |
| 0.5 | 0.508571 | 0.445762 | 0.55 | 0.064347 |
| 0.75 | 0.594286 | 0.53762 | 0.58 | 0.053588 |
| 1 | 0.657143 | 0.615863 | 0.61 | 0.048002 |
| 1.25 | 0.737143 | 0.681165 | 0.64 | 0.045094 |
| 1.5 | 0.754286 | 0.735422 | 0.65 | 0.044979 |
| 1.75 | 0.777143 | 0.780456 | 0.66 | 0.045197 |
| 2 | 0.811429 | 0.817827 | 0.67 | 0.045868 |
| 2.25 | 0.828571 | 0.848837 |  |  |
| 2.5 | 0.822857 | 0.874568 |  |  |
| 2.75 | 0.84 | 0.895919 |  |  |
| 3 | 0.845714 | 0.913636 | Diffusion |  |
| 3.25 | 0.868571 | 0.928337 | Coeff. = |  |
| 3.5 | 0.891429 | 0.940536 | 1.21 E-06 |  |
| 3.75 | 0.908571 | 0.950658 | $\mathrm{cm}^{2} /$ hour |  |
| 4 | 0.931429 | 0.959057 |  |  |
| 4.25 | 0.942857 | 0.966026 |  |  |
| 4.5 | 0.954286 | 0.971809 |  |  |
| 4.75 | 0.965714 | 0.976608 |  |  |
| 5 | 0.988571 | 0.98059 |  |  |
| 5.25 | 1.011429 | 0.983894 |  |  |
| 5.5 | 1.011429 | 0.986636 |  |  |
| 5.75 | 1.022857 | 0.98891 |  |  |
| 6 | 1.028571 | 0.990798 |  |  |
| 6.25 | 1.022857 | 0.992365 |  |  |
| 6.5 | 1.011429 | 0.993664 |  |  |
| 6.75 | 0.994286 | 0.994743 |  |  |
| 7 | 1 | 0.995638 |  |  |
| 7.25 | 1.017143 | 0.99638 |  |  |
| 7.5 | 1.017143 | 0.996996 |  |  |
| 7.75 | 1.017143 | 0.997508 |  |  |
| 8 | 1.011429 | 0.997932 |  |  |
| 8.25 | 1 | 0.998284 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 44. Comparison of experimental and calculated $M_{t} / M_{0}$ for Aclar film at 27.35-43.50\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP L4)

Table 28. Comparison of experimental and calculated $M_{t} / M_{0}$ for Aclar film at 43.50 - $58 \%$ R.H. and $25.0^{\circ} \mathrm{C}$ with determination of diffusion coefficient

| $\begin{gathered} \text { Time } \\ \text { (hours) } \end{gathered}$ | $\begin{aligned} & \text { Exp. } \\ & M_{t} / M_{0} \end{aligned}$ | $\begin{gathered} \text { Calculated } \\ M_{+} / M_{0} \\ \hline \hline \end{gathered}$ | $\begin{gathered} T_{1 / 2} \\ \text { (hours) } \\ \hline \end{gathered}$ | Sum of diff. ${ }^{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 0 | 0 | 0.25 | 0.02068 |
| 0.25 | 0.485577 | 0.454602 | 0.27 | 0.010792 |
| 0.5 | 0.644231 | 0.628646 | 0.30 | 0.004109 |
| 0.75 | 0.735577 | 0.748548 | 0.31 | 0.00372 |
| 1 | 0.826923 | 0.829778 | 0.32 | 0.00415 |
| 1.25 | 0.860577 | 0.884768 | 0.33 | 0.005298 |
| 1.5 | 0.903846 | 0.921994 |  |  |
| 1.75 | 0.932692 | 0.947194 |  |  |
| 2 | 0.971154 | 0.964253 |  |  |
| 2.25 | 0.990385 | 0.975801 | Diffusion |  |
| 2.5 | 0.995192 | 0.983618 | Coeff. = |  |
| 2.75 | 1.004808 | 0.98891 | 2.53 E -06 |  |
| 3 | 1.009615 | 0.992493 | $\mathrm{cm}^{2} / \mathrm{hour}$ |  |
| 3.25 | 1.004808 | 0.994918 |  |  |
| 3.5 | 1.009615 | 0.99656 |  |  |
| 3.75 | 1 | 0.997671 |  |  |
| 4 | 1 | 0.998423 |  |  |

Sum of diff. ${ }^{2}=$ sum of the difference ${ }^{2}$ between exp. and calc.


Figure 45. Experimental sorption of Aclar film at 43.50-58\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP L6)


Figure 46. Experimental sorption of Aclar film at 58-74.45\% R.H., $25.0^{\circ} \mathrm{C}$ (SORP L7)

## APPENDIX E

## APPENDIX E

Water Vapor Transmission Rate and Permeability of Materials

Table 29. WVTR and Permeability of blister materials at $37.78{ }^{\circ} \mathrm{C}$ and $85 \%$ R.H. (Dish Method)

|  | Weight <br> Gain <br> (grams) |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| Pkg. <br> Mat'1. | 7 days | 21 days | 35 days | WVTR |
| Aclar 1 | 0.0426 | 0.086 | 0.1099 | 0.5163 |
| Aclar 2 | 0.0097 | 0.0264 | 0.0471 | 0.2213 |
| Aclar 3 | 0.0063 | 0.0271 | 0.0457 | 0.2147 |
| PVC 1 | 0.0554 | 0.1144 | 0.1622 | 0.762 |
| PVC 2 | 0.0496 | 0.1114 | 0.165 | 0.7751 |
| PVC 3 | 0.0536 | 0.1088 | 0.1562 | 0.7338 |
| PVC/Aclar1 | 0.006 | 0.0196 | 0.0354 | 0.1663 |
| PVC/Aclar2 | 0.005 | 0.0156 | 0.0334 | 0.1569 |
| PVC/Aclar3 | 0.0655 | 0.1275 | 0.1677 | 0.7878 |

WVTR $=$ Water Vapor Transmission Rate ( $g / m^{2}$ day)
Perm. = Permeability ( g mil / $\mathrm{m}^{2}$ day mmg )
Area of dish $=0.00608 \mathrm{~m}^{2}$

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