

MELBERT W. TABER

Injector Tests by M.W.Taber & J.P.Knickerbocker



INJECTOR TESTS

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> <u>EV</u> <u>W. TABER & J. P. NNICKERBOCKER,</u> <u>AT</u> <u>MICMICAN AGRIGUÇTURAL COLLEGE</u>

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<u>1904</u>.

This thesis was contributed by

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Mr. M. W. Taber

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under the date indicated by the department stamp, to replace the original which was destroyed in the fire of March 5, 1916. .

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The object of this thesis, is, to determine the effect of the temperature of feed water upon the amount of water deliverered, by an injector on a three foot lift, per pound of steam.

The injector used was a Penberthy Auto-Position Injector; catalog No. 117. It was connected up as shown in sketch. The injector, all steam pipes and the calorimeter were wound with hair felt to prevent condensation by radiation.

As feed and delivery tanks, we used two of the old boilers in the boiler house; numbered respectively No. 1 and No. 2 in sketch. They were calibrated to read to each cubic foot at 52°5F. In calibrating tanks, a wooden frame supporting two glass tubes was attached to setting of boilers. The tubes were connected to boilers as shown in sketch. 62.4%, or one cu. ft. of water was then run into the boiler and the level of the water, as registered in glass, was marked off on scale side of the glass.

Both gauges and thermometers were calibrated before and after tests were run.

In mixing feed water so as to obtain the temperature desired for same; hot water was drawn from hot water tank into boiler No. 1, as shown in sketch. If necessary, enough cold water was added to bring temperature of feed water to temperature desired. The cold water connections were on the front of the boiler No. 1, and therefore not shown in shetch.

The method of running tests was as follows: The injector was started and the flow of feed water was regulated by walve A so that water in barrels maintained a constant level, giving a three foot lift. The steam and delivery pressures were throttled to 100# gauge by valves B and C respectively and the injector allowed to run a few minutes, until it became thoroughly heated up. At a given signal, valve A was closed and reading of two tanks taken when valve A was immediately opened again and regulated as before. The feed and delivery temperatures were also taken at this instant. The tests were continued for 45 minutes, temperatures of feed and delivery pressures were kept constantly at 100# gauge throughout the test. At the end of forty-five minutes, readings of tanks were taken as at beginning. Thus it will be seen that a flying start and finish were made. The tests were all run with valve in suction pipe wide open.

The feed tomperatures for tests were varied, as nearly as possible, by 10° F.

The temperature in the delivery tank was found to fall below that registered by thermometer in the delivery pipe, and in our computations has been used only to determine the actual number of pounds of water delivered by injector.

Calorimeter tests were run at the same time injector tests were run and the average quality of steam as found was used in computations.

All computations were made for one hour, as will be seen by observing equations in log of results.

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SKETCH SHOWING METHOD OF CONNECTING INJECTOR AND THE ARRANCEMENT OF STEAM AND WATER PIPES.

Log of Results.

	Temp.	Tenp.						
Time	F	FO		Re	ading	of Tan	<u>is</u> .	
8+25	52.6	129.0				1		
0.20		100.0	Tan	k I	nital	•	Final	
8:27.5	52,6	129.0	Fee	a	76-8 0	ni ft.	11.5 mi. ft.	
8:30	52.5	128.8		a		u		•
8:32.5	52.5	128.5	Del	ivery	9.6 C	eu. ft.	80.25 cu. ft.	
8:55	52.5	128.5	Cu.	ft. wet	er sun	bolied :	=65.3	
8:37.5	52.5	128.3	0	-0.1		A		
8:40	52.5	128.5	cu.	Cu. ft. water delivered=70.65				
8:42.5	52.5	128.5	Sto	am pross	sure=10			
8:45	52.7	128.5	Delivory pressure=100#					
8:47.5	52.7	1.23.0	Calprimeter Readings.					
8:50	52.8	128.7		Steam	Ste	em	Steam	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~
8:52.5	53.0	128.2	1:0.	Pressui	e Sep	aratou	Run Through	Steam
8:55	53.0	129.0	1	108	•	075	3.08	97.1
8:57.5	55.0	128.5	2	111	•	.070	3.10	97.9
		1.00.00					Average,	97.5
9:00	53.8	128.8						
9:02.5	53,5	129.0						
9:05	53.5	129,1						
9:07.5	54.0	129,1						
9:10	54.2	129.8						
Average	52.9	128.9						

- 1. Duration of test = 45 minutes.
- 2. Steam pressure(p)=100;
- 3. Delivery pressure (P')=100#
- 4. Delivery head (H)=233.8 ft.
- 5. Suction head (H')=3 ft.
- 6. Temp. of supply (T)=52.9°F.
- 7. Temp. of delivery in tank (T')=117.6°F.
- 8. Lbs. of water supplied per hr. (W)=5433
- 9. Lbs. of water delivered per hr. (W.)=5813.7#
- 10. Cu. ft. of water delivored per hr. (C)=34.2 cu. ft.
- 11. Wet steam delivered per hr. (W')=385.7#
- 12. Dry steam delivered per hr.(W")=375.8#
- 15. Water delivered per 1b. of wet steam=15.1#
- 14. Water delivered per 1b. of dry steam=15.5%
- 15. Velocity of discharge in ft. per sec.

V=(<u>cu. ft. delivered</u>) 144 =94.2 x 144 =76.9 3600 (area of discharge in sq. in.) 3600 x .049

- 16. Energy delivered raising injector water B.T.U. per hr. N.B.-- 1 = plus.
 - $\frac{W(H \pm H') \pm W'H}{778} = \frac{5453 \times 236.8 \pm 335.7 \times 235.8}{778} = 1771 \text{ B.T.U.}$

17. Energy delivered heating injector water B.T.U. per hr. W(Q'-Q)=5433(97-21)=402008 B.T.U.

18. Energy delivered velocity of discharge E.T.U. per hr.

 $\frac{W.V}{2g \times 778} = \frac{5318.7 \times (76.9)^2}{64.4 \times 778} = 695 \text{ B. T. U.}$

19. Total energy delivered =(16) $\frac{1}{10}$ (17) $\frac{1}{10}$ (18) $\frac{1}{10}$ $\frac{1}{10}$

1771 1 402908 1 695 1 585.7 x 97=442786.9 B.T.U.

20. Energy supplied=W'(xr 1 q)=385.7(.975 x 876.5 1 308.5)=448607.7

BT.U.

21. Efficiency=442786.9 = 99%448607.7

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Log of Results.

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ſ		Temp. Feed	Temp. Delivery	_						
	Time	FO	F		Rea	ading	of Tar	uks.		
	11:45	61.5	137.8	Tank		Init	al	Fi	nal	
	11:47.5	61.0	137.0	Feed		79	3	l	5.8	
	11:50	60 .7	136.6	Deli	very	8.	5	7	7.6	
	11:52.5	60.9	136.9							
	11:55	61.0	136.0	Cu.	ft. c	of wat	er sur	pp lie d	=63.5	
	11:57.5	61.0	136.8	Cu. :	ft. d	of wat	ter del	Livere	d=69.1	
	12:00	61.0	136.9	Stea	n pre	esure	=10 0∦			
	12:02.5	61.0	136.9	Deli	very	press	sure=10	00#		
	12:05	61.1	137.0	Colonimeter Readings.						
	12:07.5	61.3	156.9						~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	
	12:10	61.4	136.7	No.	Pres	im Ssure	Vatei Sepai	r rated	Steam Run Through	% Stoam
	12:12.5	61.5	137.1	1	11	12	•07	70		97.0
	12:15	61.5	137.2	2	11	LO	•01	75	2.98	97.6
	12:17.5	61.6	137.5	3	11	LO	•0	60	2.98	97.5
	12:20	61.7	137.8						Avorage,	97.6
	12:22.5	61.9	137.7					L		
	12:25	62.0	137.8							
	12:27.5	62.2	133.0							
	12:30	62.4	138.1							
	Avorage	61.4	137.2							

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- 1. Duration of test =45 minutes.
- 2. Steam pressure (P)=100 $\frac{n}{2}$
- 5. Delivery pressure =100#
- 4. Delivery head (H)= 254 fect.
- 5. Suction head (H')=3 feet.
- 6. Temp. of supply $(T)=61.4^{\circ}F.$
- 7. Temp. in delivery tank(T')=127°F.
- 8. Lbs. of water supplied per hr. (U)=5274.2
- 9. Lbs. of water delivered per hr. (W')=5663.1
- 10. Cu. ft. delivered por hr.(C)=92.
- 11. Wot steam dolivered per hr. (W')=595.9#
- 12. Dry steam dolivered per hr.(W")=584.4#
- 13. Water delivered per 1b. wet steam=14.5#
- 14. Water delivered per 1b. dry steam =14.9%
- 15. Velocity of discharge in feet per sec.
 - $V = (cu. ft. delivery) \times 144 = 92 \times 144 = 75.1$ 5600 x (area discharge II") 3600 x .049
- 16 J Energy delivered raising injector water B.T.U. per hr.

 $\frac{V(H + H') + V'H'}{778} = \frac{5274.2 (234 + 3) + 393.9 \times 234}{778} = 1725.1$

- 17. Energy delivered heating injector water B.T.U per hr. W(Q-Q')=5274.2(105.2-29.4)=420881.1
- 13. Energy delivered velocity of discharge B.T.U. per hr. <u>W.V²</u> = <u>5663.1 x (75.1)²</u> =653. <u>29 x 778</u> 64.4 x 773 19. Total energy delivered =(16) ± (17) ± (13) ± W'g_t =
 - 1725.1 1 420001.1 1 630 1 393.9 x 105.2 = 464601.5 D.T.U.
- 20. Energy supplied per hr. = $W'(xr \pm q) =$

503.9 (.976 x 876.5 ± 506.5)=468499.6 E.T.U.

21. Efficiency = $\frac{464601.5}{468499.6}$ =99.1%

Log of Results.

Time	Food Temp. F ^o	Delivery Temp. Po		R	eading of 1	lanits.	
9:55	72.5	149.9		Fank	Inital	Final	
9:57.5	72.5	149.7	1	Foed	70.5	9.9	
10:00	72.6	150.0	1	Delivery	8.4	74.7	
10:02.5	72.8	150.0					
10:05	73.0	150.2	cu.	ft. of wa	ter supplie	ed =60.6	
10:07.5	73.1	150.2	cu.	ft. of wa	tor deliver	red=66.3	
10:10	73.5	149.9	Stea	m pressur	e =100:"		
10:12.5	73.5	150.2	Doli	lvery pres	sure =100#		
10:15	73.6	150.1					
10:17.5	74.0	151.0			Calorimite	er Readings.	
10:20	74.0	150.8	-				
10:22.5	74.1	151.0		Steam	Separated	Steam	5toom
10:25	74.2	151.8	,	11005010		= 1c	07 0
10:27.5	74.4	151.8	1	114	.00	0.10	07.0
10:30	74.5	151.0	2	114	•07	3.16	97.6
10:32.5	74.7	151.9	3	113	•07	5.14	97.5
10:35	75.0	151.9				Avorago,-	97.63
10:37.5	75.1	152.1					
10:40	75.5	152.0					
Average	73.9	150.9					

- 1. Duration of test =45 minutes.
- 2. Steam pressure (P)=100#
- 3. Delivery pressure (P')=100#
- 4. Delivery head (H) =235.8 ft.
- 5. Suction head (H')=3 ft.
- 6. Temp. of supply (T)=73.9°F.
- 7. Temp. of delivery in tank $(T')=142.1^{\circ}F$.
- 3. Lbs. of water supplied per hr. (W)=5042#
- 9. Lbs. of water delivered per hr. (8.)=5422.4%
- 10. Cu. ft. of water delivered per hr.(C)=83.4
- 11. Wet steam delivered per hr. (W')=380.4%
- 12. Dry steam delivered per hr. $(W'')=371.9\frac{M}{d}$
- 15. Water delivered per lb. of wet steam =14.3%
- 14. Water delivered per 1b. of dry steam =14.7%
- 15. Velocity of discharge in ft. por sec.=

$$\frac{(cu. ft. delivered per hr.) \times 144}{5600 (area of discharge II")} = \frac{03.4 \times 144}{5600 \times .049} = 72.2$$

- 16. Energy delivered heating injector water B.T.U. per hr.

 W(H ± H') ± W'H'=5042 x (225.8 ± 3) ± 380.4 x 235.8 = 1663

 778
- 17. Energy delivered heating injector water B.T.U. per hr. W(Q'-Q)=5042(119-40.92)=393679.4
- 18. Energy delivered velocity of discharge B.T.U. per hr.

$$\frac{11.V^2}{29 \times 778} = \frac{54024 \times (72.2)^2}{64.4 \times 778} = 564 \text{ B.T.U.}$$

19. Total energy delivered =(16) ½ (17) ½ (18) ½ W'at =1663 ½ 393679 ½ 564 ½ 380.4 x 119 =440674 B.T.U.

20. Energy supplied =W'(xrlq)=380.4(.976 x 876.5 1 308.5)=448785.6B.T.

21. Efficiency = $\frac{440674}{442785.6}$ =09.7%

Time	Temp. Feed	Temp. Delivery		R	ading of	Tonks.		
22110	* •				001110 01			
1:25	80.5	156.0	Tan	10	Inital		Final	
1:27.5	80.0	157.0	Fee	đ	76.9		16.9	
1:50	79.6	157.5	Del	ivery	7.6		72.5	
1:32.5	79.5	157.0						
1:35	79.6	1.57.5	Cu.	ft. of w	ater sup	plied =	60.0	-
1:37.5	80.0	157.5	Cu.	ft. of w	ater del	iverod	=64.9	
1:40	80.0	158.0	Ste	am pressu	re=100#			
1:42.5	80.5	158.4	De1	ivery pre	scure =1	00#		
1:45	80,5	158.0						
1:47.5	80.7	158.0		Ca	lorimete	r Readi	ngs.	
1:50	81.0	158.8		C1	Watan			d
1.52.5	81.1	158.9	No.	Pressure	Separa	tod Ru	n Through	Steam
1:55	81.3	158.9	1	111	.070		3.10	97.8
1:57.5	81.5	158.8	2	110	.070		£ . 98	97.7
2:00	81.6	159.0	3	109	.065		2.96	97.9
2:02.5	82.0	159.4				Averag	0,	97.75
2:05	82.0	159.2						
2:07.5	82.2	159.0						
2:10	82.4	150.0						
Average	80.7	158.2						



- 1. Duration of test= 45 minutes.
 - 2. Stean pressure (P)=100#
 - 5. Delivery pressure (P')=100#
 - 4. Delivery head (H)=205.3 ft.
 - 5. Suction head (H')=5 ft.
 - 6. Temp. of supply (T)=80.7F.
 - 7. Temp. of delivery in tark (T')=150°F.
 - 3. Lbs. of water supplied per hr. (T)=4977.6%
 - 9. Lbs. of water delivered por hr. (N.)=5557.4"
 - 10. Cu. ft. of water delivered per hr.(C)=36.4 cu. ft.
 - 11. Wet steam delivered por hr. (W')=579.8#
 - 13. Dry steam delivered per hr. (W")=370.7#
 - 15. Water delivered per 1b. of wet steam=14.1%
 - 14. Water delivered per 1b. of dry steam =14.5%
 - 15. Velocity of discharge in ft. per dec.=

V=(cu. ft. delivered) 144 = 86.4 x 144 =70.5 5600(area of discharge in sq. in.) 5600 x .049 13.Energy delivered raising injector water B.T.U. per hr.

<u>W(H ± H') ± W'H=4977.6 x 258.5 ± 579.8 x 255.3</u> =1659 B.T.U. 778 778

17. Energy in heating injector water B.T.U. per hr.

W(Q'-Q)=4977.6(126.4-49.7)=581781.9 D.T.U.

13. Energy delivered velocity of discharge B.T.U. per hr.

 $\frac{W \cdot V^2}{2g \times 778} = \frac{5557 \cdot 4 \times (70 \cdot 5)}{64 \cdot 4 \times 778} = 551.4 \text{ B} \cdot \text{T} \cdot \text{U} \cdot \text{C}$

19. Total energy delivered =(16) 1 (17) 1 (18) 1 W'dt = 1639 1 301701.9 1 551.4 1 379.8 x 126.4 =451959.2 B.T.U.

20. Energy supplied =W'(xr 1 q)=379.8 x 876.5 1 508.5)=442007.2 B.T.U.

21. Efficiency = $\frac{431959.2 \times 100}{442087.2}$ = 97.7%

T 1 70	• œuo'I beoï	Temp. Delivery	Reading of Tanks.						
			Tenk	:	Inital	Final			
3:55	89.0	1.69.0	Feed		92.6	31.1			
3:57.5	0.03	1.69.0	Dali	vorv	6.0	72.3			
4:00	89.2	169.0				12.0			
4:03.5	89.5	J.63.9	C 11	ft of t	raton mnn11	od=61.5			
4:05	89.5	169.1	Cu.	red=66.5					
4:07.5	89 .7	1.69.0	Stean pressure=100 [#] Delivery pressure =100 [#]						
4:10	0. 03	169.4							
4:12.5	90.09	169.8							
4:15	90,2	169.8							
4:17.5	90,5	170.0					·		
4:20	90,8	169.9	71	Steam	Water	Steam Bun Ebrough	5+00		
4:22.5	SO .6	170.0	1.0.						
4:25	90.6	170.0	.1	110	•07	3.09	97.6		
4:27.5	91.0	170.2	2	110	•07	3,09	97.6		
4: 50	91.0	169.8	5	115	•07	5.10	97.6		
4:52.5	91.1	169.4			A	vorago,	97.6		
4:55	91.2	170.6	.	L					

169.5

169.7

169.9

91.5

01.5

90.3

4:37.5

Averago

4:40

Log of Results.

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- 1. Duaration of test=45minutes.
- 2. Stean pressure (P)=100#
- 5. Felivery pressure(P')=100#
- 4. Dolivery Head(H)=257 feet.
- 5. Suction Head =5 feet.
- 6. Temp. of supply (T)=00.3 F.
- 7. Temp. of delivery in tank 102.9°F.
- 8. Lbs. of water supplied per hr. (W)=5006.1
- 9. Lbs. of water delivered per hr. (U')=5401.2
- 10. Cu. ft. of water delivered per hr. (C)=00.7
- 11. Wet steam delivered per hr. (W')=395.1#
- 12. Dry steam delivered per hr.(W")=535.8%
- 15. Water delivered per 1b. wet steam=15.7#
- 14. Water delivered per 1b. dry steam=14.1%
- 15. Velocity of discharge in ft. por sec.

V=(<u>cu. ft. delavered</u>) x <u>144=38.7</u> x <u>144</u>=72.1 5600(area discharge II") 5600 x .949

- 16. Energy delivered raising injector water B.T.U. per hr. <u>W(N + H') + W'H'= 5006.1 x 540 + 395.1 x 237</u> =1695.2 778 773
- 17. Energy delivered heating injector water B. T. U. per hr. W(Q-Q')=5006.1 (138.4 - 50.8) =598485.5
- 18. Fnergy delivered velocity of discharge D.T.U. per hr.

 <u>V.V²</u> = 5401.2 x (72.1)

 29 x 778
- 19. Total energy delivered =

(16) 1 (17) 1 (18) 1 W'a₊=

 $1693.2 \pm 393485.5 \pm 534.3 \pm 395.1 \times 138.4 = 458394.3$

20. Energy supplied = W'(xr ½ q)=

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595.1(.976 x 876.5 ± 508.5)=459896.4

21. Efficiency=<u>458394.8</u> = 99.7% 459896.4

	Log		
No. of Test.	Feed Temp. F ^O	Delivery Temp. To	Water to Stean
l	52.9	128.9	15.1
2	61,4	137.2	14.5
S	7 3.9	150.9	14.5
4	80.7	159.2	14.1
5	90.5	169 .9	13.7

Conclusion.

The log of results show that an increase of feed temperatures causes a falling off of capacity of injector. This is caused by the **reduced** vacum within the combining tube.

Tests No. 2, 3 and 4, seen to have about the right variation in capacity, while tests No. 1 and 5 show too great a variation in capacity.

The rather unproportional fall in capacity in tests No. 1 and 5, is due to the fact that the tanks could not be read with enough certainty as the readings were effected no small amount by the temperature.

Our advice in running injector tests is, never use tanks calibrated to read volume but tanks set on scales so that the exact weight of water supplied and delivered can be weighed.



